

# Leveraging the chemo-physical interaction of halorespiring bacteria with solid surfaces To enhance halogenated organic compounds bioremediation

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# Background

## The Problem:

- Chloroethenes and polychlorinated biphenyls contaminate water resources
- Microbial dechlorination feasible, but confounded by sorption to geosorbents
- Poor understanding of how dechlorination is impacted by surfaces

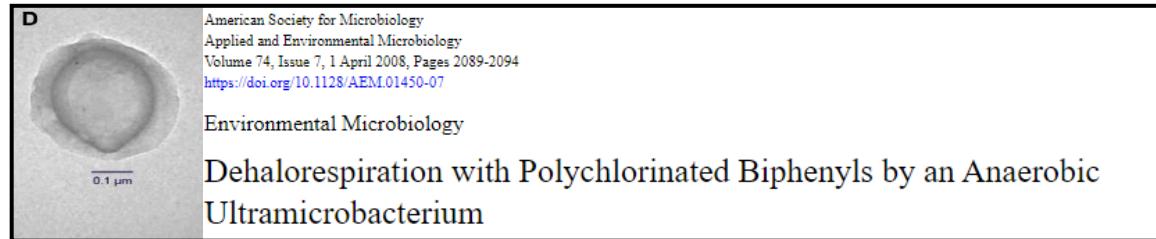
## Specific Aims:

- Quantitatively evaluate the effect of material properties on microbial dechlorination
- Evaluate the effect of materials on localized bacterial populations and develop innovative materials for enhanced bioremediation
- Predict field-scale performance of innovative bioamendment materials through advanced site models

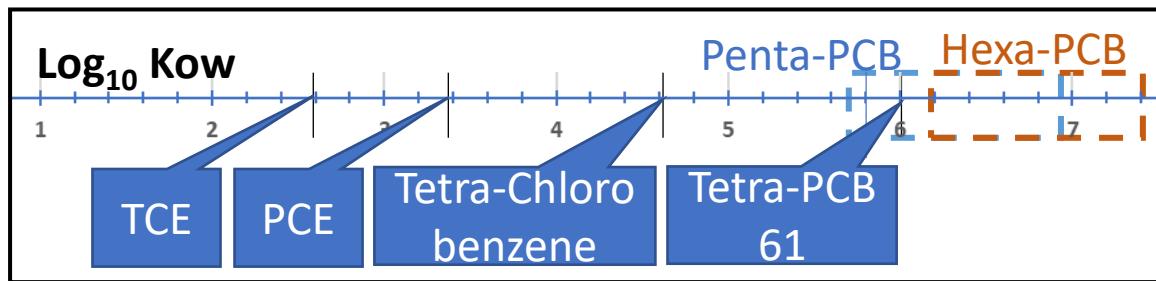
# Bacterial Model

## *Dehalobium Chlorocoercia DF-1*

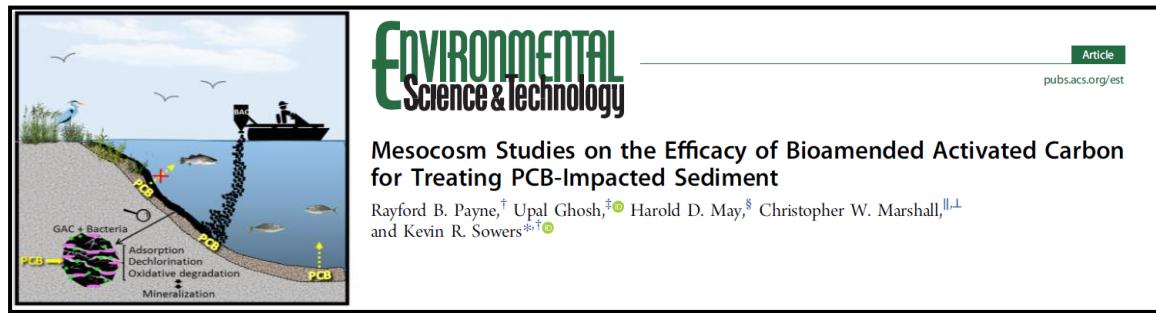
Isolated in pure culture  
since 2008  
(May et al., 2008)



Dehalogenation wide  
range of chlorinated  
compounds  
(Wu et al, 2002 a,b)



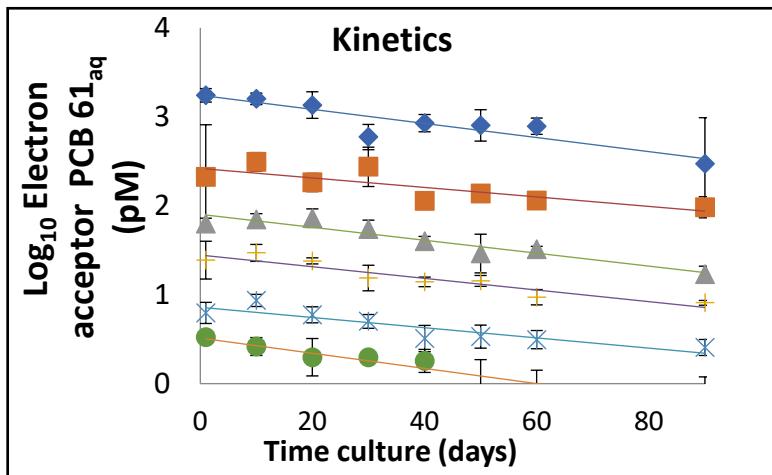
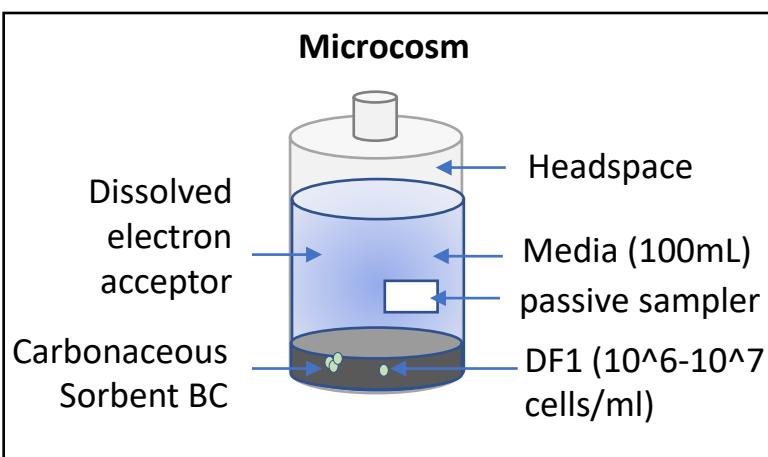
Already used for in situ  
bioremediation of PCB  
contaminated sites  
(Payne et al., 2019)



## Specificities

- Strictly anaerobic
- Slow growing (G=2-4 days)
- Low cell density ( $10^6$  -  $10^7$  cells/mL)
- Requires Desulfovibrio sp. (DSV) coculture or DSV extract

# Study design



PCE and PCB dechlorination kinetics  
accuracy, reproducibility in absence of BC

Precise DF1 cells enumeration in aqueous and solid phases

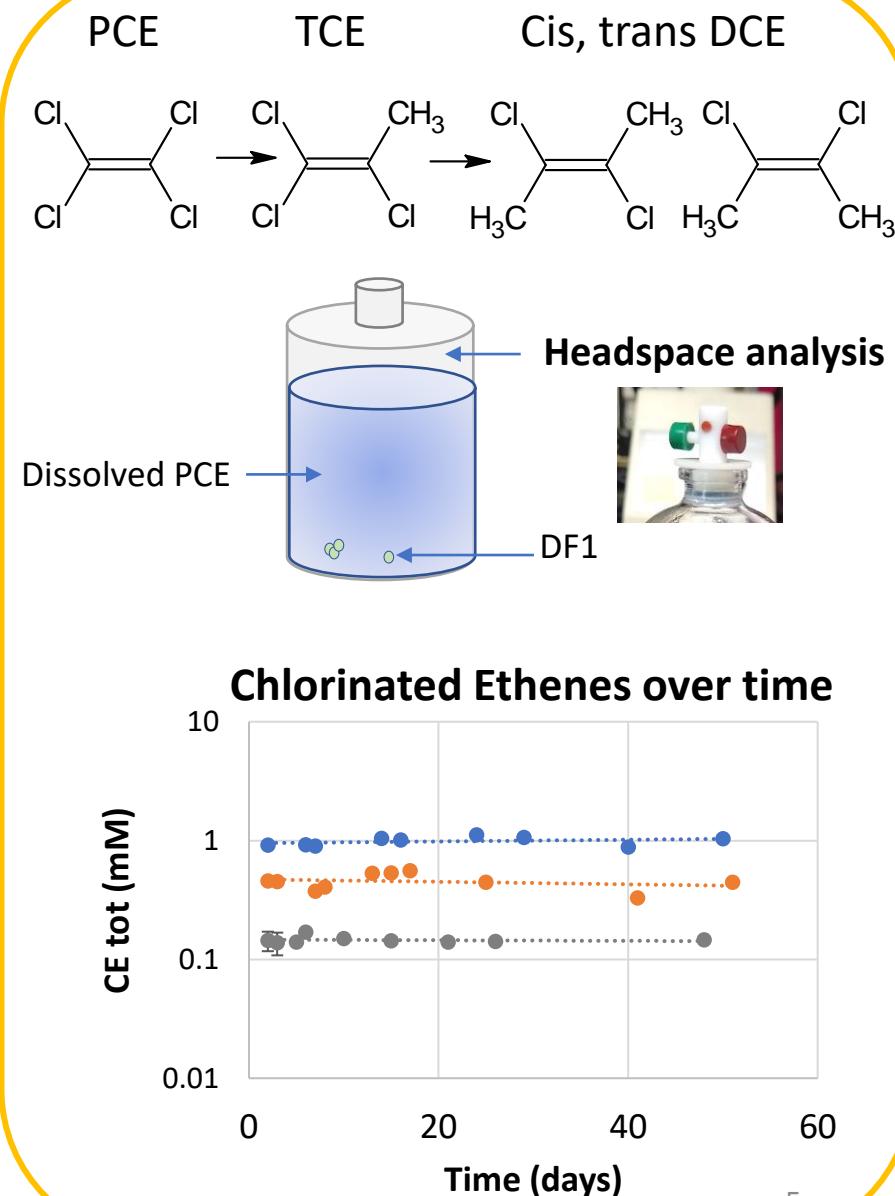
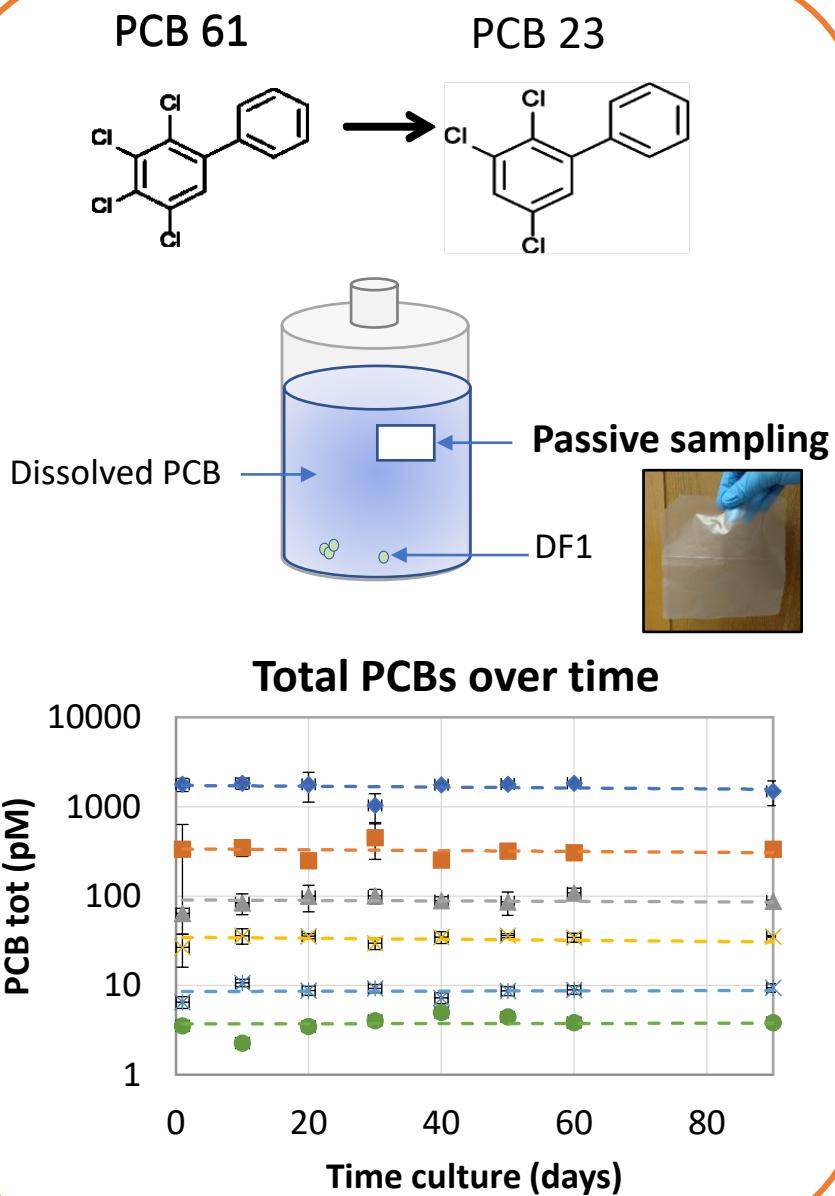
Media transition from Estuarine (E) to Freshwater (F) media

Black Carbon (BC) sorption capacity and physico chemical properties

Model True kinetics in presence of solids

Link BC properties to dechlorination kinetic changes

# PCB and PCE monitoring and mass balance



# BC selection and Sorption isotherms (1/2)



UMBC

Carbonaceous material	Manufacturer	C(%)	Surface area (g/cm <sup>2</sup> )	Skeletal density (g/cm <sup>3</sup> )	Bulk density (g/cm <sup>3</sup> )	Electron accepting cap. (mole/g)
Pine dust biochar	Biochar Eng Corp.	22.1 ± 0.5	109 ± 2	0.98	0.43	3.08
Coconut GAC	Calgon Corp.	90.8 ± 2.7	1305 ± 11	1.45	0.57	3.16
Coal GAC	Calgon Corp.	80.9 ± 1.4	1116 ± 25	1.61	0.64	3.62

## Method

- GAC sterilised and anaerobic
- 500 ml F- media(pH=6.9±0.1).
- Neat PCE is then spiked for C<sub>0</sub> 0.77 mM . Agitation 170rpm

$$\text{Total PCE} = C_0 V_{aq} = C_g V_g + C_{aq} V_{aq} + Q_e M_{BC} = \frac{HC_{aq}}{RT} \times V_g + C_{aq} V_{aq} + Q_e M_{BC}$$

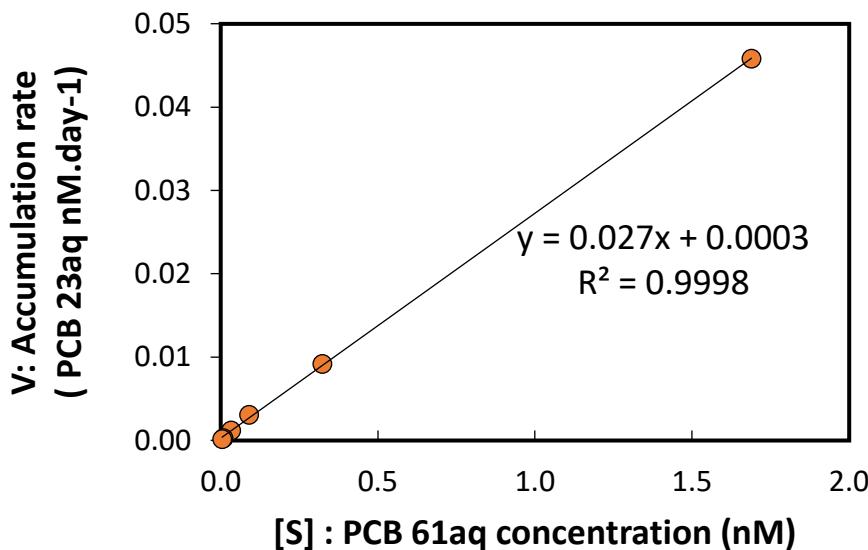
$$Q_e = (TOTPCE - \frac{HC_{aq}}{RT} \times V_g - C_{aq} V_{aq}) / M_{BC}$$



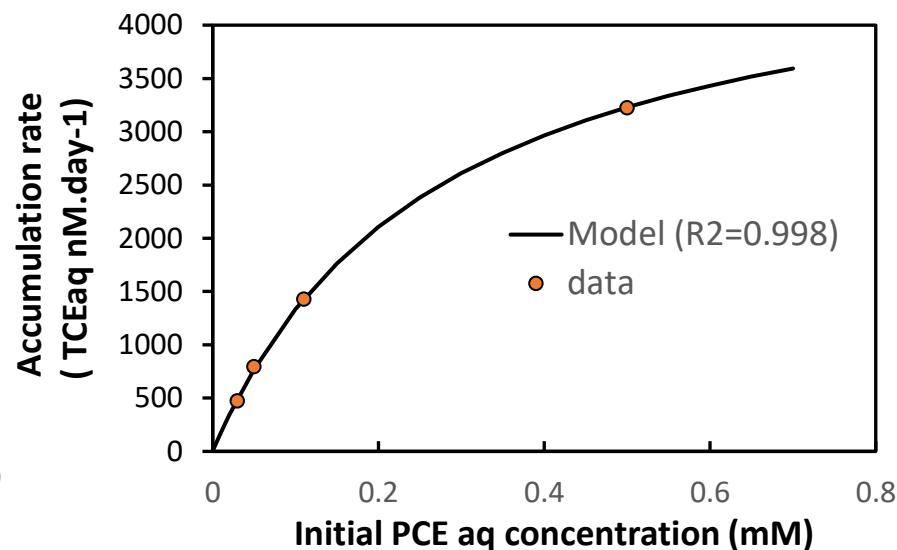
# PCB and PCE dechlorination kinetics

	PCB 61 <sub>(sat.)</sub> → PCB 23	PCE <sub>(&lt;0.2mM)</sub> → TCE
<b>Estuarine media</b> 0.14M NaCl	-0.016 +/- 0.0046 day <sup>-1</sup> (n=15)	-0.041 +/- 0.0094 day <sup>-1</sup> (n=3)
<b>Freshwater media</b> 0.05M NaCl	-0.010 day <sup>-1</sup> (n=1)	-0.018 +/- 0.0063 day <sup>-1</sup> , (n=4)

First order dechlorination kinetics  
Up to PCB 61 saturating level



PCE dechlorination kinetics approaching saturation conc.



# PCB and PCE dechlorination kinetics

PCB 61<sub>(sat.)</sub> → PCB 23

PCE<sub>(<0.2mM)</sub> → TCE

## Estuarine media

0.14M NaCl

## Freshwater media

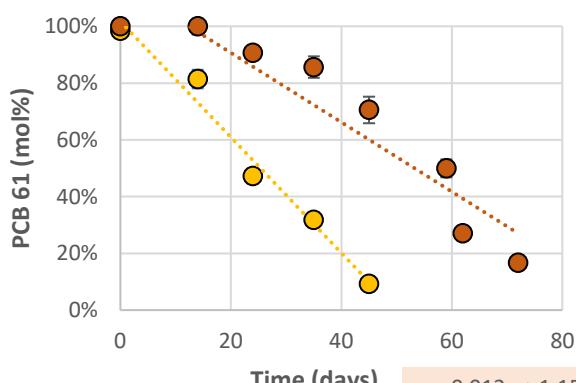
0.05M NaCl

$$-0.016 +/- 0.0046 \text{ day}^{-1} (n=15)$$

Physiological state  
inoculum

Culture  
condition

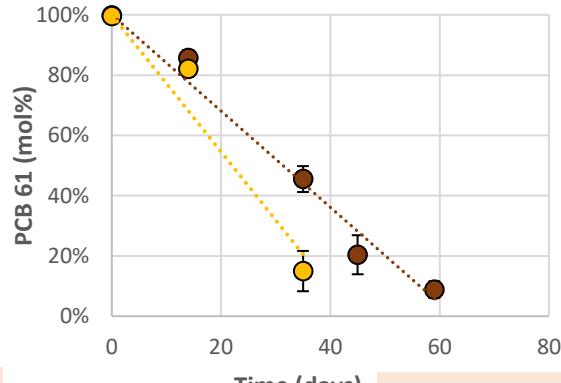
DSV extract  
quality



- Transfer at 50% dechl. Act.
- Transfer at 100% dechl. act.

$$y = -0.012x + 1.152 \quad R^2 = 0.887$$

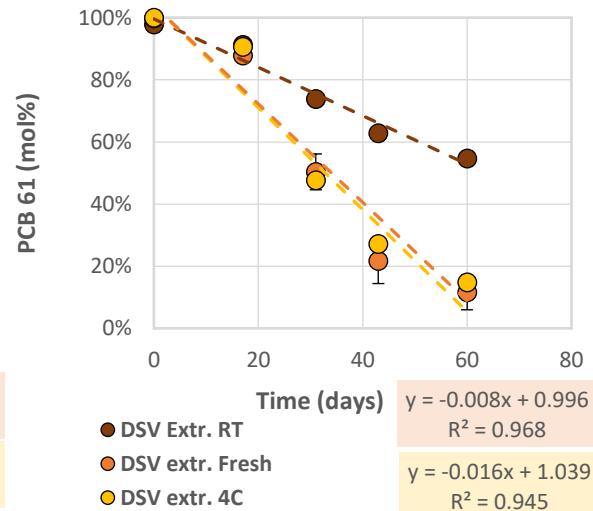
$$y = -0.020x + 1.018 \quad R^2 = 0.979$$



- Culture shaking
- Culture static

$$y = -0.016x + 1.000 \quad R^2 = 0.981$$

$$y = -0.023x + 1.000 \quad R^2 = 0.956$$



- DSV Extr. RT
- DSV extr. Fresh
- DSV extr. 4C

$$y = -0.008x + 0.996 \quad R^2 = 0.968$$

$$y = -0.016x + 1.039 \quad R^2 = 0.945$$

Variability of dechlorination kinetics linked to culture conditions  
Selected optimal parameters for future experiments

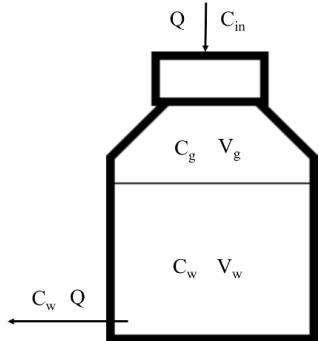
# Freely dissolved PCE generating columns

## Motivation

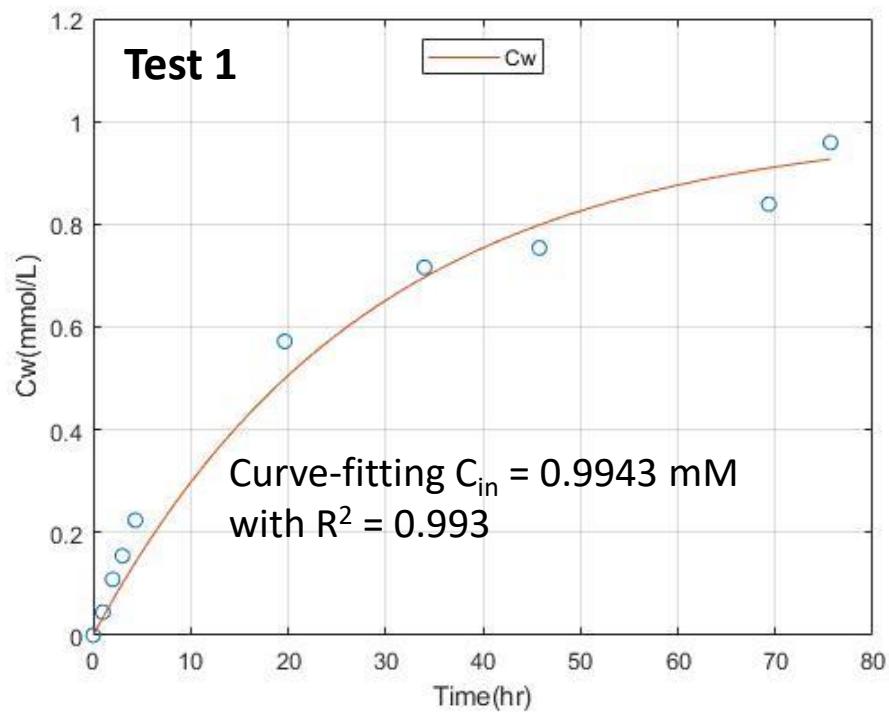
- Improving maximum cell density  
 $>10^7$  cells/ ml.
- Steady state concentration PCE in culture (continuous reactor)



## Testing the PCE profile in medium without cells



$$\frac{dC_w}{dt} = \frac{Q}{\left(\frac{HV_g}{RT} + V_w\right)} (C_{in} - C_w)$$



# Cell growth monitoring

## DNA extraction

Instagene Matrix modified

- ✓ Higher recoveries (2X)
- ✓ Higher precision (RSD: 5-9%)

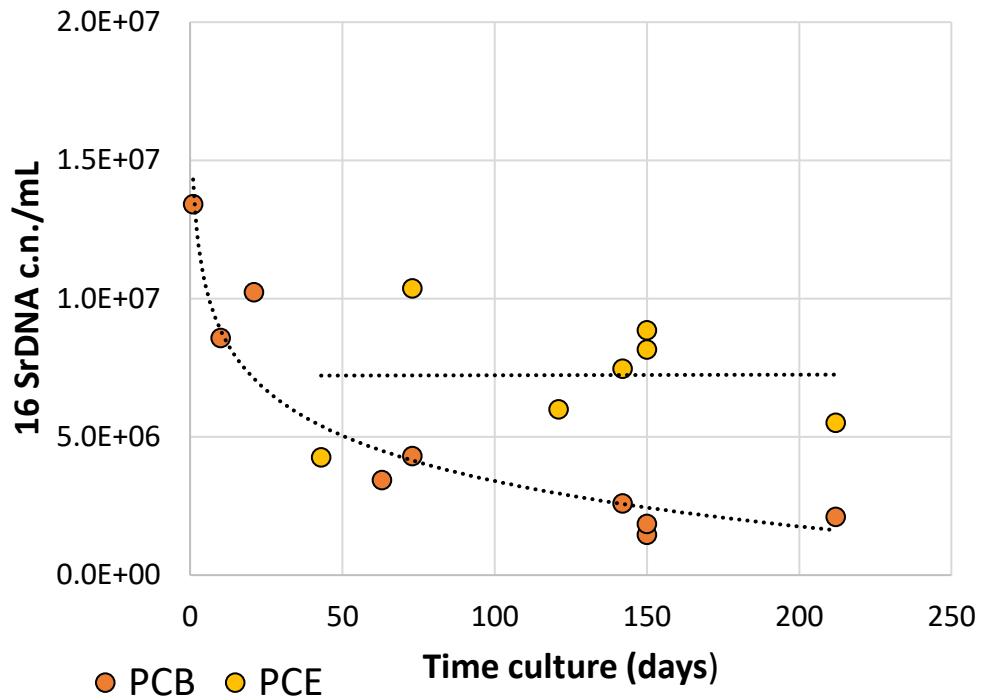
Versus Powersoil DNA isolation kit

## qPCR

348F/884R targeting

Chloroflexi phylum

(Fagervold et al. 2006)



## Results:

Variability between individual sampling linked to

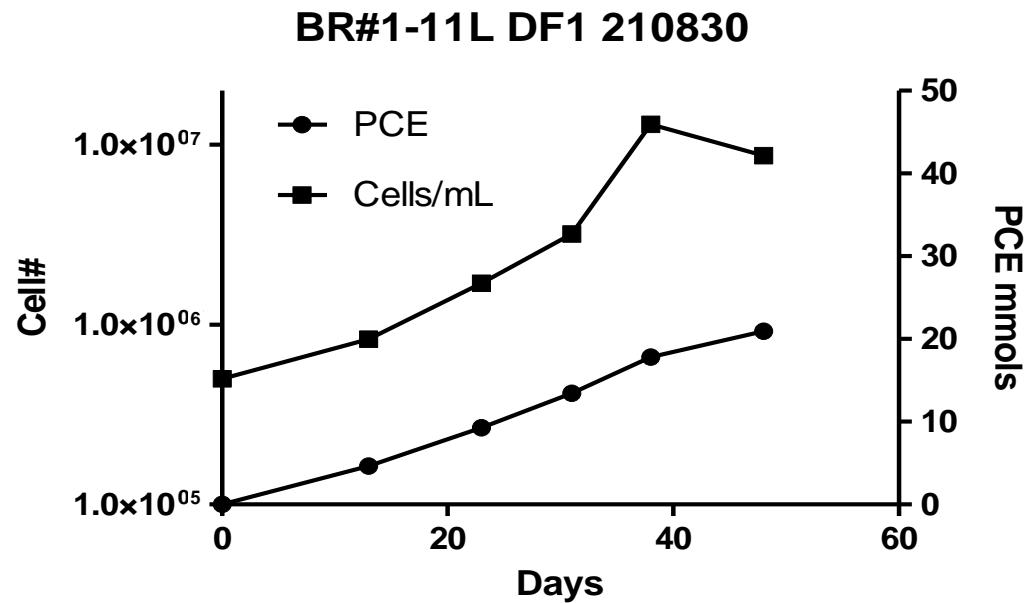
- PCE: DF1 sustained at ~1E7 cells/mL
- PCB: DF1 decrease to ~1E6 cells/mL

Similar findings for Dehalococcoides (Wang et al. 2014)

## Implications:

Adjusting cell density inoculum for kinetic study based on electron acceptor

# Anaerobic bioreactor (Scale up)



- Scale-up culture maintained at  $1 \times 10^7$  cells/mL
- Semi-continuous scale up provides inocula for kinetic experiments

# Main takeaways and next steps

## Summary:

- Experimental conditions (media, cell growth, PCE and PCB monitoring tools) optimized for the kinetic study
- Similar intrinsic dechlorination kinetics observed for chlorinated compound with different hydrophobicity ( $\log_{10} K_{ow}$  3-6)
- A range of BC materials being prepared and characterized for the study

## Next steps:

- Tailor Black Carbon for specific properties
- Measure Tailored BC on dechlorinating kinetics
- Relate dichlorination kinetics to BC physicochemical properties
- Explore native associations with natural BC particles in sediments
- Translate using advanced site models



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Matthew Schnobrich