# FINAL REPORT

In Situ Bioremediation of Perchlorate in Vadose Zone Soil Using Gaseous Electron Donors

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### Acronyms

AFCEE Air Force Center for Engineering and the Environment

AGC Aerojet General Corporation

ASTM American Society for Testing of Materials

amsl Above mean sea level bgs Below ground surface

BNA Base, neutral, acidic semi-volatiles C Concentration or degrees Celsius

°C Degrees Celsius

CDM Camp Dresser & McKee Inc.

CF<sub>i</sub> Coefficient for gas *i* cfh Cubic feet per hour cubic feet per minute

ClO<sub>4</sub> Perchlorate

cm<sup>2</sup> Square centimeters

cm<sup>2</sup>/s Square centimeters per second

CO<sub>2</sub> Carbon dioxide

COTR Contracting Officer's Technical Representative

cy Cubic yard

d Day

DAC Douglas Aircraft Company
DDT Dichlorodiphenyltrichloroethane

DoD Department of Defense

DTSC California Department of Toxic Substance Control

DWEL Drinking Water Equivalent Level

DWR California Department of Water Resources

ELAP Environmental Laboratory Accreditation Program

EPA U. S. Environmental Protection Agency
ERDC U.S. Engineers Research and Development

ESTCP Environmental Security Technology Certification Program

ft Feet

GEDIT Gaseous electron donor injection technology

h Hours H<sub>2</sub> Hydrogen

HMX High melting explosive

in w.c. Inches pressure water column

IRCTS Boeing Interactive Rancho Cordova Test Site

JATO Jet-assisted take off
LEL Lower explosive limit
LPG Liquefied petroleum gas
MCL Maximum contaminant level
MDC McDonnell Douglas Corporation

mg/kg Milligrams per kilogram

mg/kg/d Milligrams per kilogram per day

mg/L Milligrams per liter

mg-N/kg Milligrams of nitrogen per kilogram

min Minutes

msl Mean sea level

μg/kg Micrograms per kilogram

μg/kg/d Micrograms per kilogram per day

μg/L Micrograms per liter

N<sub>2</sub> Nitrogen NA Not applicable

NASA National Aeronautics and Space Administration

ND Non-detect

NDMA N-Nitrosodimethylamine

No. Number NO<sub>3</sub> Nitrate

OD Outside diameter

O&M Operations and maintenance

P Total pressure

 $P_i$  Actual pressure of gas i

OSHA Occupational Safety and Health Administration

PBA Propellant burn area
PCB Polychlorinated biphenols
PID Photo-ionization detector

P&ID Process and instrumentation diagram

ppmv Parts per million by volume psig Pounds per square inch gauge PSU The Pennsylvania State University

PVC Polyvinyl chloride

 $Q_i$  Flow rate of gas i at standard conditions

 $\widehat{Q}_i$  Rotameter reading of flow rate of gas i at standard conditions

QAPP Quality Assurance Project Plan
QAQC Quality assurance quality control
r<sup>2</sup> Square of the correlation coefficient

RDX Royal demolition explosive

RfD Reference dose

RI Remedial investigation ROI Radius of influence

RWQCB California Regional Water Quality Control Board

scfh Standard cubic feet per hour scfm Standard cubic feet per minute

SM Standard Methods SP Sample point

SVE Soil vapor extraction
TBD To be determined
TCA Trichloroethane
TCE Trichloroethene
TNB Trinitrobenzene
TNT Trinitrotoluene

TOC Total organic carbon

UIC Underground Injection Control
USCS Unified Soil Classification System
U.S. EPA U. S. Environmental Protection Agency

USGC U. S. Geological Survey VOC Volatile organic compound WDC Water Development Corporation

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## **Executive Summary**

#### **Background and Technology Description**

Perchlorate is a human health concern because of its ability to inhibit iodide uptake by the thyroid. Perchlorate is present in soil, groundwater, and many potable water supplies. Costs for mitigating these perchlorate impacts can be significant; thus demonstration and validation of cost-effective treatment technologies is critical to the Department of Defense (DoD). While extensive research and technology development on the treatment of perchlorate in water has been conducted, limited research and technology development has been focused on perchlorate in soil. Perchlorate contamination in soil is important because of it can be a source of groundwater contamination.

Currently, available technologies for the treatment of perchlorate in soil require excavation and are not always cost-effective or practical, particularly as the depth of contamination increases. When applicable, excavation followed by anaerobic biodegradation has proven to be effective. *In situ* remediation of perchlorate in soil is an alternative, potentially more cost-effective solution.

Gaseous electron donor injection technology or GEDIT (U.S. Patent No. 7,282,149 and patent pending) involves injection of gaseous electron donors into the soil with the purpose of promoting anaerobic biodegradation of perchlorate to water and chloride ion. This technology can be viewed as bioventing in reverse. Bioventing, a proven bioremediation technology for petroleum hydrocarbons, involves the injection of a gaseous electron acceptor (e.g., oxygen) into the vadose zone resulting in the biodegradation of an electron donor (e.g., hydrocarbons). In the present application, the electron acceptor and donor are reversed with the gaseous electron donor being injected in order to biodegrade the electron acceptor (i.e., perchlorate or nitrate).

Bioventing is an effective technology because it relies on the excellent mass transfer characteristics of gases resulting in an effective distribution of oxygen through the vadose zone. Similarly, the injection of gaseous electron donors for perchlorate biodegradation in vadose zone soil benefits from the same mass transfer and distribution characteristics. The superior mass transfer and distribution of gases as compared to liquids is the major advantage of this technology over attempts to introduce liquids into the vadose zone. Diffusion of gases in the vadose zone improves the ability to deliver the electron donor throughout the soil volume and helps to overcome problems associated with liquid flow through preferential pathways. Additionally, gaseous electron donor technology does not require the capture and treatment of infiltrated liquids that could otherwise adversely impact groundwater.

Potential applications of GEDIT include treatment of a wide variety of oxidized contaminants in soil. A partial list of oxidized contaminants that are potentially treatable using GEDIT include:

- Perchlorate
- Chlorate
- Nitrate
- Nitrite

- Selenate
- Arsenate
- Chromate and dichromate (i.e., hexavalent chromium)
- Uranylate
- Pertechnetate
- N-Nitrosodimethylamine (NDMA)
- Trichloroethene (TCE)
- Trichloroethane (TCA)
- Highly energetic compounds including nitro-aromatics such as TNT, RDX, and HMX

Many of the limitations or technical risks for this technology are similar to bioventing technology risks when gas injection is used. Additional limitations or technical risks are associated with the use of electron donors that are also flammable chemicals. These risks can be managed in a cost-effective and practical manner.

### **Performance Objectives and Results**

#### Perchlorate

The demonstration was conducted at the Inactive Rancho Cordova Test Site Propellant Burn Area (IRCTS-PBA) in Rancho Cordova, California. The average percent perchlorate destruction was 93±9 percent within the targeted 10-foot (ft) radius of influence (ROI) and the 10-to-40-ft below ground surface (bgs) depth interval. The performance objective of 90 percent for perchlorate destruction was exceeded. Initial perchlorate concentrations within this ROI and depth ranged from 2,600 to 75,000 micrograms per kilogram ( $\mu$ g/kg). Final perchlorate concentrations ranged from < 13 to 8,800  $\mu$ g/kg. Seven final soil samples (i.e., six sample locations plus one duplicate) were non-detect (ND) for perchlorate (< 13 to <15  $\mu$ g/kg).

Perchlorate destruction was affected by oxygen and hydrogen concentrations. Oxygen concentrations less than about one percent and hydrogen concentrations greater than 0.5 percent supported perchlorate destruction. Liquefied petroleum gas (i.e., commercial propane or LPG) did not support perchlorate destruction. Perchlorate destruction was not affected strongly by differences in soil moisture at this site. Significant perchlorate destruction was observed in soil samples with final moisture contents ranging from 6.8 to 36 percent. Perchlorate destruction was also observed in silty and clayey lower permeability soil types. These data indicate that hydrogen was able to diffuse into low permeability soil pore spaces.

A maximum of five months was required to achieve 93±9 percent perchlorate destruction during the demonstration and three months or less was required in certain locations. The performance objective was 90 percent destruction within twelve months. Thus the performance objective was met. Heterogeneity greatly complicated assessment of actual perchlorate destruction rates. Nevertheless, 88±11 percent perchlorate destruction at a rate of 380±110 micrograms per kilogram per day (µg/kg/d) was estimated. This rate compares favorably to biodegradation rates measured during optimized full-scale *ex situ* bioremediation of perchlorate in soil where the median rate was about 200 µg/kg/d and the 90<sup>th</sup> percentile rate was about 500 µg/kg/d.

#### Nitrate

The average percent nitrate destruction was  $94\pm9$  percent within the targeted 10-ft ROI and the 10-to-50-ft bgs depth interval. The performance objective of 90 percent for nitrate destruction was exceeded. When all data were considered which comprised an ROI of 55 ft, the average nitrate destruction was  $90\pm14$  percent. Nitrite was analytically quantified as the sum of nitrate and nitrite. Therefore, accumulation of the denitrification intermediate nitrite did not occur. Initial concentrations of nitrate plus nitrite within the 10-ft target ROI ranged from 2.0 to 8.6 milligrams of nitrogen per kilogram (mg-N/kg). Final nitrate plus nitrite concentrations ranged from < 0.054 to 2.9 mg-N/kg. Six final soil samples (i.e., five sample locations plus one duplicate) were ND for nitrate (< 0.054 to <0.057 mg-N/kg).

Nitrate destruction was affected less so by gas composition than perchlorate. Significant nitrate destruction occurred when oxygen concentrations were less than about ten percent. Nitrate destruction was observed under a wide range of hydrogen concentrations as low as about 0.01 percent and under propane concentrations about three percent or greater.

A maximum of five months was required to achieve  $94\pm9$  percent nitrate destruction during the demonstration and three months or less was required in certain locations. The performance objective was 90 percent destruction within six months. Thus the performance objective was met. A nitrate destruction rate of  $40\pm11~\mu g/kg/d$  was estimated.

ROI was used as a primary metric for implementability because it will determine the number of wells required to treat a given area. The ROI for perchlorate degradation was conservatively estimated to be 10 feet and likely to be 15 ft during the demonstration. The ROI for nitrate degradation was estimated to be at least 55 ft. The performance objective for implementability was an ROI of 10 ft. Therefore the performance objective was met.

These ROIs were based on injection of a total of 100 standard cubic feet per hour (scfh) of gas into a single location at 18 and 28 ft bgs. The ROI for oxygen depletion and electron donor transport was strongly affected by injection well design, gas flow rate, injection strategy. Use of six-inch long soil vapor probes as injection points and continuous injection of gas at relatively low flow rates was preferable to use of long well screens and pulsing of gas a relatively high flow rates.

Gas composition also affected the ROI and the ROI varied with respect to depth. For example, LPG was transported a greater distance than hydrogen during injection of a H<sub>2</sub>/CO<sub>2</sub>/LPG/N<sub>2</sub> gas mixture. Hydrogen, because of its buoyancy, was limited in how deep it could be transported compared to LPG. The injection of this mixture was effective in reducing oxygen concentrations not only at the injection depths (i.e., 18 and 28 ft bgs), but also above and below these depths based on measured oxygen concentrations and observed perchlorate removals. As compared to injection of the gas mixture, injection of LPG alone was transported significant distances but tended to sink resulting in elevated oxygen concentrations in shallow soil horizons. Thus, the ROI measured for this demonstration was operationally defined and should not be directly applied to other sites. Greater ROIs are possible and the most cost-effective and implementable approach will be determined by optimizing gas injection and well spacing.

#### **Implementation Issues**

In addition to well spacing, regulatory acceptance, permitting, and safety are important implementation issues. Federal or state regulations driving site cleanup will drive the need for GEDIT. The primary application for GEDIT is anticipated to be treatment of contaminants such as perchlorate in deep soil for the purpose of groundwater protection. The feasibility study process will include evaluation of GEDIT compared to other alternatives such as pump and treat, liquid flushing, and excavation. Specific permits for GEDIT will be driven by local codes and will include drilling and well installation permits and hazardous materials storage permits. Other permits may be necessary and will be dependent on local codes.

Flammability is the primary end-user concern associated with GEDIT. As shown in this demonstration, this issue was easily managed and did not necessitate unusual efforts. The level of effort was similar to that for a construction site or remediation of a gasoline station site. Specifically, the following observations and actions were part of this demonstration:

- Hydrogen was supplied in cylinders much in the same way that flammable acetylene is supplied for welding at construction sites. The number of cylinders was greater than typically used at a construction site but these cylinders were contained in a commercially available rig that stabilized and manifolded the cylinders.
- LPG was stored in a standard commercially available tank on a portable concrete pad, in accordance with local codes. This effort was no different from a remediation site that uses a propane-fired thermal oxidizer or a construction site that uses LPG.
- Use of flammable gas/no smoking placards were used at the site. Such placards would be present at any site employing the use of flammable chemicals.
- Liquid nitrogen was supplied in a commercially available trailer. From a cold surface hazard perspective, liquid nitrogen is handled the same as liquid oxygen at hospitals and other commercial facilities.
- The Sacramento County Hazardous Materials Department and Aerojet-General Corporation were satisfied with the arrangement for storage and use of flammable materials on the site. A standard hazardous materials permit was required by the County. Aerojet-General Corporation conducted a New Process Evaluation which is a standard requirement and was completed with minimal effort.
- Flammable gases were not detected above the ground surface. Thus, release of flammable gas to the atmosphere was not a safety issue. Nevertheless, monitoring of flammable gases should be conducted just as they would be during a gasoline station remediation project.

#### Costs

This cost model was based on implementation at the IRCTS-PBA. Four scenarios were considered and compared in this cost assessment. Each scenario has different treatment objectives, gas compositions, and total soil volumes to be treated. Scenarios 1 and 3 have the treatment objective of reducing perchlorate concentrations to  $60 \,\mu\text{g/kg}$  or less which is a possible California Regional Water Quality Control Board cleanup goal for protection of groundwater at the site. Scenarios 2 and 4 have a less stringent treatment objective of achieving 90 percent mass

reduction of perchlorate. Scenarios 1 and 2 are conservatively designed based on demonstration data and have an ROI of 10 ft and a gas composition based on 10 percent hydrogen. The 10-ft ROI has is the minimum value based on demonstration data. The gas composition comprised of 10 percent hydrogen was used in the demonstration. Scenarios 3 and 4 have an ROI of 15 ft based on limited demonstration data. The gas composition used in Scenarios 3 and 4 is one percent hydrogen and 99 percent nitrogen because LPG was not necessary for perchlorate reduction and hydrogen concentrations as low as 0.5 percent were able to promote perchlorate degradation.

Unit costs for the various scenarios were estimated as follows:

- Scenario 1 represents the costs based on conservative demonstration design conditions and the unit cost is \$87 per cubic yard (\$87/cy).
- Scenario 2 is based on the same gas composition and ROI as in Scenario 1, but the treatment area is reduced with a focus on mass reduction. The unit cost is reduced to \$68/cy under Scenario 2.
- Scenario 3 is comparable to Scenario 1 with respect to the treatment goal and area, but is based on a more reasonable design. These changes reduce the unit cost to \$21/cy.
- Scenario 4 is focused on mass reduction with a reasonable design and the unit cost is \$28/cy. The unit cost for Scenario 4 is greater than for Scenario 3 because the volume of soil is lower and many project costs are fixed.

An alternative approach to *in situ* treatment is excavation of vadose zone soil and ex situ bioremediation. This process includes soil excavation; rock screening and crushing; soil mixing with water, electron donor, and nutrients; storage in treatment cells during biodegradation; soil drying; and backfilling. Full-scale costs for this process were estimated to be about \$35/ton or \$45/cy. Given the depth of the vadose zone at the site (140 ft bgs), the unit cost may be even higher due to the significant benching and sloping required. Compared with this ex situ approach, GEDIT is cost effective under Scenarios 3 and 4. Other alternatives for groundwater protection such as hydraulic containment via pump and treat may also be applicable. Additional evaluations would be necessary to assess whether GEDIT is cost effective in comparison. Nevertheless, well superposition and other refinements are likely to further improve the cost-effectiveness of GEDIT.

#### 1.0 INTRODUCTION

#### 1.1 Background

Thousands of tons of perchlorate (ClO<sub>4</sub>) have been released into the environment since its first use a rocket fuel oxidant in the 1950s (Motzer, 2001). Since that time, the highly soluble and weakly adsorptive perchlorate anion has contaminated surface and groundwater throughout the United States, potentially affecting more than 15 million people and causing numerous risks to human health (Xu et al., 2003). Technologies have been developed and implemented for treatment of perchlorate in groundwater and include both *ex situ* and *in situ* anaerobic biological reduction as well as *ex situ* ion exchange.

The U.S. Environmental Protection Agency (U. S. EPA) Office of Solid Waste and Emergency Response, Federal Facilities Restoration and Reuse, has documented 58 federal sites with known perchlorate releases as of April 29, 2004 (U.S. EPA, 2004). These sites include a combination of Air Force, Navy, Army, Department of Energy, and NASA sites. Of these sites, 51 are U.S. Department of Defense (DoD) sites. In addition, the office listed 40 private sites with known releases. Many of the private sites are owned or operated by military contractors. Groundwater contamination exists at all of these sites with perchlorate concentrations as high as 3,700 milligrams per liter (mg/L). Perchlorate in vadose zone soil exists at many of these sites and can serve as ongoing sources of groundwater contamination. Twenty of the 51 DoD sites are listed as having soil contamination. EPA has not defined soil contamination at the remaining sites; however, it is likely that perchlorate exists in vadose zone soils.

Additionally, various DoD contractors have significant soil contamination problems. The former Whittaker-Bermite site north of Los Angeles was formerly used to manufacture jet-assisted take off (JATO) and Sidewinder/Chaparral/N-29 rocket motors and miscellaneous munitions for the DoD. This site is about 1,000 acres with a vadose zone up to 300 feet in depth. Perchlorate and chlorinated volatile organic compounds (VOCs) are present in vadose zone soil. Perchlorate has been detected at depths up to 200 feet (maximum depth sampled) and at concentrations up to 310 mg/kg in Operable Unit 1 alone. The McDonnell Douglas Inactive Rancho Cordova Test site (IRCTS) in California has documented perchlorate contamination in soil. These sources in soil often require treatment because they represent potential human health risks and may serve as ongoing sources of perchlorate in groundwater.

Perchlorate is a human health concern because of its documented ability to inhibit iodide uptake by the thyroid (U.S. EPA, 2005). Perchlorate is present in soil, groundwater, and many potable water supplies across the United States. The perchlorate concentrations in many of these media are greater than regulatory concentrations, as discussed in Section 1.3, and may pose risks to human health. The sources of perchlorate in these media include both naturally occurring and anthropogenic sources. Many but not all of the anthropogenic sources of perchlorate are attributable to DoD and DoD-contractor operations. Costs for mitigating these perchlorate impacts can be significant; thus, demonstration and validation of cost-effective treatment technologies is critical to the DoD.

Currently, available technologies for the treatment of perchlorate in soil require excavation and are not always cost-effective or practical, particularly as the depth of contamination increases.

When applicable, excavation followed by anaerobic composting has proven to be effective. *In situ* remediation of perchlorate in soil is an alternative, potentially more cost-effective solution. Currently, emerging *in situ* technologies for treating perchlorate in soil involve soil flushing with water or liquid electron donors. Flushing the soil with water transfers the contaminant to the aqueous phase which must then be extracted and treated. Flushing with liquid electron donors in most cases will require groundwater extraction and hydraulic containment. Shallow soil has been cost-effectively treated *in situ* using cow manure and other inexpensive electron donors.

Soil flushing technologies are limited by the ability to adequately distribute these liquids throughout the vadose zone, as a result of the tendency for fluids to flow along preferential pathways, and potential difficulty in capturing infiltrated water at certain sites. Additionally, technologies based on infiltration of liquid electron donors become even more difficult to apply as vadose zone contamination extends deeper. Therefore, there is a need for more effective *in situ* perchlorate treatment technologies applicable to vadose zone soil at any depth. Gaseous electron donor injection technology (GEDIT; U.S. Patent No. 7,282,149 and patent pending) involves injection of gases such as hydrogen and propane into the vadose zone to stimulate anaerobic biological reduction of perchlorate to water and chloride. Nitrate and nitrite are also reduced to nitrogen gas. GEDIT takes advantage of the greater diffusivity and lower density of gases compared to liquids to address lithologic heterogeneity issues in the vadose zone. GEDIT is also potentially applicable to treatment of other DoD and Department of Energy related contaminants such as hexavalent chromium, uranium, technetium, and highly energetic compounds including TNT, RDX, and HMX.

#### 1.2 Objective of the Demonstration

The overarching objective of this project was to demonstrate and validate GEDIT for treatment of perchlorate and nitrate in vadose zone soil. This project represents the first field demonstration of the technology. The demonstration yielded valuable engineering design information on GEDIT implementation. Development of an engineering guidance document was another objective of the project. Performance objectives for the project are described in Section 3.0.

### 1.3 Regulatory Drivers

The primary driver for cleanup of perchlorate in soil is protection of groundwater. Cleanup levels for perchlorate in soil based on ingestion of direct contact are typically much greater than those for protection of groundwater. One exception is shallow soil where food crops are grown. In this case certain crops such as lettuce can take up perchlorate and result in another route of exposure.

With respect to protection of groundwater, the U.S. EPA is in the process of evaluating whether to establish a maximum contaminant limit (MCL) for perchlorate in drinking water. The current drinking water equivalent level (DWEL) is 24.5  $\mu$ g/L which is based on a reference dose (RfD) of 0.0007 mg/kg/day (U.S. EPA, 2006a). If the EPA establishes an MCL for perchlorate, the current DWEL may or may not be used as the value for the MCL. Currently, U.S. EPA has established an interim drinking water health advisory level of 15  $\mu$ g/L for perchlorate (U.S. EPA, 2008). Individual states vary in their regulation of perchlorate in drinking water. California has established an MCL of 6  $\mu$ g/L and Massachusetts has established an MCL of 2  $\mu$ g/L. Other states vary with respect to how they regulate perchlorate and very few states have specific

regulatory limits for perchlorate in soil (ITRC, 2005). Most commonly, cleanup limits for perchlorate in soil are established on a site-by-site basis and can be as stringent as non-detect in order to protect groundwater. Several factors affect development of cleanup levels for protection to groundwater. These can include depth to groundwater, hydrogeology, depth of perchlorate contamination, rainfall, surface water infiltration, and soil lithology.

#### 2.0 TECHNOLOGY

### 2.1 Technology Description

GEDIT involves injection of gaseous electron donors into the soil with the purpose of promoting anaerobic bioremediation of perchlorate to water and chloride ion. This technology can be viewed as bioventing in reverse as illustrated in Figure 1. Bioventing, a proven bioremediation technology for petroleum hydrocarbons, involves the injection of a gaseous electron acceptor (e.g., oxygen) into the vadose zone resulting in the biodegradation of an electron donor (e.g., hydrocarbons). In the present application, the electron acceptor and donor are reversed with the gaseous electron donor being injected in order to biodegrade the electron acceptor (i.e., perchlorate or nitrate).

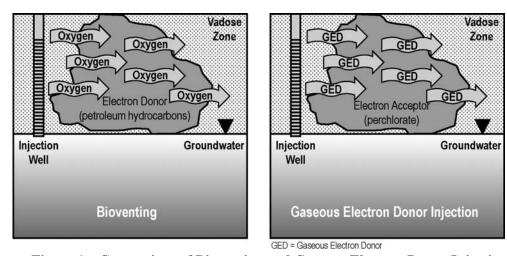


Figure 1 - Comparison of Bioventing and Gaseous Electron Donor Injection Technology

Bioventing is an effective technology because it relies on the excellent mass transfer characteristics of gases resulting in an effective distribution of oxygen through the vadose zone. Similarly, the injection of gaseous electron donors for perchlorate biodegradation in vadose zone soil benefits from these same mass transfer and distribution characteristics.

GEDIT involves injection of gaseous electron donors into the soil using injection wells in combination with optional soil vapor extraction wells. These gaseous electron donors can include hydrogen, propane, or volatile organic compounds such as methanol, ethanol, butanol, acetic acid, ethyl acetate, butyl acetate, hexene, etc. The injected concentration of the electron donor is less than its saturation vapor pressure so that the injected electron donor truly exists as a gas and not as a mist. As the gaseous electron donor material is injected into the vadose zone it partitions between soil moisture and the vadose zone pore space. After it has partitioned into the soil moisture, anaerobic, perchlorate-reducing bacteria can use the electron donor to reductively degrade perchlorate. Any soil nitrate or oxygen that is present in the pore space will also be reduced using the injected gaseous electron donor. The rate at which the gaseous electron donor

is transported through the vadose zone is primarily a function of soil moisture, electron donor Henry's constant, void volume, bulk soil density, bulk gas velocity, soil permeability, and biodegradation rate (Evans and Trute, 2006). GEDIT is similar to anaerobic bioventing (U.S. EPA, 2006b). Anaerobic bioventing has been described to involve injection of hydrogen and carbon dioxide into soil to promote anaerobic biodegradation of organic contaminants including chlorinated hydrocarbons and dichlorodiphenytrichloroethane (DDT). GEDIT can include use of hydrogen/carbon dioxide and can additionally use liquid electron donors that can be vaporized into a gaseous carrier stream.

GEDIT can be implemented in various configurations two of which are illustrated in Figures 2 and 3. In the gas injection configuration, nitrogen from a generator or a liquid nitrogen supply is amended with gaseous electron donor and then injected into the perchlorate-impacted vadose zone. The presence of nitrogen serves to flush oxygen from the soil gas, enhancing conditions for the degradation of perchlorate. In the SVE configuration, soil vapor is extracted, amended with gaseous electron donor, and then injected back into the perchlorate-impacted vadose zone. As the reductive degradation of perchlorate progresses, the oxygen content of the extracted soil is reduced, thereby facilitating further perchlorate degradation. Well spacing for both of the configurations will depend on the pneumatic radius of influence and the specific gaseous electron donor selected for use.

Potential applications of GEDIT include treatment of a wide variety of oxidized contaminants in soil. A partial list of oxidized contaminants that are potentially treatable using GEDIT include:

- Perchlorate
- Chlorate
- Nitrate
- Nitrite
- Selenate
- Arsenate
- Chromate and dichromate (i.e., hexavalent chromium)
- Uranylate
- Pertechnetate
- N-Nitrosodimethylamine (NDMA)
- Trichloroethene (TCE)
- Trichloroethane (TCA)
- Highly energetic compounds including nitro-aromatics such as TNT, RDX, and HMX.

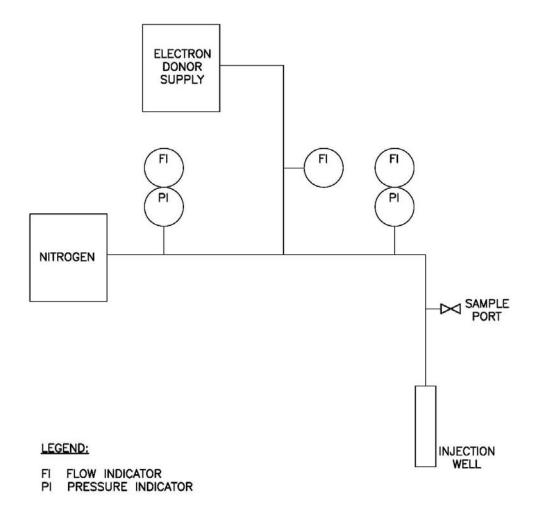
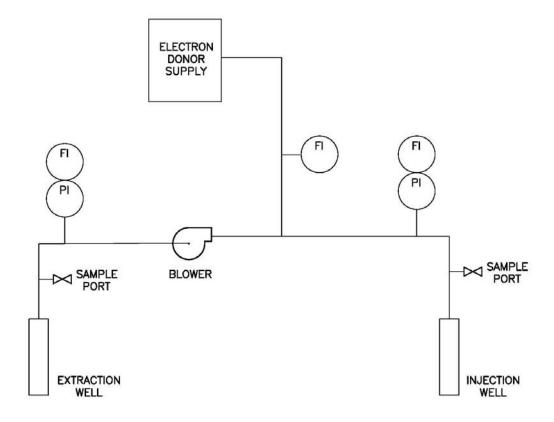


Figure 2 – Example Gas Injection GEDIT Process and Instrumentation Diagram



### LEGEND:

- FI FLOW INDICATOR
  PI PRESSURE INDICATOR

Figure 3 – Example SVE GEDIT Process and Instrumentation Diagram

## 2.2 Technology Development

A chronological summary of GEDIT development is presented in Table 1.

Table 1 – Chronological Summary of Technology Development

	0 V 0V 1		
2002	GEDIT concept conceived by CDM and perchlorate reduction in microcosms demonstrated.		
2003	Work plan for GEDIT pilot test at the former Bermite site in California submitted to and		
	accepted by California Department of Toxic Substances Control (DTSC).		
2003 - 2004	Additional development of GEDIT including evaluation of various electron donors with respect		
	to promoting perchlorate biodegradation and transport through soil.		
2005	Conducted conceptual design and cost estimate for full-scale GEDIT implementation at the		
	Inactive Rancho Cordova Test site (IRCTS) in California.		
2006	GEDIT concept, research results, and economics published (Evans and Trute, 2006).		
2007	U.S. Patent No. 7,282,149 issued to CDM for GEDIT.		
2007	Conducted ESTCP demonstration of GEDIT at IRCTS-PBA		
2008	Work plan for GEDIT pilot test at the former Bermite site in California revised and accepted by		
	DTSC.		

GEDIT technology development has been described in detail previously (Evans and Trute, 2006; Evans 2007). A brief summary of this development is presented below.

Vadose zone soil microcosms amended with ethanol or hydrogen and carbon dioxide as an electron donor were demonstrated to result in complete nitrate biodegradation within 34 days (Evans and Trute, 2006). Complete perchlorate biodegradation required a longer period of time – 105 days. The soil moisture content was an important factor affecting the rate of nitrate and perchlorate biodegradation but nutrient amendment was not important with this particular soil.

Column studies demonstrated widely varying transport rates of different electron donors through moist soil (Evans and Trute, 2006). Primary factors affecting transport included soil moisture, electron donor Henry's constant, void volume, bulk soil density, bulk gas velocity, soil permeability, and biodegradation rate. For example, hydrogen and propane are transported through moist soil rapidly because they do not partition significantly into soil moisture. On the other hand, ethanol vapor is transported slowly through moist soil because it partitions into soil moisture. Ethyl acetate is transported at an intermediate rate – it does not partition into soil moisture as extensively as ethanol but can decompose to ethanol and acetic acid by hydrolysis.

Previous work by the U.S. Engineer Research and Development Center (ERDC) has demonstrated that gaseous electron donors including ethanol, acetone, and isobutyl acetate can promote biodegradation of RDX and trinitrobenzene (TNB) (Rainwater et al., 2001). Thus, GEDIT is potentially applicable to energetic range contaminants including TNT, RDX, and HMX in addition to perchlorate and nitrate. Hydrogen has also been shown to be capable of promoting biological transformation of TNT (McCormick et al., 1976). Ethanol, acetone, isobutyl acetate, and hydrogen are applicable to GEDIT. The biological reduction of VOCs using hydrogen in groundwater has been pioneered by the Air Force Center for Engineering and the Environment (AFCEE). Use of hydrogen in the vadose zone is also possible provided that sufficiently anaerobic conditions for reductive dechlorination can be attained. Thus GEDIT may also be applicable to treatment of VOCs. In general, any contaminant that can be anaerobically biodegraded is a potential candidate for GEDIT.

## 2.3 Advantages and Limitations of the Technology

Bioventing is an effective technology because it relies on the excellent mass transfer characteristics of gases and their ability to distribute oxygen through the vadose zone. Similarly, GEDIT benefits from these same gas mass transfer and distribution characteristics.

The superior mass transfer and distribution of gases as compared to liquids is the major advantage of this technology over attempts to introduce liquids into the vadose zone. Diffusion of gases in the vadose zone improves the ability to deliver the electron donor throughout the soil volume and helps to overcome problems associated with liquid flow through preferential pathways. Additionally, GEDIT does not require the capture and treatment of infiltrated liquids that could otherwise adversely impact groundwater. In projects involving liquid electron donors, the infiltration of these electron donors to groundwater can result in mobilization of naturally occurring metals in soil minerals including iron, manganese, and arsenic. GEDIT has the advantage of not promoting metal mobilization to groundwater. Other than liquid infiltration, the only alternative technologies to GEDIT are excavation for soil and hydraulic containment for impacted groundwater.

Many of the limitations or technical risks for this technology are similar to bioventing technology risks when gas injection is used. Additional limitations or technical risks are associated with the use of electron donors that are also flammable chemicals. Other limitations or technical risks are associated with the nature of sampling and analysis of heterogeneous soils. These and other limitations and risks along with relevant responses are documented in Table 2.

Table 2 – Technical Limitations and Risks

Limitation or Risk	Responses	
Very shallow soil	Implement excavation and ex situ treatment or surface amendment of liquid or solid electron donors if more cost-effective	
Residual electron donor in soil	Operate in bioventing mode to introduce air into vadose zone and promote aerobic biodegradation	
Too low moisture content in soil to support biodegradation	Recognize limits of technology and determine appropriate application. Increasing moisture in situ is infeasible.	
Too high perchlorate in soil to support biodegradation	Recognize limits of technology and determine appropriate application	
Inhibitory conditions such as low pH	Recognize limits of technology and determine appropriate application	
Soil drying during gas injection	This is a perceived risk that has not been demonstrated to occur under actual site conditions.	
Difficulty in data interpretation because of	Conduct site characterization and develop sound sampling and	
heterogeneous concentration distribution in	analysis plan based on statistical soil sampling methods. Collect	
soil	baseline and final soil samples as close to each other as practical.	
Vapor migration to basements	Use appropriate extraction wells to contain vapors. Use sentinel wells to monitor vapors.	
Electron donor flammability	Follow National Electrical Code for Class I/Division II conditions.	
High oxygen in pore space	Inject sufficient electron donor and/or carrier gas to overcome demand and/or oxygen infiltration.	
Oxygen infiltration into vadose zone during operation	Use correctly designed wells and balance injection and extraction rates. Use plastic sheeting as ground cover to minimize air infiltration.	

## 3.0 PERFORMANCE OBJECTIVES

The performance objectives that were established in the Technology Demonstration Plan (CDM, 2007) are presented in Table 3. All of the performance objectives for this demonstration were met. This section describes the each performance objective specifically with respect to the following:

- A full explanation of the objective
- A statement as to what data were collected to evaluate the performance objectives
- A statement as to how the data were interpreted and to what extent the success criteria were met.

**Table 3 – Performance Objectives** 

Table 5 – Terrormance Objectives				
Performance	Data	Success Criteria	Results	
Objective	Requirements	Success Criteria	Results	
Quantitative Perfo	rmance Objectives			
Perchlorate Destruction	Pre- and post- treatment contaminant concentrations in soil	Average 90 percent reduction in perchlorate concentration within the radius of influence (ROI) for electron donor transport	93±9 percent reduction observed within 10 ft from P4 injection point at depths of 10 to 40 ft bgs.	
Nitrate Destruction	Pre- and post- treatment contaminant concentrations in soil	Average 90 percent reduction in nitrate/nitrite concentration within the ROI for electron donor transport	94±9 percent reduction observed within 10 ft from P4 injection point at depths of 10 to 50 ft bgs. 90±14 percent reduction observed within 56 ft from P4 injection point at depths of 10 to 50 ft bgs.	
Perchlorate Destruction Rate	Pre- and post- treatment contaminant concentrations in soil	Average 90 percent perchlorate reduction within 12 months	88±11 percent reduction observed in 3 months based on comparison of confirmation boring CB3 concentrations to baseline concentrations. 93±9 percent reduction observed in 5 months or less based on the total duration of hydrogen injection.	
Nitrate/Nitrite Destruction Rate	Pre- and post- treatment contaminant concentrations in soil	Average 90 percent nitrate/nitrite reduction within 6 months	93±5 percent reduction observed in 3 months based on comparison of confirmation boring CB3 concentrations to baseline concentrations	

**Table 3 – Performance Objectives** (Continued)

Table 5 – Terrormance Objectives (Commueu)			
Performance Objective	Data Requirements	Success Criteria	Results
Implementability	Hydrogen, propane, and oxygen concentrations in piezometers	ROI for electron donor transport > 10 ft in permeable zones	<ul> <li>Hydrogen and propane observed up to 56 ft away from injection point.</li> <li>Oxygen depletion up to 56 ft away from injection point.</li> <li>Significant perchlorate destruction was observed at distances up to 15 ft from the injection point.</li> <li>Conservative ROI for consistent hydrogen distribution and oxygen depletion was at least 10 ft and likely 15 ft.</li> <li>With respect to conditions for nitrate destruction the ROI was at least 56 ft.</li> </ul>
Qualitative Perform	mance Objectives		
Safety	OSHA     Reporting     Ambient gas     concentration	No reportable health and safety incidents, ambient above-ground air concentration of total hydrocarbons < 10 percent of the lower explosive limit (LEL)	No health and safety incidents     Ambient concentrations of hydrogen and propane were non-detectable (i.e., less than 0.1 percent and 0.5 percent, respectively) and less than 10 percent of the LEL.
Regulatory Acceptance	Letter of acceptance from regulatory agency	Demonstration approval, acceptance, or concurrence by regulatory agency	<ul> <li>Technology Demonstration         Plan approved by California         Regional Water Quality Control         Board</li> <li>Storage and use of flammable         gases approved by County of         Sacramento Hazardous         Materials Division</li> </ul>
Ease of Use	Feedback from field technician on usability of technology and time required	A single field technician able to effectively take measurements	A single field technician operated the system and collected data. site visits during normal operations were once every week or once every two weeks.

#### 3.1 Perchlorate Destruction

Perchlorate destruction was defined as the percent reduction in perchlorate concentration in soil within the radius of influence (ROI) for gaseous electron donor transport and oxygen depletion. As described in Section 3.5 below, this ROI was conservatively estimated at 10 feet. In addition, the depth of electron donor transport was estimated to be 40 ft. Therefore, the zone of influence used to estimate perchlorate destruction was a cylinder with a 10 ft radius and a 40 ft length that was centered at gas injection piezometer P4.

Data collected to evaluate perchlorate destruction included perchlorate concentrations in soil samples from the borings within the zone of influence. Initial perchlorate concentrations were measured in soil samples collected from borings conducted to install piezometers and wells within the 10-ft ROI. These included P3, P4, P5, and INJ2. Discrete sampling depths included 10, 20, 30, and 40 ft bgs. Final perchlorate concentrations were measured in soil samples from borings conducted adjacent to the initial borings. These borings included CB-17, CB-14, CB-15, and CB-16, respectively. Discrete sampling depths included 10, 20, 30, and 40 ft bgs.

Percent perchlorate removal was calculated for each initial-final data pair. The percent removals were averaged and standard deviations were calculated. The result (93±9 percent) compared favorably to the goal of 90 percent. The metric for this performance objective was met.

#### 3.2 Nitrate Destruction

Nitrate destruction was defined similarly to perchlorate destruction with two exceptions. Since nitrite can transiently accumulate during denitrification, nitrate destruction was quantified using the sum of nitrate and nitrite concentrations. Additionally, the depth of influence for nitrate destruction was 50 ft compared to 40 ft for perchlorate destruction. Therefore soil samples collected from 50 ft bgs were also used in the data analysis. Otherwise, the approach for determining nitrate destruction was as described in Section 3.1.

Percent nitrate removal was  $94\pm9$  percent and compared favorably to the goal of 90 percent. When all of the data were considered (i.e., up to 55 ft ROI), the percent removal was  $90\pm14$  percent. The metric for this performance objective was met.

#### 3.3 Perchlorate Destruction Rate

The performance objective for the rate of perchlorate destruction was based on the time required to attain a 90 percent reduction in perchlorate concentration.

As discussed in Section 5.7.5, soil heterogeneity complicated assessment of temporal trends of perchlorate concentration. Final assessment of overall perchlorate destruction was described in Section 3.1. Intermediate soil sampling and analysis events were used to develop trends in perchlorate concentration. These data only allowed a rough assessment of perchlorate concentration trends because of heterogeneity.

Nevertheless, the 90 percent removal metric appears to have been attained within five months of operation and at some locations in about three months. This result compares favorably with the 12-month performance objective. Actual perchlorate degradation rates were also calculated and are described in Section 5.7.5. The metric for this performance objective was met.

#### 3.4 Nitrate Destruction Rate

The performance objective for the rate of nitrate destruction was similar to that for perchlorate except that the sum of nitrate and nitrite was used in the assessment. The performance metric for this objective was met – within three months 93 percent nitrate+nitrite removal was observed at CB3.

### 3.5 Implementability

*In situ* destruction of perchlorate using GEDIT requires distribution of electron donors and reduction of oxygen concentrations. Achieving these requirements at a given site is affected by injection well spacing/design and gas flow rates. In general, a greater well spacing or ROI is desirable and considered more implementable. Therefore the ROI was used as a performance objective for implementability.

The concentrations of electron donors and oxygen in soil gas and perchlorate and nitrate/nitrite in soil were used to estimate the ROI. The ROI for the demonstration was based on the distance from the point of injection where favorable gas compositions existed and perchlorate destruction was 90 percent or greater.

Electron donor concentrations decreased and oxygen concentrations increased as the distance from the injection point increased. Hydrogen concentrations were generally greater than 0.5 percent at distances up to 10 to 20 ft from the point of injection and depths 10 ft below the point of injection. Oxygen concentrations were generally less than four percent at distances up to 10 to 20 ft from the point of injection. Perchlorate destruction was observed at least 10 ft away from the point of injection and nitrate/nitrite injection at least 55 ft away. Based on these data, the ROI is conservatively estimated at 10 ft and likely to be 15 ft for perchlorate destruction. This estimate compares favorably with the performance objective of 10 ft. The ROI is strongly a function of gas flow rate and will increase with greater flow rates. The metric for this performance objective was met. The ROI for nitrate destruction was at least 55 ft.

## 3.6 Safety

Safety is very important and the topic of flammability is often brought up with respect to GEDIT. GEDIT employed the hydrogen and LPG in this demonstration. Safe use of these flammable gases necessitated reasonable engineering design considerations, use of intrinsically safe monitoring equipment, placarding in the area to prevent sources of ignition, and appropriate health and safety training.

Metrics for meeting the safety performance objective included OSHA reportable health and safety incidents and flammable gas concentrations above the ground surface.

No health and safety incidents occurred during the demonstration and flammable gas concentrations above the ground surface were not detectable. While concerns regarding GEDIT safety are reasonable, the results of this demonstration indicate the technology can be implemented safely. The metric for this performance objective was met.

#### 3.7 Regulatory Acceptance

This performance objective was defined as permission by the regulatory agency to install and operate the GEDIT system. One consideration in gaining acceptance was whether Waste Discharge Requirements (WDR) – the California equivalent of the U.S. EPA Underground Injection Control (UIC) program – would be applicable.

The California Regional Water Quality Control Board (RWQCB) approved the Technology Demonstration Plan (CDM, 2007) which constituted a work plan for this project. WDR was not required because injection into groundwater was not proposed or conducted. The metric for this performance objective was met.

#### 3.8 Ease of Use

Ease of use is a qualitative performance objective that was based on operational requirements. The metric for this performance objective was the frequency at which an operator needed to visit the site. The reasons for site visitation during normal operations included gas cylinder changeouts and monitoring. This occurred once per week or every other week, which is considered reasonable. The metric for this performance objective was met.

#### 4.0 SITE DESCRIPTION

The information presented in this section is based on previously published reports (AGC & Simon HSI, 1993; Aerojet & HSI GeoTrans, 2000). The Technology Demonstration Plan (CDM, 2007) was based on data provided in these reports. Additional information and data have since been collected for the site. Therefore, the data and historical figures presented below should not be considered to be completely representative of current site conditions. Nevertheless, the data presented in the historical reports are considered adequate for planning and execution of this technology demonstration.

#### 4.1 Site Location and History

The demonstration was conducted at the Propellant Burn Area (PBA) within the Inactive Rancho Cordova Test site (IRCTS) which is located approximately 15 miles east of Sacramento (Figure 4). The PBA is located in the northwestern quadrant of the IRCTS. The PBA comprises approximately 8 acres of undeveloped land within the IRCTS. An east-west unpaved road passes through the approximate center of the PBA (Figure 5). The PBA boundary was determined by reviewing aerial photographs and by identifying residual metallic debris relative to topography, road access, and access barriers (steep dredge valleys and cobble piles).

Prior to purchase by Aerojet, the IRCTS was used for agricultural and mining purposes. During the 1940s, the PBA was dredged to a depth of approximately 70 feet to remove gold from the subsurface gravel deposits. Dredge tailings occupy 60 to 70 percent of the IRCTS, including the entire PBA and vicinity.

In 1956, the IRCTS was purchased by Aerojet General Corporation (AGC) and in 1961, Douglas Aircraft Company (DAC) purchased the property from AGC to establish a static rocket test facility. From 1957 through 1969, DAC and later McDonnell Douglas Corporation (MDC) assembled and static tested various rocket systems at facilities to the south and east of the PBA. The PBA was used by both AGC and MDC to incinerate solid and liquid waste rocket propellant and other waste materials (Aerojet & Simon HSI, 1993). Other wastes consist of non-specific laboratory chemicals. Known constituents include ammonium perchlorate, aluminum, some metals, and solvents, such as trichloroethene (TCE). Solid propellants within large motor casings were ignited within the U-shaped revetment containing a small concrete pad with metal strapdowns. Solid propellant within small casings and solid propellant fragments were ignited on the southeast side of the PBA. Liquid propellant was ignited in troughs (split rocket casings) on the north side of the revetment.

Since 1969, the IRCTS, including the PBA, has been inactive with respect to aerospace activities. In 1984, AGC re-acquired the IRCTS from MDC. Based on a review of available aerial photographs and limited records, the PBA appears to have been used intermittently between 1957 and 1963.

Gold dredging has affected topography at the PBA, creating low, hummocky topography on the south and east, and higher north-south trending windrows of cobbles on the north and west. Elevations range from approximately 196 feet above mean sea level (msl) at the top of the revetment and the dredge tailings windrow on the northeast side of the PBA, to approximately

168 feet in the shallow depression in the southwest quadrant of the PBA. The road level elevation ranges between 180 and 185 feet above msl. The area immediately around the revetment has been graded relatively flat.

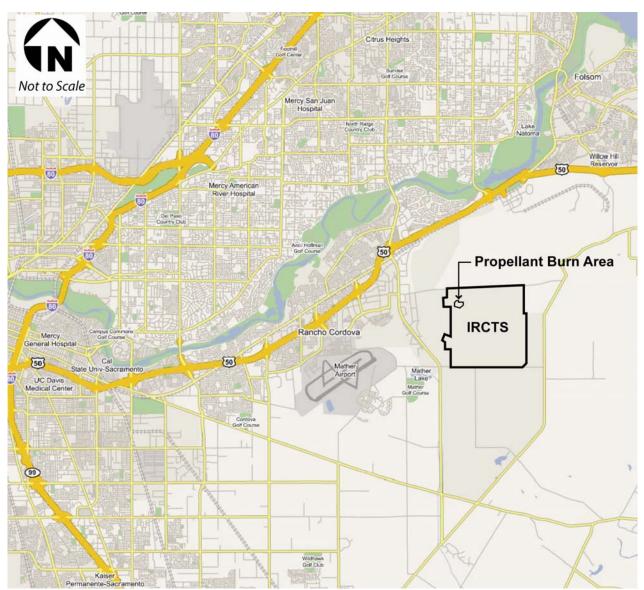
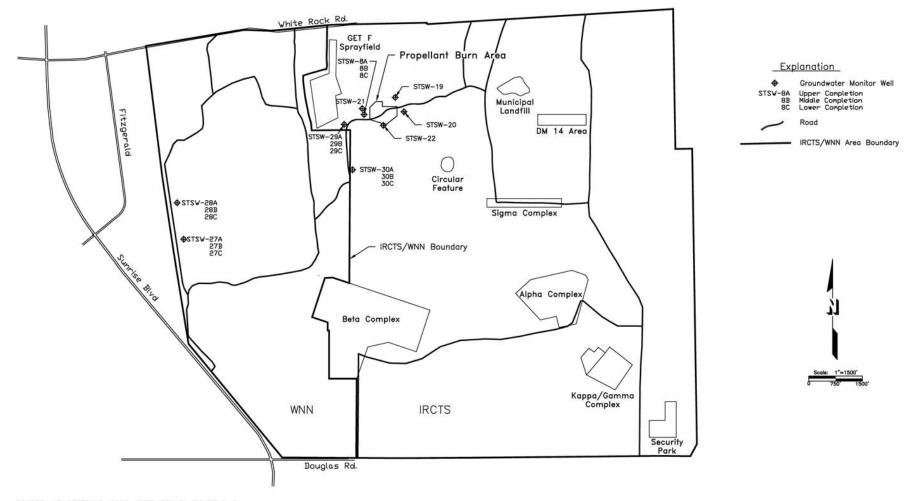


Figure 4 – Vicinity Map, Inactive Rancho Cordova Test Site



SOURCE: HSI GEOTRANS, 2000, IRCTS-PBA RI, FIGURE 1-2

Figure 5 – IRCTS Site Map

# 4.2 Site Geology/Hydrogeology

# 4.2.1 Site Geology

The PBA and immediate vicinity are underlain by dredge tailings, which are composed of an unconsolidated mixture of sand and gravel with cobbles and small boulders. A veneer of slickens is present in topographic lows. Well logs indicate that the dredged material extends to depths of at least 70 feet and overlies a layer of silt and clay. This layer overlies more sands and gravels. A PBA site plan and associated cross-section are shown on Figures 6 through 8. These subsurface materials are comprised of the Pliocene-age Laguna Formation, which overlies the Miocene-age Mehrten Formation. Both formations were deposited under fluvial conditions, creating inter-bedded layers of gravels, sands, silts, and minor clays, dipping slightly (approximately one degree) to the west-southwest. The Laguna Formation is derived from granitic and metamorphic sources, while the Mehrten Formation is derived from andesitic sources (Wagner, et al., 1981).

# 4.2.2 Site Hydrogeology

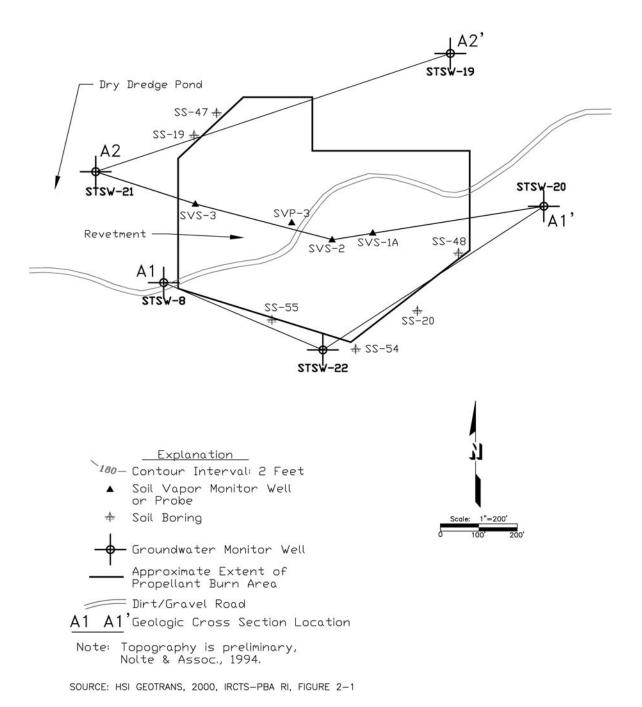
The earliest characterization of the hydrogeology in the vicinity of the IRCTS was conducted by the California Department of Water Resources (California DWR, 1964), based on more than 300 water-supply wells scattered across more than 100 square miles, including five wells within the IRCTS and 16 wells within one mile of the IRCTS. The DWR bulletin showed that groundwater beneath the PBA was flowing toward the west and west-southwest during 1962 and 1963, respectively, under gradients of 0.0038 and 0.0051 ft per ft. In addition, water level elevations in 1962 to 1963 were approximately 40 feet higher than water level elevations during February 1998.

Groundwater levels fluctuate seasonally, and since 1992, have typically varied between three and four feet over a total range of approximately eight feet. Water level elevations have decreased 25 to 35 feet since the early 1960s. This decline is probably due to several factors, including reduced recharge after the termination of dredging operations in 1962 and increased groundwater pumping for municipal use. Depth to groundwater in the PBA was about 120 to 130 feet below ground surface in 1998. This depth is 50 feet or more below the GEDIT injection zone for this demonstration.

Surface drainage is controlled by the topography and coarseness of the dredge tailings. Most precipitation into the dredge tailings infiltrates rapidly rather than flowing overland. Vertical movement of water in dredge tailings may vary from two inches to more than 20 inches per hour (SCS, 1993). Surface water may pond briefly prior to infiltration in low-lying areas that contain fine-grained materials (i.e., slickens) from the dredging. No perennial streams, pools or bodies of surface water exist in the vicinity of the PBA (USGS, 1980). One seasonal wetland depression exists within the PBA (Gibson & Skordal, 1999). Vernal pools are not present in the vicinity of the PBA (ENSR, 1993; F&WS, 1994; Coy, 1996; Gibson & Skordal, 1999).

Recharge to the shallow groundwater table is primarily from infiltration of precipitation, and the amount of recharge is greater in the areas of coarse dredge tailings than areas with undisturbed

ground. The deeper groundwater is recharged by two sources: vertical flow from the shallow groundwater aquifer and under flow from up-gradient. Water level data indicate that shallow groundwater partially recharges deeper groundwater, as there is a downward vertical gradient between the wells. Deeper groundwater receives recharge directly from precipitation to the east of the PBA, where that aquifer is closest to the ground surface.



**Figure 6 – Cross-Section Locations** 

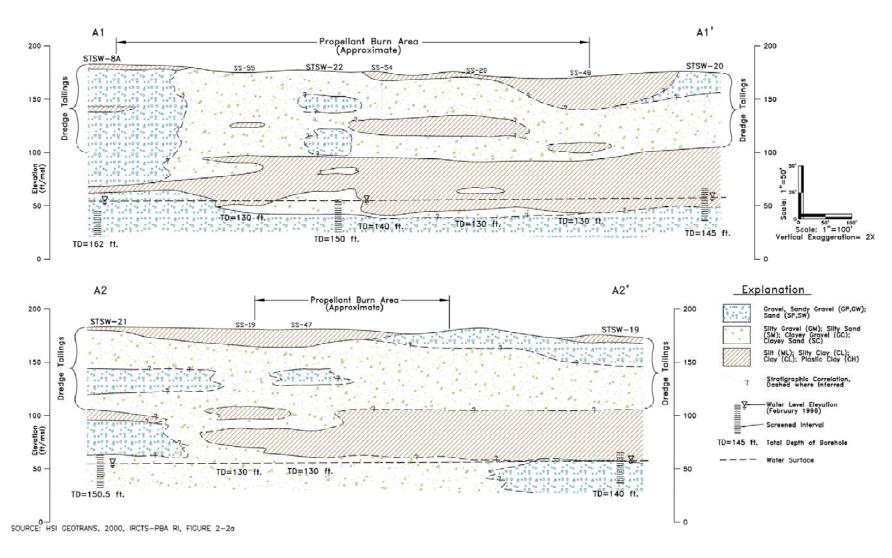


Figure 7 – Generalized Lithologic Cross-Sections A1-A1' and A2-A2'

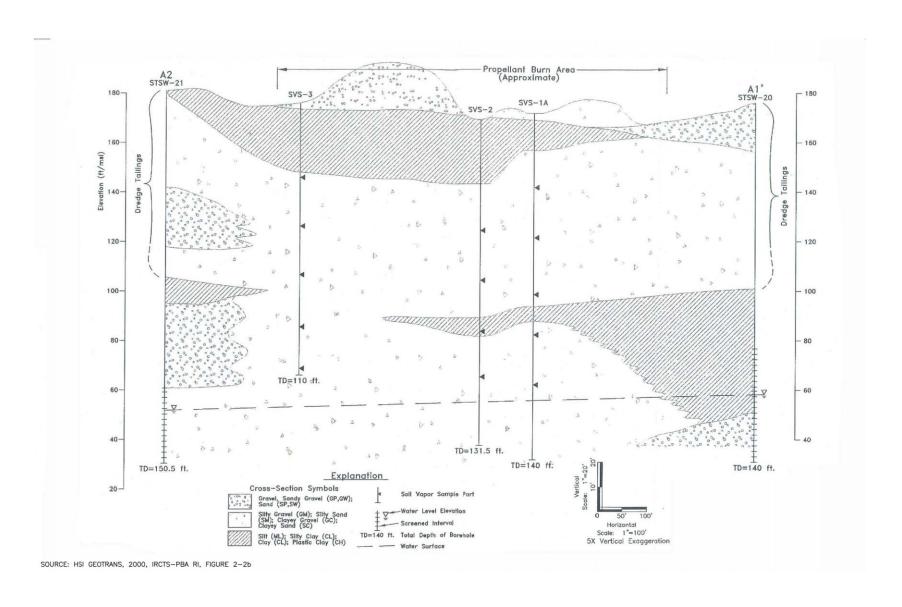


Figure 8 – Generalized Lithologic Cross-Section A2-A1'

#### 4.3 Contaminant Distribution

Based on soil and groundwater investigations, the following chemicals have been detected at the PBA: perchlorate, polychlorinated dibenzodioxins/dibenzofurans (dioxins/furans), VOCs, specifically TCE, metals, basic, neutral, and acidic semi-volatiles (BNAs) and polychlorinated biphenyls (PCBs) (Aerojet & HSI GeoTrans, 2000). Site characterization and the baseline health and ecological risk assessment have established that only perchlorate, dioxins/furans, and TCE are chemicals of concern at the PBA.

Pre-existing investigation data (Aerojet & HSI GeoTrans, 2000; Fricke and Carlton, 2005) are extensive and demonstrate that perchlorate contamination in soil is widespread within the PBA. The demonstration was conducted in the vicinity of SS-2 (later converted to well SVS-2), as indicated on Figure 9. Perchlorate concentrations in excess of 100 milligrams per kilogram (mg/kg) were observed near the surface and decreased with depth (Figures 9 through 14). The demonstration was conducted to a depth of 50 feet below ground surface (bgs) and perchlorate concentrations were generally in the single or double digit mg/kg in the vicinity of SS-2 (Figures 13 and 14).

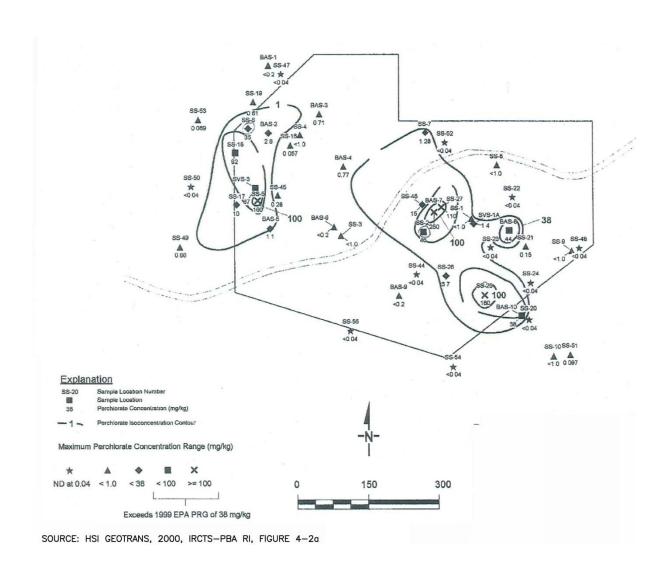


Figure 9 – Maximum Perchlorate Concentrations in Soil 0' to 20' Below Ground Surface

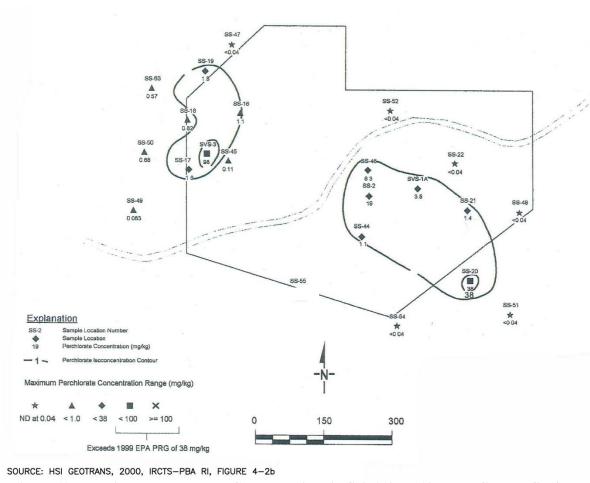


Figure 10 – Maximum Perchlorate Concentrations in Soil 21' to 70' Below Ground Surface

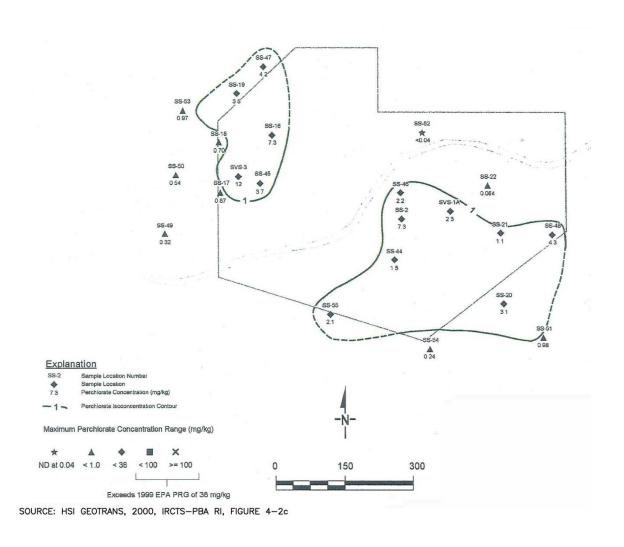


Figure 11 – Maximum Perchlorate Concentrations in Soil 71' to 140' Below Ground Surface

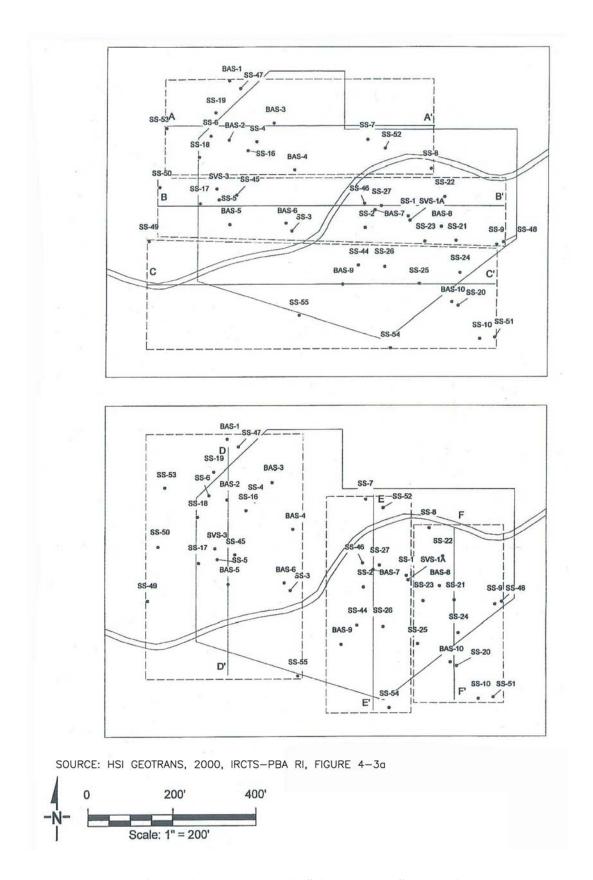
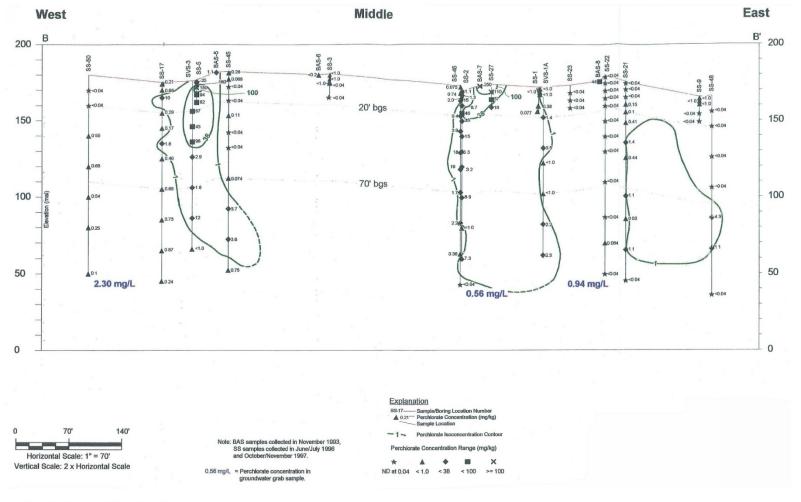
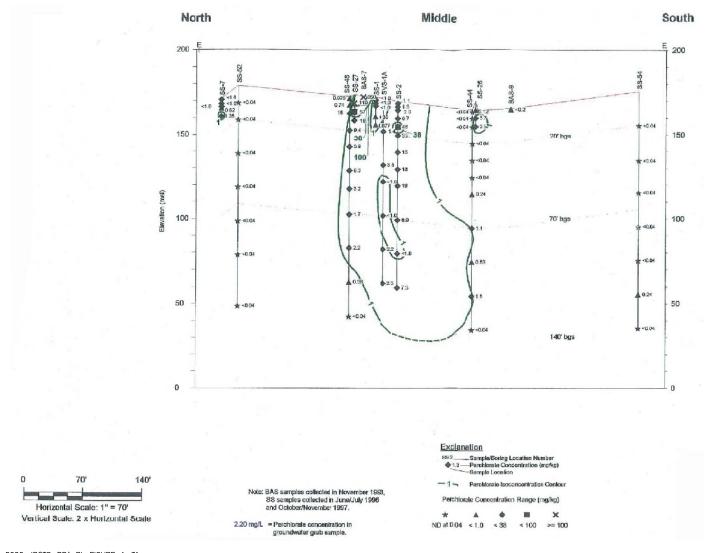


Figure 12 – Perchlorate in Soil Depth Profile Locations



SOURCE: HSI GEOTRANS, 2000, IRCTS-PBA RI, FIGURE 4-3c

Figure 13 – Perchlorate in Soil Depth Profile B-B'



SOURCE: HSI GEOTRANS, 2000, IRCTS-PBA RI, FIGURE 4-3f

Figure 14 – Perchlorate in Soil Depth Profile E-E'

# 5.0 TEST DESIGN

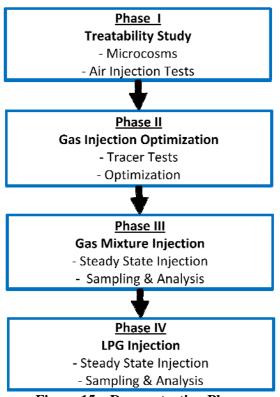
This section provides the detailed description of the system design and testing conducted during the demonstration.

# 5.1 Conceptual Experimental Design

The demonstration was conducted in four phases as illustrated in Figure 15.

Phase I comprised treatability studies conducted in the laboratory and at the site. The laboratory treatability study was a microcosm study conducted to identify gaseous electron donors that were capable of promoting perchlorate biodegradation in site soil. The field treatability study involved injection of air into a single well at various flow rates to characterize gas permeability and pneumatic radius of influence in the vadose zone.

Phase II involved tracer tests using a hydrogen/nitrogen mixture and optimization tests using various gas mixtures. The tracer tests were conducted to determine the radius of influence for hydrogen when injected under different conditions. The optimization tests were conducted to identify the combination of



**Figure 15 – Demonstration Phases** 

variables (e.g., gas composition, injection wells and locations, gas flow rates, pulsing strategy, etc.) that resulted in maximum delivery of electron donor, minimization of oxygen concentrations, and lowest gas use.

Phase III involved continuous injection of a gas mixture comprised of 79 percent nitrogen, 10 percent hydrogen, 10 percent liquefied petroleum gas (LPG), and 1 percent carbon dioxide over a period of about five months. This steady state operation was conducted to generate a vadose zone atmosphere that was supportive of perchlorate biodegradation. Gas and soil samples were collected to verify system operation and quantify perchlorate and nitrate degradation.

Phase IV involved continuous injection of pure LPG to evaluate its potential use as an electron donor. LPG was injected continuously for about three months and gas samples were collected and analyzed periodically. Soil samples were collected and analyzed at the end of this Phase to quantify perchlorate and nitrate biodegradation.

## 5.2 Baseline Characterization

This section presents the baseline characterization activities that occurred in 2006. These activities included drilling of two boreholes, collection of soil samples, and installation of one well and one piezometer. The samples were analyzed for soil characteristics and contaminant concentrations and also used for the microcosms in the treatability study.

#### 5.2.1 Drilling, Sample Collection, and Analysis

From July 27, to August 2, 2006, two boreholes were advanced by the Water Development Corporation (WDC) of Woodland, California. Both boreholes were drilled utilizing the sonic drilling method. The injection well (CDM-INJ1) was advanced to a total depth of 70.5 feet below ground surface (bgs) using a 6-inch diameter core barrel and a 10-inch diameter washover casing (Figure 16). The piezometer (CDM-P1) was advanced to a total depth of 72 feet bgs using a 4-inch diameter core barrel and a 6-inch diameter wash-over casing. Design details are presented in Section 5.4.

The boreholes were continuously cored to total depth by advancing the core barrel in 10-foot increments. As the core barrel was advanced, a continuous core sample was simultaneously collected inside the core barrel. After each 10-foot increment, the temporary wash-over casing was advanced to depth and the core barrel was tripped from the borehole. The core sample was removed from the core barrel and placed in a plastic core bag. This process was repeated until the borehole was advanced to total depth.

The continuous core was logged using the Unified Soil Classification System (USCS) in accordance to ASTM Standard D2488: Standard Practice for Description and Identification of Soils (Visual-Manual Procedure). The core was logged by a CDM field geologist under the supervision of a State of California, Professional Geologist. The log included a description of the materials encountered during drilling and noting zones impacted of visual contamination. Additionally, the core was screened for volatile organic compounds using a photo-ionization detector (PID) by placing a portion of the core in a zip-lock sealed bag. After approximately five to ten minutes, the zip-lock bag was punctured with a small hole and the tip of the PID was inserted into the bag to assess the head space in the bag for volatile organic compounds. The measurements were recorded on the boring log. The boring logs are presented in Appendix B.

Soil samples were collected from the continuous core and placed in sample containers. As required, some of the samples were placed on ice. Samples were submitted to the CDM laboratory in Bellevue, Washington; Laucks Testing Labs later acquired by Pace Analytical in Seattle, Washington; and The Pennsylvania State University (PSU) in University Park, Pennsylvania under chain-of-custody protocol. Additional details on analytical methods are presented in Section 5.6.

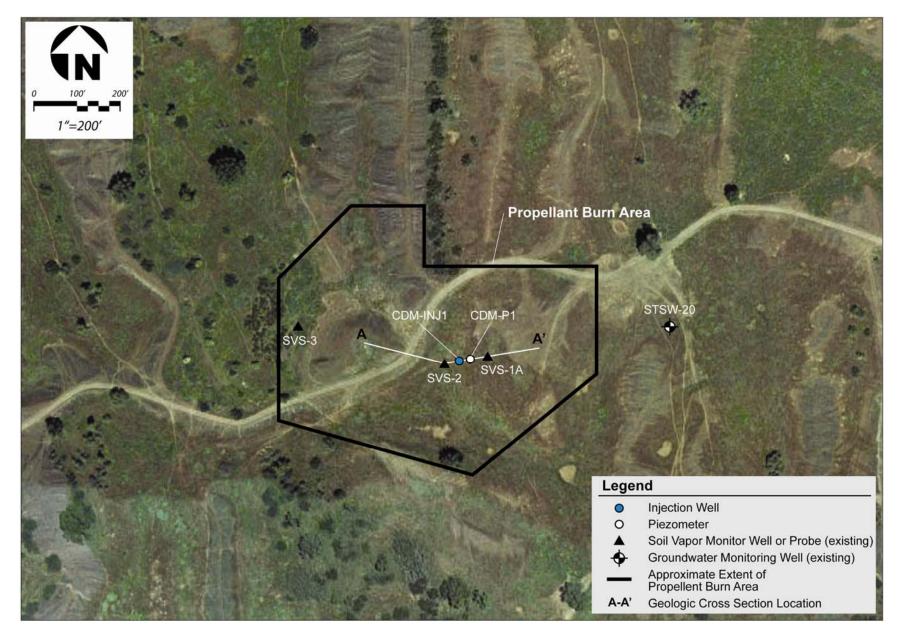


Figure 16 – Locations of Soil Borings/Pilot Test Wells

## **5.2.2** Baseline Characterization Results

The lithologic conditions encountered during drilling ranged from silt and clay to silty sand and clayey gravel to cobbles. No soil discoloration or odors were observed in the drill cuttings from either boring. All of the PID readings were ND. Groundwater was not encountered during drilling and well construction. A detailed description of the soils encountered in each borehole is presented on the boring logs (Appendix B). Figures 17 and 18 show the grain size distribution for soils encountered during boring completion and Figure 19 shows a lithologic cross-section based on these data and existing data (Aerojet & HSI GeoTrans, 2000). These data indicate that soil is generally coarse-grained and supportive of gas injection with the exception of shallow soil (i.e., 15 ft bgs) in boring CDM-INJ1.

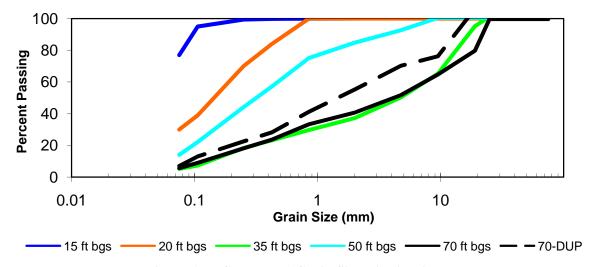


Figure 17 – CDM-INJ1 Grain Size Distribution

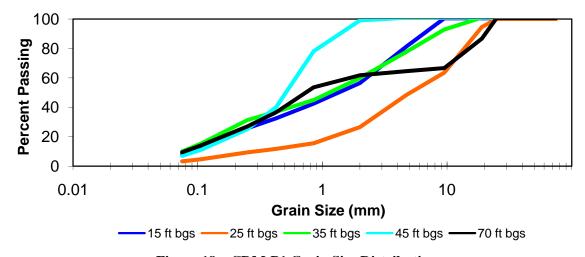


Figure 18 – CDM-P1 Grain Size Distribution

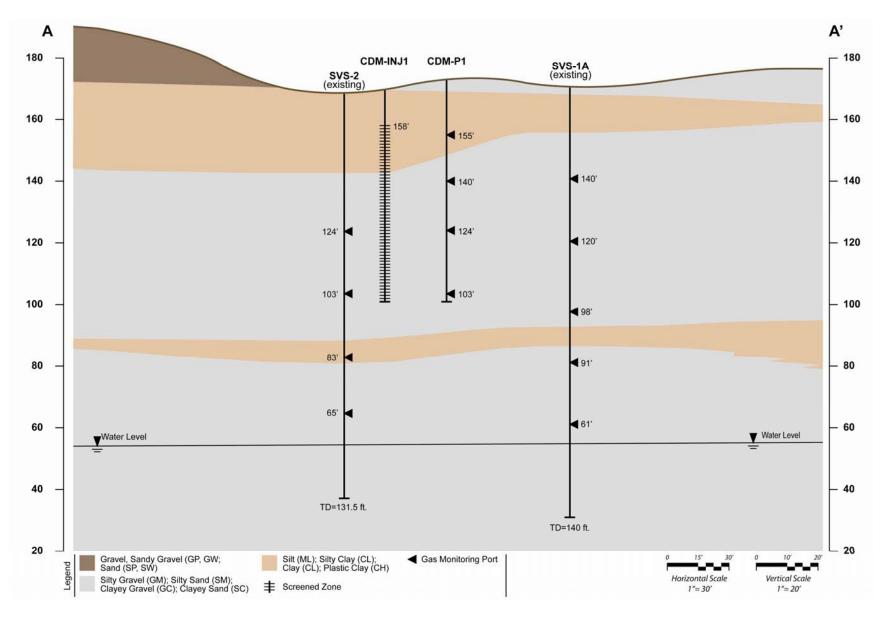


Figure 19 – Generalized Lithologic Cross Section

The analytical results for perchlorate, nitrate/nitrite (i.e., nitrogen as nitrate plus nitrite), and moisture are presented in Figures 20 and 21. For soil from boring CDM-INJ1, the data indicate that nitrate/nitrite concentrations were less than 5 mg-N/kg and perchlorate ranged from 3.7 to 59 mg/kg based on field screening analyses. Perchlorate was present in greater concentrations at shallower depths and was associated with the finer grained soils based on comparison to Figure 21. Greater concentrations of perchlorate were also associated with greater moisture contents. The maximum moisture content in soil from CDM-INJ1 was 34 percent and the minimum moisture content was 6.5 percent.

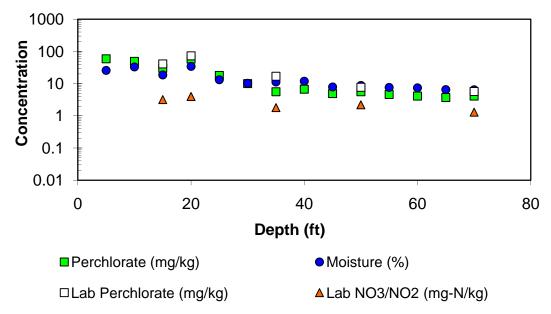


Figure 20 – CDM-INJ1 Contaminant and Moisture Distribution

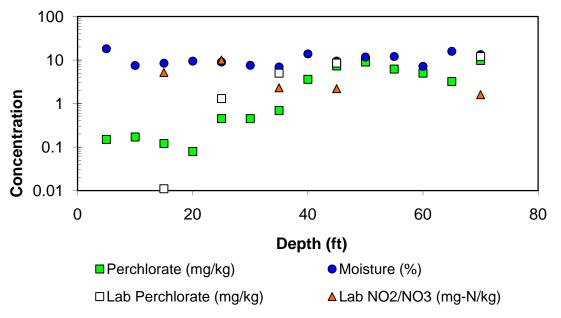


Figure 21 – CDM-P1 Contaminant and Moisture Distribution

For soil from boring CDM-P1, nitrate/nitrite concentrations were similar but perchlorate concentrations were ND at shallow depths and ranged from 0.45 to 9.8 mg/kg at greater depths. Moisture ranged from 6.9 to 18 percent. For soil from both borings, soil moisture ranged from 6.9 to 16 percent in the more permeable soils (i.e., not silt or clay).

Total organic carbon (TOC) concentrations were generally ND or near the limit of detection (0.2 to 0.3 mg/kg) and pH ranged from 6.9 to 8.1. These data and tables for all baseline characterization data are presented in Appendix C.

## 5.3 Phase I – Treatability Study

This section summarizes the results of the laboratory microcosm and the field air injection studies. Detailed methods and results are presented in Appendix D.

## **5.3.1 Microcosm Study**

Sacrificial batch microcosm tests were used to rapidly assess the ability of gaseous electron donors and various moisture contents to achieve optimal perchlorate remediation in vadose zone soil taken from the site. The electron donor candidates tested were hydrogen, 1-hexene, ethyl acetate, and LPG. Each electron donor was tested at two different concentrations under two different soil moisture contents that were representative of minimum and maximum site moisture contents at the site. Perchlorate reduction did not occur in low moisture (7 percent) microcosms after an incubation time of 125 to 187 days, and all bottles except ethyl acetate achieved complete or partial perchlorate reduction in high moisture (16 percent) bottles (Figure 22). Perchlorate reduction was observed in the negative control. However, this reduction was attributable to an experimental artifact where hydrogen was produced when the microcosm bottles were initially left on the laboratory bench in the light. This artifact is explained in detail in Appendix D.

Results from these microcosm tests indicate that hydrogen was an effective electron donor for perchlorate biodegradation in site vadose zone soil, achieving complete perchlorate degradation within 35 to 42 days. LPG may have promoted complete perchlorate reduction at the high LPG dose and 1-hexene may have promoted partial perchlorate reduction at both doses; however, when compared to hydrogen, these donors had more significant lag periods of 21 to 49 days, respectively. Additionally, the observation of perchlorate reduction in the negative does not allow definitive conclusions regarding the effects of these electron donors on perchlorate reduction.

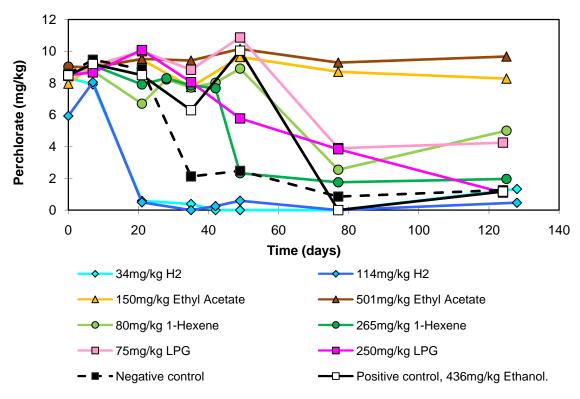


Figure 22 – Microcosm Study Results at the High Moisture Condition

## **5.3.2** Air Injection Test

An air injection test was conducted at the PBA site using the injection well CDM-INJ1 and piezometer CDM-P1 in combination with the two existing wells at the site (SVS1A and SVS2). The objectives of the air injection test were to:

- Estimate the corresponding backpressures for various gas flow rates; and
- Estimate the pneumatic zone of influence of gas injection.

The data show minimal pressure at the injection well (5 inches water column [in. w.c.] or less) and a positive effect from air injection on the piezometers located up to 84 feet from the injection well (Figure 23). The average pneumatic permeability (k) based on these data was calculated to be  $5.6 \times 10^{-4} \pm 0.9 \times 10^{-4}$  cm<sup>2</sup> at 120 ft above mean sea level (amsl) based on the observed data (Figure 24). This permeability is high and typically associated with unconsolidated gravels. Because of this high permeability, the radius of pneumatic influence at the maximum flow rate of 420 cubic feet per minute (cfm) was determined to be at least 84 ft. Pneumatic effects were observed at a distance of 34 ft at the lowest flow rate tested – 21 cfm (Figure 25). Pneumatic effects were observed at elevations down to about 50 ft bgs (i.e., 120 ft amsl). Based on this result, the remaining injection wells and piezometers were installed only to a depth of 50 ft bgs rather than 70 ft bgs.

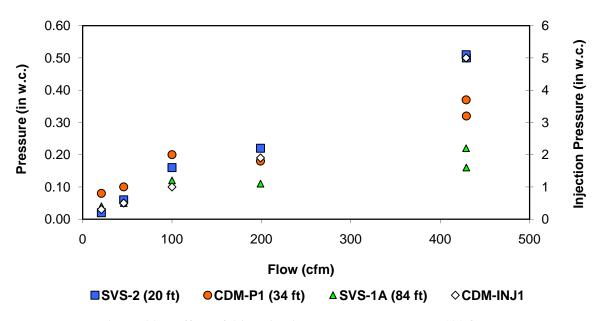


Figure 23 – Effect of Air Injection Flow on Pressure at 120 ft amsl

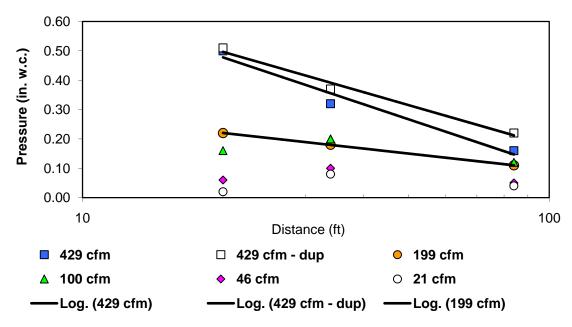


Figure 24 – Relationship between Distance from Injection Well INJ1 and Piezometer Pressure at 120 ft amsl

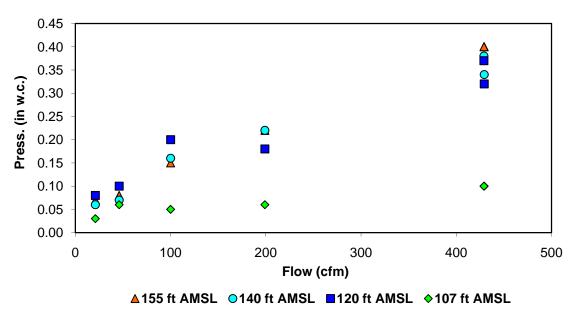


Figure 25 – Effect of Air Flow on Pressure at Piezometer P1

# 5.4 Design and Layout of Technology Components

This section presents the design and construction attributes of the wells, piezometers, and process equipment used for the demonstration.

#### **5.4.1** Wells and Piezometers

A total of three injection wells and ten piezometers were installed for the demonstration (Figure 26). The original design concept was based on three injection wells arranged in an equilateral triangle with an inter-well spacing of 20 ft. Two transects of piezometers were installed radiating from well INJ2. One transect in a general east-west orientation comprised piezometers P4 through P1 and SVS-1A. A second transect in a general north-south orientation comprised piezometers SVS-2 and P5 through P8. As described in Section 5.5, Phase III and IV gas injections were ultimately conducted using piezometer P4 rather than any of the "injection" wells. The distances of the wells and piezometers from well INJ2 and piezometer P4 are listed in Table 4.

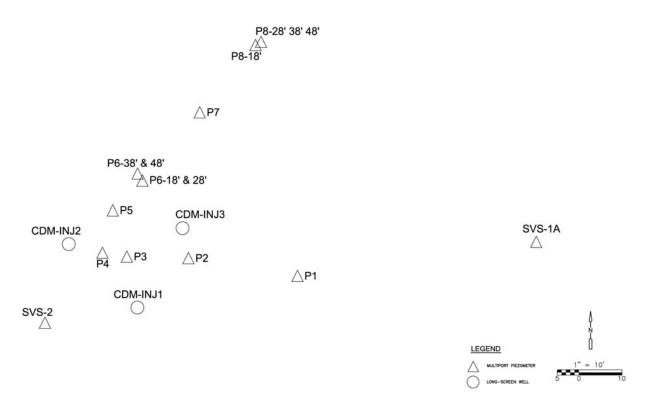


Figure 26 – Piezometer and Well Locations

**Table 4 – Well and Piezometer Distances** 

ID	Distance from INJ2 (ft)	Distance from P4 (ft)
INJ1	21.7	14.7
INJ2	0.0	8.2
INJ3	26.7	19.6
P1	53.6	45.6
P2	28.0	18.6
P3	13.9	5.33
P4	8.2	0.0
P5	12.6	9.4
P6	22.4	18.1
P7	42.7	36.7
P8	63.7	56.1
SVS-1A	134	125
SVE-2	19.5	21.0

Two of the piezometers (SVE-1A and SVE-2) were constructed prior to this project and construction details are presented in Table 5. One injection well (INJ1) and one piezometer (P1) were installed in 2006 as described in Section 5.2.1. Injection well INJ1 was constructed with 6inch diameter schedule 40 PVC from ground surface to 10 feet bgs and slotted 6-inch diameter schedule 40 PVC (0.020-inch slot size) from 10 to 70 feet bgs. Annular materials include a filter pack (No. 3 Monterey Sand) from 8 to 70.5 feet bgs, a bentonite chip seal from 6 to 8 feet bgs, and a cement grout surface seal from ground surface to 6 feet bgs. Annular materials were installed by pouring the materials into the annular space between the well casing and the washover casing. Depths were tagged periodically to ensure the materials were installed to the specified depths. Piezometer P1 was a nested piezometer with four discrete sampling depths (Table 5). The piezometer consisted of 0.25-inch diameter stainless steel vapor probes connected to 0.25-inch diameter polyethylene tubing. The probes were installed by securing the probe and tubing to a 1-inch diameter PVC pipe. The PVC pipe was then inserted into the wash-over casing. Annular materials were then poured into the annular space between the wash-over casing and the tubing. Depths were tagged periodically to ensure the materials were installed to the specified depths. The injection well and piezometer were completed with flush-mounted well boxes. Boring logs and as-built well diagrams are presented in Appendix B.

**Table 5 – Summary of Well Construction Details** 

Table 5 – Summary of Wen Construction Details							
Well Type	Vell Type   Construction Date			Total Depth	Casing/Tubing Diameter	Screen Intervals (feet	
		(feet bgs)	(inches)	bgs)			
Injection well	7/31/2006	70.5	6	10 - 70			
Injection well	10/26/2007	50	4	10 - 50			
Injection well	10/17/2007	50	4	10 - 50			
Piezometer	7/27/2006	72	0.25	18-18.5, 33-33.5, 48-48.5,			
				68-68.5			
Piezometer	10/25/2007	52	0.25	18-18.5, 28-28.5, 38-38.5,			
				48-48.5			
Piezometer	10/23/2007	52	0.25	18-18.5, 28-28.5, 38-38.5,			
				48-48.5			
Piezometer	10/29/2007	51.5	0.25	18-18.5, 28-28.5, 38-38.5,			
				48-48.5			
Piezometer	10/24/2007	51.5	0.25	18-18.5, 28-28.5, 38-38.5,			
				48-48.5			
Piezometer	10/22/2007		0.25	38-38.5, 48-48.5			
Piezometer	10/24/2007	30.5	0.25	18-18.5, 28-28.5			
Piezometer	10/16/2007	62	0.25	18-18.5, 28-28.5, 38-38.5,			
				48-48.5			
Piezometer	10/11/2007-	50	0.25	28-28.5, 37.5-38, 48-48.5			
Piezometer	10/15/2007	20.5	0.25	18-18.5			
Piezometer	8/26/1996	140	0.25	30-30.5, 50-50.5, 73-73.5,			
				90-90.5, 110-110.5			
Piezometer	7/1/1996	132	0.25	45-45.5, 65-65.5, 86-86.5,			
				104-104.5			
	Injection well Injection well Injection well Injection well Piezometer	Injection well 7/31/2006 Injection well 10/26/2007 Injection well 10/17/2007 Piezometer 7/27/2006  Piezometer 10/25/2007  Piezometer 10/23/2007  Piezometer 10/29/2007  Piezometer 10/24/2007  Piezometer 10/24/2007  Piezometer 10/16/2007  Piezometer 10/11/2007  Piezometer 10/15/2007  Piezometer 10/15/2007  Piezometer 10/15/2007  Piezometer 10/15/2007	Well Type         Construction Date (feet bgs)           Injection well         7/31/2006         70.5           Injection well         10/26/2007         50           Injection well         10/17/2007         50           Piezometer         7/27/2006         72           Piezometer         10/25/2007         52           Piezometer         10/23/2007         52           Piezometer         10/29/2007         51.5           Piezometer         10/24/2007         50           Piezometer         10/24/2007         30.5           Piezometer         10/16/2007         62           Piezometer         10/11/2007- 10/12/2007         50           Piezometer         10/15/2007         20.5           Piezometer         8/26/1996         140	Well Type         Construction Date (feet bgs)         Depth (feet bgs)         Diameter (inches)           Injection well         7/31/2006         70.5         6           Injection well         10/26/2007         50         4           Injection well         10/17/2007         50         4           Piezometer         7/27/2006         72         0.25           Piezometer         10/25/2007         52         0.25           Piezometer         10/23/2007         52         0.25           Piezometer         10/29/2007         51.5         0.25           Piezometer         10/24/2007         50         0.25           Piezometer         10/16/2007         62         0.25           Piezometer         10/11/2007- 10/12/2007         50         0.25           Piezometer         10/15/2007         20.5         0.25           Piezometer         10/15/2007         20.5         0.25           Piezometer         10/15/2007         20.5         0.25			

The remaining two injection wells (INJ2 and INJ3) and seven piezometers (P2 through P8), were installed between October 11 and October 29, 2007. The injection wells and piezometers were installed by WDC under CDM supervision using the sonic drilling method. The boreholes were continuously cored from ground surface to the total depth of the borehole using a 4.5-inch O.D. core barrel. After the core samples were collected from the borehole, a wash-over casing was installed to the total depth of the borehole. The wells and piezometers were then constructed inside the wash-over casing. The injection wells were installed using an 8-inch diameter wash-over casing. The piezometers were installed using a 6-inch diameter wash-over casing.

Injection wells INJ2 and INJ3 were constructed with 4-inch diameter schedule 40 PVC from ground surface to 10 feet bgs and slotted 4-inch diameter schedule 40 PVC (0.020-inch slot size) from 10 to 50 feet bgs. Annular materials include a filter pack (No. 3 Monterey Sand) from 8 to 50 feet bgs, a bentonite chip seal from 5 to 8 feet bgs, and a cement grout surface seal from ground surface to 5 feet bgs. Annular materials were installed by pouring the materials into the annular space between the well casing and the wash-over casing. Depths were tagged periodically to ensure the materials were installed to the specified depths. Boring logs and asbuilt well diagrams are presented in Appendix B. A generalized well design is depicted in Figure 27.

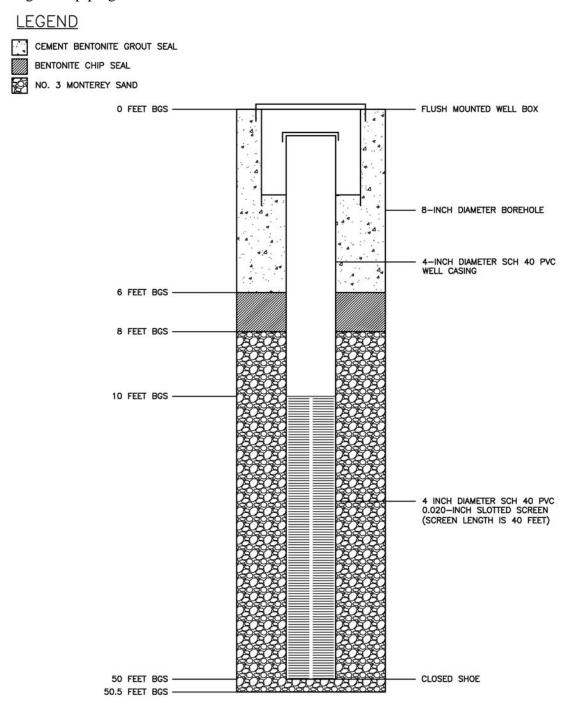
Piezometers P2 through P8 were nested piezometers with various sampling depths (Table 5) and were constructed similarly to P1. A generalized piezometer design is depicted in Figure 28). Piezometer P6 was completed in two separate boreholes. While tripping the wash-over casing out of the borehole during well construction, a suspected borehole collapse occurred, preventing proper installation of the annular materials. The upper two sampling points for P6 at 18-18.5 and 28 to 28.5 feet bgs were completed as P6A in a separate borehole located approximately two feet southeast of P6. Piezometer P8 was also completed in two separate boreholes. During construction of P8, the tubing to the sampling probe for the 18-18.5 foot sampling interval was pulled out of the borehole while tripping out the wash-over casing. This sampling point was completed as P8A in a separate borehole located approximately two feet southwest of P8.

It should also be noted that during the initial startup and trouble-shooting phase, it was discovered that gas sampling was not possible from the uppermost sampling zone in P7 (from 18-18.5 feet bgs). It is unclear whether this is a result of faulty well construction or a function of the geology (i.e., the soil may be too compacted in this location to collect soil gas samples).

## **5.4.2 Process Equipment**

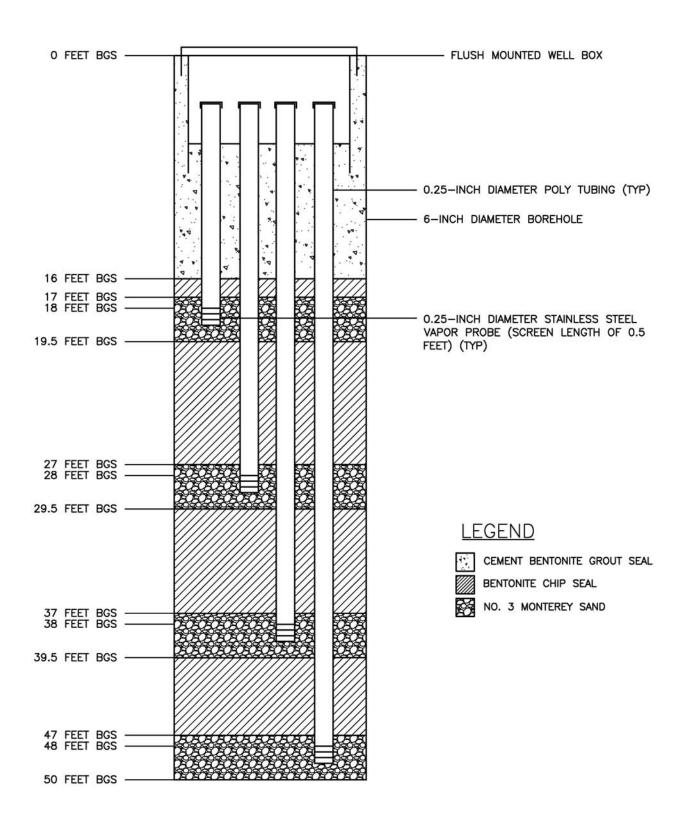
Figure 29 is a process and instrumentation diagram (P&ID) for the gaseous electron donor injection system and Table 6lists gas supply equipment and general specifications. Figures 30 and 31 are photographs of the gas supply equipment and gas flow control panel, respectively. The gas injection system was designed to allow injection of a mixture of nitrogen, hydrogen, propane (i.e., LPG), and carbon dioxide. Provisions for injection of helium as a tracer were also included. The gas injection system was designed to be operated without any electrical requirements because of the remoteness of the site. The liquid nitrogen and LPG systems were vaporized using vendor-supplied equipment prior to injection. Each gas flow was controlled using manual pressure regulators and flow control valves along with rotameters to measure flow

and gauges to monitor pressure. The gases were mixed prior to distribution to the injection wells. All above-ground piping was carbon steel.



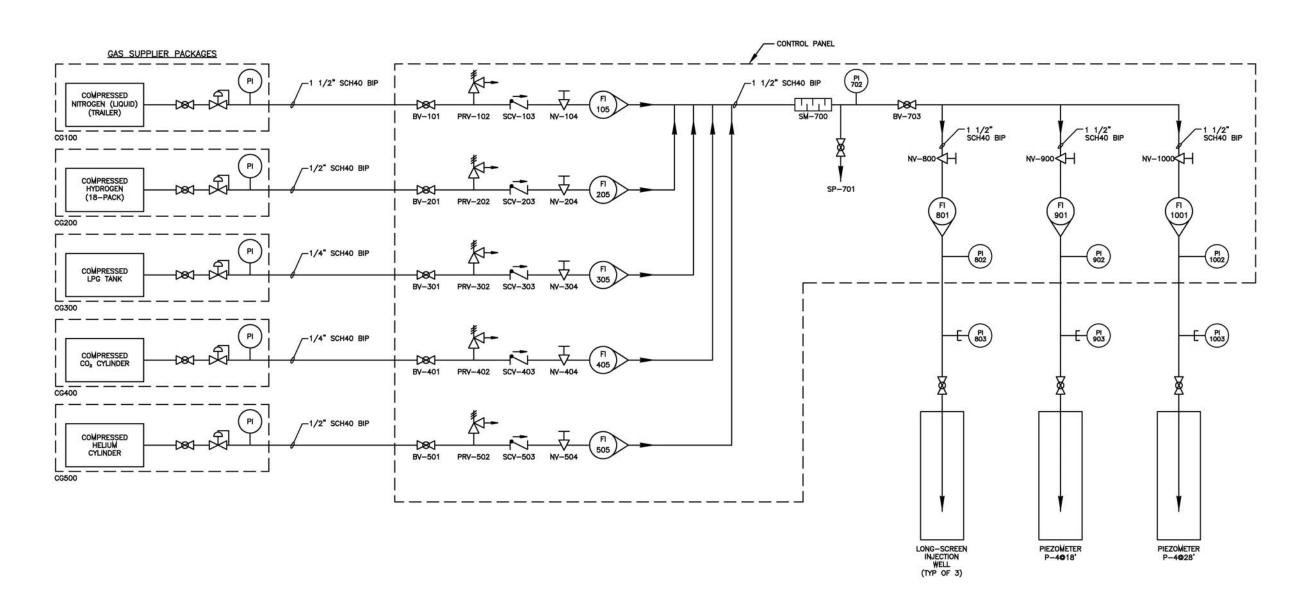
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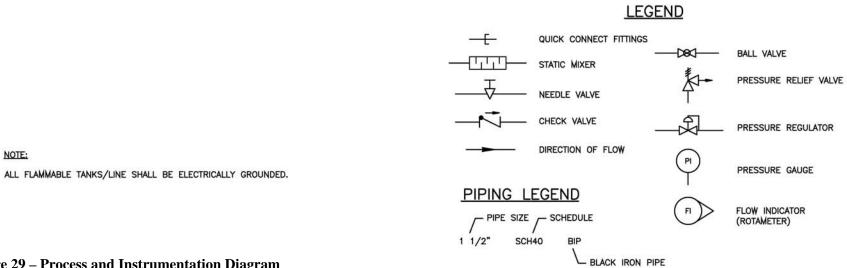
Figure 27 – Injection Well Design



NOT TO SCALE

 $Figure\ 28-Piezometer\ Design$ 





**Figure 29 – Process and Instrumentation Diagram** 

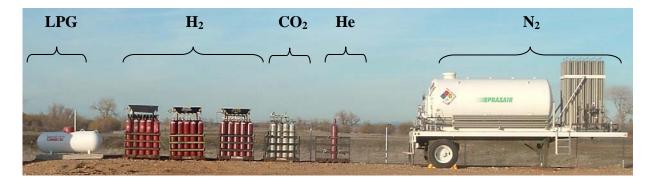


Figure 30 – Gas Supply for the Demonstration



Figure 31 – Gas Supply Control Panel

**Table 6 – Gas Supply Equipment** 

Tag	Description	Specifications
CG-100	Liquid nitrogen	Trailer, 150,000 cubic feet gas capacity
		Three 18-packs of K cylinders; 3,600 cubic feet gas
CG-200	Compressed hydrogen	capacity each 18-pack
CG-300	Liquefied petroleum gas, odorized	120 gallon, 3,500 cubic feet gas capacity
CG-400	Compressed carbon dioxide	18-pack K cylinders , 4,800 cubic feet gas capacity
CG-500	Compressed helium	T Cylinder, 290 cubic feet gas capacity

# 5.5 Field Testing

The treatability study and field demonstration comprised four phases as described in Section 5.1 (Figure 13). Phase I comprised the treatability study and was previously described in Section 5.3. Phases II through IV were conducted over a period of 10.5 months as illustrated in Figure 32. Detailed descriptions of each of the phases are provided below.

ID	Task Name	Start	Finish	2008
				Qtr 4 Qtr 1 Qtr 2 Qtr 3 Qtr 4
41	FIELD DEMONSTRATION	Wed 12/12/07	Mon 12/1/08	V
42	SYSTEM CHECKOUT	Wed 12/12/07	Wed 1/2/08	
43	PHASE II - TRACER TESTS	Thu 1/17/08	Fri 2/8/08	ΨΨ
44	TEST 1	Mon 1/21/08	Wed 1/23/08	
45	TEST 2	Fri 1/18/08	Sat 1/19/08	I
46	TEST 3	Wed 1/30/08	Thu 1/31/08	
47	TEST 4	Mon 1/28/08	Tue 1/29/08	
48	TEST 5	Tue 2/5/08	Tue 2/5/08	
49	TEST 6	Tue 2/5/08	Fri 2/8/08	
50	TEST 7	Thu 1/17/08	Fri 1/18/08	
51	TEST 8	Wed 2/6/08	Wed 2/6/08	
52	PHASE II - OPTIMIZATION	Wed 2/20/08	Wed 4/16/08	-
53	TEST 1	Wed 2/20/08	Wed 2/20/08	
54	TEST 2	Mon 2/25/08	Mon 2/25/08	
55	TEST 3A	Fri 2/29/08	Mon 3/3/08	
56	TEST 3B	Mon 3/3/08	Fri 3/7/08	
57	TEST 3C	Fri 3/7/08	Fri 3/7/08	
58	TEST 4	Mon 3/10/08	Mon 3/17/08	<b>I</b>
59	TEST 5	Mon 3/17/08	Thu 3/20/08	
60	TEST 6	Thu 3/20/08	Wed 4/2/08	
61	TEST 7A	Wed 4/2/08	Mon 4/7/08	I I
62	TEST 7B	Mon 4/7/08	Thu 4/10/08	
63	TEST 7C	Thu 4/10/08	Wed 4/16/08	<b>I</b>
64	PHASE III - STEADY STATE MIXED GAS	Thu 4/10/08	Tue 8/12/08	
65	PHASE IV - STEADY STATE LPG	Mon 9/8/08	Mon 12/1/08	

**Figure 32 – Demonstration Schedule** 

## 5.5.1 Phase II – Gas Injection Optimization

Phase II comprised tracer tests and optimization tests. The tracer tests were conducted to characterize gas transport in the vadose zone. The optimization tests were conducted to identify the most cost-effective method of delivering a 79-10-10-1 percent mixture of nitrogen, hydrogen, LPG, and carbon dioxide, respectively, to the vadose zone and minimizing oxygen intrusion.

#### **Tracer Tests**

The purpose of the tracer tests was to verify well and piezometer performance and to characterize gas transport in the vadose zone. The original approach outlined in the Technology Demonstration Plan was to inject varying flow rates of nitrogen into one or more injection wells and use helium as a tracer. During field testing the helium meter (i.e., Matheson 8067-IS Leak Detector) was found to be unreliable. Therefore, hydrogen was used as a tracer instead. Unlike helium, hydrogen is not a conservative tracer because it is capable of being oxidized to water by autotrophic and other hydrogen-oxidizing bacteria. While the rates of biological hydrogen consumption were likely to be small relative to the rate of gas transport for these tracer tests, the results of these tracer tests are representative of hydrogen transport and degradation.

A mixture of nitrogen and hydrogen was injected at different total flow rates into various injection wells as outlined in Table 7. Pure nitrogen was injected into the well(s) in between each test to flush hydrogen out of the vadose zone in preparation for the next test. Thus each tracer test was a "step test" where the concentration of hydrogen in each piezometer was monitored during the test to characterize transport of hydrogen through the vadose zone. Well INJ2 was selected for the individual test because of its placement relative to the piezometers. The flow rates to individual wells during tests 6 through 8 were equivalent and thus a third of the total flow rates listed in Table 7.

Table 7 – Phase II Tracer Test Conditions

Test	Target Flow Rate per Well	Target Total Flow Rate	Measured Total Flow Rate	Duration	Hydrogen Concentration	Inje	ction V	Vells
	(cfm)	(cfm)	(cfm)	( <b>h</b> )	( percent)	INJ1	INJ2	INJ3
1	10	10	9.6	50	6.5		X	
2	20	20	19	31	7.4		X	
3	30	30	27	27	4.1		X	
4	60	60	63	19	6.3		X	
5	90	90	87	6.4	3.6		X	
6	10	30	29	20	8.0	X	X	X
7	20	60	59	6.9	5.0	X	X	X
8	30	90	84	7.1	4.6	X	X	X

The experimental design involved injection of gas into one well (i.e., INJ2) and variation of the total flow rate from 10 to 90 cfm in tests 1 through 5. Tests 6 through 8 involved injection of gas into all three wells and the flow rates were selected to allow comparison with tests 1 through 3

and tests 3 through 5. The comparison of tests 6 through 8 with tests 1 through 3 was based on equal flow rates per well (i.e., 10, 20, and 30 cfm). The comparison with tests 3 through 5 was based on equal total flow rate (i.e., 30, 60, and 90 cfm).

Monitoring during the test involved measurement of pressures at each piezometer and collection of gas samples for analysis. The gas samples were analyzed for hydrogen using a field instrument. The details of monitoring, sampling, and analysis are presented in Section 5.6.

## **Optimization Tests**

The purpose of the optimization tests was to characterize electron donor transport and oxygen depletion and rebound in the vadose zone during various injection strategies. These tests were then used to select the optimal injection strategy. The optimal injection strategy was considered to be one that maximizes electron donor distribution, minimizes oxygen concentrations in the vadose zone, and minimizes gas use.

Gas flow rate, injection pulse duration, gas injection location(s), and gas composition were varied during the optimization tests (Table 8). The original experimental design as outlined in the Technology Demonstration Plan was based on pulsing gas injection and varying the total flow rate and the pulse duration to determine the optimal pulsing strategy. Tests 1 and 2 were based on this approach. Both of these tests involved injection of a total of 21,600 cubic feet of gas into the vadose zone. As described in Section 5.7.2, significant and rapid oxygen intrusion into the vadose zone was observed following both of these tests. Therefore, the original experimental approach was modified to identify an injection strategy that minimized oxygen intrusion. The test conditions for each test were selected based on observed results of the previous tests. Tests 3 through 5 were based on varying the number of wells, flow rate, pulse duration, gas composition, and use of staged pulsing and continuous gas injection. In addition, the gas composition was varied. None of these tests resulted in acceptable oxygen concentrations in the vadose zone. It was hypothesized that the permeable lithology (see Section 5.3.2) in combination with the long well screens (i.e., 40 to 60 feet) prevented use of the existing wells and that injection into the piezometers may prove effective. Tests 6 and 7 evaluated this hypothesis which led to an optimal gas injection strategy that minimized oxygen intrusion into the vadose zone.

Monitoring during the test involved measurement of pressures at each piezometer and collection of gas samples for analysis. The gas samples were analyzed for oxygen, hydrogen, propane, and carbon dioxide using field instruments. The details of monitoring, sampling, and analysis are presented in Section 5.6.

**Table 8 – Phase II Optimization Tests** 

			_	Gas Composition			
Optimization	Flow Rate		Injection	274		T D C	G04
Test	(cfm)	Flow Duration	Location(s)	Nitrogen	Hydrogen	LPG	CO2
1	90	4 hours	INJ2	88 percent	10 percent	1 percent	1 percent
2	30	12 hours	INJ2	88 percent	10 percent	1 percent	1 percent
3A	1.00	70 hours	INJ2	88 percent	10 percent	1 percent	1 percent
3B	1.00	98 hours	INJ1, INJ2, INJ3	88 percent	10 percent	1 percent	1 percent
3C	90	15 minutes	INJ1, INJ2, INJ3	79 percent	10 percent	10 percent	1 percent
4 - stage 1	30	45 min	INJ1, INJ2, INJ3	79 percent	10 percent	10 percent	1 percent
4 - stage 2	30	45 min	INJ2	79 percent	10 percent	10 percent	1 percent
4 - stage 3	0.5	Continuous	INJ2	79 percent	10 percent	10 percent	1 percent
5 - stage 1	20	125 min	INJ2	80 percent	10 percent	10 percent	0 percent
5 - stage 2	0.5	Continuous	INJ2	80 percent	10 percent	10 percent	0 percent
6	0.83	Continuous	P4-18/28	80 percent	10 percent	10 percent	0 percent
7A	1.00	Continuous	P4-18/28/38	80 percent	10 percent	10 percent	0 percent
7B	1.00	Continuous	P4-18/28	80 percent	10 percent	10 percent	0 percent
7C	1.67	Continuous	P4-18/28	79 percent	10 percent	10 percent	1 percent

Note – Specific injection screen depths (ft) are designated under "Injection Location" for Piezometer P4.

## 5.5.2 Phase III – Gas Mixture Injection

The objective of Phase III was to inject gas using the optimal injection strategy and quantification of perchlorate destruction in vadose zone soil. Phase III involved continuous injection of 100 cfh of the gas mixture identified in optimization test 7C (i.e., 79 percent nitrogen, 10 percent hydrogen, 10 percent LPG, and 1 percent carbon dioxide) into the 18- and 28-ft bgs screens of piezometer P4. The flow was divided equally into each screen (i.e., 50 cfh each) and was conducted for about five months. Gas injection conditions were not varied during this phase except during drilling to collect soil samples. Gas injection was not conducted during drilling for safety because of flammability. Gas sampling and analysis was conducted weekly and soil sample collection and analysis was conducted approximately monthly. Details on sampling and analysis are presented in Section 5.6.

# **5.5.3 Phase IV – LPG Injection**

The perchlorate destruction results obtained during Phase III were not definitive because of heterogeneity. Therefore, additional funds were provided by ESTCP for more intensive soil sampling and analysis (see Section 5.6). Simultaneously, Aerojet General Corporation provided additional funds to operate the system using pure LPG instead of the gas mixture. Use of pure LPG had the potential to be more cost effective than the gas mixture if it was actually capable of promoting perchlorate biodegradation. Injection of LPG was conducted at a flow rate of 100 cfh divided evenly amongst the 18- and 28-ft bgs screens of piezometer P4 for a period of about

<sup>&</sup>lt;sup>1</sup> Treatability study results were not definitive with respect to the ability of pure LPG to promote perchlorate biodegradation as described in Section 5.3.1. However, the potential for LPG to promote perchlorate biodegradation had not been completely ruled out.

3 months. Following this injection period soil samples were collected and analyzed as described in Section 5.6.

#### 5.5.4 Demobilization

Gas storage equipment was removed from the site upon completion of the demonstration. The gas control panel, wells, and piezometers were left in place. Aerojet will review this Draft Report and then make a decision whether to authorize CDM to abandon the wells and piezometers or to take ownership and responsibility of the infrastructure.

# **5.5.5 Investigation-Derived Waste**

Excess soil was collected during the well construction and confirmation boring drilling events. At the request of Aerojet, this excess soil was placed on plastic sheeting and stored in the Propellant Burn Area, approximately 200 feet east of CDM-P1.

# 5.6 Sampling Methods

This section provides methods for gas and soil sampling and analysis. Additional quality assurance data are provided in Appendix E.

## 5.6.1 Gas Sampling and Analysis

Samples of gas from the piezometers and the gas injection manifold were collected and analyzed for hydrogen, propane, oxygen, carbon dioxide, relative humidity, and temperature using field instruments (Tables 9 and 10). Gas samples from the piezometers were collected using the vacuum pump that was integral to the RKI Eagle instrument used for analysis of propane, oxygen, and carbon dioxide. This instrument was connected in series with two other instruments − an H2scan HY-ALERTA 500™ handheld hydrogen leak detector and a Vaisala HMT360 humidity and temperature meter − and this analysis train was then connected to the piezometer tubing (Figure 33). The RKI Eagle pulled the gas sample from the piezometer into the gas analysis train allowing analysis of all parameters simultaneously. The gas injection manifold was under pressure which could damage the RKI Eagle pump. Therefore, gas samples were collected in Tedlar bags which in turn were connected to the gas analysis train.

Hydrogen concentrations were measured using an H2scan HY-ALERTA 500<sup>TM</sup> handheld hydrogen leak detector. This field instrument uses palladium alloy thin films to measure hydrogen in concentrations ranging from 15 parts per million by volume (ppmv) to percent concentrations. Concentrations from 15 to 5,000 ppmv are measured using a hydrogen-specific capacitor/metal oxide semiconductor. Concentrations from 0.5 percent (i.e., 5,000 ppmv) to 100 percent are measured using a hydrogen-specific resistor. The sensor is unique in its ability to measure hydrogen in oxic and anoxic atmospheres which was critical to this demonstration.

**Table 9 - Total Number and Types of Samples Collected** 

Component	Matrix	Number of Samples	Analyte	Location
Baseline sampling	Soil: Screening measurement	67	Perchlorate, Nitrate+Nitrite Nitrogen, Moisture,	All soil borings, one sample every 5 to 10 feet
			VOCs	
	Soil:	61	Perchlorate,	All soil borings, one
	Laboratory		Nitrate+Nitrite	sample every 10 feet
	measurement Soil:	10	Nitrogen, Moisture pH, TOC, Particle	CDM-INJ1 and CDM-
	Laboratory measurement	10	size distribution	P1 at selected intervals
	Soil gas: Field measurement	1 per monitoring point	O <sub>2</sub> , H <sub>2</sub> , Propane, CO <sub>2</sub> , Temperature, Relative humidity	All subsurface monitoring devices
Technology performance sampling	Soil: Screening measurement	86	Perchlorate, Nitrate+Nitrite Nitrogen, Moisture, VOCs	All soil borings, one sample every 5 to 10 feet
	Soil: Laboratory measurement	48	Perchlorate, Nitrate+Nitrite Nitrogen, Moisture	All soil borings, one sample every 10 feet
	Soil gas: Field measurement	Weekly for Phase III and every other week for Phase IV	O <sub>2</sub> , H <sub>2</sub> , Propane, CO <sub>2</sub> , Temperature, Relative humidity	All subsurface monitoring devices
Post- demonstration sampling	Soil: Screening measurement	66	VOCs	All soil borings, one sample every 10 feet
1 6	Soil: Laboratory measurement	66	Perchlorate, Nitrate+Nitrite Nitrogen, Moisture	All soil borings, one sample every 10 feet

**Table 10 - Analytical Methods for Sample Analysis** 

Matrix	Analyte	Method	Container	Preservative	Holding Time
Soil	Perchlorate	EPA 314.0	Glass jar	4 °C	28 days
	Perchlorate – screening	Ion- selective probe	Glass jar	4°C	NA
	Nitrate+Nitrite Nitrogen	EPA 353.2	Glass jar	4°C	28 days
	Nitrate - screening	Chemetrics K-6905	Glass jar	4°C	NA
	Moisture	SM2540B	Glass jar	4°C	28 days
	Moisture - screening	SM 2540B	Glass jar	4°C	
	Total organic carbon	EPA 415.1	Glass jar	4 °C	28 days
	Particle size distribution	ASTM D422	Glass jar	4 °C	28 days
	pН	SM 9045C	Glass jar	4°C	28 days
	VOCs – screening	PID	NA	NA	NA
Soil gas	Oxygen	Field	NA	NA	NA
•	Hydrogen	Field	NA	NA	NA
	Propane	Field	NA	NA	NA
	Relative humidity	Field	NA	NA	NA
	Temperature	Field	NA	NA	NA

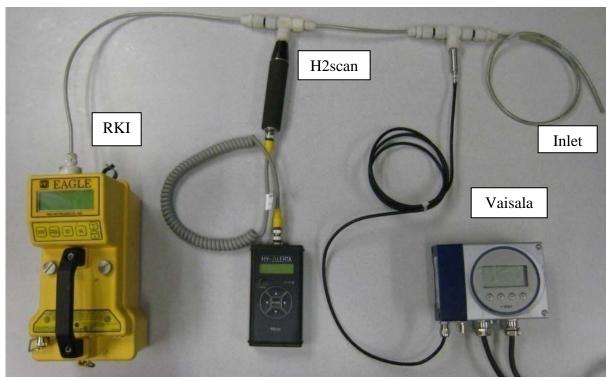


Figure 33 – Gas Sampling and Analysis Train

Propane, oxygen, and carbon dioxide concentrations were measured using an RKI Eagle portable gas detector. The RKI Eagle uses an infrared sensor for propane measurement, an electrochemical cell for oxygen measurement, and an infrared sensor for carbon dioxide measurement. The RKI Eagle was not capable of reporting propane concentrations greater than 30 percent. Propane concentrations of 30 percent or greater were reported as "> 30 percent".

Temperature and relative humidity were measured using a Vaisala HMT360 humidity and temperature meter. Barometric pressure was measured using a Novalynx digital handheld barometer-altimeter. Atmospheric (above-ground) concentrations of flammable gases were monitored using a BW Technologies Micro Clip lower explosive limit (LEL) detector. Pressure in the piezometers was measured using Dwyer Magnehelic gauges.

Sampling frequency varied depending on the particular phase of the demonstration. During Phase II sampling was conducted multiple times per day and was varied in order to obtain transient data. During Phase III. sampling was conducted weekly. During Phase IV, sampling was conducted every two weeks. Depending on the particular piezometer and depth being measured, it normally took approximately one to two minutes for the gas concentration reading to stabilize after being connected to the sampling apparatus; gas concentrations were recorded after the readings stabilized. In addition to measuring gas concentrations at the piezometers, gas injection composition, flow rates, and pressures were also monitored using the same instruments plus rotameters and pressure gauges. The rotameters were standard meters calibrated for air at

atmospheric pressure. Rotameter readings are affected by gas pressure and density. The rotameter readings were thus corrected for gas density and pressure using the following equation provided by the instrument manufacturer (Key Instruments):

$$Q_i = CF_i \widehat{Q}_i \sqrt{\frac{P_i}{P}},$$

where,

 $Q_i$  is the actual flow rate of gas i (i.e.,  $H_2$ ,  $N_2$ ,  $CO_2$ , or LPG) in units of scfm or scfh;

 $CF_i$  is the correction factor for gas i and is based on the relative densities of gas i and the rotameter calibration gas (i.e., air). The values of  $CF_i$  were provided by the rotameter manufacturer (Key Instruments) and are presented in Table 11;

 $\widehat{Q}_{i}$  is the rotameter reading for gas *i* in units of scfm or scfh;

 $P_i$  is the absolute pressure of gas i at the rotameter; and

**P** is the atmospheric pressure (1 atmosphere or 14.696 psia).

**Table 11 – Rotameter Correction Factors** 

<u>i</u>	$CF_i$
$N_2$	$1.0\overline{2}$
Propane (LPG)	0.80
$H_2$	3.81
$CO_2$	0.81

## 5.6.2 Soil Sampling and Analysis

In addition to the details presented in Table 9, Table 12 presents a detailed list of all soil samples collected including sampling dates and depths. Soil samples were collected during well and piezometer installation and confirmation boring drilling events. The soil samples collected during well and piezometer installation were representative of baseline conditions before gas injection. The confirmation borings were collected during Phases III and IV and the locations are depicted on Figure 34. Confirmation borings CB1 through CB8 were conducted during Phase III at four different times and each time at two different distances from the injection piezometer P4. Confirmation borings CB9 through CB19 were conducted at the end of Phase IV and were located as close to the existing wells and piezometers as practical. The Phase III confirmation borings were used to assess nitrate and perchlorate removal kinetics and the Phase IV confirmation borings were used to assess overall nitrate and perchlorate removal.

Table 12 – List of Soil Samples Collected

Sampling Location	Sampling Date	Sampling Depths (feet bgs)
	1 0	1 0 1 0
INJ1	7/31/2006	5, 10, 15, 20, 25, 30, 35, 40, 45, 50, 55, 60, 65, 70
INJ2	10/26/07	5/5D, 10, 15, 20, 25/25D, 30, 35, 40, 45, 50
INJ3	10/17/2007	5/5D, 10, 15, 20, 25, 30, 35, 40, 45, 50
P1	7/27/2006	5, 10, 15, 20, 25, 30, 35, 40, 45, 50, 55, 60, 65, 70
P2	10/25/2007	5/5D, 10, 15, 20/20D, 25, 30, 35, 40, 45, 50
P3	10/23/2007	5, 10/10D, 15, 20, 25/25D, 30, 35, 40, 45, 50
P4	10/29/2007	5, 10, 15/15D, 20, 25, 30, 35, 40/40D, 45, 50
P5	10/24/2007	5, 10/10D, 15/15D, 20, 25, 30, 35, 40, 45, 50
P6	10/22/2007	5, 10, 15, 20/20D, 25, 30/30D, 35, 40, 45, 50
P7	10/16/2007	5, 10, 15, 20, 25, 30, 35/35D, 40
P8	10/11/2007-10/12/2007	5, 10, 15/15D, 30, 35, 40, 45, 50
CB1	4/18/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB2	4/18/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB3	6/10/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB4	6/10/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB5	7/10/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB6	7/10/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB7	9/2/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB8	9/2/2008	5, 10, 15, 20, 25, 30/30D, 35, 40, 45, 50
CB9	12/2/2008	10, 20, 30/30D, 40, 50
CB10	12/2/2008	10, 20, 30/30D, 40, 50
CB11	12/3/2008	10, 20, 30/30D, 40, 50
CB12	12/3/2008	10, 20, 30/30D, 40, 50
CB13	12/3/2008	10, 20, 30/30D, 40, 50
CB14	12/3/2008	10, 20, 30/30D, 40, 50
CB15	12/3/2008	10, 20, 30/30D, 40, 50
CB16	12/3/2008	10, 20, 30/30D, 40, 50
CB17	12/3/2008	10, 20, 30/30D, 40, 50
CB18	12/3/2008	10, 20, 30/30D, 40, 50
CB19	12/3/2008	10, 20, 30/30D, 40, 50

D = duplicate sample collected

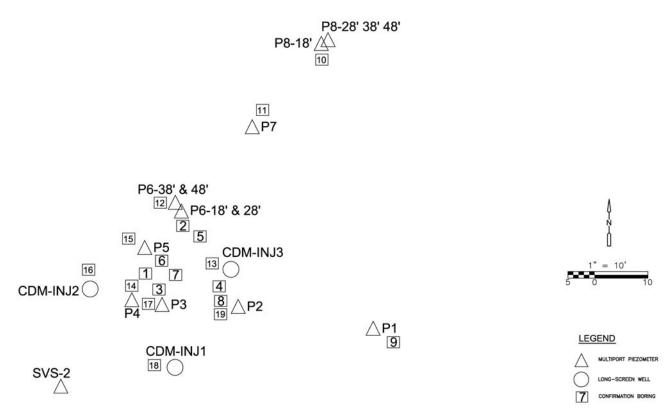


Figure 34 – Well Piezometer and Confirmatory Boring Locations

As described in Sections 5.2.1 and 5.4.1, each borehole was continuously cored from ground surface to total depth. The cores were logged by a CDM geologist in accordance with ASTM Standard D2488 and boring logs with soil descriptions are included in Appendix B). Core samples were screened in the field for volatile organic compounds (VOCs) by placing a portion of the sample into a zip-lock bag, waiting approximately 10 minutes, placing the tip of a photoionization detector (PID) into the bag, and then taking a measurement.

Soil samples were collected at 5-foot intervals and placed in 8-ounce glass jars. Sample jars were then sealed in zip-locks bags which were placed in an ice-chilled cooler prior to shipment to the lab. Soil samples were shipped to Laucks Testing Laboratory which was acquired by Pace Analytical (Seattle, Washington) for analysis (Table 10). Some sample analyses were subcontracted to Weck Laboratories (Industry, California).

In addition to the laboratory analyses, screening analyses of soil samples for perchlorate, nitrite+nitrite nitrogen, and moisture were conducted on baseline samples and technology performance samples (Table 9). A quality assurance review of these data determined that they were not comparable to the laboratory analyses. Therefore the screening results for these analytes are not discussed further in this report.

# 5.7 Sampling Results

Phase I results were presented in Section 5.3. This section presents the results of Phases II through IV.

#### **5.7.1 Tracer Tests**

Tracer tests were conducted during Phase II to characterize hydrogen transport through the vadose zone under various injection strategies. Table 13 presents the injection conditions for each test. The gas flow rate was varied (e.g., from about 10 cfm to 90 cfm) and the number of injection wells was varied (either one or three wells). During each test the hydrogen and oxygen concentrations were monitored in the piezometers. Figure 35 shows example data for Test 4. Complete tracer test data are presented in Appendix C.

Analysis of tracer test data was accomplished by calculating the volume of injected gas required to attain 50 percent of the injected hydrogen concentration in each piezometer sampling point. Figure 36 shows a graphical representation of this analysis. The rectangles that are colored green or blue indicate piezometer locations where the hydrogen concentration attained at least 50 percent of the injected concentration during the indicated test. The rectangles that are labeled blue indicate the test condition that resulted in the minimum gas volume needed to attain the 50 percent target at the indicated piezometer location. For example, Test 1 resulted in attainment of the 50 percent target in P3 at 18, 28, and 38 ft bgs but not at 48 ft bgs. Test 1 also was the test condition that resulted in the minimum gas volume needed to attain the 50 percent target in P3 at 18 ft bgs. Test 3 was the test condition that resulted in the minimum gas volume needed to attain the 50 percent target in P3 and 28 and 38 ft bgs. Actual gas volume data are summarized in Table 14.

**Table 13 – Tracer Test Operating Conditions** 

	Target Flow	Measured Flow				Injected Hydrogen
	Rate	Rate	Inje	ction W	/ells	Concentration
Test	(cfm)	(cfm)	INJ1	INJ2	INJ3	( percent)
1	10	9.6		X		6.5
2	20	19		X		7.4
3	30	27		X		4.1
4	60	63		X		6.3
5	90	87		X		3.6
6	30	29	X	X	X	8.0
7	60	59	X	X	X	5.0
8	90	84	X	X	X	5.0

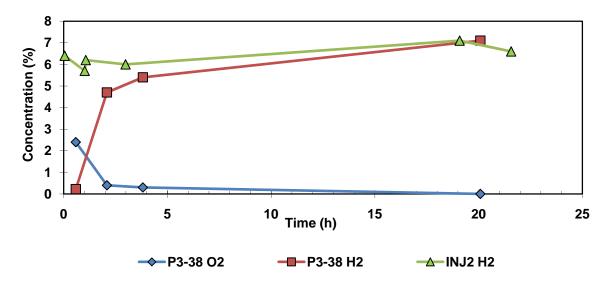


Figure 35 – Example Transient Gas Concentrations During Tracer Test 4

				Depth (feet)														
			18	33	48	68	18	28	38	48	18	28	38	48	18	28	38	48
Test	Wells	Flow (cfm)		P4-8	8.2ft			P3-	14 ft			P2-2	28 ft			P1-	54 ft	
1	1	10																
2	1	20																
3	1	30																
4	1	60																
5	1	90																
6	3	30																
7	3	60																
8	3	90																

				Depth (feet)													
			18	28	38	48	18	28	38	48	28	38	48	18	28	38	48
Test	Wells	Flow (cfm)		P5-	13ft			P6-	22ft		Р	7-43	ft		P8-	64ft	
1	1	10															
2	1	20															
3	1	30															
4	1	60															
5	1	90															
6	3	30															
7	3	60															
8	3	90															

Note - Distances listed after piezometer labels refer to distance from INJ2.

50% of injected H<sub>2</sub> concentration attained with minimum gas volume relative to other tests

50% of H<sub>2</sub> concentration attained

50% of H<sub>2</sub> concentration not attained

Figure 36 – Summary Analysis of Tracer Test Data.

Table 14 – Distribution of Gas Volumes Required to Attain 50 Percent of Injected Hydrogen Concentration in Piezometers

Parameter	Injected Gas Volume (cubic feet)
Average	10,000
Median	6,900
Standard deviation	10,000
Minimum	410
Maximum	70,000

Several conclusions can be derived from the tracer tests:

- Hydrogen gas was capable of being transported 64 feet away from the point of injection under all injection conditions.
- Hydrogen transport diminished with depth due to the buoyancy of this low molecular weight gas.

- Hydrogen transport was better in the northerly direction (i.e., P5 to P8) compared to the easterly direction (i.e., P4 to P1) likely because of historical gold dredging operations that operated in a north-south direction.
- In general, Test 3 conditions injection of an intermediate flow rate of 30 cfm into one well resulted in minimum gas volume requirements to achieve 50 percent of hydrogen concentrations throughout the treatment area. However, transport of hydrogen to the distal eastern piezometers (i.e., P1 and P2) was most efficient when high flow rates of 60 to 90 cfm were injected into all three wells.
- Gas volumes required to achieve 50 percent of injected hydrogen concentrations in a given piezometer ranged from 410 to 70,000 cubic feet.

While these tracer tests demonstrated that hydrogen could effectively be transported in the vadose zone, the gas flow rates that were required would not be economical if they needed to be injected continuously. During these tests, oxygen concentrations were often reduced to less than one percent, but upon cessation of injection, oxygen concentrations were observed to increase. Thus, additional optimization testing was required to identify cost-effective conditions capable of maintaining elevated electron donor concentrations and diminished oxygen concentrations in the vadose zone. These tests are described in the next section.

## **5.7.2 Optimization Tests**

Several optimization tests were conducted during Phase II to determine the best method to minimize oxygen concentrations, maximize electron donor concentrations, and minimize gas volume. Table 15 illustrates the various test conditions that were evaluated. Table 16 presents the minimum oxygen concentrations that were observed during each test. Appendix C presents complete gas concentration and operating data from these tests.

**Table 15 – Optimization Test Conditions** 

	Flow Rate	Flow	Injection		Gas Composi	ition	
<b>Optimization Test</b>	(cfm)	Duration	Location(s)	Nitrogen	Hydrogen	LPG	$CO_2$
1	90	4 hours	INJ2	88%	10%	1%	1%
2	30	12 hours	INJ2	88%	10%	1%	1%
3A	1.00	70 hours	INJ2	88%	10%	1%	1%
3B	1.00	98 hours	INJ1, INJ2, INJ3	88%	10%	1%	1%
3C	90	15 minutes	INJ1, INJ2, INJ3	79%	10%	10%	1%
4 - stage 1	30	45 min	INJ1, INJ2, INJ3	79%	10%	10%	1%
4 - stage 2	30	45 min	INJ2	79%	10%	10%	1%
4 - stage 3	0.5	Continuous	INJ2	79%	10%	10%	1%
5 - stage 1	20	125 min	INJ2	80%	10%	10%	0%
5 - stage 2	0.5	Continuous	INJ2	80%	10%	10%	0%
6	0.83	Continuous	P4-18/28	80%	10%	10%	0%
7A	1.00	Continuous	P4-18/28/38	80%	10%	10%	0%
7B	1.00	Continuous	P4-18/28	80%	10%	10%	0%
7C	1.67	Continuous	P4-18/28	79%	10%	10%	1%

**Table 16 – Optimization Test Minimum Oxygen Concentrations** 

								Depth	(feet)							
Piezometer	18	28	38	48	18	28	38	48	18	28	38	48	18	33	48	68
		Р	4		P3					Р	2		P1			
Test					N	∕linimı	ım Ox	cygen	Conc	entrati	ion (%	<sub>o</sub> )				
1	0.2	0	1.6	0.1	1.7	0.1	0.2	3.8	2.8	1.6	3.5	2.8	17.3	11.9	17.5	14.3
2	0.1	0	1	1	1.2	0.1	0.1	7	6.8	4.5	6.4	6.4	18.8	16.7	16.9	0
3A	0.6	5.1	7.3	18.8	2.9	7.7	7.3	6.8	14.6	13.9	8.3	6.2	19.1	18.5	17.1	0
3B	0.4	8.3	8.4	19.3	0.8	10.1	12.1	7.2	8.9	14	10.8	19.9	19	18.8	16.9	15.7
3C	1.2	8.7	8.8	16.5	0.9	8.8	9.9	16.4	5.1	12.4	11.7	19.5	19.1	19	NA	NA
4	0	1.6	6.1	12.7	1.6	1.7	7.2	15	14.1	16	NA	NA	NA	NA	NA	NA
5	0.9	0.3	4.2	8.5	2.1	0.3	6.3	12.9	NA	NA	NA	NA	NA	NA	NA	NA
6	NA	NA	0.2	1.8	0	0	0	5.4	3.5	1.1	5.2	9.8	18.7	10.3	17	14.3
7A	NA	NA	NA	1.6	0.1	0.1	0	3.9	2.3	2.1	4.5	4.1	17.5	8.9	16.9	13.4
7B	NA	NA	1.3	1.8	0.3	5.7	4.5	8.3	8.2	7.1	5.3	4.8	16.2	12.6	16.5	12.9
7C	NA	NA	0.3	0.2	0	0	0	1.5	4.2	2.6	3.5	0.7	17.4	13	16.8	12.4

		Depth (feet)													
Piezometer	18	28	38	48	18	28	38	48	28	38	48	18	28	38	48
		P	5		P6 P7							P	P8		
Test		Minimum Oxygen Concentration (%)													
1	0.2	0	0	2.6	0	0	0.4	8.7	0	0	14.7	0.1	0.5	13.4	12.5
2	0.2	0	0.2	7.5	0	0	1	11.6	0.1	0	14.6	0.1	0.2	13.8	13
3A	0	7.1	8.3	10.6	1.2	8.6	6.4	18.9	11	11.8	14.5	10.2	8.8	14.2	13.4
3B	0.5	11	8.5	11.2	2.3	11.6	8.7	20.1	11.4	12.2	14.5	10.1	9.1	14.3	13.5
3C	0.6	8.7	9.4	11	4.4	9.4	10	20.2	11.1	11.6	14.3	11	9.1	14.2	13.7
4	0	0.4	7.2	11.6	8.5	1.4	NA	NA	NA	NA	NA	NA	NA	NA	NA
5	0.4	0.1	4.7	10.8	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
6	0	0	0.9	6.7	0	0.4	6.2	10	0.1	0.1	6	6.5	7.8	13.2	NA
7A	0	0.3	0.4	5.1	0	0.6	3.1	9.2	0.2	0.1	13.5	6.6	7.3	10.3	NA
7B	0.2	6	1.5	6.9	2	6.2	3.1	6.9	8.9	6.4	12.9	11.9	12.3	9.5	NA
7C	0	0.6	0	4.1	0	1.4	2.8	5.3	2.3	2.7	10.4	10.8	12.7	8.8	NA

	Color Key - Minimum Oxygen Concentration (%)													
0	1	2	3	4	5	6	7	8	9	10	15	21		

Optimization Tests 1 and 2 evaluated equal-volume (i.e., 21,600 cubic feet) injection pulses of nitrogen, hydrogen, LPG, and carbon dioxide using different combinations of flow rate and duration. The objective of these tests was to determine whether gas pulses depleted oxygen in the vadose zone. Table 16 shows that oxygen was capable of being depleted in many of the piezometers and Test 1 conditions were slightly better at achieving this objective. However, the data in Figure 37 show that oxygen concentrations likely increased to greater than one percent within hours. Tests 3A through 3C evaluated alternative pulsing strategies but these were incapable of decreasing oxygen concentrations to less than one percent in many of the piezometers. Thus pulsing did not appear to be an effective injection strategy at this site.

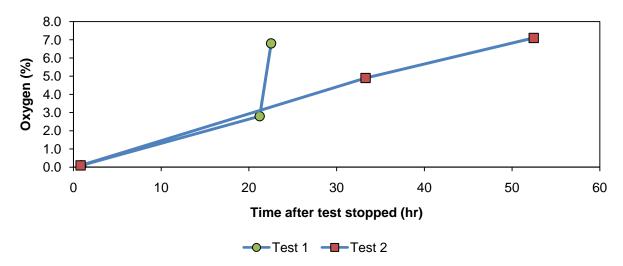


Figure 37 - Oxygen Concentration Transients in Piezometer P3 at 28 ft bgs after Gas Injection Stopped

Tests 4 and 5 were conducted to evaluate an initial gas pulse at a high flow rate followed by a continuous low flow rate. The results of these tests indicated that significant depletion of oxygen was observed only at the 18 and 28 ft bgs depths. For example, Table 16 shows that oxygen concentrations in P3, P4, and P5 were four percent or greater at depths of 38 and 48 ft bgs. The reason that ineffective oxygen depletion was observed at depth was attributed to the long 40-to-70-feet well screens used in injection wells INJ1, INJ2, and INJ3. Gas flow was preferentially directed toward the top of the screen and minimal flow exited the bottom of the screen.

Based on these results, gas injection into piezometer P4 was attempted in Tests 6 and 7 in an effort to better direct gas throughout the 50-feet deep target treatment zone. Gas was injected into the top two or three piezometer screens at total flow rates ranging from 0.83 to 1.7 cfm. Table 16 shows that oxygen concentrations in P3 and P5 were one percent or less at depths of 18, 28, and 38 ft bgs but not at 48 ft bgs. This injection approach was successful and superior to that used in Tests 4 and 5. Test 7B was not as successful as Tests 6 and 7 and the reasons for this difference was not determined. Nevertheless, Test 7C was initiated with a slightly greater flow rate (1.67 cfm compared to 1.00 cfm) and results were positive. Oxygen concentrations were readily depleted both with respect to distance from the injection point and depth. Test 7C conditions were selected as steady state operating conditions for the N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> gas mixture. Results for steady state operation are described in the next section.

## **5.7.3 Steady State Gas Concentrations**

Continuous gas injection into P4 at 18 and 28 ft bgs at a total flow rate of 1.67 cfm (100 cfh) was conducted during Phase III with a mixture of nitrogen (79 percent), hydrogen (10 percent), LPG (10 percent) and carbon dioxide (one percent). Figures 38 through 41 show the steady state oxygen, hydrogen, and propane concentrations measured during this injection period. The data presented in these figures include data from all piezometers. Measured oxygen concentrations within the 10-feet target ROI ranged from 0.04±0.14 percent to 1.4±2.0 percent. Low oxygen

concentrations were attainable at depths of 38 and 48 ft bgs even though gas was injected only into the 18 and 28 ft bgs piezometer screens. Oxygen concentrations increased with the distance from the point of injection (Figure 38).

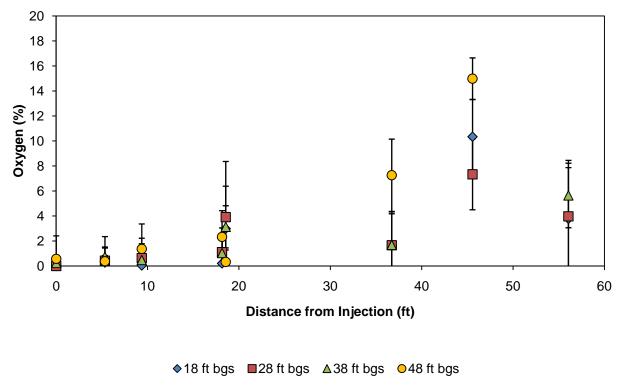


Figure 38 - Average Oxygen Concentrations during  $N_2/H_2/LPG/CO_2$  Injection. Error bars are  $\pm 1$  standard deviation.

Hydrogen concentrations approaching the injected concentration of 10 percent were most readily obtained at the 18 ft bgs location (Figure 39). Hydrogen concentrations decreased as the depth increased and as the distance from injection increased. Nevertheless, hydrogen was detectable at depths below the point of injection within the 10-feet target ROI (Figure 40). Hydrogen concentrations ranged from  $0.25\pm0.20$  percent to  $1.1\pm1.7$  percent at 38 ft bgs and from  $0.070\pm0.034$  percent to  $0.11\pm0.16$  percent at 48 ft bgs. Hydrogen was detected at concentrations greater than one percent in P8 located 56 feet north east from the point of injection at 18 and 28 ft bgs. This piezometer is located northerly from the point of injection. In comparison, hydrogen concentrations were less than 0.01 percent in P1 located 41 feet east of the point of injection. This difference is likely attributable to lithologic heterogeneities introduced from historical gold dredging operations that induced greater pneumatic permeability in the northerly direction.

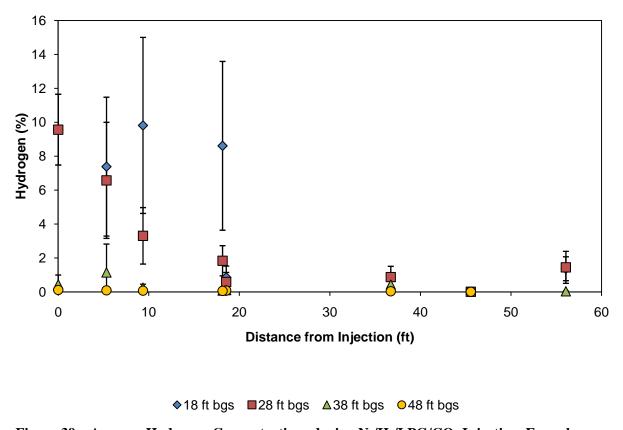


Figure 39 – Average Hydrogen Concentrations during  $N_2/H_2/LPG/CO_2$  Injection. Error bars are  $\pm 1$  standard deviation.

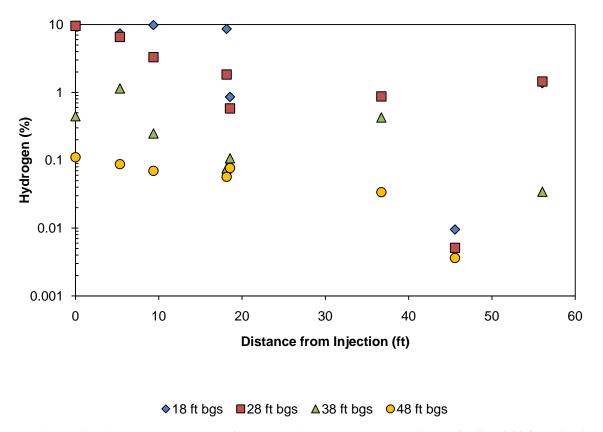


Figure 40 – Average Hydrogen Concentrations (log scale) during  $N_2/H_2/LPG/CO_2$  Injection

Propane was more easily distributed than hydrogen both with respect to distance from injection and depth (Figure 41). Measured propane concentrations within the 10-feet target ROI ranged from  $8.6\pm1.6$  percent to  $9.6\pm2.4$  percent. The lowest detected concentration anywhere was  $0.40\pm0.45$  percent in piezometer P1 at 48 ft bgs.

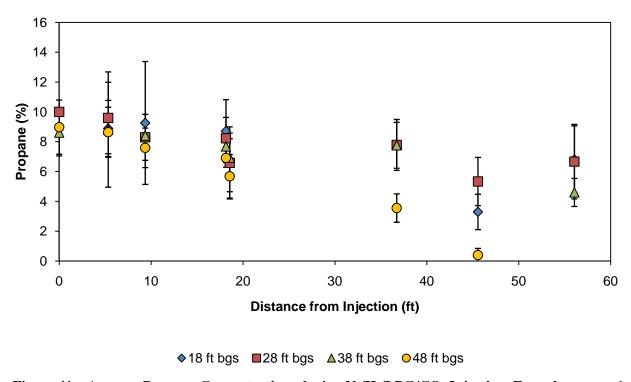


Figure 41 – Average Propane Concentrations during N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Injection. Error bars are ±1 standard deviation.

The above results indicate that continuous injection of the N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> gas mixture resulted in oxygen depletion and electron donor distribution within the 10-ft target ROI especially at depths ranging from 18 to 38 ft bgs. While hydrogen was detected at 48 ft bgs within the 10-ft target ROI, the concentrations were only 0.1 percent. Oxygen depletion and electron donor distribution outside of the 10-ft target ROI was observed; however, the results were variable. Historical gold dredging operations affected soil lithologic conditions such that greater oxygen depletion and electron donor distribution were observed in a northerly direction (i.e., P4 to P8) compared to an easterly direction (i.e., P4 to P1). While propane was readily distributed at all depths, hydrogen was preferentially distributed at shallower depths.

Continuous gas injection into P4 at 18 and 28 ft bgs at a total flow rate of 1.67 cfm (100 cfh) was conducted in Phase IV with pure LPG. Figures 42 and 43 show the steady state oxygen and propane concentrations measured during this injection period. Measured oxygen concentrations within the 10-feet target ROI ranged from  $0.029\pm0.049$  percent to  $5.9\pm1.5$  percent (Figure 42). Low oxygen concentrations were attainable at depths of 38 and 48 ft bgs even though gas was injected only into the 18 and 28 ft bgs piezometer screens. These low oxygen concentrations were observed at distances up to 56 ft away from the point of injection. However, oxygen concentrations were high at depths of 18 and 28 ft bgs both inside and outside of the 10-ft target ROI. The reason was attributable to the density of propane causing it to sink. Thus LPG alone was not capable of satisfactorily depleting oxygen within the 10-ft target ROI. On the other hand,

LPG alone was capable of depleting oxygen at depth at greater distances from the point of injection compared to the gas mixture (Figure 43).

Propane was easily distributed at significant distances from the point of injection at the 28, 38, and 48-ft bgs depths (Figure 43). The gas analyzer was not capable of reporting propane concentrations greater than 30 percent. Thus, concentrations shown on Figure 43 with values of 30 percent were likely greater than 30 percent. Distribution of propane at 18 ft bgs was relatively poor and this result is consistent with the observed oxygen concentration profiles (Figure 42). However, propane distribution at 28 ft bgs was relatively good which makes the elevated oxygen concentrations surprising.

The above results indicate that continuous injection of pure LPG was less effective than the gas mixture with respect to oxygen depletion and electron donor distribution. However, injection of pure LPG did have a distinct advantage with respect to oxygen depletion and electron donor distribution at depths greater than the point of injection.

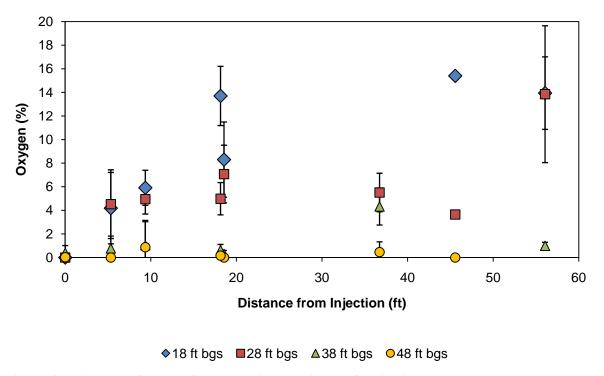


Figure 42 – Average Oxygen Concentrations during LPG Injection. Error bars are ±1 standard deviation.

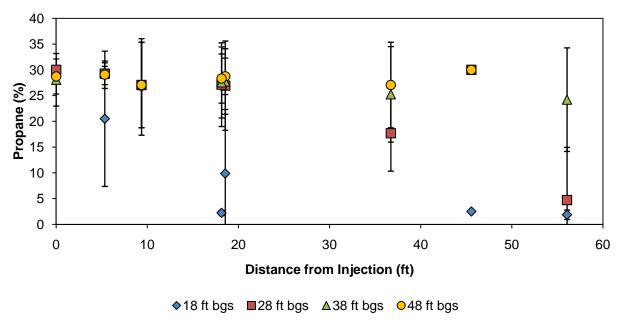


Figure 43 – Average Propane Concentrations during LPG Injection. Maximum propane concentration measurable by instrument was 30 percent. Error bars are  $\pm 1$  standard deviation.

### 5.7.4 Perchlorate and Nitrate Concentrations in Soil

Baseline concentrations of perchlorate and nitrate plus nitrite in soil were determined during installation of injection wells and piezometers. Final concentrations of these analytes in soil were determined after completion of Phase IV. To minimize complicating effects of soil heterogeneity on data analysis, final soil samples were collected directly adjacent to each injection well and piezometer. The distance between the well or piezometer and each adjacent soil boring ranged from 1.5 to 2.0 feet. Comparisons of baseline and final soil concentrations of perchlorate and nitrate plus nitrite (dry weight basis) are shown in Figures 44 through 55. These data represent samples collected along a transect from P4 to P1 (the "EW transect") and along the transect from P4 to P8 (the "NS transect"). Baseline concentrations are representative of soil samples collected during piezometer installation. Final concentrations are representative of the final confirmation borings. Figures 49 and 55 summarize the data for samples collected within the 10-ft target ROI.

Significant perchlorate concentration reductions were observed within the 10-ft target ROI and these reductions were especially pronounced in the shallower vadose zone horizons. The concentration reductions within the 10-ft target ROI ranged from one to three orders of magnitude except in the 45-to-50 ft bgs horizon. Initial concentrations of perchlorate within the 10-ft target ROI and the 10-to-40-ft bgs depth interval ranged from 2,600 to 75,000  $\mu$ g/kg. Final perchlorate concentrations ranged from < 13 to 8,800  $\mu$ g/kg. Seven final soil samples (i.e., six sample locations plus one duplicate) were ND for perchlorate (< 13 to <15  $\mu$ g/kg).

Significant nitrate concentration reductions were observed within the 10-ft target ROI and, unlike perchlorate, nitrate concentration reductions were observed at all depths. Reductions in nitrate concentrations were also observed outside the 10-ft target ROI and these reductions appeared to be more pronounced at the greater depths. The concentration reductions within the 10-ft target ROI ranged from one to two orders of magnitude. Initial concentrations of nitrate

plus nitrite within the 10-ft target ROI ranged from 2.0 to 8.6 mg-N/kg. Final nitrate plus nitrite concentrations ranged from < 0.054 to 2.9 mg-N/kg. Six final soil samples (i.e., five sample locations plus one duplicate) were ND for nitrate plus nitrite (< 0.054 to < 0.057 mg-N/kg).

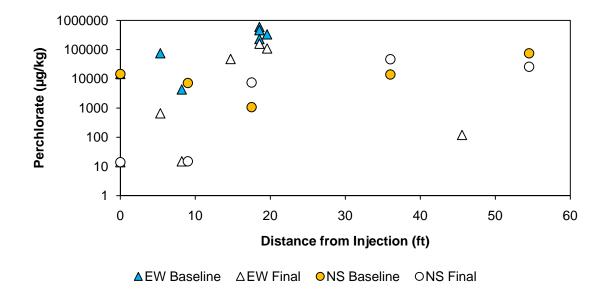


Figure 44 – Perchlorate Concentrations 5 to 10 ft bgs

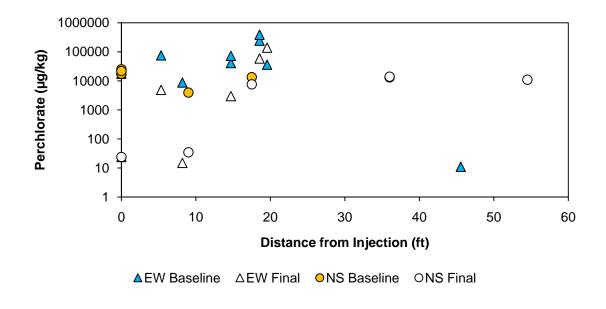


Figure 45 – Perchlorate Concentrations 15 to 20 ft bgs

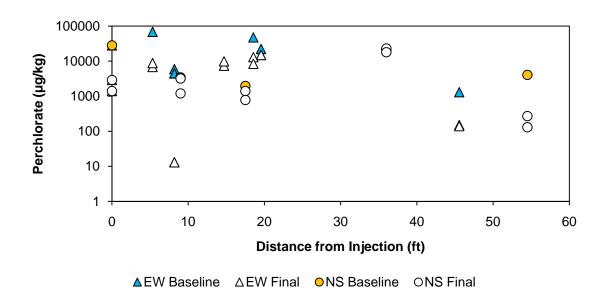


Figure 46 – Perchlorate Concentrations 25 to 30 ft bgs

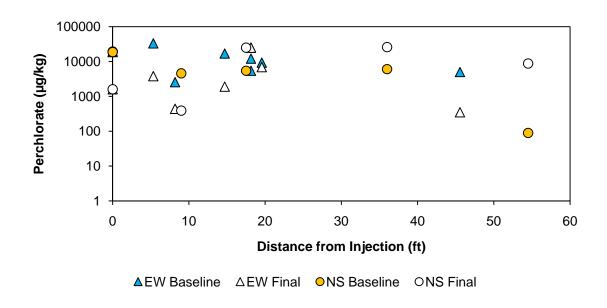


Figure 47 – Perchlorate Concentrations 35 to 40 ft bgs

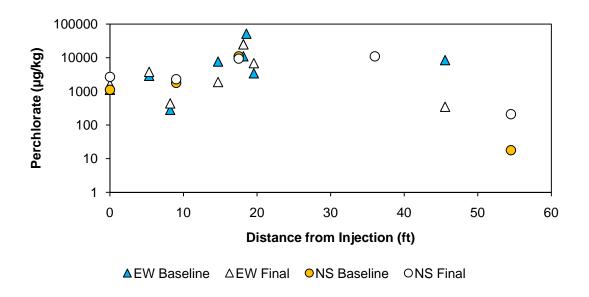


Figure 48 – Perchlorate Concentrations 45 to 50 ft bgs

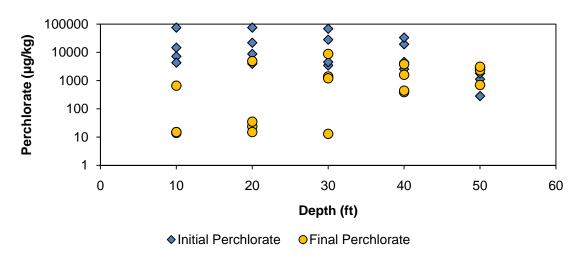


Figure 49 – Perchlorate Concentrations within the 10-ft Target ROI

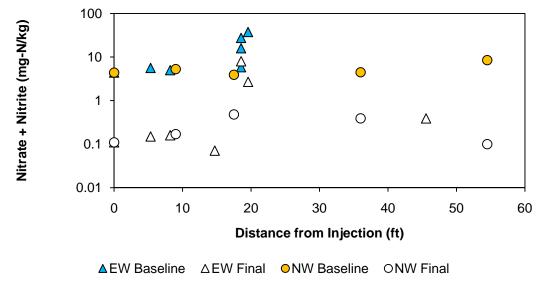


Figure 50 – Nitrate/Nitrite Concentrations 5 to 10 ft bgs

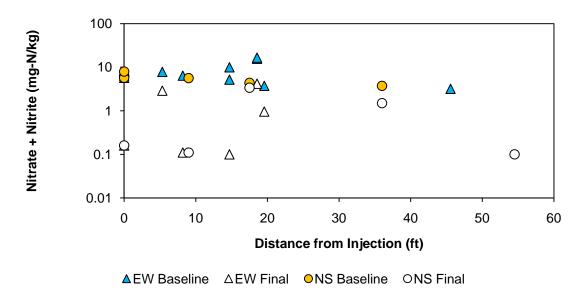


Figure 51 – Nitrate/Nitrite Concentrations 15 to 20 ft bgs

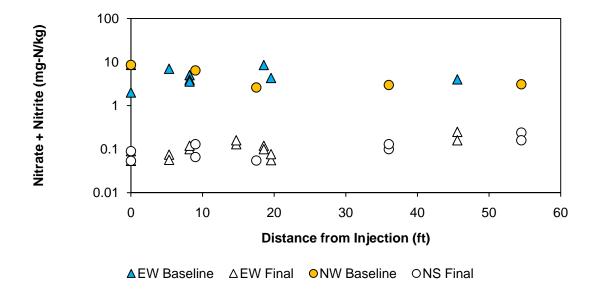


Figure 52 – Nitrate/Nitrite Concentrations 25 to 30 ft bgs

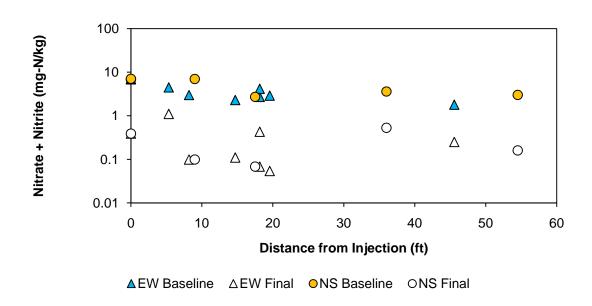


Figure 53 – Nitrate/Nitrite Concentrations 35 to 40 ft bgs

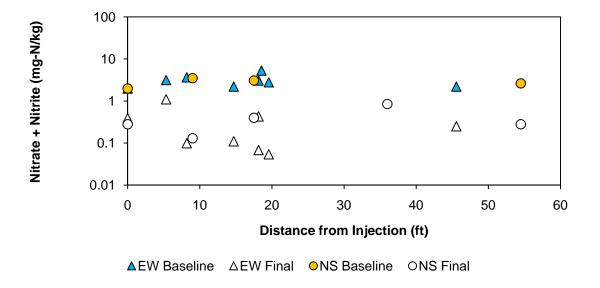


Figure 54 – Nitrate/Nitrite Concentrations 45 to 50 ft bgs

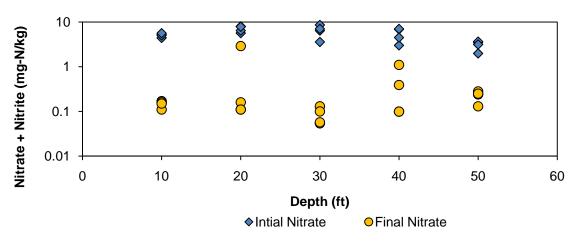


Figure 55 – Nitrate/Nitrite Concentrations within the 10-ft Target ROI

Percent perchlorate removals are shown in Figures 56 through 58. These data illustrate the dependence of perchlorate reduction on distance from the point of injection and depth below ground surface. A precipitous decline in percentage removal was observed between 15 and 20 feet from the point of injection (Figure 56). Perchlorate removal was consistently greater than 60 percent at distances less than 15 feet from the point of injection except at 50 ft bgs. At this depth perchlorate removal was inconsistent at all distances from the point of injection. Perchlorate removal was highly variable with respect to depth when the complete data set was evaluated (Figure 57) but was consistent at depths up to 40 ft bgs within the 10-ft target ROI (Figure 58). The average perchlorate removal within the 10-ft target ROI and at depths ranging from 10 to 40 ft bgs was 93±9 percent.

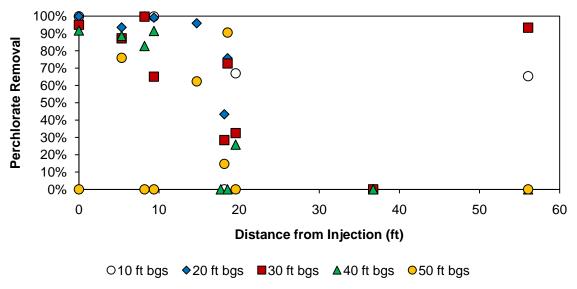


Figure 56 - Perchlorate Removal Based on All Data

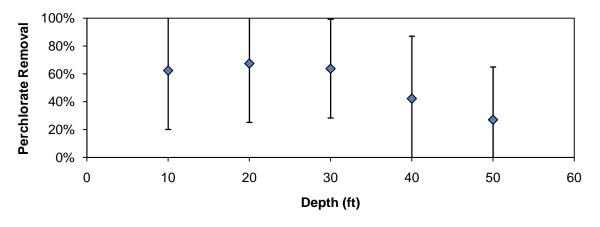


Figure 57 - Average Perchlorate Removal Based on All Data

75

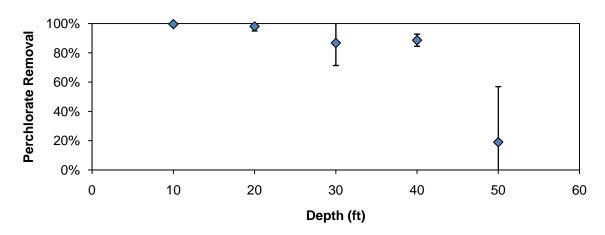


Figure 58 – Average Perchlorate Removal within the 10-ft ROI Target

Percent nitrate plus nitrite removals are shown in Figures 59 through 61. These data illustrate the relative independence of nitrate reduction on distance from the point of injection and depth below ground surface. Unlike perchlorate, nitrate removal was observed at the maximum distance sampled from the point of injection (Figure 59). Nitrate removal was consistently greater than 60 percent at all depths with the exception of 20 ft bgs. At this depth nitrate removal was inconsistent at all distances from the point of injection. Nitrate removal was generally consistent with respect to depth when the complete data set was evaluated (Figure 60) and within the 10-ft target ROI (Figure 61). The average nitrate removal within the 10-ft target ROI and at depths ranging from 10 to 50 ft bgs was 94±9 percent. The average nitrate removal based on all data was 90±14 percent.

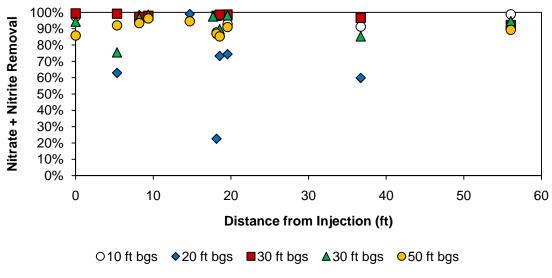


Figure 59 - Nitrate/Nitrite Removal Based on All Data

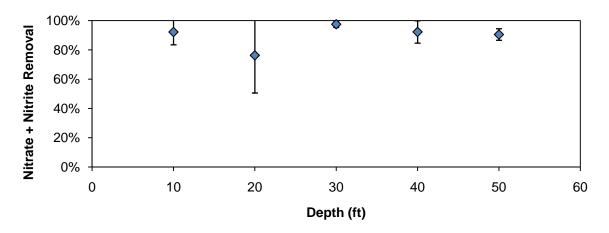


Figure 60 – Average Nitrate/Nitrate Removal Based on All Data

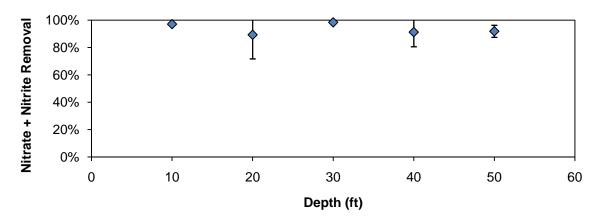


Figure 61 – Average Nitrate/Nitrite Removal within 10-ft ROI Target

### 5.7.5 Trends in Perchlorate and Nitrate Destruction

Continuous injection of the  $N_2/H_2/LPG/CO_2$  gas mixture began on 3/20/08 with the initiation of Optimization Test 6 and ended on 8/12/08 for a total of five months (Figure 32 and Table 15). Continuous injection of LPG was initiated on 9/8/08 and ended on 12/1/08 for a total of three months.

The initial demonstration approach detailed in the ESTCP Technology Demonstration Plan involved periodic completion of two soil borings approximately 5 and 15 feet away from the point of injection. These soil borings were completed during the five-month period of N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> gas mixture injection. Evaluation of the resultant data indicated strong heterogeneity with respect to soil perchlorate concentrations as illustrated in Figures 49 and 62. Perchlorate concentrations increased dramatically from west to east in the demonstration area. Therefore, the sampling and analysis approach was modified to involve collection of additional soil borings immediately adjacent to each well and piezometer. This approach minimized the effects of heterogeneity and facilitated data analysis. These soil borings were completed following the three-month LPG injection period. The results and conclusions presented in the preceding section were based on this modified approach.

This approach did not lend itself to a detailed analysis of perchlorate degradation rates. An example of this challenge is shown in Figures 63 through 66 (see Appendix C for additional figures). These figures illustrate the trends in perchlorate and nitrate/nitrite concentrations during the demonstration. Each figure includes the baseline concentrations (P3 and P5), intermediate time points for soil borings near but not immediately adjacent to the baseline locations (CB3 and CB6), and final time points for soil borings immediately adjacent to the baseline locations (CB17 and CB15). The perchlorate and nitrate concentrations near P3 decreased during the period of N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> gas mixture injection (Figures 63 and 65). Assuming the initial perchlorate concentration in the vicinity of CB3 was representative of the baseline perchlorate concentration in P3, the rate of perchlorate degradation in the vicinity of P3 was 380±110 µg/kg/d over the five-month period of gas mixture injection. A nitrate destruction rate of 40±11 µg/kg/d was estimated in the vicinity of P3. Significant perchlorate reductions in the vicinity of P5 were not verified until final soil sampling was conducted at the end of Phase IV LPG injection on 12/3/08 (Figure 64). However, soil boring CB6 was completed on 7/10/08 which was one month prior to completion of Phase III gas mixture injection. As will be discussed in Section 5.7.6, hydrogen was required for perchlorate reduction. The perchlorate reduction during the three-month period of LPG injection was unlikely and perchlorate reduction probably occurred only during the fivemonth period of N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> gas mixture injection. Heterogeneity greatly complicated assessment of actual nitrate destruction rates. Nitrate reduction near P5 was observed during Phase III (Figure 66).

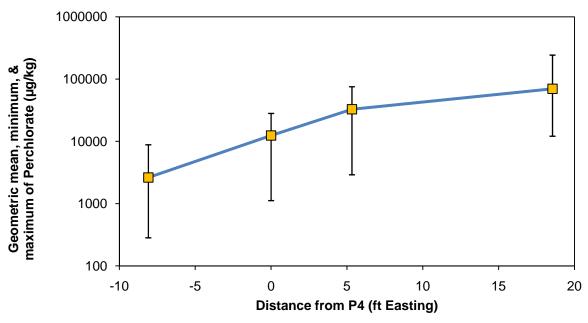


Figure 62 – Heterogeneity of Baseline Perchlorate Concentrations. Error Bars Represent Minimum and Maximum Observed Concentrations.

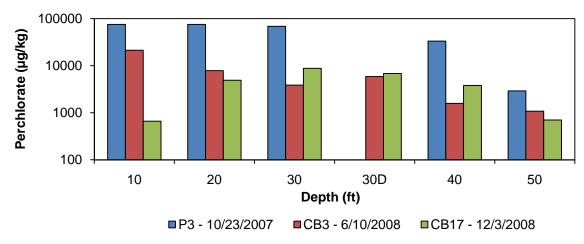


Figure 63 – Perchlorate Concentration Trends 5 ft East of the Point of Injection

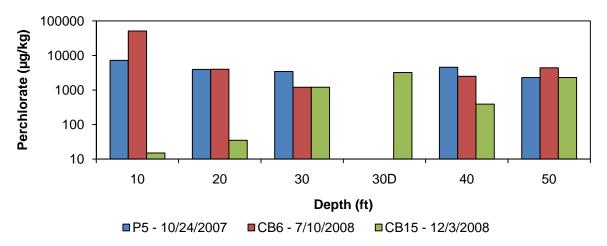


Figure 64 – Perchlorate Concentration Trends 9 ft North of the Point of Injection

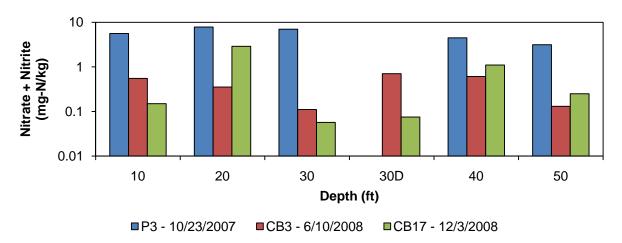


Figure 65 – Nitrate plus Nitrite Concentration Trends 5 ft East of the Point of Injection

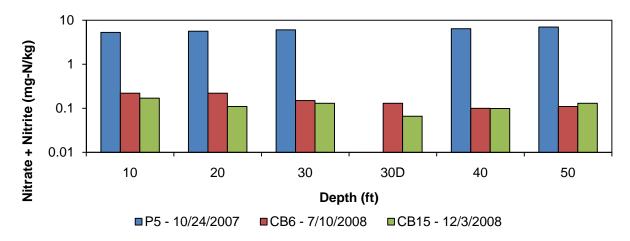


Figure 66 – Nitrate plus Nitrite Concentration Trends 9 ft North of the Point of Injection

## 5.7.6 Relationship between Contaminant Destruction and Gas Composition

Perchlorate reduction was high at depths of 10 to 40 ft bgs and at distances up to at least 10 ft and possibly up to 15 ft away from the point of injection (Figure 56). Perchlorate reduction was not significant at 50 ft bgs and at distances greater than 15 ft from the point of injection. The hydrogen concentration appears to be the primary factor that affected perchlorate reduction based on data presented in Figure 67 and 68. These figures illustrate the average gas concentrations and percent contaminant removal during mixed  $N_2/H_2/LPG/CO_2$  gas and pure LPG injection, respectively.

The data in Figure 67 suggest that hydrogen and possibly oxygen may have contributed to the decline in perchlorate reduction within the 10-ft target ROI. As the depth increased from 40 to 50 ft bgs and average perchlorate reduction declined from 89±4 to 19±38 percent, average hydrogen concentration decreased from  $0.61\pm0.77$  to  $0.09\pm0.07$  percent – a decline of 85 percent. Average oxygen concentration increased insignificantly from  $0.48\pm0.60$  to  $0.78\pm0.50$  percent – an increase of 38 percent. The more significant change in hydrogen concentration relative to oxygen concentration suggests that hydrogen was the primary factor affecting perchlorate reduction. Treatability study data conclusively demonstrated perchlorate reduction in the presence of hydrogen whereas perchlorate reduction in the presence of LPG was not significantly different from the control.

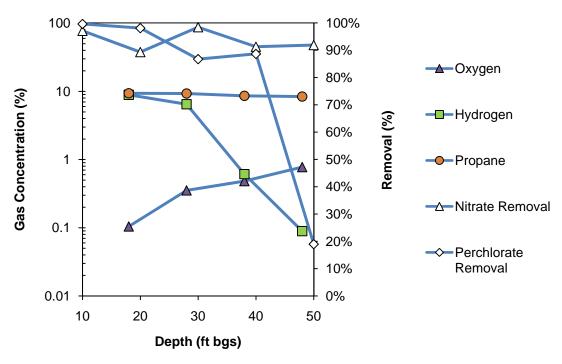


Figure 67 – Relationship between Contaminant Removal and Gas Composition within the 10-ft Target ROI during Phase III mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

Interestingly, as the depth increased from 30 to 40 ft bgs, perchlorate reduction did not change (i.e., 87±15 versus 89±4 percent), average hydrogen concentration decreased from 6.5±0.9 to 0.61±0.77 percent, and oxygen increased insignificantly from 0.35±0.82 to 0.48±0.60 percent. Thus perchlorate reduction was supported equally by 0.61±0.77 and 6.5±0.9 percent hydrogen and high hydrogen concentrations are not required to support significant perchlorate reduction. Propane did not change significantly and was not the cause of changes in perchlorate reduction. On the other hand, nitrate reduction was relatively constant suggesting that LPG supported nitrate reduction.

The data in Figure 68 support the conclusion that low hydrogen concentration was the primary factor preventing perchlorate reduction at 50 ft bgs. Hydrogen concentrations were nondetectable during LPG injection. Propane concentrations were relatively constant and oxygen concentrations were lowest at 50 ft bgs. The average oxygen concentration at 48 ft bgs during LPG injection was  $0.3\pm1.3$  percent compared to  $0.78\pm0.50$  percent during mixed gas injection. The average LPG concentration at 48-ft bgs was  $28\pm3$  percent<sup>2</sup>. Still, no perchlorate reduction occurred at this depth. Thus hydrogen supplied during Phase III was required for perchlorate reduction.

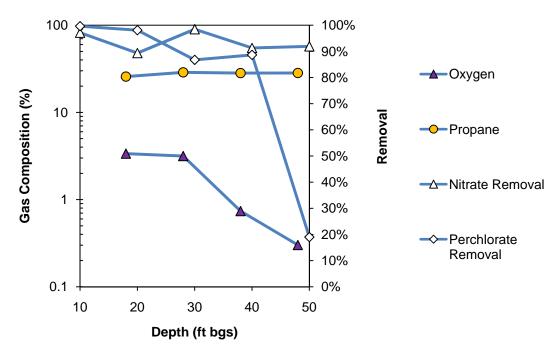


Figure 68 – Relationship between Contaminant Removal and Gas Composition within the 10-ft
Target ROI during Phase IV LPG Injection

While hydrogen appears to have been the primary factor affecting perchlorate reduction within the 10-ft target ROI, oxygen appears to have prevented perchlorate reduction outside of this zone especially at distances greater than 15 ft from the point of injection.

Figure 69 illustrates that when all of the data are evaluated (i.e., inside and outside the 10-ft target ROI and at all depths), the oxygen concentration increased in a roughly exponential manner as the distance from the point of injection increases ( $r^2 = 0.56$ ). Signficant perchlorate reduction was observed when the oxygen concentration was less than about one percent. Perchlorate reduction was negligible or inconsistent when oxygen concentrations were greater than about one percent. Very low oxygen concentrations (e.g., less than 0.1 percent) were not

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<sup>&</sup>lt;sup>2</sup> The RKI Eagle had a maximum reporting level of 30 percent for propane. Therefore this value should be considered a minimum value.

required for significant perchlorate reduction. Hydrogen concentration decreased with distance from the point of injection as illustrated in Figure 70, but the correlation coefficient was low ( $r^2 = 0.14$ ). Even though hydrogen concentrations near one percent were observed at distances greater than 20 feet from the point of injection (Figure 70), consistent perchlorate removal was not observed because of elevated oxygen concentrations (Figure 69). When the data presented in Figures 67 through 70 along with additional data presented in Section 5.7.3 are considered, the required conditions for perchlorate reduction at this site appear to be less than one percent oxygen and greater than 0.2 percent hydrogen.

Figure 71 indicates that nitrate reduction was not nearly as sensitive to oxygen inhibition as perchlorate reduction and significant nitrate reduction was observed with oxygen concentrations up to 10 percent or greater. Figures 72 and 73 indicate that hydrogen concentrations as low as about 0.01 percent and/or propane concentrations about three percent or greater supported nitrate reduction.

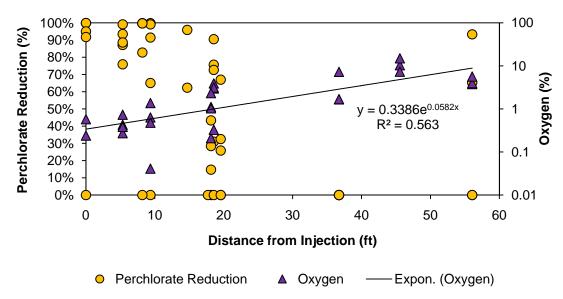


Figure 69 – Relationship between Perchlorate Reduction and Oxygen Concentration Inside and Outside the 10-ft Target ROI during Phase III Mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

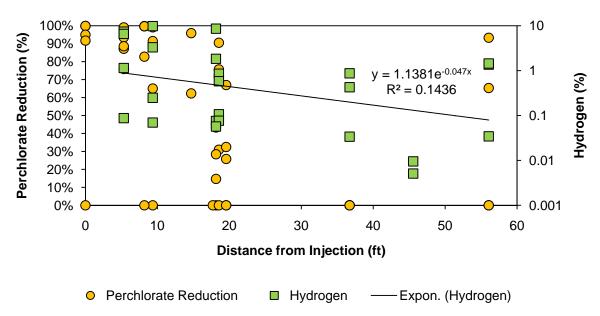


Figure 70 – Relationship between Perchlorate Reduction and Hydrogen Concentration Inside and Outside the 10-ft Target ROI during Phase III Mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

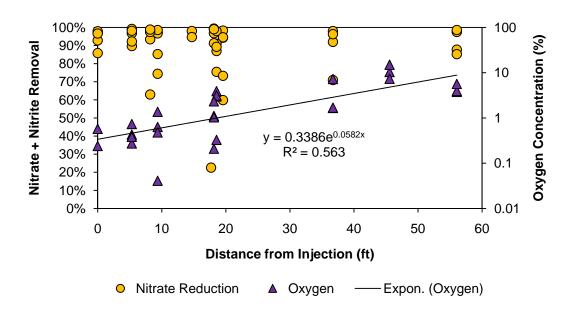


Figure 71 – Relationship between Nitrate Reduction and Oxygen Concentration Inside and Outside the 10-ft Target ROI during Phase III Mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

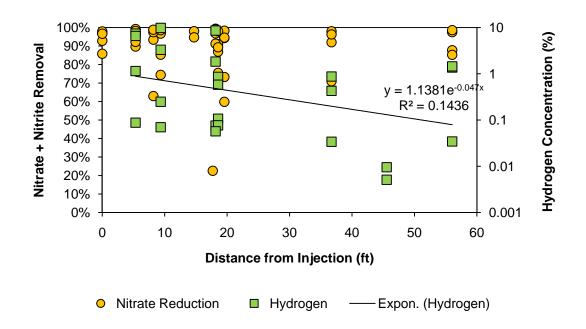


Figure 72 – Relationship between Nitrate Reduction and Hydrogen Concentration Inside and Outside the 10-ft Target ROI during Phase III Mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

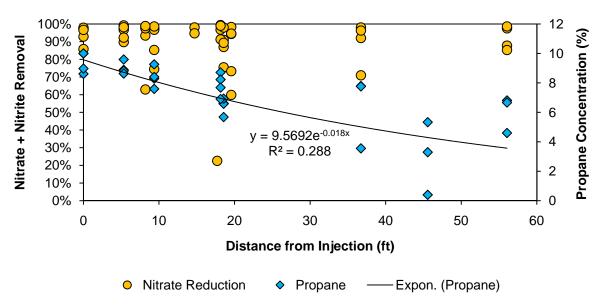


Figure 73 – Relationship between Nitrate Reduction and Propane Concentration Inside and Outside the 10-ft Target ROI during Phase III Mixed N<sub>2</sub>/H<sub>2</sub>/LPG/CO<sub>2</sub> Gas Injection

### **5.7.7 Soil Moisture Effects**

In addition to gas composition, perchlorate biodegradation can be influenced by soil moisture in two ways. One is with respect to biological activity and the other is with respect to gas transport. If soil moisture is too low then biological activity could be inhibited. Treatability tests conducted using site soil demonstrated that perchlorate reduction was possible with 16 percent moisture but not with eight percent moisture. Additionally, if soil moisture is very high, for example in clay, then gas transport may be hindered and insufficient electron donors will be available to promote perchlorate biodegradation. Figure 74 illustrates that a wide range of soil moistures were measured and these variations were attributable to variations in soil lithologic conditions. In general, shallower soils (e.g., 10 to 20 ft bgs) were predominately clays and silts and deeper soils (e.g., 30, 40, and 50 ft bgs) were predominately silty sands and gravels. Perchlorate degradation was observed less than 15 ft from the point of injection and at depths of 10 to 40 ft bgs (Figure 56). Initial moisture contents in this zone ranged from 10 to 36 percent as shown on Figure 75. Initial moisture contents ranged from 6.1 to 36 percent (Figure 76). Thus perchlorate biodegradation was observed at moisture contents as low as 6.8 to 10 percent which is less than that observed in the treatability study. Thus field performance was better than laboratory treatability performance. At this site, moisture content did not control perchlorate removal based on a lack of correlation with moisture content within the 10-ft target ROI and across the entire demonstration area (Figures 75 through 78). Nitrate removal was not affected by moisture content and significant removal was observed at moisture contents as low as 6.1 percent (Figures 79 and 80).

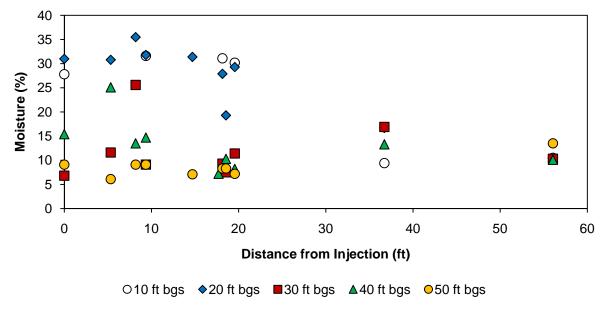


Figure 74 – Final Moisture Distribution

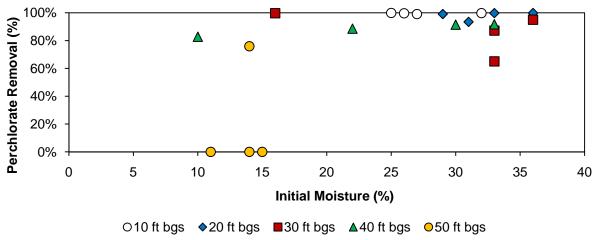


Figure 75 – Perchlorate Removal within the 10-ft Target ROI at Different Initial Moisture Contents

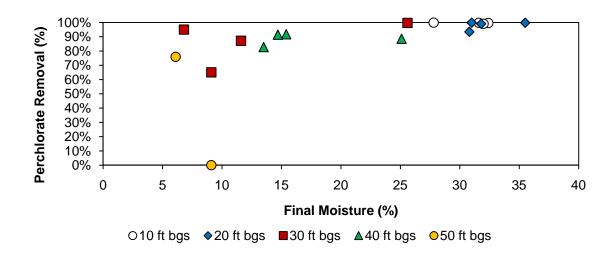


Figure 76 – Perchlorate Removal within the 10-ft Target ROI at Different Final Moisture Contents

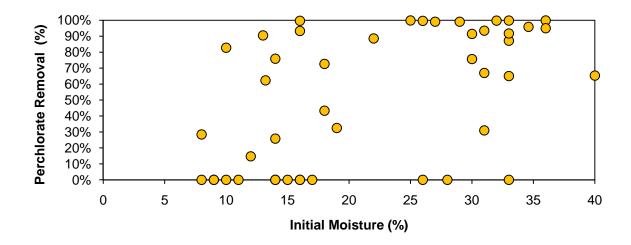


Figure 77 – Perchlorate Removal Inside and Outside the 10-ft Target ROI at Different Initial Moisture Contents

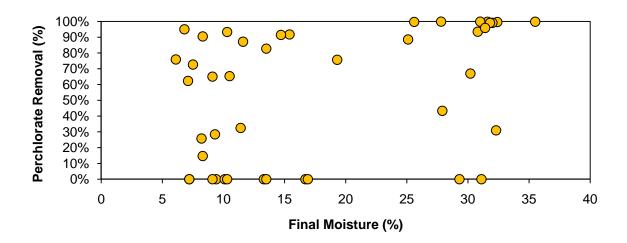


Figure 78 – Perchlorate Removal Inside and Outside the 10-ft Target ROI at Different Final Moisture Contents

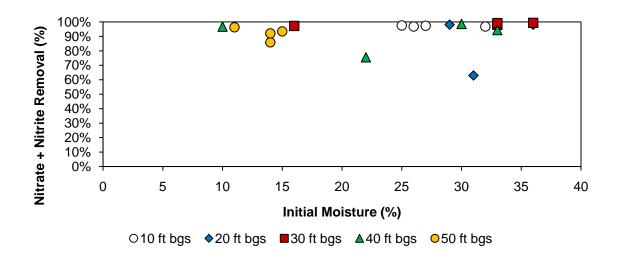


Figure 79 – Nitrate Removal within the 10-ft Target ROI at Different Initial Moisture Contents

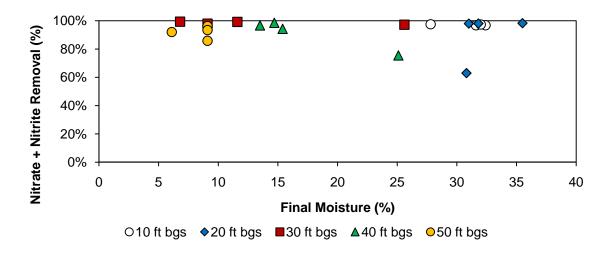


Figure 80 – Nitrate Removal within the 10-ft Target ROI at Different Final Moisture Contents

The potential for soil drying because of dry gas injection was evaluated. Figures 81 and 82 indicate that changes in soil moisture were highly variable. The average change in soil moisture was an 18 percent decrease which was statistically significant (P=0.0098). Soil drying appeared to be especially significant in the immediate vicinity of the point of injection. Soil drying is typically expected in the immediate vicinity of gas injection (Leeson and Hinchee, 1996). Thus the observed soil drying was not necessarily attributable to GEDIT and may have been attributable to seasonal variation of rainwater infiltration. Nevertheless, this drying did not result in bone-dry soil that could have inhibited perchlorate biodegradation.

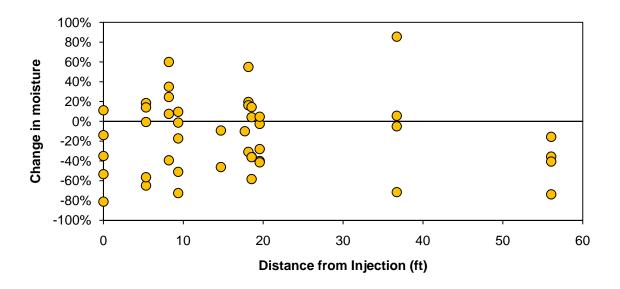


Figure 81 – Change in Moisture as a Function of Distance from the Point of Injection

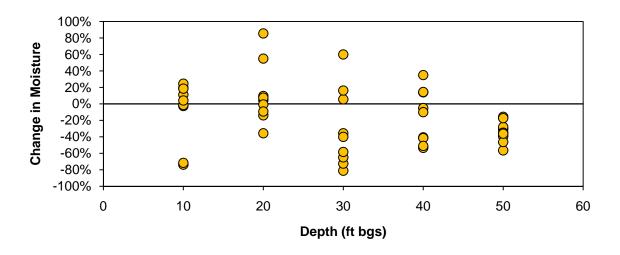
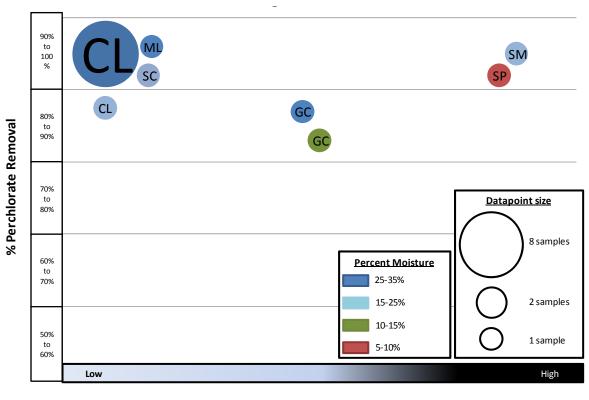


Figure 82 - Change in Moisture as a Function of Depth

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### 5.7.8 Soil Lithology Effects

Perchlorate destruction was observed across a wide range of moisture contents. These moisture contents in general correlated with soil lithologic conditions – finer grained soil types (e.g., clays and silts) had greater moisture contents than larger grained soil types (e.g., sands and gravels). Figures 83 and 84 illustrate that higher perchlorate destruction was observed across a wide range of soil lithologic conditions. The data in these figures are based on samples collected within the 10-ft target ROI and depths from 10 to 40 ft bgs. A qualitative assessment of permeability was based on USCS<sup>3</sup> soil types. Most samples upon which perchlorate destruction was quantified were fine-grained, low-permeability USCS soil type (e.g., CL). High perchlorate destruction was also observed in coarse-grained, high-permeability soil types.



**Permeability** 

Figure 83 – Relationship between Perchlorate Destruction and Baseline Soil Moisture and USCS Soil Type

Unified Soil Classification System definitions used in Figures 83 and 84 are as follows: CL – clay; ML – silt; SC – clayey sand; GC – clayey gravel; GM – silty gravel; GW – well graded gravel; SP – poorly graded sand; SM – silty sand.

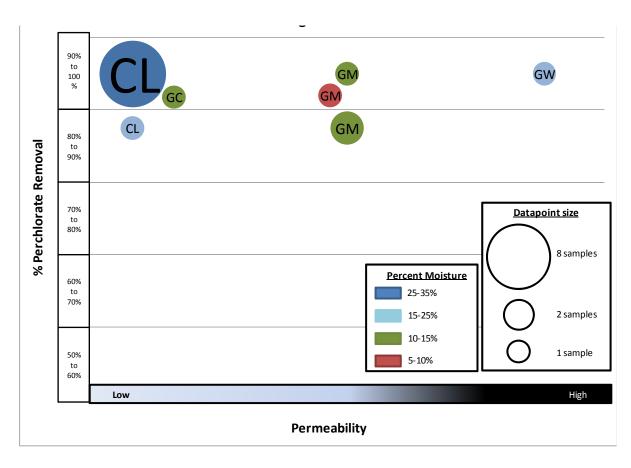


Figure 84 – Relationship between Perchlorate Destruction and Final Soil Moisture and USCS Soil Type

#### 6.0 PERFORMANCE ASSESSMENT

A summary of the performance objectives for this demonstration along with an overview of technology performance was presented in Section 3. This section includes an assessment of technology performance that is supported by data presented in Section 5.

#### **6.1** Perchlorate Destruction

The average percent perchlorate destruction was  $93\pm9$  percent within the 10-ft radius of influence and the 10-to-40-ft bgs depth interval (see Section 5.7.4). This ROI and depth interval was based on hydrogen transport and oxygen concentrations as described in Section 6.5. The performance objective of 90 percent for perchlorate destruction was exceeded. Initial perchlorate concentrations within this ROI and depth ranged from 2,600 to 75,000  $\mu$ g/kg. Final perchlorate concentrations ranged from < 13 to 8,800  $\mu$ g/kg. Seven final soil samples (i.e., six sample locations plus one duplicate) were ND for perchlorate (< 13 to <15  $\mu$ g/kg).

Perchlorate destruction was affected by oxygen and hydrogen concentrations (see Section 5.7.6). As illustrated in Figure 67, oxygen concentrations less than about one percent and hydrogen concentrations greater than 0.5 percent supported perchlorate destruction. These concentrations were observed within the 10-ft ROI and 40-ft bgs depth. At greater distances from the point of injection (i.e., P4) and greater depths, the oxygen concentrations were greater than one percent and/or the hydrogen concentrations were less than 0.5 percent.

Perchlorate destruction did not appear to be promoted by LPG serving as an electron donor for anaerobic perchlorate biodegradation (see Section 5.7.6). During the three-month Phase IV LPG/N<sub>2</sub> injection, oxygen concentrations at 48-ft bgs were 0.3±1.3 percent and average LPG concentrations were 28±3 percent though insignificant perchlorate reduction was observed at 50 ft bgs (Figure 68). While LPG did not directly promote perchlorate biodegradation, it is capable of serving as an electron donor for aerobic bacteria. Therefore, it may have indirectly promoted perchlorate biodegradation during the five-month Phase III injection of H<sub>2</sub>/CO<sub>2</sub>/LPG/N<sub>2</sub> by reducing oxygen concentrations via aerobic propane biodegradation.

Perchlorate destruction was not affected strongly by differences in soil moisture at this site (see Section 5.7.7). Significant perchlorate destruction was observed in soil samples with final moisture contents ranging from 6.8 to 36 percent (Figure 75). Too low of a moisture content has the potential to inhibit perchlorate biodegradation. Some inhibition may have occurred at low moisture contents compared to high moisture contents, but 95 percent perchlorate destruction was observed at a moisture content of 6.8 percent. Laboratory treatability data demonstrated perchlorate biodegradation at 16 percent moisture but not at 7 percent moisture. Thus perchlorate destruction performance in the field was greater than predicted by the laboratory treatability study. High moisture contents were representative of silt and clay soil types. These soil types would be expected to hinder electron donor transport. However, high perchlorate destruction was observed at the highest moisture contents indicating that hydrogen was able to diffuse into low permeability soil pore spaces. Hydrogen with a molecular weight of two has a high diffusivity relative to other gases. For example, the diffusivities of hydrogen and oxygen (molecular weight of 32) in air are 0.611 and 0.178 cm<sup>2</sup>/s, respectively (Perry and Chilton, 1973). The diffusivities

of hydrogen and oxygen in water are  $5.85 \times 10^{-5}$  and  $2.5 \times 10^{-5}$  cm<sup>2</sup>/s, respectively (Perry and Chilton, 1973).

Perchlorate destruction was not affected by differences in soil lithologic conditions associated differences in pneumatic permeability (Section 5.7.8 and Figures 83 and 84).

#### **6.2** Nitrate Destruction

The average percent nitrate destruction was 94±9 percent within the 10-ft radius of influence and the 10-to-50-ft bgs depth interval (see Section 5.7.4). This ROI and depth interval was based on hydrogen and LPG transport and oxygen concentrations as described in Section 6.5. The performance objective of 90 percent for perchlorate destruction was exceeded. When all data were considered which comprised an ROI of 56 ft, the average nitrate destruction was 90±14 percent. Nitrate was analytically quantified as the sum of nitrate and nitrite. Therefore, accumulation of the denitrification intermediate nitrite did not occur. Initial concentrations of nitrate plus nitrite within the 10-ft target ROI ranged from 2.0 to 8.6 mg-N/kg. Final nitrate plus nitrite concentrations ranged from < 0.054 to 2.9 mg-N/kg. Six final soil samples (i.e., five sample locations plus one duplicate) were ND for nitrate plus nitrite (< 0.054 to <0.057 mg-N/kg).

Nitrate destruction was affected less by gas composition than perchlorate destruction (see Section 5.7.6). Significant nitrate destruction occurred when oxygen concentrations were less than about 10 percent (Figure 71). Nitrate destruction was observed under a wide range of hydrogen concentrations as low as about 0.01 percent and under propane concentrations about three percent or greater (Figures 72 and 73). Whether hydrogen or propane was predominant electron donor for nitrate biodegradation cannot be ascertained based on these data. Also, naturally occurring organic carbon could have served as an electron donor. Data from the Remedial Investigation indicated that total organic carbon in soil was generally ND at reporting limits ranging from 105 to 132 mg/kg. Although, one soil sample contained 3,210 mg/kg of TOC (Aerojet & HSI GeoTrans, 2000).

Similar to perchlorate, nitrate destruction was not affected by differences in soil moisture at this Site (Section 5.7.7 and Figures 79 and 80).

#### **6.3** Perchlorate Destruction Rate

A maximum of five months was required to achieve  $93\pm9$  percent perchlorate destruction during the demonstration and three months or less was required in certain locations (Section 5.7.5). The performance objective was 90 percent destruction within twelve months. Thus, the performance objective was met. Heterogeneity greatly complicated assessment of actual perchlorate destruction rates. Nevertheless,  $88\pm11$  percent perchlorate destruction at a rate of  $380\pm110$  µg/kg/d was estimated in the vicinity of P3. This rate compares favorably to biodegradation rates measured during optimized full-scale *ex situ* bioremediation of perchlorate in soil (Evans et al., 2008). There, the median rate was about  $200 \,\mu\text{g/kg/d}$  and the  $90^{\text{th}}$  percentile rate was about  $500 \,\mu\text{g/kg/d}$ .

#### **6.4** Nitrate Destruction Rate

A maximum of five months was required to achieve  $94\pm9$  percent nitrate destruction during the demonstration and three months or less was required in certain locations (Section 5.7.5). The performance objective was 90 percent destruction within six months. Thus, the performance objective was met. Nitrate plus nitrite was quantified to account for the potential of nitrite accumulation during denitrification. Therefore the destruction rate is representative of nitrate and nitrite destruction rather than partial nitrate transformation to nitrite. Heterogeneity greatly complicated assessment of actual nitrate destruction rates. Nevertheless, a nitrate destruction rate of  $40\pm11~\mu\text{g/kg/d}$  was estimated in the vicinity of P3.

### 6.5 Implementability

ROI was used as a primary metric for implementability because it will determine the number of wells required to treat a given area. The ROI for perchlorate degradation was conservatively estimated to be 10 feet and likely to be 15 ft during the demonstration. (Section 5.7.4 and Figure 56). This ROI for nitrate degradation was estimated to be at least 56 ft (Section 5.7.4 and Figure 59). The performance objective for implementability was an ROI of 10 ft. Therefore, the performance objective was met.

These ROIs were based on injection of a total of 100 scfh of gas into P4 at 18 and 28 ft bgs. The ROI for oxygen depletion and electron donor transport was strongly affected by injection well design, gas flow rate, injection strategy (Sections 5.7.1 and 5.7.2). Use of six-inch long soil vapor probes as injection points and continuous injection of gas at relatively low flow rates was preferable to use of long well screens and pulsing of gas a relatively high flow rates. Gas composition also affected the ROI and the ROI varied with respect to depth. For example, LPG was transported a greater distance than hydrogen during Phase III injection of the H<sub>2</sub>/CO<sub>2</sub>/LPG/N<sub>2</sub> gas mixture (Figures 39 through 41). Hydrogen, because of its buoyancy, was limited in how deep it could be transported compared to LPG. The injection of this mixture was effective in reducing oxygen concentrations not only at the injection depths (i.e., 18 and 28 ft bgs), but also above and below these depths based on measured oxygen concentrations and observed perchlorate removals (Figure 67). Injection of pure LPG during Phase IV demonstrated that this gas could be transported significant distances but tended to sink resulting in elevated oxygen concentrations in shallow soil horizons (Figures 42 and 43). Thus, the ROI measured for this demonstration was operationally defined and should not be directly applied to other sites. Greater ROIs are possible and the most cost-effective and implementable approach will be determined by optimizing gas injection and well spacing.

### 7.0 COST ASSESSMENT

This section provides an assessment of full-scale GEDIT costs and drivers. The IRCTS-PBA site was used as a basis for developing the cost estimates. Four different scenarios were developed for in situ treatment of perchlorate in soil at this site. These scenarios were developed to compare actual demonstration design and operating conditions to likely full-scale design and operating conditions.

#### 7.1 Cost Model

This section provides the technical basis of the cost estimates including descriptions of the scenarios, a list of assumptions, a discussion of significant design considerations, and a description of the project tasks for which costs were developed.

#### 7.1.1 Technical Basis

This cost model is generally transferrable to other sites, however, it is important to note that the design basis (e.g., treatment goals, injection well design, gas injection strategy, etc.) will need to be tailored to site-specific conditions.

Four scenarios were considered and compared in this cost assessment for the IRCTS-PBA. Each scenario has different treatment objectives, gas compositions, and total soil volumes to be treated as listed in Table 17. Scenarios 1 and 3 have the treatment objective of reducing perchlorate concentrations to  $60~\mu g/kg$  or less which is a potential cleanup goal for projection of groundwater as required by the California Regional Water Quality Control Board. Scenarios 2 and 4 have the treatment objective of achieving 90 percent mass reduction of perchlorate. Scenarios 1 and 2 are conservatively designed based on demonstration data and have an ROI of 10 ft and a gas composition based on 10 percent hydrogen. The 10 ft ROI is the minimum value based on demonstration data. The gas composition comprised of 10 percent hydrogen was used in the demonstration and lesser concentrations (i.e., 0.5 percent) were effective. Scenarios 3 and 4 have an ROI of 15 ft because limited demonstration data indicated this value was likely. Furthermore, the gas composition is one percent hydrogen and 99 percent nitrogen because hydrogen concentrations as low as 0.5 percent appear to be able to promote perchlorate degradation; LPG was not necessary for perchlorate reduction.

In summary, Scenario 1 represents the successful design used in the demonstration, and Scenario 2, 3, and 4 are alternative designs based on the demonstration data. Scenario 2 adopts the design from Scenario 1 but with a different treatment objective. Scenarios 3 and 4 have not been demonstrated per se, but have a reasonable chance of success based on demonstration data.

Table 17 – Design Basis for Each Scenario

	Scenario 1	Scenario 2	Scenario 3	Scenario 4
		90 percent		90 percent
	60 μg/kg	mass	60 μg/kg	mass
Treatment Objective	perchlorate	reduction	perchlorate	reduction
ROI (ft)	10	10	15	15
Nitrogen composition (percent)	79 percent	79 percent	99 percent	99 percent
Hydrogen composition				
(percent)	10 percent	10 percent	1 percent	1 percent
LPG composition ( percent)	10 percent	10 percent	0 percent	0 percent
Total soil volume (cy)	550,000	310,000	550,000	310,000

#### 7.1.2 Assumptions

The assumptions made during this cost assessment are summarized below:

- 1) Site characterization is complete and additional site investigation outside of treatability and pilot testing is not required.
- 2) The total areas of perchlorate contamination in different depth intervals (i.e., 0 to 20 ft bgs, 21 to 70 ft bgs, and 71 to 140 ft bgs) were estimated based on the data presented in the Remedial Investigation Report (Aerojet & HSI GeoTrans, 2000).
- 3) Surface soil (0 to 20 ft bgs) will be treated using excavation and costs are not included. GEDIT will only be used to treat the vadose zone from 21 ft to 140 ft bgs.
- 4) For Scenarios 2 and 4, 90 percent of the perchlorate mass in the 21 to 70 ft bgs interval was assumed to be contained in 70 percent of the total area associated with Scenarios 1 and 3. Similarly for the 71 to 140 ft bgs interval, 90 percent of the perchlorate mass was assumed to be contained in 50 percent of the total area.
- 5) Review of RI cross sections indicated significant heterogeneity with respect to perchlorate concentrations as a function of lateral and vertical distribution. Based on review of these data, only 20 percent of the area that was contaminated from 21 to 70 ft bgs was also contaminated from 71 to 140 ft bgs. Therefore, 20 percent of the wells were constructed with a gas injection interval from 21 to 140 ft bgs. The remaining wells were constructed with a gas injection interval either from 21 to 70 ft bgs or from 71 to 140 ft bgs. The gas injection interval was comprised of six-inch vapor probes located every 10 feet of depth and was based on the demonstration piezometer design.
- 6) The ratio of monitoring wells to injection wells is 1:10 and the monitoring wells are designed identically to the injection wells.
- 7) One full-time geologist will be on site during injection and monitoring well installation. A geologist will need to be on site only periodically to oversee well abandonment.
- 8) The treatment area would be treated 10 percent at a time. Therefore, treatment will be conducted in 10 stages, each of which will run for six months. The whole project will take five years.
- 9) Twenty soil borings will be needed in each scenario to demonstrate attainment of cleanup goals.
- 10) Unit costs such as those for electricity and supplied injection gases would not change over the course of the project.

11) A contingency of 15 percent was included on construction, operations, maintenance, and demobilization costs.

#### 7.1.3 Design Considerations

Supply requirements for gases, water, and electricity will be site-specific. The rationale for each of these supplies is discussed in this section.

### Nitrogen Generator

This cost estimate includes a nitrogen generator. Because of the high volume of nitrogen needed for injection, it is more economical to purchase a generator and produce nitrogen on-site than to buy nitrogen in tube trailers or liquid nitrogen tanks. If GEDIT is applied at a small site, it is possible that purchasing compressed or liquid nitrogen is more cost effective.

### Hydrogen Generator

A hydrogen generator is included in the cost estimate for Scenarios 1 and 2 because of the large amount of hydrogen required. For Scenarios 3 and 4, hydrogen would be purchased from a gas vendor in tube trailers since that is more cost-effective. Because the volume of gas needed is site-specific, when estimating GEDIT implementation costs at another site, a cost comparison is needed to decide whether a hydrogen generator should be used.

### Water Supply

Water is needed at the site to serve drilling activities (a secured water source located within ¼ miles of drilling operations reduces the drillers' effort). For Scenarios 1 and 2, water is also needed to supply the hydrogen generator. Two temporary water service options were considered: installation of a water line and water truck service. Cost comparison showed the former would be more economical at this site, so that was what included in the cost estimate. However, this decision should also be based on site-specific conditions when estimating GEDIT costs at other sites.

### Electrical Supply

Electricity is required for operation of the gas generators and thus an electrical drop was required and the cost was estimated. Use of gas in compressed or liquefied forms at smaller sites would likely eliminate the need for an electrical drop.

#### 7.1.4 Tasks Included in the Cost Model

The cost estimate for implementation of GEDIT at the IRCTS-PBA site includes seven tasks:

- Treatability Study
- Gas Permeability Test
- Injection System Design
- Installation
- Operation and Maintenance (O&M)
- Final Report and Demobilization
- Project Management

## 7.2 Cost Analysis

This section provides a cost comparison of each of the scenarios. The cost inputs for this estimate were based on demonstration data, vendor quotes, or professional guidance (e.g., Timberline) or judgment. The costs of nitrogen and hydrogen generators and required accessories are based on quotes from vendors. Construction costs were estimated with Timberline software. Drillers who previously worked at the site were contacted to quote drilling costs. Certified analytical laboratories located in California and Washington provided quotes for analytical costs. The cost breakdown for each scenario is presented in Table 18.

Scenario 1 represents the costs based on conservative demonstration design conditions and the unit cost is \$87/cy. Scenario 2 is based on the same gas composition and ROI as in Scenario 1, but the treatment area is reduced with a focus on mass reduction. The unit cost is reduced to \$68/cy under Scenario 2. Scenario 3 is comparable to Scenario 1 with respect to the treatment goal and area, but is based on a more reasonable design. These changes reduce the unit cost to \$21/cy. Scenario 4 is focused on mass reduction with a reasonable design and the unit cost is \$28/cy. The unit cost for Scenario 4 is greater than for Scenario 3 because the volume of soil is lower and many project costs are fixed.

When comparing each task across the different scenarios, the costs of the treatability study, gas permeability test, engineering design, and project management are similar under different scenarios. The cost of installation and demobilization under Scenario 1 is much greater than that under other scenarios because of higher labor cost for geologist labor, higher drilling cost and higher construction cost. The gas cost under O&M in Scenarios 1 and 2 is much greater than that of Scenarios 3 and 4 because of the high cost of LPG. The cost drivers are analyzed in more detail in Section 7.3.

Table 18 – Project Implementation Costs for GEDIT at IRCTS Site under Different Scenarios

Cost Element	Costs - Scenario 1 Treatment to 60 μg/		Costs - Scenario	0 2	Costs - Scenar	rio 3	Costs - Scenar	rio 4	
	Treatment to 60 µg/	_							
		kg	90 percent Mass Red	duction	Treatment to 60	μg/kg	90 percent Mass R	eduction	
			10 percent H <sub>2</sub> , 10 percent LI	PG, and N <sub>2</sub> , 10-					
	10 percent H <sub>2</sub> , 10 percent LPG, ar	nd N <sub>2</sub> , 10-ft ROI	ft ROI		1 percent H <sub>2</sub> and N <sub>2</sub> ,	15-ft ROI	1 percent H <sub>2</sub> and N <sub>2</sub> ,	, 15-ft ROI	
Task 1 & 2: Treatability Study and Gas Permeability Test	<b>Task 1 &amp; 2 Total =</b>	\$ 158,000	Task 1 & 2 Total =	\$ 160,000	Task 1 & 2 Total =	\$ 160,000	Task 1 & 2 Total =	\$ 160,000	
· Personnel required and associated labor	Sr. Technical, 220 h	\$ 28,000	Sr. Technical, 220 h	\$ 28,000	Sr. Technical, 220 h	\$ 28,000	Sr. Technical, 220 h	\$ 28,000	
· Drilling	Lab Scientist, 530 h	\$ 46,000	Lab Scientist, 530 h	\$ 46,000	Lab Scientist, 530 h	\$ 46,000	Lab Scientist, 530 h	\$ 46,000	
· Analytical laboratory	Administrative, 11 h	\$ 1,000	Administrative, 11 h	\$ 1,000	Administrative, 11 h	\$ 1,000	Administrative, 11 h	\$ 1,000	
· Sample Shipping	Drilling	\$ 47,000	Drilling	\$ 49,000	Drilling	\$ 49,000	Drilling	\$ 49,000	
· Monthly laboratory usage fee	Analytical	\$ 16,000	Analytical	\$ 16,000	Analytical	\$ 16,000	Analytical	\$ 16,000	
· Waste disposal	Miscellaneous costs	\$ 20,000	Miscellaneous costs	\$ 20,000	Miscellaneous costs	\$ 20,000	Miscellaneous costs	\$ 20,000	
· Travel cost to the field									
Task 3: Engineering Design	Task 3 Total =	\$ 67,000	Task 3 Total =	\$ 67,000	Task 3 Total =	\$ 55,000	Task 3 Total =	\$ 55,000	
Personnel required and associated labor	Sr. Technical, 280 h	\$ 36,000	Sr. Technical, 280 h	\$ 36,000	Sr. Technical, 220 h	\$ 28,000	Sr. Technical, 220 h	\$ 28,000	
· Travel cost to the field	Project Engineer, 220 h	\$ 21,000	Project Engineer, 220 h		Project Engineer, 180 h	\$ 17,000	Project Engineer, 180 h	\$ 17,000	
	Administrative, 96 h	\$ 9,000	Administrative, 96 h	\$ 9,000	Administrative, 96 h	\$ 9,000	Administrative, 96 h	\$ 9,000	
	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	
Task 4: Installation	Task 4 Total =	\$ 17,612,000	Task 4 Total =	\$ 9,566,000	Task 4 Total =	\$ 7,422,000	Task 4 Total =	\$ 4,703,000	
Personnel required and associated labor	Sr. Technical, 22000 h	\$ 2,153,000	Sr. Technical, 12000 h	\$ 1,168,000	Sr. Technical, 9600 h	\$ 957,000	Sr. Technical, 5200 h	\$ 517,000	
· Drilling	Project Engineer, 1100 h	\$ 102,000	Project Engineer, 580 h	\$ 55,000	Project Engineer, 480 h	\$ 45,000	Project Engineer, 260 h	\$ 24,000	
· Materials (monitoring equip, H2/N2 Gen, Manifold and Piping)	Administrative, 40 h	\$ 4,000	Administrative, 40 h	\$ 4,000	Administrative, 24 h	\$ 2,000	Administrative, 24 h	\$ 2,000	
· Installation (System, power, water)	Drilling	\$ 10,770,000	Drilling	\$ 5,744,000	Drilling	\$ 4,808,000	Drilling	\$ 2,619,000	
	Construction	\$ 4,238,000	Construction		Construction	\$ 1,447,000	Construction	\$ 1,447,000	
	Miscellaneous costs	\$ 345,000	Miscellaneous costs	\$ 193,000	Miscellaneous costs	\$ 163,000	Miscellaneous costs	\$ 94,000	
Task 5: Operation and Maintenance	Task 5 Total =	\$ 15,740,000	Task 5 Total =	\$ 7,728,000	Task 5 Total =	\$ 2,190,000			
Personnel required and associated labor	Sr. Technical, 3600 h	\$ 369,000	Sr. Technical, 3600 h		Sr. Technical, 3600 h	\$ 369,000	Sr. Technical, 3600 h	\$ 368,000	
· Drilling	Project Engineer, 56 h	\$ 5,000	Project Engineer, 56 h	\$ 5,000	Project Engineer, 56 h	\$ 5,000	Project Engineer, 56 h	\$ 5,000	
· Analytical laboratory	Drilling	\$ 191,000	Drilling	\$ 180,000	Drilling	\$ 184,000	Drilling	\$ 180,000	
· Sample shipping	Analytical	\$ 17,000	Analytical	\$ 16,000	Analytical	\$ 17,000	Analytical	\$ 16,000	
· Gas	Gas	\$ 11,403,000	Gas	\$ 6,067,000	Gas	\$ 711,000	Gas	\$ 466,000	
· Electricity	Electricity	\$ 3,566,000	Electricity	\$ 958,000	Electricity	\$ 845,000	Electricity	\$ 845,000	
· System transfer, maintenance, and demobilization	Construction	\$ 184,000	Construction	\$ 129,000	Construction	\$ 54,000	Construction	\$ 54,000	
Travel cost to the field	Miscellaneous costs	\$ 5,000	Miscellaneous costs	\$ 5,000	Miscellaneous costs	\$ 5,000	Miscellaneous costs	\$ 5,000	
Task 6: Final Report and Demobilization	Task 6 Total =	\$ 8,088,000	Task 6 Total =	\$ 575,000	Task 6 Total =	\$ 491,000		\$ 286,000	
Personnel required and associated labor	Sr. Technical, 210 h	, ,	Sr. Technical, 210 h		Sr. Technical, 210 h	,	Sr. Technical, 210 h	\$ 28,000	
· Drilling	Project Engineer, 180 h		Project Engineer, 180 h		Project Engineer, 180 h		Project Engineer, 180 h	\$ 17,000	
· Electrical demobilization	Administrative, 32 h		Administrative, 32 h		Administrative, 32 h	\$ 2,000	Administrative, 32 h	\$ 2,000	
· Travel cost to the field	Drilling	\$ 8,034,000	Drilling	\$ 521,000	· · · · · · · · · · · · · · · · · · ·	\$ 437,000	Drilling	\$ 232,000	
	Miscellaneous costs	\$ 7,000	Miscellaneous costs		Miscellaneous costs	\$ 7,000	Miscellaneous costs	\$ 7,000	
Task 7: Project Management	Task 7 Total =	\$ 114,000	Task 7 Total =	\$ 85,000	Task 7 Total =	\$ 78,000		\$ 66,000	
Personnel required and associated labor	Project Manager, 710 h	\$ 99,000	Project Manager, 510 h			\$ 66,000	Project Manager, 410 h	\$ 57,000	
•	Administrative, 240 h	\$ 14,000	Administrative, 220 h	\$ 13,000	Administrative, 180 h	\$ 11,000	Administrative, 140 h	\$ 8,000	
	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	Miscellaneous costs	\$ 1,000	
Contingency		\$ 6,221,000		\$ 2,687,000		\$ 1,519,000		\$ 1,045,000	
Total Cost		\$ 48,000,000		\$ 20,868,000		\$ 11,915,000		\$ 8,254,000	
Cost per Cubic Yard		\$ 87		\$ 68		\$ 21		\$ 27	

#### 7.3 Cost Drivers

The total costs of implementing GEDIT are mainly driven by drilling-related costs and gasrelated costs as presented in Table 19. The two major cost drivers together contributed 90 to 97 percent of the total costs. Both of these costs were significant but drilling was dominant in Scenarios 3 and 4. Each of the cost drivers is defined in the sections below.

Table 19 – Percentages of Total Costs Contributed by Major Cost Drivers

Cost Driver	Scenario 1	Scenario 2	Scenario 3	Scenario 4
Drilling	52 percent	44 percent	66 percent	55 percent
Gas	45 percent	48 percent	27 percent	35 percent
Sum	97 percent	93 percent	92 percent	90 percent

### 7.3.1 Sensitivity Analysis for Drilling Costs

The drilling-related costs include the drilling costs charged by the driller and geologists' labor. Both the drilling cost and the geologists' time are mainly dependent on the number of wells required and are therefore essentially dependent on the expected ROI of the injection wells. Taking Scenario 3 as an example, Figure 85 presents how the total costs change when the ROI is varied. By increasing the ROI from 10 ft to 15 ft, the total cost of Scenario 3 is reduced by half. As mentioned in Section 7.1.1, an ROI of 10 ft has been demonstrated at this site and an ROI of 15 ft is more likely. This sensitivity underscores the need for an accurate estimate of site ROI.

ROI is related to several factors including soil lithology and heterogeneity, gas flow rate and composition, well design, and superposition. Superposition is the synergistic effect of multiple injection wells working in concert to minimize effects of oxygen intrusion into the treatment zone. An injection well that is surrounded by other injection wells will be more efficient than a single well because lateral oxygen infiltration is minimized. The demonstration involved use of a single well location with injection at two depths. Installation of multiple wells in a grid pattern will result in greater ROI and/or lesser gas use as a result of superposition. Estimation of how much the ROI will be increased or the gas use will be decreased will require testing and/or modeling. Development of scenarios based on superposition was not conducted, but it is reasonable to conclude that additional cost reductions are possible.

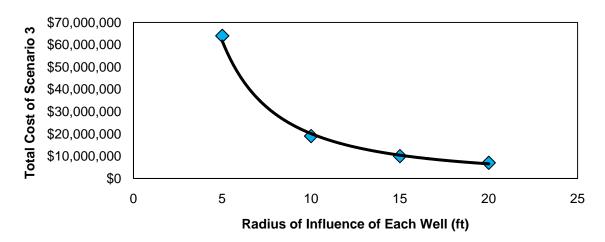


Figure 85 - Sensitivity Analyses for Drilling-Related Costs

### 7.3.2 Sensitivity Analysis for Gas Costs

Gas-related costs include gas generator equipment, purchase of compressed gas, and electricity including power drop and consumption. Gas-related costs are a larger percentage of the total cost in Scenarios 1 and 2 than in Scenarios 3 and 4 (Table 19) primarily because LPG was used in Scenarios 1 and 2 but not in Scenarios 3 and 4 (Table 17). Demonstration results indicated LPG did not play a critical role in promoting perchlorate degradation. Excluding LPG and just using hydrogen significantly reduces the total cost. LPG cost alone was nearly \$11 million for Scenario 1. The concentration of hydrogen also affects the total cost, but not as much. Figure 86 presents how the total cost of Scenario 3 would change as the hydrogen concentration increases. The total cost of Scenario 3 increases by 50 percent as the hydrogen concentration is increased from 1 to 10 percent.

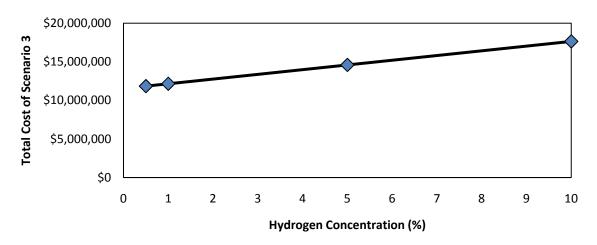


Figure 86 - Sensitivity Analyses for Gas-Related Costs

The majority of the gas expense is for nitrogen. The primary purpose of injecting nitrogen is to keep the vadose zone under anaerobic conditions since perchlorate can only be reduced anaerobically. Oxygen can infiltrate into treatment zone soil from above (e.g., barometric pumping from the atmosphere and/or diffusion), below (e.g., vadose zone soil deeper than the treatment zone or possibly dissolved oxygen in groundwater), and laterally (e.g., diffusion or advection along horizontal lithologic units). One possible way to reduce oxygen infiltration from above is to cover the treatment zone with plastic. Since the contact between the air and the soil has been reduced, it is reasonable to predict that less nitrogen is needed to keep the soil anaerobic. As discussed in Section 7.3.1, well superposition is likely to be most effective with respect to reduction of gas use. Centrally located wells (i.e., surrounded by adjacent wells) will require lower gas flow rates to prevent oxygen infiltration

#### 7.4 Comparison to Alternative Approaches

An alternative approach to *in situ* treatment is excavation of vadose zone soil and ex situ bioremediation. This process includes soil excavation, rock screening and crushing, soil mixing with water and nutrients, storage in treatment cells during biodegradation, soil drying, and backfilling (Evans et al, 2008). Full-scale costs for this process were estimated to be about \$35/ton or \$45/cy. Given the depth of the vadose zone at the site (140 ft bgs), the unit cost would be even higher due to the significant benching and sloping that would be required. Compared with this *ex situ* approach, GEDIT is cost effective under Scenarios 3 and 4. Other alternatives for groundwater protection such as hydraulic containment via pump and treat may also be applicable. Additional evaluations would be necessary to assess whether GEDIT is cost effective in comparison. Nevertheless, well superposition and other refinements are likely to further increase the cost-effectiveness of GEDIT.

#### 8.0 IMPLEMENTATION ISSUES

General engineering guidance for GEDIT implementation has been developed and is presented in Appendix F. This guidance includes guiding principles for design and operation of a GEDIT system. Additional implementation issues are described in this section.

#### 8.1 Regulations and Permits

Federal or state regulations driving site cleanup will drive the need for GEDIT. The primary application for GEDIT is anticipated to be treatment of contaminants such as perchlorate in deep soil for the purpose of groundwater protection. The feasibility study process will include evaluation of GEDIT compared to other alternatives such as pump and treat, liquid flushing, and excavation.

Specific permits for GEDIT will be driven by local codes and will include drilling and well installation permits and hazardous materials storage permits. Other permits may be necessary and will be dependent on local codes.

#### 8.2 End-User Concerns

Flammability is the primary end-user concern associated with GEDIT. As shown in this demonstration, this issue was easily managed and did not necessitate extraordinary efforts. The level of effort was similar to that for a construction site or remediation of a gasoline station site. Specifically the following observations and actions were part of this demonstration:

- Hydrogen was supplied in cylinders much in the same way that acetylene is supplied for welding at construction sites. The number of cylinders was greater than typically used at a construction site but these cylinders are contained in a commercially available rig that stabilizes and manifolds the cylinders.
- LPG was placed in a standard commercially available tank on a portable concrete pad. This effort is no different from a remediation site that uses a propane-fired thermal oxidizer or a construction site that uses LPG.
- Flammable gas/no smoking placards were used at the site. Such placards would be present at any gasoline station remediation site.
- Liquid nitrogen was supplied in a commercially available trailer. From a cold surface hazard perspective, liquid nitrogen is handled the same as liquid oxygen at hospitals and other commercial facilities.
- The Sacramento County Hazardous Materials Department and Aerojet-General Corporation were satisfied with the arrangements for the storage and use of flammable materials on the site. A standard hazardous materials permit was required by the County. Aerojet-General Corporation conducted a New Process Evaluation which is a standard requirement.
- Flammable gases were not detected above the ground surface. Thus, release of flammable gas to the atmosphere was not a safety issue. Nevertheless, monitoring of flammable gases should be conducted just as they would be during a gasoline station remediation project.

#### 8.3 Procurement

Procurement of drilling services will be typical of any environmental remediation project. Procurement of compressed or liquefied gases can be accomplished through a variety of national vendors. Gas generators are specialized pieces of equipment but are available from several manufacturers. Gas manifolds and distribution systems are not off-the-shelf and will require engineering design and custom fabrication.

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## **APPENDICES**

## **Appendix A: Points of Contact**

POINT OF CONTACT Name	ORGANIZATION Name Address	Phone Fax E-mail	Role in Project
Patrick	CDM, 14432 S.E. Eastgate	425 519 8300	Principal
Evans	Way, Suite 100, Bellevue, WA	425 746 0197	Investigator
	98007	evanspj@cdm.com	
Rachel	The Pennsylvania State	814 865 9428	Co-
Brennan	University, Department of	rbrennan@engr.psu.edu	Principal
	Civil and Environmental		Investigator
	Engineering, University Park,		
	PA 16802		
Rodney	Aerojet-General Corp.,	916 355 5161	Site Owner
Fricke	P.O. Box 13222, MS-5519,	916 355 6145	
	Sacramento, CA 95813	rodney.fricke@aerojet.com	
Alexander	California Regional Water	916 464 4625	Site
MacDonald	Quality Control Board, Central	amacdonald@waterboards.ca.gov	Regulator
	Valley Region, 11020 Sun		
	Center Drive, Suite 200,		
	Rancho Cordova, CA 95670		
Andrea	ESTCP Program Office, 901	703 696 2118	ESTCP
Leeson	Stuart Street, Suite 303,	andrea.leeson@osd.mil	Program
	Arlington, VA 22203		Manager
Bryan Harre	NAVFAC ESC, 1100 23 <sup>rd</sup>	805 982 1795	COTR
	Avenue, Port Hueneme, CA	bryan.harre@navy.mil	
	93043		

# **Appendix B: Boring Logs and Well/Piezometer Construction Details**

O PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	DEPTH (ft. bgs)	U.S.C.S.	⊒ C	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900  DECT NUMBER 4000-46738  BORING/WELL NUMBER CDM-INJ1  DATE DRILLED 07/31/06  CASING TYPE/DIAMETER Sch 40 PVC/6-inch  SCREEN TYPE/SLOT 6-inch Sch 40 PVC/20 Slot  GRAVEL PACK TYPE No. 3 Monterey Beach Sand  DUND SURFACE ELEVATION (FT MSL) NA  OF CASING ELEVATION (FT MSL) NA  OF CASING ELEVATION (FT MSL) NA  GROUT TYPE/QUANTITY Bentonite Grout  STATIC WATER LEVEL (FT BELOW TOC) NA  GROUND WATER ELEVATION (FT MSL)  GROUND WATER ELEVATION (FT MSL)  GROUND WATER ELEVATION (FT MSL)								
0.0					U.S	GRAPHIC LOG	LITHO	DLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM					
0.0					- ML		no odor.	4/3); 100% silt, firm, low plasticity; dry,	10.0	Cement Grout (0-6 ft bgs)  Casing (0-10 ft bgs)  Bentonite (6-8 bgs)					
0.0				  - 15- 	CL ML			4/3); 100% silt, firm, low plasticity;	13.0	Screen (10-70 ft bgs)					
0.0					GC		high plasticity; moist  CLAYEY GRAVEL: graded, fine and coa inches, angular to ro	brown (7.5YR 4/3); 60% gravel, well arse grained, maximum diameter of 3 bunded; 30% clay, soft, medium les, maximum diameter of 5 inches,	20.0	Sand (8-70.5 f bgs)					
0.0				-25-   30-			sand, well graded, fi rounded; 30% silt, s graded, fine and coa inches, angular to ro	GRAVEL: brown (7.5YR 4/3); 40% ine to coarse grained, angular to oft, non-plastic; 30% gravel, well arse grained, maximum diameter of 3 bunded; trace cobbles, maximum s, rounded; moist, no odor.	25.0						
0.0							Cobbles from 35 to	38 feet below ground surface.							



 PROJECT NUMBER
 4000-46738
 BORING/WELL NUMBER
 CDM-INJ1

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 07/31/06

	JECTN			-,	- GEDI			Continued from Previous Page			
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WEL	L DIAGRAM
0.0					   45 	SM		SILTY SAND WITH GRAVEL: brown (7.5YR 4/2); 60% sand, well graded, fine to coarse grained, angular to subrounded; 20% silt, soft, non-plastic; 20% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to rounded; trace cobbles, maximum diameter of 5 inches, rounded; moist, no odor.			-Screen (10-70 ft bgs)
0.0					 50  						<b>-</b> Sand (8-70.5 f bgs)
0.0					 55  						
0.0					 60  			SILTY SAND WITH GRAVEL: brown (7.5YR 4/2); 60% sand, well graded, fine to coarse grained, angular to subrounded; 20% silt, soft, non-plastic; 20% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to angular; moist, no odor.			
0.0					65   						
0.0					70- - - -			Total depth of borehole was 70.5 feet below ground surface.	70.5		
					75 - - -						
					80 -						
					- 85 -						PAGE 2 OF

CDI	M	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900
PROJECT NUMBER	<u>5611</u>	1-6169.001.TK5.MOBIL
PROJECT NAME	Aerojet	- GEDIT
LOCATION Rand	ho Cord	ova CA

Sonic

SAMPLING METHOD Continuous Core

GROUND SURFACE ELEVATION (FT MSL) NA

TOP OF CASING ELEVATION (FT MSL) NA

DRILLING METHOD

## **BORING/WELL CONSTRUCTION LOG**

BORING/WELL NUMBER CDM-INJ2
DATE DRILLED 10/26/07
CASING TYPE/DIAMETER Sch 40 PVC/4-inch
SCREEN TYPE/SLOT 4-inch Sch 40 PVC/20 Slot
GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUT TYPE/QUANTITY Portland Type I/II Cement
STATIC WATER LEVEL (FT BELOW TOC) NA
GROUND WATER ELEVATION (ET MSL)

LOGGED BY T.Titus **REMARKS** RECOVERY (inches) PID (ppm) BLOW GRAPHIC LOG CONTACT DEPTH EXTENT U.S.C.S. DEPTH (ft. bgs) SAMPLE LITHOLOGIC DESCRIPTION WELL DIAGRAM SILT: brown (10YR 4/3); 100% silt, soft, low plasticity; dry, Cement Grout (0-5 ft bgs) ML Casing (0-10 ft bgs) 0.0 100 6.0 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, low plasticity; moist, no odor. Bentonite (5-8 ft bgs) CL 10.0 0.0 100 SILT: brown (10YR 4/3); 100% silt, soft, low plasticity; dry, no odor. ML 15.0 Screen (10-50 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, 0.0 100 ft bgs) CL moderate plasticity; moist, no odor. 17.0 CLAY: dark yellowish brown (10YR 3/4); 100% clay, firm, moderate plasticity; moist, no odor. CL Sand (8-50 ft 20 0.0 100 bgs) 23.0 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, moderate plasticity; moist, no odor. CL 25.0 25 100 CLAY: dark yellowish brown (10YR 3/4); 100% clay, firm, 0.0 moderate plasticity; moist, no odor. CL 29.0 SILTY SAND WITH GRAVEL: brown (7.5YR 4/3); 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, non-plastic; 30% gravel, well graded, SM 100 0.0 31.0 fine and coarse grained, maximum diameter of 2 inches, angular to rounded; moist, no odor. CLAYEY GRAVEL WITH SAND: dark yellowish brown (10YR 4/4); 45% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to rounded; 30% clay, soft, low plasticity; 20% sand, well Continued Next Page PAGE 1 OF 2



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

## **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-INJ2

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/26/07

PROJECT NAME	_ Aerojet - GEDIT	DATE DRILLED	
		Continued from Previous Page	
PID (ppm) BLOW COUNTS RECOVERY (inches)	SAMPLE ID.  EXTENT DEPTH (ft. bgs) U.S.C.S. GRAPHIC LOG	LITHOLOGIC DESCRIPTION	WELL DIAGRAM  WELL DIAGRAM
0.0 100	GC	graded, fine to coarse grained, angular to rounded; 5% cobbles, maximum diameter of 6 inches, rounded to subangular; moist, no odor.	Screen (10-50 ft bgs)
0.0 100	SP- - SM	SAND WITH SILT AND GRAVEL: brown (10YR 4/3); 50% sand, poorly graded, fine to coarse grained, mostly fine grained, subangular to subrounded; 35% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to rounded; 10% silt, soft, non-plastic, 5% cobbles, maximum diameter of 4 inches, subangular to rounded; moist, no odor.	Sand (8-50 ft bgs)
0.0	55 - 55 - 60 - - 65 - - 70 -	Total depth of borehole was 50 feet below ground surface.	

0.0 100 100 100 100 100 100 100 100 100	PROD PROD LOCA DRILL SAM GRO TOP	JECT NO JECT NA ATION LING MI PLING N UND SU OF CAS	NUMBER 56111-6169.001.TK5.MOBIL  NAME Aerojet - GEDIT  Rancho Cordova, CA  METHOD Sonic  METHOD Continuous Core  SURFACE ELEVATION (FT MSL) NA  SING ELEVATION (FT MSL) NA  Y T.Titus  COM-INJ3  BORING/WELL NUMBER CDM-INJ3  BORING/WELL NUMBER CDM-INJ3  CASING TYPE/DIAMETER Sch 40 PVC/4-inch Sch 40 PVC/4-inch SCREEN TYPE/SLOT 4-inch Sch 40 PVC/20 SCREEN TYPE/SLOT 4-inch Sch 40 PVC/4-inch SCH 40 PVC/4-i								Sacramento, CA 95833 (916) 567-9900  BECT NUMBER 56111-6169.001.TK5.MOBIL BORING/WELL NUMBER CDM-INJ3  BECT NAME Aerojet - GEDIT DATE DRILLED 10/17/08  CASING TYPE/DIAMETER Sch 40 PVC/4-inch SCREEN TYPE/SLOT 4-inch Sch 40 PVC/20 Slot PLING METHOD Continuous Core GRAVEL PACK TYPE No. 3 Monterey Beach Sand GROUT TYPE/QUANTITY Portland Type I/II Cement OF CASING ELEVATION (FT MSL) NA  GED BY T.Titus GROUND WATER ELEVATION (FT MSL)  ARKS							
0.0 100 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, high plasticity; moist, no odor.  CLAYEY GRAVEL: brown (7.5YR 4/3); 60% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; 30% clay, soft, moderate plasticity; 10% cobbles, maximum diameter of 6 inches, subrounded to rounded; moist, no odor.  0.0 100 -15- GC  Screen (10-5 ft bgs)  **Bentonite (5-bgs)  Screen (10-5 ft bgs)  **Sand (8-50 ft bgs)	PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHC	DLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM						
SILTY SAND WITH GRAVEL: brown (7.5YR 4/3); 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, soft, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor.  SM  SAND: pale brown (10YR 6/3); 100% sand, poorly graded, fine grained; dry, no odor.  32.0  SAND: pale brown (10YR 6/3); 100% sand, poorly graded, fine grained; dry, no odor.  34.0	0.0		100				CL		CLAY: dark yellowish high plasticity; moist, graded, fine and coa inches, angular to ro plasticity: 10% cobbl.	n brown (10YR 3/4); 100% clay, soft, no odor.  brown (7.5YR 4/3); 60% gravel, well rse grained, maximum diameter of 3 unded; 30% clay, soft, moderate es, maximum diameter of 6 inches,	8.0	Casing (0-10 fbgs)  -Bentonite (5-8bgs)  -Screen (10-50ftbgs)						
の」	INT_SAC_AEROJET_120908.GPJ NEWGINT.GDT_11/13/C 0.00000000000000000000000000000000000					  	SP		sand, well graded, fir rounded; 30% silt, so graded, fine and coa inches, angular to ro diameter of 6 inches,  SAND: pale brown (fine grained; dry, no	ne to coarse grained, angular to oft, non-plastic; 30% gravel, well rse grained, maximum diameter of 3 unded; trace cobbles, maximum rounded; moist, no odor.	32.0							
Service State of Stat	×   					-35-	GC			•	_35.0							



**PROJECT NUMBER** 56111-6169.001.TK5.MOBIL

PROJECT NAME Aerojet - GEDIT

BORING/WELL NUMBER CDM-INJ3

\_\_\_\_\_ DATE DRILLED \_\_\_\_\_\_\_10/17/08

									Continued from Previous Page
	PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION  CONTACT CONTACT CONTACT WELL DIAGRAM
•	0.0		100			  	ML		(10YR 4/4); 50% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to rounded; 30% clay, soft, low plasticity; 20% sand, poorly graded, medium to coarse grained, mostly coarse, angular to subrounded; trace cobbles, maximum diameter of 6 inches, subrounded to rounded; moist, no odor.  SANDY SILT WITH GRAVEL: brown (10YR 4/3); 50% silt, soft, non-plastic; 30% sand, poorly graded, fine to coarse
	0.0		70			  	SP		grainled, mostly line grainled, angular to subangular, 20% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subrounded to subangular; trace cobbles, subrounded to subangular, maximum diameter of 6 inches; moist, no odor.  SAND WITH GRAVEL: brown (10YR 4/3); 60% sand, poorly graded, fine to coarse grained, mostly coarse, subrounded to angular; 40% gravel, well graded, fine and
	0.0		70			45   	SW		coarse grained, maximum diameter of 3 inches, subrounded to angular; moist, no odor.  SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 60% sand, well graded, fine to coarse grained, angular to subrounded; 40% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subrounded to subangular; trace cobbles, maximum diameter of 5 inches, subrounded to subangular; moist, no odor.
	0.0		100			50 - - - -		0.0.0.0	Total depth of borehole was 50 feet below ground surface.
						55 - - - -			
/13/09						60 - - -			
GPJ NEWGINT.GDT 11						65 - - -			
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09						70 - - -			
NEWGINT_						- 75 -			

#### 2295 Gateway Oaks Suite 240 Sacramento, CA 95833 BORING/WELL CONSTRUCTION LOG (916) 567-9900 PROJECT NUMBER 4000-46738 BORING/WELL NUMBER CDM-P1 PROJECT NAME Aerojet - GEDIT DATE DRILLED 07/27/06 CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID LOCATION Rancho Cordova, CA **DRILLING METHOD** Sonic SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe SAMPLING METHOD Continuous Core **GRAVEL PACK TYPE** No. 3 Monterey Beach Sand GROUND SURFACE ELEVATION (FT MSL) NA GROUT TYPE/QUANTITY Bentonite Grout STATIC WATER LEVEL (FT BELOW TOC) NA TOP OF CASING ELEVATION (FT MSL) NA LOGGED BY T.Titus GROUND WATER ELEVATION (FT MSL) REMARKS RECOVERY (inches) BLOW GRAPHIC LOG CONTACT DEPTH PID (ppm) EXTENT U.S.C.S. DEPTH (ft. bgs) SAMPLE LITHOLOGIC DESCRIPTION WELL DIAGRAM SILT: yellowish brown (10YR 5/4); 100% silt, soft, non-plastic; dry; no odor. ML Cement Grout 0.0 6.0 (0-16 ft bgs) GRAVELLY SILT: yellowish brown (10YR 5/4); 60% silt, soft, non-plastic; 40% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subround to rounded; dry, no odor. ML Poly Tubing 0.0 (0-18, 0-33, 0-48, and 0-68 ft bgs) 13.0 GRAVELLY SILT WITH SAND: brown (7.5YR 4/3); 50% silt, soft, non-plastic; 35% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, 0.0 subangular to rounded; 15% sand, poorly graded, medium to coarse grained, subrounded; moist, no odor. Bentonite

(16-17 ft bgs) Sand (17-19.5 ML ft bgs) Vapor Probe (18-18.5 ft bgs) 20 0.0 23.0 CLAYEY GRAVEL WITH SAND: dark yellowish brown (10YR 4/4); 45% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to 0.0 rounded; 35% clay, soft, low plasticity; 20% sand, poorly -Bentonite graded, coarse grained, subrounded to rounded; moist, no NEWGINT SAC AEROJET 120908.GPJ NEWGINT.GDT 11/13/09 (19.5-32 ft bgs) Sand (32-34.5 ft bgs) Vapor Probe 34 0 (33-33.5 ft bgs) SAND: pale brown (10YR 6/3): 100% sand, poorly graded. 35.0 fine grained; dry, no odor. 0.0 CLAYEY GRAVEL WITH SAND: dark yellowish brown (10YR 4/4); 45% gravel, well graded, fine and coarse Bentonite grained, maximum diameter of 3 inches, subangular to (34.5-47 ft bgs) rounded; 35% clay, soft, low plasticity; 20% sand, poorly graded, coarse grained, subrounded to rounded; moist, no Continued Next Page PAGE 1 OF 2



 PROJECT NUMBER
 4000-46738
 BORING/WELL NUMBER
 CDM-P1

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 07/27/06

								Continued from Previous Page						
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM				
0.0					  - 45 	GC		SILTY SAND: dark yellowish brown (10YR 4/4); 70% sand, poorly graded, fine to medium grained, subrounded to subangular; 30% silt, firm, non-plastic; moist, no odor.	_45.0	Poly Tubing (0-18, 0-33, 0-48, and 0-6 ft bgs)  Sand (47-49 ft bgs) Vapor Probe (48-48.5 ft bg				
					50   55 	SM		SILTY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse grained, subangular to subrounded; 30% silt, firm, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; moist, no odor.	_52.0	◆ Bentonite				
						sc		CLAYEY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse grained, subangular to subrounded; 30% clay, firm, low plasticity; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; moist, no odor.  SILTY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse grained,	62.0 65.0	(49.6-67 ft bo				
					70 	SM		subangular to subrounded; 30% silt, firm, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; moist, no odor.  Total depth of borehole was 72 feet below ground surface.	72.0	Wapor Probe (68-68.5 ft b				
					80 -									

CD	M	2295 Gateway Oaks Suite 240 Sacramento, CA 9583 (916) 567-9900
<b>U</b>		Sacramento, CA 9583 (916) 567-9900

BORING/WELL NUMBER CDM-P2
DATE DRILLED 10/25/07
CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUT TYPE/QUANTITY Portland Type I/II Cement
STATIC WATER LEVEL (FT BELOW TOC) NA
GROUND WATER ELEVATION (FT MSL)
,

REM	ARKS									
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.3		100				CL		CLAY: moderate brown (5YR 4/4); 100% sandy clay, moderate to high plasticity, trace very fine grained quartz; dry, no odor.		Cement Grout (0-14 ft bgs)
0.0		100			10   	CL		GRAVELLY CLAY: moderate brown (5YR 4/4); 60% sandy clay, moderate to high plasticity, trace very fine grained quartz; 40% gravel, subrounded to subangular, maximum diameter 3 inches; dry, no odor.	10.0	Poly Tubing (0-18, 0-28, 0-38, and 0-48 ft bgs)
0.0		100			15  	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, subrounded, maximum diameter of 3 inches; 40% silty sand, fine grained, moderately poorly graded, subrounded; dry, no odor.	15.0	(14-17 ft bgs)  Sand (17-19.5 ft bgs)  Vapor Probe (18-18.5 ft bgs)  Bentonite
0.2		100			20   	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 75% gravel, maximum diameter 2 inches, rounded to subrounded; 25% clayey sand to sand, fine grained; dry, no odor.	25.0	(19.5-27 ft bgs)
0.0		75			25   	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 50% gravel, maximum diameter 2 inches, rounded to subrounded; 50% clayey sand to sand, fine grained; dry, no odor.	30.0	Sand (27-29.5 ft bgs)  Vapor Probe (28-28.5 ft bgs)
0.0		75			30   	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, maximum diameter 2 inches, rounded to subrounded; 40% silty sand, fine grained, rounded to subrounded; dry, no odor.	35.0	(29.5-37 ft bgs)
					<del></del> 35		101 /	Continued Next Page		PAGE 1 OF 2



 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-P2

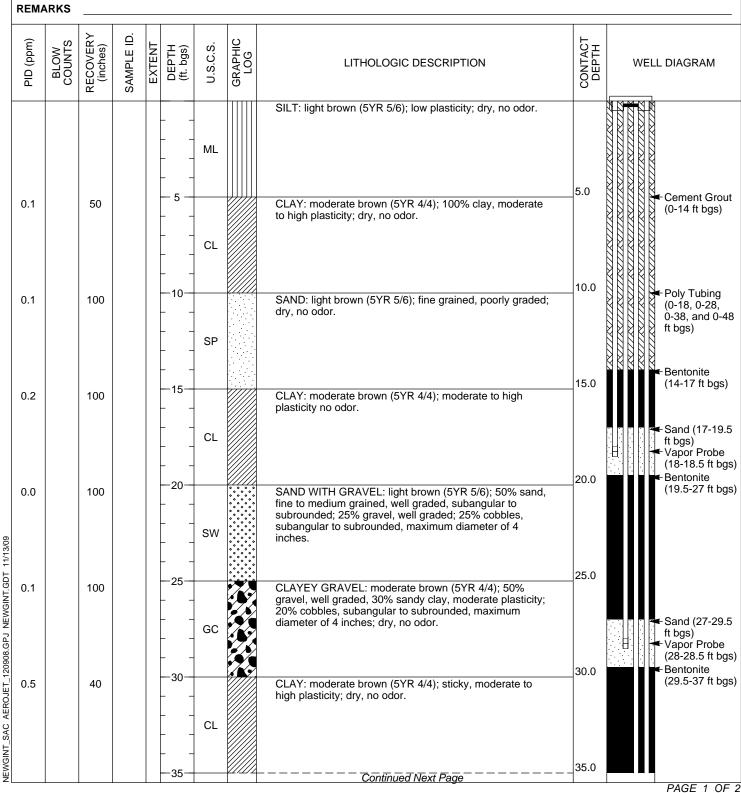
 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/25/07

PROJEC	TNAME	Aer	ojet	- GED	IT		DATE DRILLED10/25/07		
							Continued from Previous Page		1
PID (ppm) BLOW	COUNTS RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.2	100			  	SP		SAND WITH GRAVEL: moderate brown (5YR 4/4); 70% clayey sand, fine grained, rounded to subrounded, low plasticity; 30% gravel, subrounded to subangular, maximum diameter 1.5 inches.	40.0	Sand (37-39.5 ft bgs)  Vapor Probe (38-38.5 ft bgs)
0.0	100			40   			GRAVELLY CLAY: moderate brown (5YR 4/4); 50% sandy clay, low plasticity; 50% gravel and cobbles, maximum diameter 4 inches, subangular to angular; dry, no odor.	10.0	(39.5-47 ft bgs -Poly Tubing (0-18, 0-28, 0-38, and 0-48 ft bgs)
0.0	100			45   	CL				Sand (47-52 ft bgs) 
0.0	100			50 - - -			Drill cuttings not collected between 50 and 52 feet below ground surface. Lithology assumed to be same as 40 to 50 feet below ground surface.  Total depth of borehole was 52 feet below ground surface.	52.0	
				55 - - -					
				60 -					
				-65 - - -					
				70 - - -					
				- 75 -					PAGE 2 OF

#### 2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900

### **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-P3
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/23/07
OCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD _ Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
OGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	, , ,





NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

## **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-P3

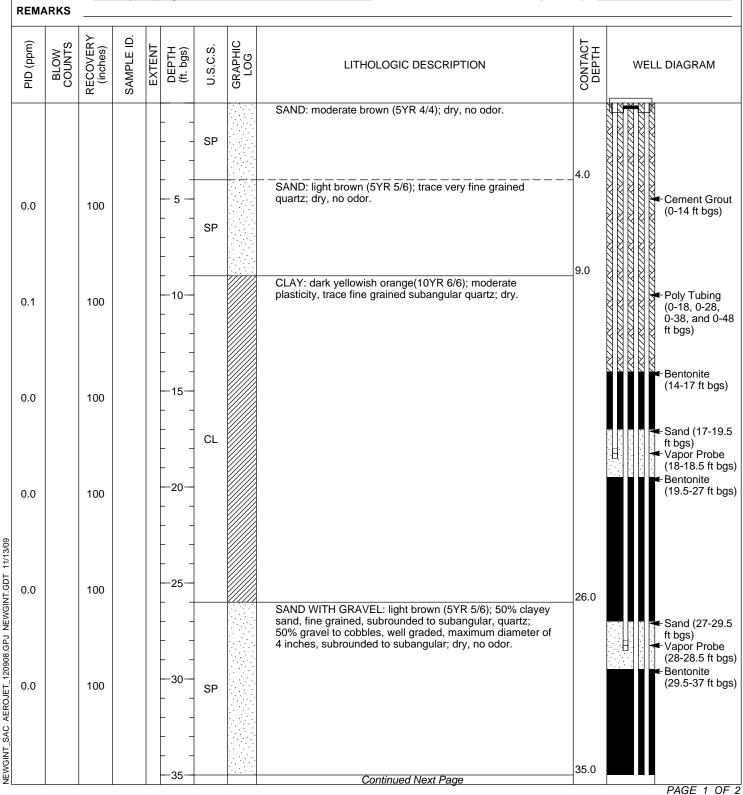
 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/23/07

PROJ	ECT N	AWE	Ae	rojet	: - GED	11		DATE DRILLED10/23/07		
								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
0.2		100				CL		CLAY: moderate brown (5YR 4/4); sticky, low to moderate plasticity; dry, no odor.	40.0	
0.0		50			40   	CL		GRVELLY CLAY: moderate brown (5YR 4/4); 60% sandy clay, low to moderate plasticity, quartz; 40% gravel, well graded, subangular to subrounded, maximum diameter of 2 inches; dry, no odor.	45.0	(39.5-47 ft bgs) <b>◄</b> -Poly Tubing (0-18, 0-28, 0-38, and 0-48 ft bgs)
0.6		50			45  	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, well graded, subangular to angular, maximum diameter of 3 inches; 40% silty sand, fine grained, moderately poorly graded, quartz, subrounded to subangular.		Sand (47-52 ft bgs) Vapor Probe (48-48.5 ft bgs)
1.2		50			50 - - - -			Drill cuttings not collected between 50 and 52 feet below ground surface. Lithology assumed to be same as 40 to 50 feet below ground surface.  Total depth of borehole was 52 feet below ground surface.	_52.0	
					55 - - - -					
					60 -					
					65 -					
					70 -					
					75 -					PACE 2 OF 2

#### 2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900

## **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER <u>56111-6169.001.TK5.MOBIL</u>	BORING/WELL NUMBER CDM-P4
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/29/07
OCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	





 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-P4

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/29/07

	JECT N			iojoi	: - GED			Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.0		70			  	CL		CLAY: moderate brown (5YR 4/4); soft, low to moderate plasticity; dry, no odor.		Sand (37-39) ft bgs) Vapor Probe (38-38.5 ft bg Bentonite (39.5-47 ft bg
0.4		70			   45-	CL		CLAY WITH GRAVEL: moderate brown (5YR 4/4); 80% sandy clay, moderate plasticity; 20% gravel, subangular to angular, maximum diameter of 3 inches; dry, no odor.	41.0	<ul> <li>← Poly Tubing (0-18, 0-28, 0-38, and 0-4 ft bgs)</li> </ul>
0.0		70			   50-	SW		SAND WITH GRAVEL: pale yellowish brown (10YR 6/2); 60% sand, fine to medium grained, well graded, subangular, abundant quartz; 40% gravel, well graded, subrounded to subangular, maximum diameter of 3 inches.  Drill cuttings not collected between 50 and 51.5 feet below ground surface. Lithology assumed to be same as 46 to	46.0	Sand (47-51 ft bgs) ■ Vapor Probe (48-48.5 ft b
					- - - 55 -			50 feet below ground surface.  Total depth of borehole was 51.5 feet below ground surface.	51.5	
					  60 					
					- 65 - - -					
					70 - 					
					- 75 -					PAGE 2 0

#### 2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900 PROJECT NUMBER <u>56111-6169.001.TK5.MOBIL</u> PROJECT NAME Aerojet - GEDIT LOCATION Rancho Cordova, CA

DRILLING METHOD Sonic

#### **BORING/WELL CONSTRUCTION LOG**

BORING/WELL NUMBER CDM-P5 DATE DRILLED 10/24/07 CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe GRAVEL PACK TYPE No. 3 Monterey Beach Sand SAMPLING METHOD Continuous Core GROUND SURFACE ELEVATION (FT MSL) NA GROUT TYPE/QUANTITY Portland Type I/II Cement TOP OF CASING ELEVATION (FT MSL) NA STATIC WATER LEVEL (FT BELOW TOC) NA

PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL D	IAGRAM
					  	CL		CLAY: moderate brown (5YR 3/4); silty, low to moderate plasticity; dry, no odor.	5.0		
0.0		100			- 5 -  			CLAY: moderate brown (5YR 4/4); moderate to high plasticity, trace fine grained quartz; dry, no odor.	0.0	CO	ement Gro -14 ft bgs)
0.0		100			10  					(0 O- ft	oly Tubing -18, 0-28, 38, and 0- bgs)
0.0		100			 15  	CL				(1 Ft. ∀Vá	entonite 4-17 ft bgs and (17-19 bgs) apor Probe
0.0		30			 20  					Be Be	8-18.5 ft t entonite 9.5-27 ft t
0.1		30			 25 	Cl		CLAY: moderate brown (5YR 4/4); moderate to high plasticity, firm; dry, no odor.	25.0	ENRRE	and (27-29
0.2	60			  -30	CL		SAND WITH GRAVEL: dark yellowish brown (10YR 2/2); 50% silty sand, fine to medium grained, well graded,	30.0	☐	bgs) apor Probe 8-28.5 ft b entonite 9.5-37 ft b	
					  	SW		subrounded to subangular; 50% gravel, subrounded to subangular, maximum diameter of 3 inches; dry, no odor.			
					-35-		******	Continued Next Page	35.0		

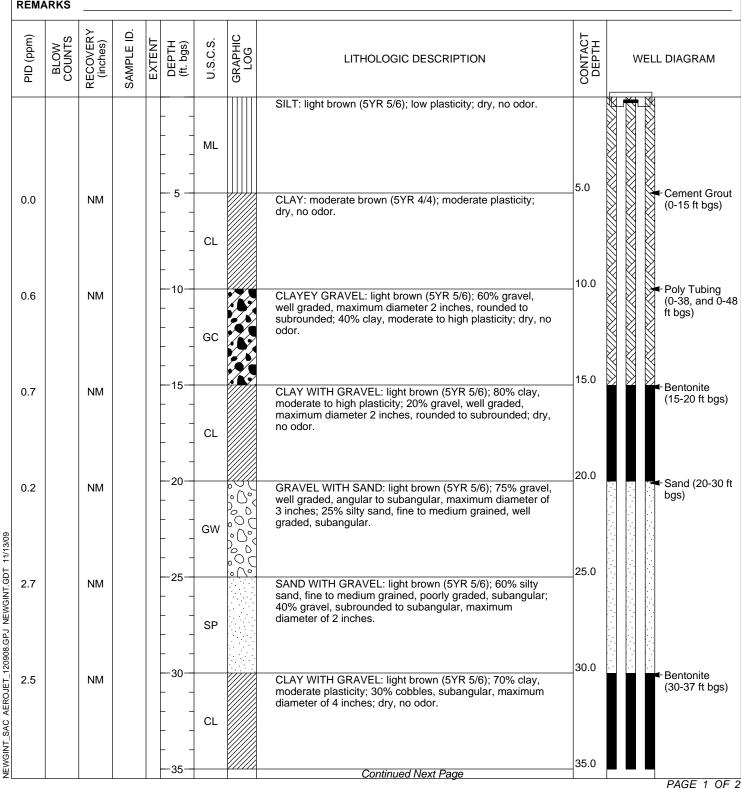


 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-P5

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/24/07

PRUJ	JECT N	AIVIE	Ae	rojet	- GED	"11		Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.2		60			  	CL		CLAY: moderate brown (5YR 4/4); moderate to high plasticity, firm; dry, no odor.	40.0	Sand (37-39. ft bgs)  Vapor Probe (38-38.5 ft bg
0.0		100			  	SC		CLAYEY SAND: moderate brown (5YR 4/4); 100% clayey sand, low plasticity; dry, no odor.	45.0	(39.5-46 ft bg
0.0		100			45   	SP		SAND WITH GRAVEL: moderate brown (5YR 4/4); 60% silty sand, moderately poorly graded, fine grained, subangular; 40% cobbles, subangular to subrounded, maximum diameter of 4 inches; dry, no odor.		Sand (46-51) ft bgs)  Vapor Probe (48-48.5 ft bg
0.0		100			50 - - -	-		Drill cuttings not collected between 50 and 51.5 feet below ground surface. Lithology assumed to be same as 45 to 50 feet below ground surface.  Total depth of borehole was 51.5 feet below ground surface.	51.5	
					55 - - - -					
					60 - - -					
					- 65 - - -					
					70 - -					
					- - 75 -					PAGE 2 O.

PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-P6
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/22/07
OCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	, ,





 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-P6

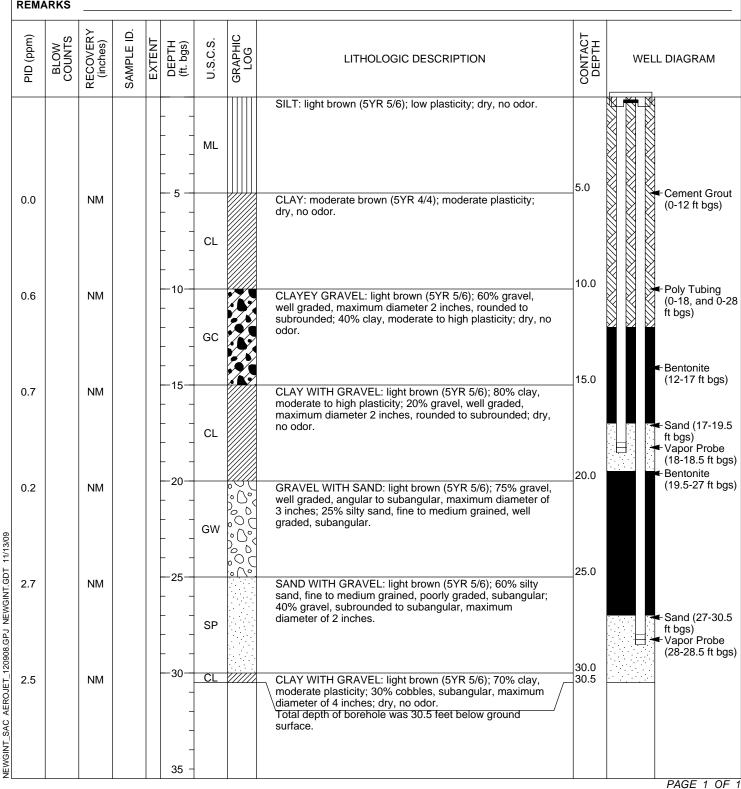
 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/22/07

PROJEC	CT NAME	_	Aeroj	et - GED	DIT		DATE DRILLED10/22/07		
							Continued from Previous Page		
PID (ppm)	COUNTS COUNTS RECOVERY	(callolles)	SAMPLE ID.	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.2	NM				GM		SILTY GRAVEL: moderate brown (5YR 4/4); 50% gravel, subrounded to subangular, maximum diameter of 3 inches; 50% silt, low to moderate plasticity.	40.0	Sand (37-39 f bgs) Vapor Probe (38-38.5 ft bgs) Bentonite
0.0	NM	1		40  	sw		SAND WITH GRAVEL: moderate brown (5YR 4/4); 70% silty sand, fine grained, well graded, subangular to subrounded; 30% gravel, well graded, subangular, maximum diameter of 3 inches.	45.0	(39-46.5 ft bgs <b>◄</b> -Poly Tubing (0-38, and 0-4 ft bgs)
0.2	NM	1		45 - · - ·	sw		SAND: moderate brown (5YR 4/4); 90% silty sand, fine to coarse, well graded, rounded to angular, quartz; 10% gravel, subrounded to subangular, maximum diameter of 1 inch.		Sand (46.5-50 ft bgs)  Vapor Probe (48-48.5 ft bgs
0.0	NM	1		-50-	-		Total depth of borehole was 50 feet below ground surface.	50.0	
				55 -	-				
				60	-				
				65	-				
				70	-				
				75					PAGE 2 OF

#### 2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900

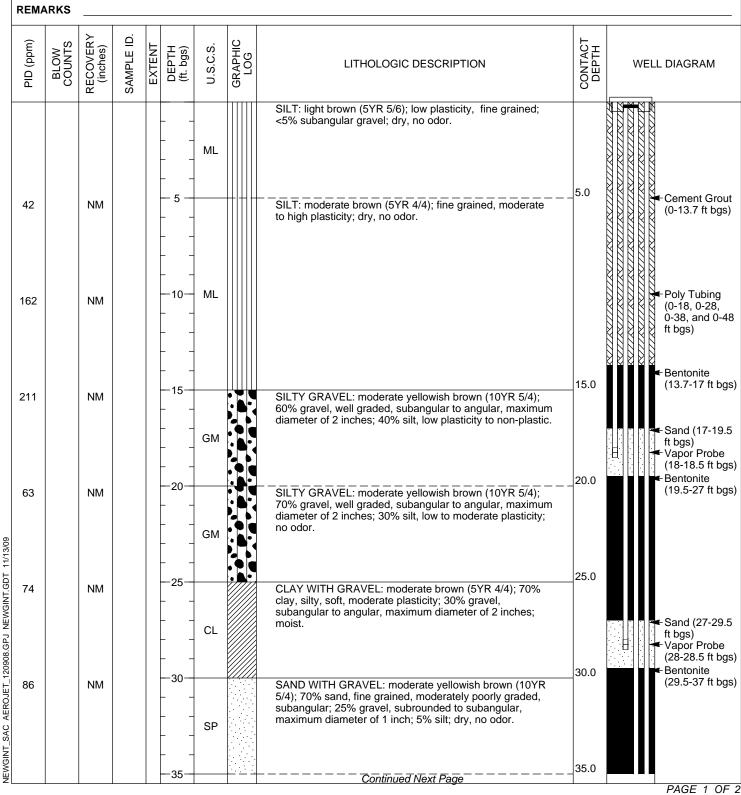
#### **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-P6A
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/24/07
OCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD _ Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
OGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	, ,



CDM	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900
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PROJECT NUMBER _56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER _ CDM-P7
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/16/07
LOCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	





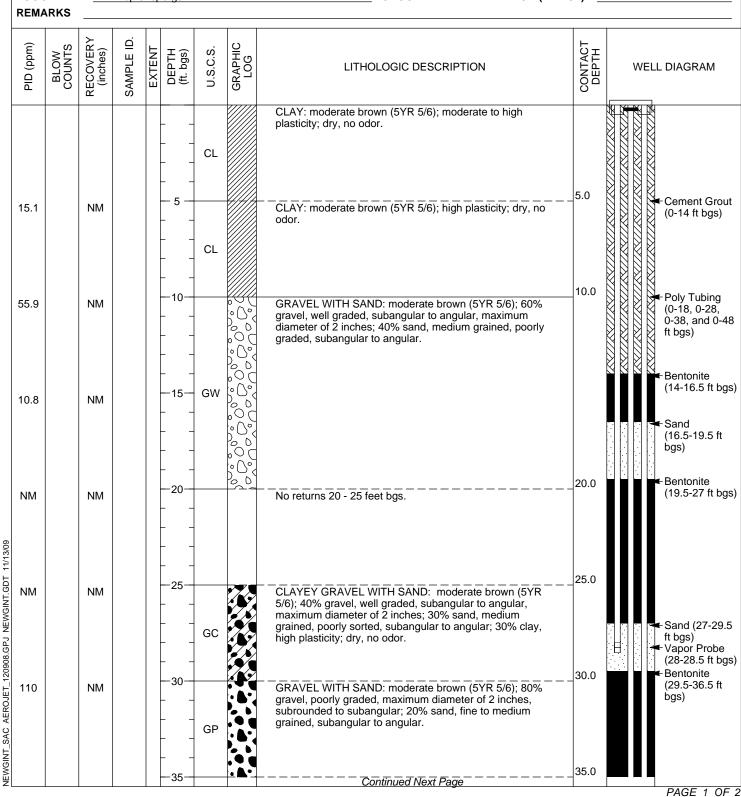
 PROJECT NUMBER
 \_56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 \_CDM-P7

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 10/16/07

PROJECT NAME	Aeı	rojet	t - GED	<u>IT                                    </u>		<b>DATE DRILLED</b> 10/16/07		
						Continued from Previous Page		
PID (ppm) BLOW COUNTS RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
68 NM			 	SP		SAND WITH GRAVEL: moderate yellowish brown (10YR 5/4); 70% sand, fine grained, moderately poorly graded, subangular; 20% gravel, subrounded to subangular, maximum diameter of 1 inch; 10% silt; dry, no odor.	40.0	Sand (37-39. ft bgs)  Vapor Probe (38-38.5 ft bg
28 NM			40  			40 - 50 feet bgs no returns; well drilled to 50 feet bgs; potential void from 50 - 62 feet bgs (void filled using #3 sand filter).		(39.5-47 ft bg  Poly Tubing (0-18, 0-28, 0-38, and 0-4 ft bgs)
NM NM			45   					Sand (47-62 bgs)  Vapor Probe (48-48.5 ft bg
NM NM			50 - - -					
			55 -					
			60 -			Total depth of borehole was 62 feet below ground surface.	62.0	
			65 - - -					
			70 -					
			- - - 75 -					

<b>CDM</b>	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900
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PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-P8
PROJECT NAME Aerojet - GEDIT	<b>DATE DRILLED</b> 10/11/07-10/12/07
OCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	, ,





 PROJECT NUMBER
 \_56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 \_CDM-P8

 PROJECT NAME
 \_Aerojet - GEDIT
 DATE DRILLED
 \_10/11/07-10/12/07

PROJE	ECT N	AIVIE	Ae	rojei	t - GED	111		DATE DRILLED10/11/07-10/12/0	/	
								Continued from Previous Page		T
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
14.2		NM			 	GP- GC		GRAVEL WITH CLAY: moderate brown (5YR 5/6); 85% gravel, subangular, maximum diameter of 2 inches; 15% clay, soft, low to moderate plasticity; slightly moist.	40.0	Sand (36.5-3) ft bgs) Vapor Probe (37.5-38 ft bg Bentonite (39-47 ft bgs)
217		NM			40   	SP- SC		SAND WITH CLAY: moderate brown (5YR 5/6); 90% sand, medium to coarse grained, subangular, moderately poorly graded; 10% clay, soft, low to moderate plasticity; slightly moist.		<ul><li>← Poly Tubing (0-18, 0-28, 0-38, and 0-4 ft bgs)</li></ul>
180		NM			45  	GW		GRAVEL WITH SAND: dark yellowish brown (10YR 4/2); 50% gravel, poorly graded, angular, maximum diameter of 2 inches, abundant chert; 50% sand, coarse grained, moderately poorly graded, subrounded to subangular.	45.0	Sand (47-50   bgs)  ∃ Vapor Probe (48-48.5 ft bg
184		NM			50 - - -			Total depth of borehole was 50 feet below ground surface.	50.0	
					55 - - - -					
					60 -					
					65 - -					
					70 -					
					- - 75 -	-				PAGE 2 OF

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#### **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-P8A
PROJECT NAME Aerojet - GEDIT	DATE DRILLED 10/15/07
LOCATION Rancho Cordova, CA	CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID
DRILLING METHOD Sonic	SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE No. 3 Monterey Beach Sand
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Portland Type I/II Cement
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)
REMARKS	, ,

L R RECOVERY (inches) SAMPLE ID. PID (ppm) BLOW GRAPHIC LOG CONTACT DEPTH EXTENT U.S.C.S. DEPTH (ft. bgs) LITHOLOGIC DESCRIPTION WELL DIAGRAM CLAY: moderate brown (5YR 5/6); moderate to high plasticity; dry, no odor. CL 5.0 Cement Grout CLAY: moderate brown (5YR 5/6); high plasticity; dry, no 15.1 NM (0-14 ft bgs) CL 10.0 Poly Tubing GRAVEL WITH SAND: moderate brown (5YR 5/6); 60% gravel, well graded, subangular to angular, maximum diameter of 2 inches; 40% sand, medium grained, poorly NM 55.9 (0-18 ft bgs) graded, subangular to angular. Bentonite (14-17 ft bgs) GW 10.8 NM Sand (17-20.5 ft bgs) Vapor Probe (18-18.5 ft bgs) 6 0<u>,</u> 20.0 20 NM NM 20.5 Total depth of borehole was 20.5 feet below ground surface. NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 25 30 35

CDI	V	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900
PROJECT NUMBER	56111	I-6169.001.TK5.MOBIL

PROJECT NUMBER 56111-6169.001.TK5.MOBIL	BORING/WELL NUMBER CDM-CB-1				
PROJECT NAME Aerojet - GEDIT	<b>DATE DRILLED</b> 04/18/08				
LOCATION Rancho Cordova, CA	CASING TYPE/DIAMETER NA				
DRILLING METHOD Sonic	SCREEN TYPE/SLOT NA				
SAMPLING METHOD Continuous Core	GRAVEL PACK TYPE NA				
GROUND SURFACE ELEVATION (FT MSL) NA	GROUT TYPE/QUANTITY Bentonite Grout				
TOP OF CASING ELEVATION (FT MSL) NA	STATIC WATER LEVEL (FT BELOW TOC) NA				
LOGGED BY K. Hopfensperger	GROUND WATER ELEVATION (FT MSL)				
REMARKS	, ,				

		≿		1.		_			  -	
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
1.5		100			  - 5 	CL		CLAY: light brown (5YR 5/6); 100% clay, silty, moderate plasticity; dry, no odor.		No well constructed. Borehole abandoned v bentonite gro
2.2		100			 - 10 			CLAY: moderate brown (5YR 4/4); 100% clay, silty, soft,	12.0	
4.2		100			  15 	CL		low plasticity; dry, no odor.		
1.4		100			 20	GC		CLAYEY GRAVEL: moderate brown (5YR 4/4); 60% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches; 40% clay, silty, soft, low plasticity; dry, no odor.	18.0	
					 	ML		SILT: moderate brown (5YR 4/4); 100% silt, low to moderate plasticity; dry, no odor.	23.0	
1.5		100			 25  	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 50% gravel, well graded, fine to coarse grained, maximum diameter of 4 inches, subrounded to subangular; 50% sand, well graded, fine to medium grained, subangular to angular.		
2.2		100			30 	CL	000	CLAY: moderate brown (5YR 4/4); 100% clay, silty, soft, low plasticity; dry, no odor.	30.0	
					 			GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, well graded, fine to coarse grained, maximum diameter of 4 inches, subrounded to subangular; 40% Continued Next Page	33.0	



CDM-CB-1

PROJECT NUMBER 56111-6169.001.TK5.MOBIL BORING/WELL NUMBER

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 04/18/08

Continued from Previous Page RECOVERY (inches) SAMPLE ID. PID (ppm) BLOW GRAPHIC LOG CONTACT DEPTH EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM 2.4 100 sand, well graded, fine to medium grained, subangular to  $\langle \circ \bigcirc \circ \rangle$ angular; dry, no odor. GW 100 2.6 45 2.8 100 46.0 SILTY SAND: moderate brown (5YR 3/4); 100% silty SM 47.0 sand, soft, moderately well graded, fine to coarse grained, rounded to subrounded; slightly moist, no odor. GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% GW gravel, well graded, fine to coarse grained, maximum diameter of 4 inches, subrounded to subangular; 40% 50.0 sand, well graded, fine to medium grained, subangular to 3.0 100 angular; dry, no odor. Total depth of borehole was 50.0 feet below ground 55 60 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 65 70 75

CDI	M	2295 Gateway Oaks Suite 240 Sacramento, CA 9583 (916) 567-9900
PROJECT NUMBER	5611	1-6169.001.TK5.MOBIL
PROJECT NAME	Aerojet	- GEDIT
LOCATION Ran	cho Cord	ova, CA
DRILLING METHOD	Sonic	

SAMPLING METHOD Continuous Core

GROUND SURFACE ELEVATION (FT MSL) NA

TOP OF CASING ELEVATION (FT MSL) NA

LOGGED BY K. Hopfensperger

### **BORING/WELL CONSTRUCTION LOG**

_	BORING/WELL NUMBER	R _	CDM-CB-2								
_	DATE DRILLED 04/1	8/08									
_	CASING TYPE/DIAMETE	ER .	NA								
_	SCREEN TYPE/SLOT	NA									
_	GRAVEL PACK TYPE	NA									
_	GROUT TYPE/QUANTIT	GROUT TYPE/QUANTITY Bentonite Grout									
	STATIC WATER LEVEL (FT BELOW TOC) NA										
_	<b>GROUND WATER ELEV</b>	ATIO	N (FT MSL)								

PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
					 	ML		SILT: moderate brown (5YR 4/4); 100% silt, firm; dry, no odor.		No well constructed. Borehole abandoned wit bentonite grou
2.2		100		-	5 	CL		CLAY: moderate brown (5YR 4/4); 100% clay, silty, soft, low plasticity; slightly moist, no odor.	5.0 7.0	
24.9		100			  - 10- 	ML		SILT: moderate brown (5YR 4/4); 100% silt, firm; dry, no odor.	12.0	
				-	  15	SW		SAND WITH GRAVEL: moderate brown (5YR 4/4); 70% sand, well graded, fine to coarse grained; 30% gravel, well graded, medium to coarse grained, subrounded to subangular, maximum diameter of 2 inches; dry, no odor.	15.0	
19.8		100		-	 	CL		CLAY: moderate brown (5YR 4/4); 100% clay, soft; dry, no odor.  SAND AND GRAVEL: moderate brown (5YR 4/4); 50% sand, well graded, fine to coarse grained; 50% gravel, well graded, medium to coarse grained, subrounded to subangular, maximum diameter of 2 inches; dry, no odor.	16.0	
1.7		100			20  	SW				
6.4		100			25 	CL		CLAY: moderate brown (5YR 4/4); 100% clay, soft; dry, no odor.	25.0 26.0	
6.2		100			  - 30	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subrounded to subangular; 40% sand, well graded, fine to medium grained, subrounded to subangular; dry, no odor.	32.0	
					 	ML		SILT: moderate brown (5YR 4/4); 100% silt, firm, non-plastic; dry, no odor.  GRAVEL WITH SAND: moderate brown (5YR 3/4); 65% gravel, well graded, fine to coarse grained, maximum	33.0	
				╽	<del></del> 35		0,0]	Continued Next Page		PAGE 1 OF



CDM-CB-2

56111-6169.001.TK5.MOBIL PROJECT NUMBER

75

**BORING/WELL NUMBER** 

**PROJECT NAME** DATE DRILLED Aerojet - GEDIT 04/18/08 Continued from Previous Page RECOVERY (inches) SAMPLE ID. BLOW GRAPHIC LOG PID (ppm) EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM diameter of 4 inches, subrounded to subangular; 35% 2.1 100  $\langle \circ \bigcirc \circ \rangle$ sand, well graded, fine to medium grained, subangular; dry, no odor. GW 100 4.6 45.0 SILT: moderate brown (5YR 4/4); 100% silt, firm, 6.7 100 non-plastic; dry, no odor. ML 47.0 GRAVEL WITH SAND: moderate brown (5YR 3/4); 65% gravel, well graded, fine to coarse grained, maximum diameter of 4 inches, subrounded to subangular; 35% GW sand, well graded, fine to medium grained, subangular; 50.0 dry, no odor. -50 12.5 100 Total depth of borehole was 50.0 feet below ground surface. 55 60 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 65 70

			V		Suite Sacra	240	vay Oa o, CA 9 9900		BORING/WELL CO	NSTF	RUCT	ON LOG							
									BORING/WELL NUMBER CDM-C	B-3									
	JECT N ATION				- GED ova, C														
		ETHOD							SCREEN TYPE/SLOT NA										
		METHO																	
GRO	UND SU	JRFACE	EELE	VA٦	TION (F	T MS				nite Grou	ıt								
										TOC) _	NA								
LOGO		<u>K.</u>	Hopfe	ensp	erger				GROUND WATER ELEVATION (FT N	ISL) _									
			<u>.</u>	Ī. I			0			  -									
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S	GRAPHIC LOG	LITHO	PLOGIC DESCRIPTION	CONTACT	WEL	L DIAGRAM							
NM NM		100 100 100				GP GP		GRAVEL WITH SAN 5/4); 60% gravel, po inches, subangular to subangular. CLAY: moderate broto high plasticity; dry. GRAVEL WITH SAN gravel, poorly graded subangular to subrou coarse grained, subrou coarse grained, subrou coarse gravel, poorly ginches, subrounded to su	D: moderate yellowish brown (10YR orly graded, maximum diameter of 2 o subrounded; 40% sand, poorly im grained, subrounded to	19.0 21.0 23.0		No well constructed. Borehole abandoned with bentonite ground bentonite gr							
NM		100			  	GM		subrounded; 25% sill											
					-35-		• <b> </b> • •	Co	entinued Next Page										



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

### **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-CB-3

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 6/10/08

PRO	JECT N	AME	Ae	rojet	- GED	<u>IT</u>		<b>DATE DRILLED</b> 6/10/08			
								Continued from Previous Page			
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WEL	L DIAGRAM
NM		100							36.0		
					 	ML		SILT WITH GRAVEL: moderate brown (5YR 4/4); 80% silt, non-plastic; 20% gravel, well graded, maximum diameter of 1 inch, subrounded; dry, no odor.	39.0		
NM		100			40   45	GP		GRAVEL WITH SAND: moderate brown (5YR 4/4); 60% gravel, poorly graded, maximum diameter of 2 inches, subrounded to subangular; 40% sand, well graded, fine to coarse grained, subangular to angular.			
NM NM		100			45    50			Total depth of borehole was 50.0 feet below ground	50.0		
					- - - 55 -			surface.			
					60 -						
					65 - -						
					70 -						
					- 75 -						PAGE 2 OF

PROJ PROJ LOCA DRILI SAME GROU TOP (	2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900  ROJECT NUMBER 56111-6169.001.TK5.MOBIL  ROJECT NAME Aerojet - GEDIT  DOCATION Rancho Cordova, CA  RILLING METHOD Sonic  AMPLING METHOD Continuous Core  ROUND SURFACE ELEVATION (FT MSL) NA DOP OF CASING ELEVATION (FT MSL) NA  DOGGED BY K. Hopfensperger  EMARKS								CASING TYPE/DIAMETER NA SCREEN TYPE/SLOT NA GRAVEL PACK TYPE NA GROUT TYPE/QUANTITY Bent STATIC WATER LEVEL (FT BELOW	CB-4  onite Grou	it NA
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHO	LOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
NM NM		50				CL		plasticity; dry, no odo	wn (5YR 4/4); 100% clay, silty, low to	6.0	No well constructed. Borehole abandoned with bentonite grout
NM		100			 15  	GC		4/4); 60% gravel, poor inches; 20% clay, silt	/ITH SAND: moderate brown (5YR brly graded, maximum diameter of 2 y, low to moderate plasticity; 20% fine to medium grained, subrounded	14.0	
NM NM		100			20	CL GC		to high plasticity; dry, CLAYEY GRAVEL W 4/4); 50% gravel, pod inches; 30% sand, pod	wn (5YR 4/4); 100% clay, moderate no odor.  ITH SAND: moderate brown (5YR orly graded, maximum diameter of 2 porly graded, fine to medium grained, gular, 20% clay, silty, low to	20.0	
NM		100			30 	ML			oderate brown (5YR 4/4); 60% silt, vel, well graded, maximum diameter r.	30.0	

GRAVEL WITH SILT AND SAND: moderate brown (5YR 4/4); 50% gravel, poorly graded, subrounded to angular, maximum diameter of 2 inches; 40% sand, well graded, Continued Next Page

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

33.0



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

#### **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-CB-4

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 6/10/08

Aerojet - GEDIT 6/10/08 Continued from Previous Page RECOVERY (inches) SAMPLE ID. BLOW GRAPHIC LOG PID (ppm) EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM fine to medium grained, subangular; 10% silt, low NM 100 plasticity; dry, no odor. GP-GM NM 100 45.0 SILTY GRAVEL WITH SAND: moderate brown (5YR 4/4); NM 100 40% gravel, poorly graded, subrounded to angular, maximum diameter of 2 inches; 40% sand, well graded, fine to medium grained, subangular; 20% silt, low plasticity; dry, no odor. 50.0 NM 100 Total depth of borehole was 50.0 feet below ground surface. 55 60 65 70 75

			N		Suite Sacra	Gateve 240 amento 567-9	o, CA		BORING/WELL
PROJ LOCA DRILI SAME GROU	TECT NATION LING M PLING I JND SU OF CAS	METHOI METHO JRFAC SING E	Aeincho ( D S DD S E ELE LEVA	Cord Conic C	: - GED lova, Co c ntinuou FION (F	IT A IS Core FT MS	) L) NA		DATE DRILLED 7/10/08  CASING TYPE/DIAMETER _ SCREEN TYPE/SLOT _ NA
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC	LITHO	DLOGIC DESCRIPTION
NM		100			  	ML		SILT: brown; 100% s	silt, firm, non-plastic; moist, no odd

NM

NM

NM

 $\mathsf{NM}$ 

NM

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

100

100

100

100

100

CL

SM

### **BORING/WELL CONSTRUCTION LOG**

SCREEN TYPE/SLOT NA GRAVEL PACK TYPE NA	te Grou	ut NA
LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
SILT: brown; 100% silt, firm, non-plastic; moist, no odor.		No well constructed. Borehole abandoned with bentonite grout.
CLAY: reddish brown; 100% clay, firm, moderate plasticity; moist, no odor.	15.0	
SILTY SAND WITH GRAVEL: 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor.	35.0	

Continued Next Page



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

### **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL BORING/WELL NUMBER CDM-CB-5

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 7/10/08

	Continued from Previous Page										
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM	
NM		75			   40-			SILTY SAND WITH GRAVEL: 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor.			
NM		75			  45-  	SM					
NM		75			 50- - - - -			Total depth of borehole was 50.0 feet below ground surface.	_50.0		
					55 - - - - - - 60 -						
					- - - 65 -						
					70 -						
					- - 75 -					PAGE 2 OF 2	

2295 Gateway Oaks Suite 240 Sacramento, CA 95833 (916) 567-9900

	PROJ LOCA DRILI SAMF GROU TOP ( LOG( REMA	ECT N TION LING M PLING I JND SU JND	AME Ra IETHOI METHO JRFAC SING E	Aencho ( D S DD S EE ELE LEVA Titus	Cord Conic Conic Con EVAT	ova, Continuou rion (FT N	IT A IS Core FT MSI MSL)	L) NA NA	CASING TYPE/DIAMETER NA SCREEN TYPE/SLOT NA GRAVEL PACK TYPE NA GROUT TYPE/QUANTITY Bei STATIC WATER LEVEL (FT BELC	CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA  GROUT TYPE/QUANTITY Bentonite Grout  STATIC WATER LEVEL (FT BELOW TOC) NA  GROUND WATER ELEVATION (FT MSL)				
	PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
	0		100			   - 5 -	ML		SILT: brown; 100% silt, soft, non-plastic; dry, no odor.  CLAY: dark yellowish brown; 100% clay, firm, high plasticity; moist, no odor.	3.0	No well constructed. Borehole abandoned with bentonite grout			
	0		100			  10  	ML		SILT: brown; 100% silt, firm, low plasticity; moist, no odor.	10.0				
	0		100			 15  	CL		CLAY: dark yellowish brown; 100% clay, firm, high plasticity; moist, no odor.	15.0				
Т 11/13/09	0		100			 20   			SILTY SAND WITH GRAVEL: 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor.	20.0				
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09	0		100			25   	SM							
VEWGINT_SAC AEROJET	0		100			  			Continued Next Page	35.0				



75

#### **BORING/WELL CONSTRUCTION LOG**

56111-6169.001.TK5.MOBIL **BORING/WELL NUMBER** CDM-CB-6 PROJECT NUMBER

PROJECT NAME DATE DRILLED Aerojet - GEDIT 7/10/08 Continued from Previous Page RECOVERY (inches) SAMPLE ID. BLOW PID (ppm) GRAPHIC LOG EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM 0 100 SILTY GRAVEL: brown; 60% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; 40% silt, soft, non-plastic; moist, no odor. GM 40.0 SILTY SAND WITH GRAVEL: 40% sand, well graded, fine to coarse grained, angular to rounded; 30% silt, 100 0 non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor. SM 0 100 50.0 100 0 Total depth of borehole was 50.0 feet below ground surface. 55 60 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 65 70

PR PR LO DR SA GR TO	SAMPLING METHODContinuous Core  GROUND SURFACE ELEVATION (FT MSL)_NA  TOP OF CASING ELEVATION (FT MSL)_NA  LOGGED BYK. Hopfensperger  REMARKS								5833 BIL	DATE DRILLED 9/2/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA  GROUT TYPE/QUANTITY Benton STATIC WATER LEVEL (FT BELOW	B-7  nite Grou	ut NA
PID (ppm)	(11124) 21 -	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHO	DLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09             Z	M M		100 100 100 100				CL		moderate to high pla  ———————————————————————————————————	EL: moderate brown (5YR 4/4); 90% to high plasticity; 10% gravel, well ded to subangular; slightly moist, no moderate brown (5YR 4/4); 60% clay, 40% gravel, well graded, fine to the clay, and the cl	_16.0	No well constructed. Borehole abandoned with bentonite grout
NEWGINT_SAC AE						   35				ontinued Next Page	_35.0	



 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-CB-7

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 9/2/08

				Continued from Previous Page											
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM					
MM		50			 	CL		GRAVELLY CLAY: moderate brown (5YR 3/4); 80% clay, soft, high plasticity; 20% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subrounded to subangular; dry, no odor.	38.0						
ΝM					 40 			SILTY GRAVEL: moderate brown (5YR 4/4); 75% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subrounded to subangular; 25% silt, soft, moderate plasticity: dry, no odor.							
NМ					 45  	GM									
NM					50 - -			Total depth of borehole was 50.0 feet below ground surface.	50.0						
					- 55 - - -										
					60 - -										
					- 65 - -										
					- 70 - -										
					- - 75 -										

PROJI LOCA DRILL SAMP GROU	ECT NA TION ING ME LING M	ME Ra THOE ETHO	Aeincho (Contraction) Solution Documents	Cond Conic	t - GED lova, Ca c ntinuou TION (F	IT A is Core	e L <u>) N</u> A	DATE DRILLED 9/2/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA  GROUT TYPE/QUANTITY Bento	DATE DRILLED 9/2/08 CASING TYPE/DIAMETER NA				
	ED BY							STATIC WATER LEVEL (FT BELOW GROUND WATER ELEVATION (FT I					
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
NM NM		100				ML CL		SILT: light brown (5YR 5/6); 100% silt, low plasticity to non-plastic; dry, no odor.  CLAY: moderate brown (5YR 4/4); 100% clay, soft, moderate to high plasticity; dry, no odor.	2.0	No well constructed. Borehole abandoned w bentonite gro			
NM NM		100				GC		CLAYEY GRAVEL: moderate brown (5YR 4/4); 60% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subangular to subrounded; 40% clay, soft, moderate to high plasticity; dry, no odor.					
NM		50				GW		GRAVEL WITH SAND: dark yellowish orange (10YR 6/6); 70% gravel, well graded, fine to coarse grained, maximum diameter of 2.5 inches, subrounded; 30% sand, poorly graded, fine grained, subrounded; dry, no odor.	_22.0				



 PROJECT NUMBER
 \_56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 \_CDM-CB-8

 PROJECT NAME
 Aeroiet - GEDIT
 DATE DRILLED
 9/2/08

PROJ	ROJECT NAME Aerojet - GEDIT						DATE DRILLED 9/2/08						
							Continued from Previous Page						
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.  EXTENT  DEPTH  (ft. bgs)  U.S.C.S.				GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
NM NM		70			  40 	GM		SILTY GRAVEL: dusky yellow (5Y 6/4); 70% gravel, well graded, medium to coarse grained, maximum diameter of 1.5 inches, subrounded to subangular; 30% silt, non-plastic: dry, no odor.	_37.0				
NM		70			45	OWI			50.0				
NM		70			50 - - - - 55 - -			Total depth of borehole was 50.0 feet below ground surface.					
					60 -								
					65 -								
					- - 75 -					PAGE 2 OF			

			N		Suite Sacr	240	vay Oak o, CA 98 900		BORING/WELL CO	NSTR	UCTION LOG			
PROJ	JECT N	UMBER	<b>२</b> 5	611	1-6169	.001.T	K5.MOI	BIL	BORING/WELL NUMBER CDM-CB-9					
	JECT N				t - GED				DATE DRULED 40/0/00					
LOCA	ATION	Ra	ncho (	Corc	lova, C				· · · · · · · · · · · · · · · · · · ·					
DRILI	LING M													
SAME	LING N	ИЕТНО	D _	Со	ntinuou				GRAVEL PACK TYPE NA					
									GROUT TYPE/QUANTITY Bentonite Grout					
TOP (	OF CAS	ING E	LEVA <sup>-</sup>	τιοι	N (FT N	/ISL)	NA		STATIC WATER LEVEL (FT BELOW	/ TOC)N	IA			
LOG	GED BY	K.	Hopfe	ensp	erger				GROUND WATER ELEVATION (FT	MSL)				
REMA	ARKS													
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHO	DLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
NM		50			   - 5 -	ML		SILT: moderate brownon-plastic; dry, no o	vn (5YR 4/4); 100% silt, soft, odor.	7.0	No well constructed. Borehole abandoned with bentonite grout.			
NM		100			  10	GW		5/4); 60% gravel, we maximum diameter	ND: moderate yellowish brown (10YR) sell graded, fine to coarse grained, of 2 inches; 40% sand, well graded, d, subrounded to subangular; dry, no					
NM		100			  15	GW		5/4); 50% gravel, we maximum diameter of fine to coarse graine odor.	ND: moderate yellowish brown (10YR bill graded, fine to coarse grained, of 2 inches; 50% sand, well graded, ed, subrounded to subangular; dry, no	12.0				
NM		100			   20-			silty, low plasticity; 3 medium to coarse gr	moderate brown (5YR 4/4); 70% clay, 0% gravel, moderately well graded, rained, maximum diameter of 3 subrounded; dry, no odor.					
NM		100			  25-  	CL		silty, low plasticity; 4 medium to coarse g	moderate brown (5YR 4/4); 60% clay, 0% gravel, moderately well graded, rained, maximum diameter of 3 subrounded; dry, no odor.	27.0				

SILTY GRAVEL: moderate brown (5YR 4/4); 70% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 30% silt, soft; dry, no odor.

Continued Next Page

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

NM

100

CL

32.0



 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-CB-9

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 12/2/08

	1							Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NM		100			 	GM				
NM		50			40  			SAND WITH CRAVEL: moderate brown (5VR 4/4): 80%	43.0	
NM		100			 45  	sw		SAND WITH GRAVEL: moderate brown (5YR 4/4); 80% sand, moderately well graded, fine to medium grained, subrounded to subangular; 20% gravel, well graded, maximum diameter of 1 inch, subangular; dry, no odor.		
NM		100			 50 - - -			Total depth of borehole was 50.0 feet below ground surface.	_50.0	
					- 55 - - -					
					- 60 - - -					
					- 65 - -					
					- 70 - - -					
					- - 75 -					

PROD LOCA DRIL SAMI GROU TOP	JECT N JECT N ATION LING M PLING I UND SU	AME Ra IETHOI METHO JRFAC SING E	Aeincho ( D S DD S E ELE LEVA	rojet Cord Conic Co EVAT	Suite Sacra (916) 1-6169 - GED lova, C. c ntinuou FION (F	240 amento ) 567-9 .001.T IT A as Core	K5.MO	BORING/WELL CO  BIL BORING/WELL NUMBER CDM- DATE DRILLED 12/2/08 CASING TYPE/DIAMETER NA SCREEN TYPE/SLOT NA GRAVEL PACK TYPE NA GROUT TYPE/QUANTITY Bent STATIC WATER LEVEL (FT BELOV	DATE DRILLED 12/2/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA			
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM		
NM		100				SP GM		SAND: dark yellowish orange (10YR 6/6); 100% sand, poorly graded, fine grained, subangular; dry, no odor.  SILTY GRAVEL: light brown (5YR 5/6); 60% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches; 40% silt, soft, non-plastic; dry, no odor.	2.0	No well constructed. Borehole abandoned v bentonite gro		
NM NM		100			 10   	GW		GRAVEL WITH SAND: moderate brown (5YR 4/4); 70% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subrounded to subangular; 30% sand, well graded, fine to medium grained, subrounded to subangular; dry, no odor.	8.0			
NM		100			   20-  	CL	000	CLAY WITH GRAVEL: moderate brown (5YR 4/4); 75% clay, soft, low plasticity; 25% gravel, poorly graded, coarse grained, maximum diameter of 1 inch, subrounded to subangular; moist, no odor.	16.0			
908.GPJ NEWGINT.GDT 11  Z  M		100			25 			SILTY CDAVEL: 60% grouply poorly and all control	29.0			
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09		100			30   	GM		SILTY GRAVEL: 60% gravel, poorly graded, coarse grained, maximum diameter of 1 inch, subrounded to subangular; 40% silt, soft, non-plastic; slightly moist, no odor.	35.0			
<u> </u>					<del></del> 35		-	Continued Next Page				



CDM-CB-10

**BORING/WELL NUMBER** 

PROJECT NUMBER 56111-6169.001.TK5.MOBIL
PROJECT NAME Aerojet - GEDIT

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

Aerojet - GEDIT DATE DRILLED 12/2/08

Continued from Previous Page RECOVERY (inches) SAMPLE ID. PID (ppm) BLOW GRAPHIC LOG EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM NM 100 GRAVEL WITH SAND: moderate brown (5YR 4/4); 50%  $\circ \bigcirc \circ$ gravel, well graded, medium to coarse grained, maximum 200 diameter of 2 inches, subrounded to subangular; 50% sand, well graded, fine to coarse grained, subangular; dry, no odor. GW 40.0 SILTY GRAVEL: moderate brown (5YR 4/4); 70% gravel, NM 50 well graded, medium to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 30% silt, soft; slightly moist, no odor. 43.0 GRAVEL WITH SAND: 70% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subangular to subrounded; 30% sand, well graded, fine to 45 coarse grained, subrounded to subangular, dry, no odor. NM 100 GW 50.0 NM 100 Total depth of borehole was 50.0 feet below ground surface. 55 60 65 70 75

PRO.		JMBEF	₹ <u>_</u> 5	611	(916) <u>1-6169</u>	567-9 .001.T	K5.MOE	BIL BORING/WELL NUMBER CDM	BORING/WELL NUMBER					
	LING ME							SCREEN TYPE/SLOT   NA     NA     NA     NA     NA     NA						
								GROUT TYPE/QUANTITY Ben						
								STATIC WATER LEVEL (FT BELOV						
								GROUND WATER ELEVATION (FT						
REM	ARKS				·				<u> </u>	1				
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WEI	LL DIAGRAM			
						ML		SILT: dark yellowish orange (10 YR 6/6); 100% silt, soft, low plasticity; dry, no odor.	2.0		No well constructed.			
					-	CL		CLAY: moderate yellowish brown (10 YR 5/4); 100% clay,	3.0		Borehole abandoned w			
					-		KY (	soft, moderate plasticity, dry, no odor.  GRAVEL WITH SAND: light brown (5YR 4/4); 70% gravel,	<u></u>		bentonite gro			
					_		000	well graded, fine to coarse grained, maximum diameter of						
NM		100			<del>-</del> 5		PÕd	3 inches, subrounded to subangular; 30% sand, well graded, fine to medium grained, subrounded to						
					-	GW	500	subangular; dry, no odor.						
					-	0,,,	bo.							
							603							
					-10-		600		10.0					
NM		100			_			SILTY GRAVEL: light brown (5YR 5/6); 60% gravel, well graded, fine to coarse grained, maximum diameter of 3						
					L _			inches, subrounded to subangular; 40% silt, soft, low						
								plasticity; slightly moist, no odor.						
					_		1							
NM		100			-15-									
					-	GM								
					-									
					ļ -									
N 1 N 4					-20-									
NM		50			<u> </u>									
					<u> </u>				22.0					
								CLAYEY GRAVEL: moderate yellowish brown (10YR 5/4); 50% gravel, well graded, medium to coarse grained,						
								maximum diameter of 2 inches, subrounded; 50% clay,						
								silty, low plasticity; dry, no odor.						
NM		100			25									
					-									
					-	GC								
					-									
NM		100			-30-									
INIVI		100			_									
					L -									
					L		70		33.0					
					<u> </u>			GRAVELLY SILT: moderate yellowish brown (10YR 5/4); 70% silt, soft, low plasticity; 30% gravel, well graded,						
					—35 <i>—</i>			medium to coarse grained, maximum diameter of 3  Continued Next Page						

GRAVELLY SILT: moderate yellowish brown (10YR 5/4); 70% silt, soft, low plasticity; 30% gravel, well graded, medium to coarse grained, maximum diameter of 3

Continued Next Page



PROJECT NUMBER 56111-6169.001.TK5.MOBIL **BORING/WELL NUMBER** CDM-CB-11 PROJECT NAME Aerojet - GEDIT

DATE DRILLED	12/3/08	

		_	٠.						1. 1	
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
NM		100				ML		inches, subrounded; dry, no odor.		
NM		100			40	ML		SILT WITH GRAVEL: moderate yellowish brown (10YR 5/4); 80% silt, soft, non-plastic; 20% gravel, well graded, fine to coarse grained, maximum diameter of 1 inch, subrounded; dry, no odor.	39.0 41.0	
					  45	SW		SAND WITH GRAVEL: moderate brown (5YR 4/4); 60% sand, well graded, medium to coarse grained, subrounded; 40% gravel, poorly graded, coarse grained, maximum diameter of 0.5 inches; dry, no odor.  SILT: moderate brown (5YR 4/4); 90% silt, soft, population; 10% grayel, poorly graded, except grained.	44.0	
NM		100				GW		diameter of 1.5 inches, subrounded to subangular; 30% sand, well graded, fine to coarse grained, subangular to	_46.0	
NM		100			-50-		000	angular; dry, no odor.  Total depth of borehole was 50.0 feet below ground surface.	50.0	
					- - 55 -					
					- - -					
					60 -					
					- - 65 -					
					- - -					
					70 -					
					- -					

PROJ	ECT N	JMBEF	<b>R</b> _5	611	, ,	567-9 .001.T		BIL BORING/WELL NUMBER CDM-C					
	ECT NA							DATE BRULER 40/0/00					
								CASING TYPE/DIAMETER NA					
	ING MI							SCREEN TYPE/SLOT NA					
								GRAVEL PACK TYPE NA					
								GROUT TYPE/QUANTITY Benton					
								STATIC WATER LEVEL (FT BELOW GROUND WATER ELEVATION (FT N					
	ARKS			ор	0.90.								
(mc	N TS	ERY is)	<u>.</u>	F	H. (SI	ο.	<b>₽</b>		H-H-H-H-H-H-H-H-H-H-H-H-H-H-H-H-H-H-H-				
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
						ML		SILT: dark yellowish orange (10YR 6/6); 100% silt, soft, non-plastic; dry, no odor.	2.0	No well constructed. Borehole			
								CLAY: light brown (5YR 5/6); 100% clay, soft, low to moderate plasticity; dry, no odor.		abandoned w bentonite gro			
NM		100			— 5 —								
						CL							
NM		100			<del></del> 10								
INIVI		100											
								GRAVEL WITH SAND: dark yellowish orange (10YR 6/6);	13.0				
		100						70% gravel, well graded, medium to coarse grained, maximum diameter of 3 inches, subangular; 30% sand,					
NM					—15—	GW	%0 Q	well graded, fine to medium grained, subangular, dry, no					
							0	000	odor.				
							P O C		100				
								SILTY GRAVEL: moderate brown (5YR 4/4); 70% gravel,	_18.0				
								well graded, medium to coarse grained, maximum diameter of 1.5 inches, subrounded to subangular; 30%					
NM		50			20		R	silt, soft, low plasticity; dry, no odor.					
						GM	RS						
NM		100			25								
						L			27.0				
							000	GRAVEL WITH SAND: pale yellowish brown (10 YR 6/2); 70% gravel, well graded, fine to coarse grained, maximum	7				
					_		20	diameter of 3 inches, subangular; 30% sand, well graded,					
					20			fine to coarse grained, subangular; dry, no odor.					
NM		100			30 -	GW	601						
					_								
					_		000						
					_		600		_34.0				
					O.F		600						
					 35			GRAVEL WITH SAND: pale yellowish brown (10 YR 6/2);  Continued Next Page					



**PROJECT NUMBER** <u>56111-6169.001.TK5.MOBIL</u>

BORING/WELL NUMBER CDM-CB-12

								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
NM		100			  	GW		50% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subangular; 50% sand, well graded, fine to coarse grained, subangular; dry, no odor.	40.0	
NM		100			40   	GM		SILTY GRAVEL: light brown (5YR 5/6); 65% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 35% silt, soft, low plasticity; dry, no odor.	45.0	
NM		100			45   	GW		GRAVEL WITH SAND: pale yellowish brown (10 YR 6/2); 50% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 50% sand, poorly graded, fine to medium grained, subangular; dry, no odor.		
NM		100			50 - - -			Total depth of borehole was 50.0 feet below ground surface.	50.0	
					55 - - - -					
					60 -					
					65 - - - -					
					70 - - -					

CDN	2295 Gateway Oaks Suite 240 Sacramento, CA 9583: (916) 567-9900
PROJECT NUMBER	56111-6169.001.TK5.MOBIL
PROJECT NAME	Aerojet - GEDIT
LOCATION Ranch	o Cordova, CA
DRILLING METHOD	Sonic
SAMPLING METHOD	Continuous Core

GROUND SURFACE ELEVATION (FT MSL) NA
TOP OF CASING ELEVATION (FT MSL) NA

### **BORING/WELL CONSTRUCTION LOG**

BORING/WELL NUMBER CDM-CB-13
DATE DRILLED 12/3/08
CASING TYPE/DIAMETER NA
SCREEN TYPE/SLOT NA
GRAVEL PACK TYPE NA
GROUT TYPE/QUANTITY Bentonite Grout
STATIC WATER LEVEL (FT BELOW TOC) NA
GROUND WATER ELEVATION (FT MSL)

PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
					  	ML		SILT: light brown (5YR 5/6); 100% silt, soft, non-plastic; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, high plasticity; dry, no odor.	2.0	No well constructed. Borehole abandoned w bentonite grou
NM		100			5  	CL				
NM		100			10 			GRAVEL WITH SAND: 75% gravel, well graded, fine to	12.0	
NM		100			 15 	GW ML		coarse grained, maximum diameter of 1.5 inches, subangular; 25% sand, poorly graded, fine grained, subangular; dry, no odor.  SILT: light brown (5YR 5/6); 100% silt, soft, moderate plasticity; dry, no odor.	15.0	
NM		50			 20  			SILTY GRAVEL: moderate brown (5YR 4/4); 70% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subrounded to subangular; 30% silt, soft, non-plastic; dry, no odor.	18.0	
NM		50			25  	GM				
NM		50			 30 				33.0	
					  35			GRAVEL WITH SAND: dark yellowish orange (10YR 6/6); 65% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subangular to angular; 35% sand, Continued Next Page	33.0	



75

#### **BORING/WELL CONSTRUCTION LOG**

**BORING/WELL NUMBER** CDM-CB-13 **PROJECT NUMBER** 56111-6169.001.TK5.MOBIL **PROJECT NAME** DATE DRILLED Aerojet - GEDIT 12/3/08

Continued from Previous Page RECOVERY (inches) SAMPLE ID. PID (ppm) BLOW GRAPHIC LOG CONTACT DEPTH EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM NM 50 well graded, fine to coarse grained, subangular; dry, no  $^{\circ}$   $^{\circ}$ odor. 0 37.0 SILTY GRAVEL: light brown (5YR 5/6); 70% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded; 30% silt, soft, moderate plasticity; dry, no odor. 100 NM GM 45.0 GRAVEL WITH SAND: pale yellowish brown (10YR 6/2); 60% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subrounded; 40% sand, well graded, NM 100 000 fine to coarse grained, subrounded to subangular, dry, no GW odor. 0 C 50.0 NM 100 Total depth of borehole was 50.0 feet below ground surface. 55 60 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 65 70

PROJ PROJ LOCA DRILL SAMP GROU	ECT NATION LING MI PLING N JND SU OF CAS GED BY	JMBEF AME Rai ETHOL METHO IRFAC	Aerncho CO SOD E ELE	611 cojet cord conic Cord VAT	Suite Sacri (916) 1-6169 :- GED lova, C. c ntinuou TION (F	240 amento ) 567-9 .001.T IT A as Core T MSI	K5.MOE	5833 BIL	DATE DRILLED 12/3/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA  GROUT TYPE/QUANTITY Bentonite Grout  STATIC WATER LEVEL (FT BELOW TOC) NA  GROUND WATER ELEVATION (FT MSL)				
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHC	DLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM		
NM NM		100				CL		plasticity; dry, no odo		_13.0	No well constructed. Borehole abandoned with bentonite grout		
NM NM		100			 15     20	ML		dry, no odor.	YR 5/6); 100% silt, soft, low plasticity; YR 5/6); 100% clay, soft, moderate or.	16.0			
NM		100			  - 25-  			60% gravel, well grad diameter of 3 inches	TH SAND: moderate brown (5YR 4/4); ded, fine to coarse grained, maximum, subrounded to subangular; 20% ne to coarse grained, subangular; asticity; dry, no odor.	25.0			

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

NM

100

35.0



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

# **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL BORING/WELL NUMBER CDM-CB-14

PROJECT NAME Aerojet - GEDIT DATE DRILLED 12/3/08

								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
NM		100			  	CL		CLAY: light brown (5YR 5/6); 100% clay, soft, moderate plasticity; dry, no odor.  SILTY GRAVEL WITH SAND: light brown (5YR 5/6); 50% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches; 25% sand, well graded, fine to coarse grained, subangular; 25% silt, soft, low plasticity; dry, no odor.	37.0	
NM		100			40   	GM		diy, no odor.		
NM		100			45   				50.0	
NM		100			50 - - - -			Total depth of borehole was 50.0 feet below ground surface.	50.0	
					55 - - - -					
					60 -					
					65 - - - -					
					70 - - - -					
					- 75 -	-				

PROJ PROJ LOCA	ECT NA	JMBEF AME Ra	R <u>5</u> Aer	rojet Cord	1-6169 - GED ova, C	IT A	K5.MOI		DATE DRILLED 12/3/08 CASING TYPE/DIAMETER NA					
	ING MI								SCREEN TYPE/SLOT NA					
									GRAVEL PACK TYPE NA GROUT TYPE/QUANTITY Bento					
									STATIC WATER LEVEL (FT BELOW TOC) NA					
LOG									GROUND WATER ELEVATION (FT MSL)					
- INLIVIA														
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHO	LOGIC DESCRIPTION	CONTACT	WELL DIAGRAM			
						ML		SILT: light brown (5Y dry, no odor.	R 5/6); 100% silt, soft, non-plastic;	2.0	No well constructed			
					 			CLAY: light brown (5 plasticity; dry, no odc	YR 5/6); 100% clay, soft, high or.	2.0	Borehole abandoned bentonite gr			
NM		100			5  									
NM		100			 - 10									
					 	CL								
NM		100			 15 									
NM		50			20  									
							000	GRAVEL WITH SAN	D: light brown (5YR 5/6), 50% gravel,	24.0				
NM		100			25  			3 inches, subrounded	oarse grained, maximum diameter of d to subangular; 50% sand, well im grained, subangular; dry, no odor.					
NM		100			  30	GW								
. 4141		.00			 									
					 35				ntinued Next Page	35.0				



# **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL PROJECT NAME

NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

Aerojet - GEDIT

BORING/WELL NUMBER CDM-CB-15

DATE DRILLED 12/3/08

							Continued from Previous Page		
PID (ppm) BLOW COUNTS	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NM	100				GC		CLAYEY GRAVEL: moderate brown (5YR 4/4); 60% gravel, well graded, fine to coarse grained, maximum diameter of 1 inch, subrounded to subangular; 40% clay, soft, low to moderate plasticity; dry, no odor.		
M	100		-	45   	GW		GRAVEL WITH SAND: pale yellowish orange (10YR 6/2); 50% gravel, well graded, fine to coarse grained, maximum diameter of 3 inches, subangular to angular; 50% sand, well graded, fine to coarse grained, subangular; dry, no odor.	46.0 50.0	
MM .	100			-50			Total depth of borehole was 50.0 feet below ground surface.		

PROD PROD LOCA DRIL SAMI GRO TOP	JECT NATION LING M PLING I UND SU OF CAS	UMBEI AME Ra ETHOI METHO JIRFAC	R 5 Aeincho (D S DD 5 EE ELE	Sonic Corc Conic Co	Suite Sacri (916) 1-6169 t - GED dova, C. c ntinuou TION (F	240 amento ) 567-9 .001.T IT A as Core	K5.MO	BIL BORING/WELL NUMBER CDM-CE DATE DRILLED 12/3/08 CASING TYPE/DIAMETER NA SCREEN TYPE/SLOT NA GRAVEL PACK TYPE NA GROUT TYPE/QUANTITY Benton STATIC WATER LEVEL (FT BELOW T	DATE DRILLED 12/3/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GRAVEL PACK TYPE NA				
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELI	L DIAGRAM		
						ML		SILT: light brown (5YR 5/6); 100% silt, soft, low plasticity; dry, no odor.	3.0		No well constructed. Borehole abandoned wi		
NM NM		100			5	CL		CLAY WITH GRAVEL: light brown (5YR 5/6); 80% clay, soft, moderate to high plasticity; dry, no odor.  CLAY WITH GRAVEL: light brown (5YR 5/6); 80% clay, soft, moderate to high plasticity; 20% gravel, poorly graded, fine to medium grained, mximum diameter of 0.5 inches, subangular; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity dry, no odor.	16.0		bentonite grou		
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09  Z Z Z Z Z		100			20   25  	CL		high plasticity; dry, no odor.	30.0				
WGINT_SAC AEROJET_12  Z  M		100			30   35	GW		GRAVEL WITH SAND: light brown (5YR 5/6); 50% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded; 50% sand, well graded, fine to coarse grained, subangular; dry, no odor.	_30.0 _35.0				
<b></b>								Continued Next Page					



# **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 56111-6169.001.TK5.MOBIL
 BORING/WELL NUMBER
 CDM-CB-16

 PROJECT NAME
 Aerojet - GEDIT
 DATE DRILLED
 12/3/08

								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NM		100			   40 	CL		CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.  SILTY GRAVEL WITH SAND: pale yellowish brown (10YR 6/2); 50% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 25% sand, well graded, fine to coarse grained, subrounded to subangular; 25% silt, soft, low plasticity; dry, slight odor of propane.	36.0	
NM		100			45  				50.0	
NM		100			50 - - - -			Total depth of borehole was 50.0 feet below ground surface.	50.0	
					55 -					
					65 -					
					- - 70 -					
					- - - 75 -					

PRODE LOCAL PROPERTY IN THE PR	PROJECT NAME Aerojet - GEDIT  LOCATION Rancho Cordova, CA  DRILLING METHOD Sonic  SAMPLING METHOD Continuous Core  GROUND SURFACE ELEVATION (FT MSL) NA  TOP OF CASING ELEVATION (FT MSL) NA  LOGGED BY K. Hopfensperger  REMARKS								BORING/WELL NUMBER CDM-CB-17  DATE DRILLED 12/3/08  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA				
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOL	OGIC DESCRIPTION	CONTACT DEPTH	WELL	_ DIAGRAM	
IT.GDT 11/13/09  NA N	Л	100 100 100				CL CL		moderate plasticity; dr  CLAY: light brown (5Y plasticity; dry, no odor  CLAY: light brown (5Y	'R 5/6); 100% clay, soft, high	_3.0		No well constructed. Borehole abandoned wit bentonite grou	
NEWGINT_SAC AEROJET_120908.GPJ NEWGINT.GDT 11/13/09	Л	100				- GM - GW		graded, fine to coarse inches, subrounded; 4 plasticity; dry, no odor  GRAVEL WITH SAND 75% gravel, well graddiameter of 3 inches, since to coarse grained.	D: pale yellowish brown (10YR 6/2); ed, fine to coarse grained, maximum subrounded; 25% sand, well graded, , subangular; dry, no odor.	28.0 32.0 35.0			
<b>ಶ</b> ∟		1						Con	tinued Next Page				



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## **BORING/WELL CONSTRUCTION LOG**

56111-6169.001.TK5.MOBIL **BORING/WELL NUMBER** \_\_CDM-CB-17 **PROJECT NUMBER PROJECT NAME** DATE DRILLED

Aerojet - GEDIT 12/3/08 Continued from Previous Page RECOVERY (inches) SAMPLE ID. BLOW GRAPHIC LOG PID (ppm) EXTENT DEPTH (ft. bgs) U.S.C.S. LITHOLOGIC DESCRIPTION WELL DIAGRAM NM 100 CLAY WITH GRAVEL: moderate brown (5YR 4/4); 60% clay, soft, moderate to high plasticity; 30% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 10% silt, soft, low to moderate plasticity; dry, no odor. CL NM 50 43.0 GRAVEL WITH SAND: light brown (5YR 5/6); 60% gravel, well graded, fine to coarse grained, maximum diameter of 0 2 inches, subrounded to subangular; 40% sand, well 45 graded, fine to medium grained, subangular, dry, no odor. NM 100 GW 50.0 NM 100 Total depth of borehole was 50.0 feet below ground surface. 55 60 NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09 65 70

PROJECT NAME Aerojet - GEDIT  LOCATION Rancho Cordova, CA  DRILLING METHOD Sonic  SAMPLING METHOD Continuous Core  GROUND SURFACE ELEVATION (FT MSL) NA  TOP OF CASING ELEVATION (FT MSL) NA  LOGGED BY K. Hopfensperger  REMARKS  CASING TYPE/DIAMETER NA  SCREEN TYPE/SLOT NA  GROUT TYPE/QUANTITY Bentonite Grout  STATIC WATER LEVEL (FT BELOW TOC) NA  GROUND WATER ELEVATION (FT MSL)  GROUND WATER ELEVATION (FT MSL)  LOGGED BY K. Hopfensperger  GROUND WATER ELEVATION (FT MSL)  CASING TYPE/DIAMETER  NA  SCREEN TYPE/SLOT  NA  GROUT TYPE/QUANTITY BENTONITE GROUT  STATIC WATER LEVEL (FT BELOW TOC)  NA  LOGGED BY K. Hopfensperger  GROUND WATER ELEVATION (FT MSL)	
LOCATION Rancho Cordova, CA  CASING TYPE/DIAMETER NA  SCREEN TYPESLOT NA  SAMPLING METHOD Sonic SCREEN TYPESLOT NA  GROUND SURFACE ELEVATION (FT MSL) NA  TOP OF CASING ELEVATION (FT MSL) NA  LOGGED BY K. Hopfensperger GRANKS  REMARKS  REMARKS  GRUND WATER ELEVATION (FT MSL)  LITHOLOGIC DESCRIPTION  LITHOLOGIC DESCRIPTION  LITHOLOGIC DESCRIPTION  LITHOLOGIC DESCRIPTION  LITHOLOGIC DESCRIPTION  LOGGED BY K. Hopfensperger GRANG MATER LEVATION (FT MSL)  REMARKS  CLAYEY GRAVEL. light brown (5YR 5/6); 50% gravel, well graded, medium to coarse grained, maximum diameter of 2 inches, rounded to subrounded; 50% clay, soft, moderate to high plasticity; dry, no odor.  NM  100  NM  100  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.	
DRILLING METHOD  SAMPLING METHOD  Continuous Core  GRAVEL PACK TYPE  NA  GROUND SURFACE ELEVATION (FT MSL) NA  TOP OF CASING ELEVATION (FT MSL) NA  LOGGED BY  REMARKS  REMARKS  LITHOLOGIC DESCRIPTION  LITHOLOGIC DESCRIPTIO	
GROUND SURFACE ELEVATION (FT MSL) NA TOP OF CASING ELEVATION (FT MSL) NA LOGGED BY REMARKS    (u d) O O O O O O O O O O O O O O O O O O	
TOP OF CASING ELEVATION (FT MSL)  NA  STATIC WATER LEVEL (FT BELOW TOC)  ROUND WATER ELEVATION (FT MSL)  REMARKS    A	
CLAYEY GRAVEL: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.   15.0	
NM   100	
CLAYEY GRAVEL: light brown (5YR 5/6); 50% gravel, well graded, medium to coarse grained, maximum diameter of 2 inches, rounded; 50% clay, soft, moderate to high plasticity; dry, no odor.    NM	
NM 100 CLAY: light brown (5YR 5/6); 50% gravel, well graded, medium to coarse grained, maximum diameter of 2 inches, rounded; 50% clay, soft, moderate to high plasticity; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.  CLAY: light brown (5YR 5/6); 100% clay, soft, moderate to high plasticity; dry, no odor.	WELL DIAGRAM
NM 100	No well constructed. Borehole
	abandoned w bentonite gro
NM 100  CLAYEY GRAVEL: light brown (5YR 5/6); 50% gravel, well graded, fine to coarse grained, maximum diameter of 1 inch, subrounded to subangular; 50% clay, soft, moderate to high plasticity; dry, no odor.  ORAVEL WITH SAND: moderate brown (5YR 4/4); 60%	
gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 40% sand, well graded, fine to coarse grained, subangular to angular; dry. no odor.  Continued Next Page	



NEWGINT\_SAC AEROJET\_120908.GPJ NEWGINT.GDT 11/13/09

# **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER56111-6169.001.TK5.MOBILBORING/WELL NUMBERCDM-CB-18PROJECT NAMEAerojet - GEDITDATE DRILLED12/3/08

PRO	JECT N	AWE	Aei	rojet	- GED	11		DATE DRILLED12/3/08		
								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NM		100			  	CL		GRAVELLY CLAY: light brown (5YR 5/6); 60% clay, soft, high plasticity; 40% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subangular to subrounded; dry, no odor.	39.0	
NM NM		75 75				GM		SILTY GRAVEL WITH SAND: light brown (5YR 5/6); 60% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subangular to subrounded; 20% sand, well graded, fine to coarse grained, subangular; 20% silt, soft, low to moderate plasticity; dry, no odor.		
NM		75			50			Total depth of borehole was 50.0 feet below ground surface.	50.0	

PP: 1	IECT NI	IMRE	<b>)</b>	611	1_6160	001 T	K5 MO	BIL	BORING/WELL NUMBER CDM-C	R_10						
	IECT N				- GED			BIL								
									CASING TYPE/DIAMETER NA							
DRIL	LING MI															
SAME	LING N	/IETHC	D _	Cor	ntinuou	s Core	)		GRAVEL PACK TYPE NA							
									GROUT TYPE/QUANTITY Benton	ite Grou	t					
									STATIC WATER LEVEL (FT BELOW TOC) NA							
	OGGED BY K. Hopfensperger  EMARKS								GROUND WATER ELEVATION (FT MSL)							
	Ø	<b>≻</b> (	<u>.</u>				U			<u></u>						
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHC	PLOGIC DESCRIPTION	CONTACT	WEL	L DIAGRAM				
NM NM		100				CL		SILTY GRAVEL: ligh graded, fine to coars inches, angular to sudry, no odor.	t brown (5YR 5/6); 60% gravel, well e grained, maximum diameter of 2 bangular; 40% silt, soft, low plasticity;	_14.0		No well constructed. Borehole abandoned wi bentonite grou				
NM		100				CL		plasticity, dry, no odd SILTY GRAVEL: ligh graded, fine to coars	t brown (5YR 5/6); 50% gravel, well e grained, maximum diameter of 3 ubrounded; 50% silt, soft, low	_19.0						
NM		100				GW- GM		60% gravel, well grad diameter of 2 inches,	AND SAND: light brown (5YR 5/6); ded, fine to coarse grained, maximum subangular to angular; 30% sand, oarse grained, subangular; 10% silt, y, no odor.	_28.0						
										35.0						



# **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER 56111-6169.001.TK5.MOBIL BORING/WELL NUMBER CDM-CB-19

**PROJECT NAME** 

Aerojet - GEDIT

DATE DRILLED 12/3/08

PROJECT	NAIVIE	Ae	rojei	t - GED	11		DATE DRILLED12/3/08		
				1			Continued from Previous Page		
PID (ppm) BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
NM NM	50				GW-		GRAVEL WITH SILT AND SAND: light brown (5YR 5/6); 60% gravel, well graded, fine to coarse grained, maximum diameter of 2 inches, subrounded to subangular; 30% sand, well graded, fine to coarse grained, subrounded to subangular; 10% silt, soft, low plasticity; dry, no		
NM	100			45   					
NM	100			50 - - -		• <b>(</b>   <b>(   <b>(</b></b>	Total depth of borehole was 50.0 feet below ground surface.	_50.0	
				55 - - -					
				60 -					
				65 - - - -					
				70 -					
				- 75 -					PAGE 2 C

# **Appendix C: Supplemental Data**

Phase II Piezometer Monitoring Data

Well ID \_\_\_P1\_\_\_\_ Depth \_\_\_various\_\_\_\_

			1		Injection G				Well	Ambient Air	Estimated Depth
-		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure	(ft bgs)
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(Cº)	(mbar)	
Ontimizatio	n Test #8 (1	00 ofb of 10	00% Propon	o to D4 10	9 D4 20 (50	ofh to oool	h noint\				
Optimizatio	1 1621 #0 (1	OO CIII OI 10	10% PTOPATI	e 10 F4-10,	& F4-20 (30	Ciri to each	n point)				
9/8/2008	8 0905 Test	Start									
9/8/2008	3 Tubing to F	P1 cut at all	points, will	measure ne	xt visit					999	
9/15/2008	3 954	5.4	1.62	30	0.002		32.3		24.1	1007	
9/15/2008	955	19.4	0.24	0.06	0.002		32.5		24.3	1007	
9/15/2008	958	5.9	1.94	3.5	0.002		32.4		24.7	1007	
9/15/2008	959	9.5	1.58	2.5	0.002		33.3		24.8	1007	
11/2/2008	3 1320	4.0	2.10	30	0.005		73.2		19.1	1016	18
11/2/2008	3 1322	0.0	2.08	30	0.005		77.7		19.1	1016	
11/2/2008	3 1323	12.1	2.00	0.70	0.005		77.2		19.1	1016	
11/2/2008	3 1325	16.6	1.96	1.58	0.005		80.1		19.2	1016	48
11/17/2008	1136	15.3	1.66		0.005		80.5		26.6	1014	18
11/17/2008	1138	3.7	1.94	30	0.005		38.2		27.5	1014	33
11/17/2008	1140	0.0	1.72	30	0.005		60.9		28.7	1014	48
11/17/2008	1141	9.8	2.24	2.0	0.005		55.5		29.2	1014	68
12/1/2008							38.1		20.4	1014	
12/1/2008	1051	3.6	2.18	30	0.002		67.9	·	20.5	1014	
12/1/2008			1.64	30	0.002		66.5	·	20.8	1014	
12/1/2008	1053	9.5	2.46	3.5	0.002		62.5	•	20.9	1014	

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P1\_\_\_\_ Depth \_\_\_\_\_18\_

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1353	20.6	0.20	0	0.002	100,000	77.1	0.02	10.8	1020
12/12/2007	1544							0.02		
12/13/2007	1038	20.4	0.00	0	0.22		58.1		11.3	
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	200 invalid			
12/13/2007	1357	19.9	0.38	0	0.022		67.9		13.4	1013
12/14/2007	903	20.4	0.32	0	0.22		69.5	0.01	8.3	1017
12/21/2007	1249	20.9	0.32	0	0.022		76.0	0.05	11.4	1012
12/26/2007	1121	20.9	0.36	0	0.002		72.1	0.03	10.2	1017
12/27/2007	1102	20.7	0.44	0	0.022		70.6	0.04	6.6	1017
12/27/2007	1347	20.2	0.32	0	0.022		76.8		9	1016
12/27/2007	1512	20.3	0.34	0	0.022		80.5		8.4	1017
1/2/2008	1114	20.8	0.40	0	0.022		50	0.02	16.3	1012

Tracer Test	#1 (10 cfm t	o INJ2, ~7%	и́ Н2)						
1/21/2008	1046 Test s	start							
1/21/2008	1203	13.3	0.48	0	0.10	75.6	0.03	10.0	1007
1/21/2008	1335	14.0	0.42	0	0.22	69.6		11.2	1006
1/21/2008	1504	14.6	0.40	0	0.22	75.5		10.9	1006
1/22/2008	939	16.7	0.36	0.02	0.22	75.3	0.02	6.6	1011
1/22/2008	1358	16.9	0.32	0	0.10	79.2		8.6	1009

Phase II Piezometer Monitoring Data

Well ID \_\_\_P1\_\_\_\_ Depth \_\_\_18\_

Well or Injection Gas Sample

Well Marbient Air

O2 CO2 Propane H2 He RH Pressure Temperature Barometric pressure

Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C0) (mbar)

				well or	Injection G	as Sampie			well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/23/2008	1004	17.9	0.34	0	0.22		77.1	0.06	8.9	1007
1/23/2008	1150*	17.6								

Tracer Test	#2 (20 cfm t	o INJ2, ~8%	6 H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1222	12.2	0.42	0	1.2	68.5		13.3	1015
1/18/2008	1339	12.6	0.38	0	1.1	69.9		16.1	1014
1/18/2008	1459	12.7	0.36	0	1.1	55.5	0.02	17.7	1014
1/19/2008	920	14.0	0.46	0	0.79	60.7	0.02	7.4	1019
1/19/2008	1121*	13.1	0.46	0	0.75	43.0		18.9	1018

Tracer Test	#3 (30 cfm t	o INJ2, ~4%	6 H2)						
1/30/2008	1036 Test s	start							
1/30/2008	1129	11.9	0.52	0	0.77	83.4	0.04	10.0	1020
1/30/2008	1245	11.4	0.50	0	0.81	77.4		11.2	1019
1/30/2008	1449	11.3	0.48	0	0.81	66.4	0.06	15.0	1018
1/31/2008	1006	5.5	0.52	0	0.66	81.9	0.07	9.4	1019
1/31/2008	1144	5.7	0.52	0	0.46	81.0		9.6	1018
1/31/2008	1407	7.2	0.52	0	0.22	81.6	0.10	8.7	1016
1/31/2008	1435								
1/31/2008	1535	10.5	0.52	0	0.22	84.9	0.05	8.4	1014

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P1\_\_\_\_ Depth \_\_\_\_18\_ Well or Injection Gas Sample Well **Ambient Air O**<sub>2</sub> CO<sub>2</sub> H<sub>2</sub> RH **Pressure** Temperature **Barometric pressure** Propane He Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (mbar) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1356 19.5 0.40 0.002 59.0 1010 16.4 1/28/2008 1633 18.8 0.44 0 0.001 74.6 0.07 8.9 1012 1/29/2008 8.9 2.2 5.1 821 0.54 80.8 0.05 1017 1/29/2008 Final O2\* 8.9 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1152 17.3 0.26 0 0.010 73.2 0.08 11.2 1019 1358 15.8 0.30 78 0.08 2/5/2008 0.010 12.8 1018 14.0 0.38 0.010 2/5/2008 1521 0 47.1 22.5 1019 2/5/2008 1605 12.4 0.38 0.005 54.5 19.6 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 1545 0.3 0.42 0 0.86 56.7 22.3 1016 2/7/2008 1634 0.3 0.42 0.66 56.8 20.1 1016 2/8/2008 1027 0.2 0.32 0 1.2 68.6 10.0 1017 0.2 1.3 2/8/2008 1100 0.30 0 74.3 1017 11.1

**Phase II Piezometer Monitoring Data** Well ID P1\_\_\_\_ Depth \_\_\_\_\_18\_ Well or Injection Gas Sample Well **Ambient Air Barometric pressure**  $O_2$ CO<sub>2</sub> Propane H<sub>2</sub> He RH **Pressure** Temperature Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (mbar) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1430 19.1 0.40 0.22 61.7 1013 13.8 1/17/2008 1529 18.0 0.40 0 0.22 44.2 0.04 19.0 1012 17.0 1/17/2008 1556 0.40 0.82 38.8 20.2 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1055 5.4 0.40 0.62 78.4 0.09 1020 11.1 2/6/2008 1206 2.9 0.40 0.72 73.9 13.4 1020 2/6/2008 1301 1.5 0.40 0.56 73.0 14.5 1019 2/6/2008 1453 0.4 0.34 1.5 73.4 0.08 16.1 1017 0.3 0.32 2.0 2/6/2008 1551 57.7 19.1 1017 2/6/2008 1637 0.2 0.44 2.6 54.5 19.4 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 19.2 1124 0.28 0.01 69.8 15.1 1010 2/20/2008 1206 Test start 2/20/2008 1606 Test End 2/20/2008 17.3 0.34 0.005 45.1 22.8 1616 1008 923 0.24 1005 2/21/2008 18.0 0 0.01 73.9 10.8 0 82 2/22/2008 1030 18.7 0.24 0.01 9.8 1003

Well ID P1\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth \_\_\_\_\_18\_ Well or Injection Gas Sample Well **Ambient Air** Barometric pressure  $O_2$ CO2 Propane H<sub>2</sub> He RH **Pressure** Temperature Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (mbar) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 725 19.1 0.44 0.08 0.005 88.8 4.1 1017 2/27/2008 1553 18.8 0.2 0.005 29.3 39 1009 1044 0 2/28/2008 19.9 0.18 0.01 73.8 15.7 1008 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1455 19.1 0.1 0.005 47.4 1009 31.1 3/3/2008 1038 19.1 0.12 0.002 63.1 14.8 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 949 3/4/2008 19.1 0.16 0.01 57.7 1013 14 3/7/2008 1049 19 0.06 0.01 60.8 18.3 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/10/2008 1047 19.1 0.12 0.022 62.6 16.3 1016

Phase II Piez	zometer M	onitoring D	ata	Well ID	P1		Depth	18_		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #4 ( 2	. 45-minutes	s pulses: da	ilv 15-minut	tes pulses w	//30cfh con	stant flow)			
	(2	,	p and do, and							
Ontimization	Test #5 (20	ofm to IN I	2 for 125 mi	inutes while	maintaina 1	30 ofh the r	act of the tim	o - 20% N2 1	0% H2 & LPG)	
Optimization	1651 #5 (20	CIIII TO IING	2 101 125 1111	nutes write	mainaing .			le, ~00 /6 INZ, 1	0 % 112 & LFG)	
	T			000/ NO	400/ 110 0 1	50)				
Optimization	Test #6 (50	) cth to P4-1	8 & P4-28;	~80% N2, 1	10% H2 & L	PG)				
3/20/2008	1330 Start	Test								
3/26/2008	1014	20.3	0.16	0	0.005		53.8		11.8	1017
3/28/2008	936	20.0	0.24	0	0.01		57.6		9.7	1009
3/31/2008	937	20.0	0.24	0	0.01		72.8		8.6	1013
4/2/2008	1100	18.7	0.22	0.3	0.022		60.3		15.9	1008
Optimization	Test #7 (20	) cfh to P4-1	8,28, -38	(60 cfh tota	al); ~80% N2	2, 10% H2	& LPG)			
4/2/2008	1233 Start	Test								
4/4/2008	945	17.6	0.18	0.56	0.022		57.7		13.1	1013
4/7/2008	1414	17.5	0.24	0.7	0.022		61.0		19.2	1011
Optimization	Test #7B (3	30 cfh to P4	-18, & P4-2	8 (60 cfh to	tal); ~80% N	N2, 10% H2	2 & LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1112	16.2	0.16	1.0	0.01		66.4		15.0	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P1\_\_\_\_ Depth \_\_\_\_\_18\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)		

Date	111110	(,,,)	(70)	(70)	(,,,)	(рр) (70)	( 110)	(IIIbai)
Optimization	Test #7C (	50 cfh to P4	-18. & P4-2	8 (100 cfh t	otal): ~79%	N2, 10% H2 & LPG, 1	% CO2)	
	1121 Start			(100 0111		, , , , , , , , , , , , , , , , , , , ,		
4/11/2008		17.4	0.22	0.8	0.0	52.3	22.3	1012
4/16/2008	1033	15.1	0.20	1.26	0.01	50.1	15.9	1011
4/22/2008	1021	16.1	0.26	1.12	0.005	55.6	17.4	1009
4/25/2008	1004	9.7	0.28	3.0	0.010	43.9	23.2	1015
4/29/2008	1114	12.3	0.28	2.5	0.005	55.8	23.8	1007
5/5/2008	1318	10.6	0.26	3.0	0.010	49.2	36.1	1001
5/13/2008	940	8.1	0.28	5.0	0.002	21.2	34.6	1007
5/20/2008	939	11.9	0.34	2.5	0.002	34.2	26.6	1004
5/23/2008	1525	8	0.36	4.0	0.005	28.3	29.8	990
5/27/2008	911	13.1	0.52	2.5	0.002	44.6	17.0	1007
6/4/2008	913	11.7	0.46	3.0	0.005	36.8	25.8	1002
6/12/2008	1205	8.4	0.50	4.5	0.005	26.4	42.0	1003
6/20/2008	1032	8.8	0.60	4.0	0.046	30.2	40.1	1005
6/25/2008	1053	8.8	0.62	3.5	0.005	36.9	33.0	1005
7/2/2008	1154	9.3	0.76	3.5	0.010	66.4	30.4	1004
7/7/2008	1141	7.6	0.66	4.5	0.046	51	36.3	998
7/18/2008	1106	8.6	0.84	4	0.002	71.9	26.0	
7/24/2008	1023	8.5	0.92	4.0	0.005	53.0	26.5	1005
7/31/2008	1019	8.5	1.08	3.5	0.010	54.0	25.6	1003
8/7/2008	900	7.5	1.08	4.5	0.010	46.1	20.6	1004
8/12/2008	1003	7.1	1.04	4.5	0.005	42.8	28.0	1002

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P1\_\_\_\_ Depth \_\_\_\_\_18\_

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #8 (10	00 cfh of 100	)% Propane	to P4-18, 8	& P4-28 (50	cfh to each	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	Tubing to P	1 cut at all	points, will r	neasure ne	xt visit					999
9/29/2008	Tubing to P	1 cut again	at all points	5,						
11/17/2008	1136	15.3	1.66	2.5	0.005		80.5		26.6	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_\_\_33\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1355	19.9	0.68	0	0.002	100,000	78.6	0.06	10.9	1020
12/12/2007	1543							0.06		
12/13/2007	1040	20.4	0	0	0.22		63.4		10.5	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	200 invalid			
12/13/2007	1359	12.7	0.80	0	2.2		69.1		13.2	1013
12/14/2007	904	14.5	0.90	0	0.75		66.3	0.02	8.6	1017
12/21/2007	1252	20.6	1.24	0	0.022		78.2	0.03	11.1	1012
12/26/2007	1125	20.9	1.2	0	0.002		71.6	0.02	10.6	1017
12/27/2007	1105	20.5	1.28	0	0.022		77.4	0.03	6.5	1017
12/27/2007	1349	20.2	1.04	0	0.022		81		9	1016
12/27/2007	1514	20.2	1.04	0	0.022		82.5		8.3	1017
1/2/2008	1118	20.5	1.2	0	0.022		44.7	0.03	18.1	1012

Tracer Test #	#1 (10 cfm to	INJ2, ~7%	H2)						
1/21/2008	1046 Test st	art							
1/21/2008	1204	7.7	0.44	0	0.046	77.0	0.05	10.0	1007
1/21/2008	1336	6.9	0.42	0	0.046	71.6		11.1	1006
1/21/2008	1506	6.6	0.42	0	0.022	76.1		11.0	1006
1/22/2008	942	6.9	0.48	0	0.022	75.9	0.03	6.7	1011
1/22/2008	1400	6.9	0.46	0	0.046	79.5		8.7	1009
1/23/2008	1006	10.8	0.58	0	0.022	78.0	0.04	8.0	1007
1/23/2008	1153*	10.1							

Phase II Piezometer Monitoring Data

Well ID \_\_\_P1 \_\_\_\_ Depth \_\_\_33 \_\_\_

Well or Injection Gas Sample

Well Ambient Air

				Well or		Well	Ambient Air			
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure								Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #	‡2 (20 cfm to	INJ2, ~8% l	H2)						
1/18/2008	1120 Test sta	art							
1/18/2008	1225	5.4	0.36	0	0.10	68.8		13.4	1015
1/18/2008	1340	5.8	0.34	0	0.046	70.7		15.2	1014
1/18/2008	1500	5.8	0.32	0	0.50	57.5	0.03	17.7	1014
1/19/2008	922	6.7	0.54	0	0.62	69.6	0.02	7.3	1019
1/19/2008	1129*	5.2	0.52	0		46.6		17.7	1018

Tracer Test #	‡3 (30 cfm to I	NJ2, ~4% l	H2)						
1/30/2008	1036 Test sta	ırt							
1/30/2008	1130	1.6	0.36	0	0.46	82.4	0.06	10.0	1020
1/30/2008	1246	1.3	0.34	0	0.1	75.3	3	11.3	1019
1/30/2008	1451	1.1	0.30	0	0.046	65.2	0.08	15.0	1018
1/31/2008	1008	1.8	0.32	0	1.9	80.6	0.09	9.5	1019
1/31/2008	1146	1.9	0.34	0	1.7	81.0	)	9.6	1018
1/31/2008	1409	2.2	0.32	0	1.5	80.3	0.10	8.7	1016
1/31/2008	1435								
1/31/2008	1536	2.4	0.34	0	1.1	81.9	0.06	8.4	1014

Phase II Pie	Phase II Piezometer Monitoring Data Well IDP1 Depth33												
				Well or	Injection G	as Sample			Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			
Tracer Test a	#4 (60 cfm to	INJ2, ~7%	H2)										
1/28/2008	1236 Test st	art											
1/28/2008	1357	17.3	0.86	0	0.002		63.0		15.6	1010			
1/28/2008	1634	10.7	0.74	0	0.98		78.0	0.09	8.8	1012			
1/29/2008	822	4.3	0.62	0	4.9		79.9	0.03	5.1	1017			
1/29/2008	Final O2*	4.3											
Tracer Test	#5 (90 cfm to	INJ2, ~3%	H2)										
2/5/2008	1015 Test st	art											
2/5/2008	1153	8.4	0.38	0	0.022		73.8	0.10	11.2	1019			
2/5/2008	1359	5.7	0.34	0	1.1		78.9	0.12	12.8	1018			
2/5/2008	1522	4.9	0.38	0	1.5		44.8		22.9	1019			
2/5/2008	1606	4.5	0.36		1.6		55.3		19.5	1018			
Tracer Test	#6 (30 cfm tot	al; 10 cfm to	o each INJ1	, 2, and 3; -	-8% H2)								
2/7/2008	1500 Test st	art											
2/7/2008	1547	0.6	0.18	0	0.046		55.2		22.8	1016			
2/7/2008	1636	0.5	0.16	0	0.10		55.6		20.3	1016			
2/8/2008	1029	0.6	0.14	0	6.6		70.0		10.0	1017			
2/8/2008	1101	0.6	0.12	0	6.6		72.4		11.1	1017			

Phase II Piezometer Monitoring Data Well IDP1 Depth33												
	ĺ			Well or	Injection G	as Sample	1		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)		
Tracer Test #	+7 (60 of m tot	tali 20 ofm t	a agab INI I4	2 and 2	E0/ U2\							
	900 Test sta		J each my i	, 2, and 3, ~	5% HZ)							
			0.54	0	2.0		72.6	0.05	10.0	4045		
1/17/2008		10.3	0.54					0.05	10.0	1015		
1/17/2008		9.5	0.52	0			74.4		10.7	1014		
1/17/2008	1432	8.2	0.72	0			64.3		13.8	1013		
1/17/2008		7.6	0.66	0			45.0	0.04	18.9	1012		
1/17/2008	1558	7.2	0.64	0	4.9		39.7		19.8	1012		
Tracer Test #			each to INJ1	, 2, and 3; ~	-4.5% H2)							
	1000 Test st											
2/6/2008		1.7	0.22	0			79.2	0.14	11.1	1020		
2/6/2008	1208	1.5	0.20	0	2.6		75.1		13.4	1020		
2/6/2008	1302	1.4	0.18	0	2.9		72.5		14.6	1019		
2/6/2008	1456	1.3	0.16	0	3.7		72.0	0.16	16.1	1017		
2/6/2008	1553	1.1	0.12	0	3.8		58.5		19.1	1017		
2/6/2008	1639	1.2	0.20	0	3.9		54.1		19.4	1017		
Optimization	Test #1 (90 d	ofm to INJ2	for 4 hours	then shut do	own: ~88%	N2. 10% H2	2. 1% CO2 8	k LPG)				
2/20/2008	,	17.8	0.56	0			69.7	,	15.2	1010		
	1206 Test st								-			
	1606 Test E											
2/20/2008		11.9	0.42	0.1	2.8		46.5		22.7	1008		
2/21/2008		17.3	0.54	0.02	0.022		73.2		10.7	1004		
2/22/2008		18.2	0.6	0.02	0.01		79.9		9.7	1003		

Phase II Pie	zometer Mor	nitoring Dat	ta	Well ID	P1		Depth	_33		
					Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #2 (30 d	ofm to INJ2	for 12 hours	then shut o	down; ~88%	N2, 10% F	12, 1% CO2	& LPG)		
	1845 Test St							, , , , , , , , , , , , , , , , , , ,		
	653 Test En									
2/26/2008			0.78	0.14	0.046		86.8		4.3	1017
2/27/2008	1556	18.1	0.56	0	0.002		28		38.5	1009
2/28/2008	1046	18.8	0.56	0	0.005		74.1		15.7	1007
Optimization	Test #3A (1 d	ofm to INJ2;	~88% N2,	10% H2, 1%	6 CO2 & LP	G)				
2/29/2008	1319 Test St	tart								
2/29/2008	1456	18.5	0.42	0	0.002		46.8		31.3	1009
3/3/2008	1039	19	0.52	0	0.002		59.6		14.8	1019
3/3/2008	1130 Test E	nd								
Optimization	Test #3B (1 o	ofm to INJ1,	INJ2 & INJ	3; ~88% N2	2, 10% H2, 1	1% CO2 & L	_PG)			
3/3/2008	1130 Test S	tart								
3/4/2008	950	19.1	0.56	0	0.005		56.9		14.1	1013
3/7/2008	1050	18.8	0.44	0	0.005		57.1		18.2	1018
3/7/2008	1306 Test E	nd								
Optimization	Test #3C (90	cfm to IN.I	1. INJ2 & IN	J3 for 15 m	inutes then	shut down:	~79% N2 1	0% H2 & LPG	i. 1% CO2)	
	1306 Start P		,				70 . 12,	2,2,1,2,0,21	,	
	1321 End Pu									
3/10/2008		19	0.52	0	0.005		61.7		16.3	1016

Phase II Piez	zometer Mor	nitoring Dat	ta	Well ID	P1		Depth	_33		
				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Ontimination	Tant #4 ( 0 )	15 minutos	sulses deili	. 45 minutos		Oofb const	ant flave)			
Optimization	Test #4 ( 2, 2	to-minutes	buises, daily	/ 15-minutes	s puises w/s	SOCITI CONSTA	ant now)			
0 11 11 11	T							000/ NO 40		
Optimization	Test #5 (20 c	ofm to INJ2	for 125 mini	utes while m	naintaing 30	off the res	t of the time	; ~80% N2, 10	% H2 & LPG)	
Optimization	Test #6 (50 c	ofh to P4-18	& P4-28; ~	80% N2, 10	% H2 & LP	G)				
3/20/2008	1330 Start T	est								
3/26/2008	1015	18.7	0.54	0.26	0.005		24.0		11.8	1017
3/28/2008	937	19.0	0.62	0.12	0.01		53.4		9.8	1009
3/31/2008	938	18.0	0.56	0.72	0.01		70.2		8.7	1013
4/2/2008	1102	10.3	0.34	6.5	0.46		65.7		16.1	1008
Optimization	Test #7 (20 c	ofh to P4-18	,28, -38 (6	60 cfh total)	; ~80% N2,	10% H2 & I	LPG)			
4/2/2008	1233 Start T	est								
4/4/2008	946	8.9	0.26	7.5	0.046		56.2		13.1	1013
4/7/2008	1415	11.8	0.38	4.5	0.01		60.4		19.3	1011
Optimization	Test #7B (30	cfh to P4-1	8, & P4-28	(60 cfh total	); ~80% N2	, 10% H2 &	LPG)			
4/7/2008	1458 Start T	est								
4/9/2008	1114	12.6	0.34	3.5	0.005		62.0		15.0	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_\_\_33\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

				. ,		- ;; ; ; ; ; ; ; ; ; ; ; ; ; ; ; ; ; ;		
Optimization	Test #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tot	al); ~79% N	I2, 10% H2 & LPG, 1%	CO2)	
4/10/2009	1121 Start To	est						
4/11/2008	1240	13	0.46	3.0	0.0	62.8	22.7	1012
4/16/2008	1034	10.7	0.46	4.0	0.005	48.9	16.0	1011
4/22/2008	1022	12.5	0.56	2.5	0.005	57.3	17.5	1009
4/25/2008	1005	10.4	0.54	3.0	0.010	43.7	23.2	1015
4/29/2008	1115	10.0	0.54	3.5	0.005	55.3	24.0	1007
5/5/2008	1319	8.0	0.48	4.5	0.005	46.2	36.5	1001
5/13/2008	941	6.3	0.54	5.5	0.002	21.3	34.6	1007
5/20/2008	940	9.0	0.66	4.5	0.002	32.5	26.1	1004
5/23/2008	1526	9.2	0.56	4.0	0.005	28.1	29.7	990
5/27/2008	912	9.4	0.80	4.0	0.001	45.0	16.9	1007
6/4/2008	914	5.8	0.54	7.0	0.005	36.5	25.6	1002
6/12/2008	1207	4.8	0.54	7.0	0.005	26.5	42.2	1003
6/20/2008	1035	6.4	0.60	6.0	0.010	27.6	40.0	1005
6/25/2008	1054	4.9	0.66	6.5	0.005	36.8	33.1	1005
7/2/2008	1155	5.5	0.72	6.0	0.005	67.4	30.4	1004
7/7/2008	1142	5.2	0.66	6.0	0.01	58.6	36.3	998
7/18/2008	1109	4.2	0.84	7.0	0.002	73.1	26.3	
7/24/2008	1024	5.1	0.90	7.0	0.005	54.6	26.5	1005
7/31/2008	1021	4.7	1.02	7.0	0.005	52.7	25.6	1003
8/7/2008	901	4.4	1.04	7.5	0.005	38.1	20.6	1004
8/12/2008	1004	4.5	1.00	7.0	0.005	43.6	28.0	1002

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_\_\_33\_\_\_\_

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #8 (100	cfh of 100%	6 Propane t	o P4-18, &	P4-28 (50 c	fh to each p	oint)			
9/8/2008	0905 Test S	tart								
9/8/2008	Tubing to P1	cut at all p	oints, will m	easure next	t visit					999
9/29/2008	Tubing to P1	l cut again a	at all points,							
11/17/2008	1138	3.7	1.94	30	0.005		38.2		27.5	1014

Phase II Piezometer Monitoring Data	Well IDP1	Depth48
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				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	<b>Temperature</b>	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1357	19.0	0.78	0	0.002	100,000	78.2	0.04	11.0	1020
12/12/2007	1544							0.11		
12/13/2007	1043	20.4	0	0	0.022		67.0		9.8	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	00 invalid			
12/13/2007	1400	18.6	1.14	0	0.22		68.6		13.1	1013
12/14/2007	906	18.7	1.3	0	0.22		67.1	0.03	9.0	1017
12/21/2007	1254	18.7	2.02	0	0.022		77.1	0.05	11.0	1012
12/26/2007	1128	18.9	2.04	0	0.002		71.7	0.08	10.6	1017
12/27/2007	1107	18.7	2.18	0	0.022		80.1	0.03	6.5	1017
12/27/2007	1350	18.5	1.84	0	0.022		79.6		8.9	1016
1/2/2008	1120	18.6	2.04	0	0.022		42.6	0.03	18.6	1012

Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1206	19.1	1.52	0	0.010	76.3	0.06	10.0	1007
1/21/2008	1337	19.0	1.36	0	0.010	72.0	)	11.1	1006
1/22/2008	943	19.1	1.64	0	0.010	75.0	0.00	6.7	1011
1/22/2008	1401	19.0	1.58	0	0.010	78.	5	8.7	1009
1/23/2008	1007	19.2	1.66	0	0.022	77.9	0.06	8.8	1007
1/23/2008	1154*	19.1							

Well ID Р1 Phase II Piezometer Monitoring Data Depth 48

1/31/2008

1/31/2008

1435

1537

18.5

2.14

Phase II Piezometer Monitoring Data Well IDP1 Depth48										
				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)							
1/18/2008	1120 Test s	start								
1/18/2008	1227	18.8	1.44	0	0.010		64.3		13.4	1015
1/18/2008	1343	18.8	1.38	0	0.005		68.1		15.1	1014
1/18/2008	1502	18.8	1.34	0	0.022		56.4	0.02	17.7	1014
1/19/2008	925	19.2	1.88	0	0.010		58.9	0.02	7.3	1019
1/19/2008	1126*	18.6	1.84	0	0.002		47.4		16.8	1018
Tracer Test #	3 (30 cfm to	INJ2, ~4%	H2)							
1/30/2008	1036 Test s	start								
1/30/2008	1132	18.5	2.10	0	0.010		81.8	0.04	10.1	1020
1/30/2008	1247	18.4	2.06	0	0.010		76.1		11.3	1019
1/30/2008	1453	18.2	2.04	0	0.005		65.7	0.08	14.9	1018
1/31/2008	1009	18.4	2.10	0	0.010		80.0	0.09	9.5	1019
1/31/2008	1147	18.5	2.08	0	0.010		81.2		9.6	1018
1/31/2008	1410	18.5	2.12	0	0.010		79.7	0.12	8.7	1016

0.022

0

0.08

81.0

8.4

1014

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P1\_\_\_\_ Depth 48 Well or Injection Gas Sample Well **Ambient Air** CO2 Temperature Barometric pressure 0, Propane H<sub>2</sub> He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1359 0 0.001 67.2 1/28/2008 18.2 2.30 14.6 1010 1/28/2008 1637 18.4 2.24 0.02 0.010 77.0 0.08 8.8 1012 1/29/2008 18.3 2.36 0.010 0.03 5.1 1017 824 80.4 1/29/2008 Final O2\* 18.3 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1155 18.0 1.32 0 0.010 2/5/2008 74.4 0.12 11.2 1019 2/5/2008 1401 1.32 0 0.010 80.4 0.17 17.9 12.8 1018 0.010 2/5/2008 1523 1.40 0 22.8 18.4 45.6 1019 2/5/2008 0 55.3 1607 18.3 1.40 0.010 19.0 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 1548 18.3 1.54 0 0.022 53.6 23.6 1016 1.52 1636 55.1 2/7/2008 18.3 0 0.022 20.4 1016 1.42 0 0.022 2/8/2008 1030 18.0 69.1 10.0 1017

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_48\_\_\_\_\_

				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #7	7 (60 cfm tot	al; 20 cfm to	o each INJ1	, 2, and 3, -	~5% H2)				
1/17/2008	1/17/2008 900 Test start								
1/17/2008	1136	19.1	1.24	0	0.022	67.0	0.03	10.0	1015
1/17/2008	1238	19.0	1.22	0	0.22	68.6		10.7	1014
1/17/2008	1435	19.2	1.66	0	0.022	62.4		13.8	1013
1/17/2008	1534	19.1	1.62	0	0.22	44.8	0.02	18.6	1012
1/17/2008	1559	19.1	1.64	0	0.22	39.7		19.4	1012

Tracer Test #8	3 (90 cfm tot	al; 30 cfm e	ach to INJ1	, 2, and 3; -	~4.5% H2)				
2/6/2008	1000 Test s	start							
2/6/2008	1058	18.0	1.34	0	0.010	76.7	0.12	11.2	1020
2/6/2008	1210	18.0	1.34	0	0.010	74.5		13.4	1019
2/6/2008	1303	17.9	1.32	0	0.010	73.2		14.5	1018
2/6/2008	1457	17.8	1.28	0	0.010	72.3	0.10	16.4	1017
2/6/2008	1554	17.6	1.24	0	0.010	58.4		19.0	1017

Well ID \_\_\_\_P1\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth 48 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure 0, CO2 Propane H<sub>2</sub> He RH **Pressure** Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 1127 18 2/20/2008 1.72 0.01 68.7 15.2 1010 2/20/2008 1206 Test start 2/20/2008 1606 Test End 1619 2/20/2008 17.5 1.5 0 0.022 46.9 22.6 1008 925 2/21/2008 73.9 17.7 1.62 0 0.01 10.6 1005 2/22/2008 1032 17.7 1.64 0.005 79.9 9.7 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 2 731 18.1 0.08 0.005 86.7 1017 4.3 1558 1.4 28.2 38.3 2/27/2008 16.9 0.002 1009 1047 1.42 2/28/2008 17.4 0 0.005 72.5 15.7 1007 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1458 17.1 1.18 0 0.002 48.1 31.8 1009 1040 1.36 0.002 3/3/2008 17.2 58.5 14.8 1019 3/3/2008 1130 Test End

Phase II Piezo	ometer Mor	nitoring Dat	ta	Well ID	P1		Depth4	8		
	Well or Injection Gas Sample									Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #3B (1 o	ofm to INJ1,	, INJ2 & INJ	3; ~88% N2	2, 10% H2, ′	1% CO2 & l	_PG)			
3/3/2008	1130 Test \$	Start								
3/4/2008	951	17.1	1.42	0	0.005		56.8		14.1	1013
3/7/2008	1051	16.9	1.18	0	0.005		57.4		18.1	1018
3/7/2008	1306 Test I	≣nd								
Optimization T	est #3C (90	cfm to INJ	1, INJ2 & IN	J3 for 15 m	inutes then	shut down;	~79% N2, 1	0% H2 & LPG,	1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
Optimization T	est #4 ( 2, 4	15-minutes	pulses; daily	/ 15-minute:	s pulses w/3	30cfh consta	ant flow)			
Optimization T	est #5 (20 d	ofm to INJ2	for 125 min	utes while n	naintaing 30	cfh the res	t of the time	; ~80% N2, 10°	% H2 & LPG)	
Optimization T	est #6 (50 d	ofh to P4-18	& P4-28; ~	80% N2, 10	% H2 & LP	G)				
3/20/2008	1330 Start	Test								
3/26/2008	1024	17.1	1.44	0	0.002		53.0		12.1	1017
3/28/2008	938	17.0	1.56	0	0.005		52.9		10.0	1009
3/31/2008	939	17.0	1.50	0	0.01		69.4		8.9	1013
4/2/2008	1104	17.1	1.42	0	0.01		58.3		16.1	1008

Well ID \_\_\_\_P1\_\_\_ **Phase II Piezometer Monitoring Data** Depth 48 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure 0, CO2 Propane H<sub>2</sub> He RH Pressure Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 947 0 4/4/2008 16.9 1.44 0.01 56.2 13.2 1013 1416 1.54 0.0 0.005 4/7/2008 17.0 60.8 19.4 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 1.32 0.0 4/9/2008 1116 16.5 0.005 63.9 15.0 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 4/11/2008 1241 16.8 1.44 0.0 0.0 52.8 22.6 1012 4/16/2008 1035 16.6 1.40 0.0 0.002 48.5 16.1 1011 4/22/2008 1024 16.7 1.48 0.02 0.005 53.5 17.7 1009 4/25/2008 1006 16.8 1.46 0.02 0.005 44.7 23.2 1015 1116 16.6 1.40 0.04 0.005 52.1 24.0 1007 4/29/2008 1320 5/5/2008 16.0 1.36 0.06 0.005 36.6 44.7 1001 5/13/2008 944 16.2 1.46 0.08 0.001 26.3 34.2 1007 1.56 5/20/2008 942 16.5 0.01 0.002 35.8 25.6 1004 5/23/2008 1527 16.0 1.30 0.02 0.005 28.6 29.5 990 913 1.72 0.001

46.0

17.1

5/27/2008

16.4

0.03

1007

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_48\_\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
6/4/2008	916	15.7	1.56	0.03	0.002		37.0		25.1	1002
6/12/2008	1208	14.9	1.50	0.42	0.002		22.7		42.6	1003
6/20/2008	1036	14.6	1.44	0.5	0.005		26.5		40.7	1005
6/25/2008	1055	14.3	1.44	0.56	0.005		36.1		33.4	1005
7/2/2008	1156	13.8	1.48	0.64	0.005		67.2		30.3	1004
7/7/2008	1144	13.5	1.36	0.68	0.005		49.8		36.3	998
7/18/2008	1112	13.2	1.56	0.88	0.001		69.3		26.7	
7/24/2008	1026	13.0	1.56	1.0	0.005		52.9		26.5	1005
7/31/2008	1022	12.7	1.72	1.1	0.005		50.1		25.5	1003
8/7/2008	902	12.4	1.68	1.2	0.005		37.3		20.6	1004
8/12/2008	1005	12.0	1.58	1.24	0.005		43.3		28.1	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane t	o P4-18, & l	P4-28 (50 ct	fh to each p	oint)			
9/8/2008	0905 Test S	Start								
9/8/2008	Tubing to P	1 cut at all	points, will r	neasure ne	xt visit					999
9/29/2008	Tubing to P	1 cut again	at all points	5,						
11/17/2008	1140	0.0	1.72	30	0.005		60.9		28.7	1014

Phase II Piezometer Monitoring Data Note - slight flow restriction on P1-68 feet

Well ID \_\_\_\_P1\_\_\_ Depth \_\_\_\_68\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1358	17.0	0.72	0	0.002	8x10^5	71.0	0.10	11.1	1020
12/12/2007	1544							0.12		
12/13/2007	1041	20.4	0	0	0.22		65.7		10.1	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	200 invalid			
12/13/2007	1400	12.7	1.98	0	0.22		67.9		12.9	1013
12/14/2007	906	13.0	2.22	0	0.22		64.7	0.02	9.4	1017
12/21/2007	1256	13.2	3.02	0	0.022		75.0	0.01	10.9	1012
12/26/2007	1130	13.3	3.06	0	0.002		72.1	0.09	10.3	1017
12/27/2007	1108	13.5	3.34	0	0.022		77.0	0.03	6.3	1017
12/27/2007	1352	13.4	2.8	0	0.022		75.2		8.8	1016
1/2/2008	1121	13.4	3.06	0	0.022		41.4	0.01	19.0	1012

Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1208	20.9	0	0	0.002	76.5	0.02	10.0	1007
1/21/2008	1336	20.3	0.26	0	0.002	72.4		11.1	1006
1/22/2008	944	20.2	0.44	0	0.005	75.8	-0.02	6.8	1011
1/23/2008	1009	19.0	0.72	0	0.010	77.8	0.20	8.9	1007
1/23/2008	1156*	18.3		0					

Phase II Piezometer Monitoring Data Note - slight flow restriction on P1-68 feet Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_\_\_68\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			

Tracer Test #2	2 (20 cfm to	INJ2, ~8% I	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1503	19.0	0.44	0	0.010	57.7	0.02	17.7	1014
1/19/2008	928	20.4	0.46	0	0.002	59.8	0.02	7.2	1014
1/19/2008	1127*	18.2	0.98	0	0.001	46.3		16.3	1018

Tracer Test #3	3 (30 cfm to l	INJ2, ~4% l	H2)							
1/30/2008	1036 Test s	start								
1/30/2008	1134	19.0	0.90	0	0.010		80.7	0.02	10.2	1020
1/30/2008	1249	18.9	1.02	0	0.001		4.1		11.5	1019
1/30/2008	1455	18.4	1.28	0	0.002	(	6.3	0.08	15.1	1018
1/31/2008	1010	18.8	1.08	0	0.005		9.1	0.08	9.5	1019
1/31/2008	1148	18.4	1.12	0	0.005		9.1		9.6	1018
1/31/2008	1412	18.4	1.18	0	0.005		9.6	0.09	8.7	1016
1/31/2008	1435									
1/31/2008	1539	18.3	1.16	0	0.005		31.5	0.25	8.4	1014

Phase II Piez Note - slight fl				Well ID	P1		Depth	_68		
rtoto ongricii	ow roomono	110111100	1001	Well or	Injection G	as Sample	•		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #4	1 (60 cfm to	IN.12 ~7% I	H2)							
	1236 Test									
1/28/2008	1401									
1/29/2008	825	20.3	0.02	0	0.005		79.9	0.04	5.0	1017
1/29/2008	Final O2*	20.3								
Tracer Test #5	(90 cfm to	INJ2, ~3% I	H2)							
2/5/2008	1015 Test :	start								
2/5/2008	1156	18.7	0.62	0	0.005		79.1	0.04	11.2	1019
2/5/2008	1402	18.5	0.64	0	0.005		77.8	0.13	12.8	1018
2/5/2008	1524	19.0	0.68	0	0.000		43.4		22.5	1019
2/5/2008	1609	18.7	0.78	0	0.001		55.4		18.3	1018
Tracer Test #6	6 (30 cfm tot	al; 10 cfm to	each INJ1	, 2, and 3; ~	-8% H2)					
2/7/2008	1500 Test :	start								
2/7/2008	1550	17.6	1.06	0	0.000		48.9		24.8	1016
2/7/2008	1638	17.6	1.06	0	0.005		53.1		20.5	1016
2/8/2008	1031	17.2	1.06	0	0.010		69.7		10.0	1017

**Phase II Piezometer Monitoring Data** Well ID P1 Depth 68 Note - slight flow restriction on P1-68 feet Well Well or Injection Gas Sample **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Time (%) Date (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 0 1239 19.6 0.24 0.002 66.3 10.8 1014 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 11.2 2/6/2008 1059 18.8 0.62 0 0.005 75.3 0.07 1020 2/6/2008 0.64 0 73.5 1211 18.6 0.002 13.4 1020 2/6/2008 1305 0.68 0 0.001 72.1 18.2 14.6 1019 0.72 0 70.3 2/6/2008 1458 17.8 0.005 0.12 16.0 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 1128 0 68 2/20/2008 16.6 1.78 0.01 15.2 1010 2/20/2008 1206 Test start 2/20/2008 1606 Test End 2/20/2008 1620 1.56 0 0.005 1008 16.0 45.1 22.4 2/21/2008 926 1.62 0 0.005 16.2 74 10.5 1005 2/22/2008 1033 15.1 1.98 0 0.005 79.2 9.7 1003

**Phase II Piezometer Monitoring Data** Well ID P1 Depth 68 Note - slight flow restriction on P1-68 feet Well Well or Injection Gas Sample **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Time (%) Date (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 732 15.1 2.48 0.08 0.005 86.1 1017 4.3 1.84 26.8 2/27/2008 1602 14.1 0 0.001 38.1 1009 2/28/2008 1049 1.88 0 1007 14.2 0.005 71.4 15.7 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 0 1459 13.9 1.62 0.002 44.2 31.8 1009 1041 3/3/2008 14.7 1.64 0 0.001 56.3 14.9 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 953 14.3 1.78 0 0.002 56.4 14.2 1013 1052 14.5 1.48 0 0.005 56.4 18.2 3/7/2008 1018 3/7/2008 1306 Test End

**Phase II Piezometer Monitoring Data** Well ID P1 Depth 68 Note - slight flow restriction on P1-68 feet **Well or Injection Gas Sample** Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Time (%) (%) Date (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 0 3/26/2008 1025 16.9 1.34 0.002 45.7 12.1 1017 1.74 0 52.3 3/28/2008 939 16.2 0.005 10.1 1009 1.76 0 3/31/2008 940 15.7 0.01 69.2 9.0 1013 4/2/2008 1105 15.5 1.72 0 0.005 56.2 16.2 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 1.76 949 0.005 4/4/2008 15.0 0 57.2 13.3 1013 4/7/2008 1417 14.8 2.02 0.0 0.005 60.4 19.5 1011

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_P1\_\_\_\_ Depth \_\_\_\_68\_\_\_\_

5/27/2008

6/4/2008

6/12/2008

6/20/2008

6/25/2008

914

917

1209

1039

1056

13.6

13.2

12.9

12.9

12.9

1.58

1.76

1.98

1.94

1.98

0.01

0.0

0.0

0.0

0.0

0.001

0.002

0.002

0.000

0.005

9	ow restriction			Well or	Injection G	as Sample	1		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
	•		` ′		`	`` '	` '	,		,
Optimization 7	Test #7B (30	cfh to P4-1	8, & P4-28	(60 cfh total)	); ~80% N2,	10% H2 &	LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1117	14.3	1.70	0.0	0.002		60.0		14.9	1009
	•						•			
Optimization 7	Test #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tota	al); ~79% N	2, 10% H2	& LPG, 1% (	CO2)		
4/10/2009	1121 Start <sup>-</sup>	Test								
4/11/2008	1242	14.3	1.86	0.0	0.005		49.5		22.6	1012
4/16/2008	1036	15.4	1.66	0.0	0.002		47.5		16.2	1011
4/22/2008	1025	15	1.84	0.0	0.005		52.1		17.7	1009
4/25/2008	1007	15	1.84	0.0	0.005		44.1		23.1	1015
4/29/2008	1117	14.3	1.86	0.0	0.005		52.6		24.0	1007
5/5/2008	1321	13.5	1.82	0.0	0.005		43.4		36.7	1001
5/13/2008	945	13.8	1.94	0.02	0.001		21.1		34.2	1007
5/20/2008	944	14.0	2.08	0.02	0.001		35.8		25.2	1004
5/23/2008	1529	13.4	1.80	0.02	0.005		26.8		29.3	990
						,		•		•

46.0

38.0

21.7

24.8

33.7

17.3

24.9

42.9

41.8

33.7

1007

1002

1003

1005

1005

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_\_P1\_\_\_\_\_ Depth \_\_\_\_68\_\_\_\_

Note - slight flow restriction on P1-68 feet

Note - Siight iit				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/2/2008	1158	12.8	1.98	0.0	0.005		64.2		30.4	1004
7/7/2008	1145	12.4	1.8	0	0.002		54.1		36.3	998
7/18/2008	1113	12.4	2.06	0.02	0.002		68.9		26.7	
7/24/2008	1028	12.4	2.06	0.0	0.005		53.7		26.7	1005
7/31/2008	1023	12.5	2.20	0.0	0.005		50.9		25.5	1003
8/7/2008	903	12.4	2.08	0.0	0.005		40.7		20.4	1004
8/12/2008	1006	12.3	2.00	0.02	0.002		44.4		28.1	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane to	P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test S	Start								
9/8/2008	Tubing to P	1 cut at all	points, will n	neasure nex	t visit					999
9/29/2008	Tubing to P	1 cut again	at all points	,						
11/17/2008	1141	9.8	2.24	2.0	0.005		55.5		29.2	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1216	20.4	0.04	0	0.002	40,000	84.5	0.01	12.2	1020
12/12/2007	1538							0.08		
12/13/2007	910	17.7	0	0	0.22		72.1		8.4	1016
12/13/2007	948	17.1	0	0	0.22		71.8		11.3	1016
12/13/2007	1046									1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	00 invalid			
12/13/2007	1319							0.07		
12/13/2007	1333	1.4	0.22	0	5.9		74.9		16.8	1013
12/13/2007	1501	0.7	0.26	0	7.9		88.1		13.4	1013
12/13/2007	1532	0.6	0.24	0	7.9		86.6		12.8	1013
12/14/2007	838	1.4	0.24	0.18	3.2		72.0	0.02	6.5	1016
12/21/2007	1143	19.2	0.38	0	0.22		83.2	0.04	9.9	1013
12/26/2007	1146	19.4	0.3	0	0.022		85.1	0.04	10.6	1017
12/27/2007	1000	19.8	0.34	0.02	0.22		73.7	0.02	6.1	1018
12/27/2007	1257	18.9	0.26	0	0.22		81.7		9.2	1016
12/27/2007	1429	18.8	0.24	0	0.46		86.6		8.4	1017
12/27/2009	1545	18.7	0.26	0	0.46		88.8	0.03	7.5	1017
1/2/2008	1018	10.6	0.38	0	0.022		61.8	0.03	17.7	1012
1/21/2008	958¹	0.7	0.02	0	0.005		89.1		8.7	1007
1/21/2008	1005²	1.6	0.02	0	0.010		85.1		8.4	1007
1/21/2008	1010³	1.4	0.02	0	0.010		90.0		8.2	

Phase II Pi	ezometer Mor	nitoring Dat	ta	Well ID	P2		Depth	_18		
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1147	2.2	0.04	0	0.010	80.1	0.04	9.7	1008
1/21/2008	1304	1.3	0.04	0	0.046	73.6		10.1	1006
1/21/2008	1458	1.7	0.04	0	0.010	77.1	0.02	10.7	1006
1/21/2008	1619	1.7	0.04	0	0.046	77.8		10.8	1006
1/22/2008	1039	1.5	0.12	0	0.76	83.3	0.06	6.4	1011
1/22/2008	1329	1.3	0.08	0	1.0	90.9		7.5	1009
1/23/2008	1044	2.1	0.1	0	2.4	96.3	0.04	7.6	1008
1/23/2008	1157*	1.4							

Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1149	1.4	0.04	0	0.022	96.5		13.1	1015
1/18/2008	1243	1.3	0.06	0	0.046	93.8	0.02	13.8	1014
1/18/2008	1332	1.5	0.06	0	0.046	90.0		15.3	1014
1/18/2008	1507	1.5	0.04	0	0.046	75.8	0.04	18.3	1014
1/19/2008	932	1.7	0.18	0	4.0	88.4	0.04	8.4	1019
1/19/2008	1113*	1.0	0.14		4.8	60.7		19.1	1018

Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_18\_\_\_\_ Phase II Piezometer Monitoring Data Ambient Air Well or Injection Gas Sample Well Temperature Barometric pressure  $O_2$ CO<sub>2</sub> Propane  $H_2$ Не RH Pressure Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1137 0.0 1/30/2008 0 0 0.10 93.1 0.06 10.2 1020 1/30/2008 1255 0.0 0 0.046 92.9 12.0 1019 1/30/2008 1501 0.0 0.046 82.6 0.04 15.3 1018 0 1/31/2008 1017 0.0 87.2 4.0 0.07 9.3 1019 1/31/2008 1151 0 0 3.7 83.3 9.6 1018 1/31/2008 1423 3.7 86.5 0.08 8.3 0 1015 1/31/2008 1435 1/31/2008 1545 84.1 0.06 0 0 3.6 8.3 1014 1/31/2008 1612 0 3.6 85.4 8.3 1014

Tracer Test #4	(60 cfm to	INJ2, ~7%	H2)						
1/28/2008	1236 Test s	start							
1/28/2008	1314	12.8	0.12	0	0.010	96.6		10.3	1010
1/28/2008	1445	8.0	0.10	0	0.22	92.1	0.08	12.8	1011
1/28/2008	1618	3.4	0.06	0	2.1	86.0	0.06	9.6	1012
1/29/2008	847	0	0.08	0	7.2	92.2	0.06	5.0	1017
1/29/2008	Final O2*	0							

Phase II Piezo	ometer Mor	nitoring Dat	ta	Well ID	_P2		Depth	_18		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH		Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #5	(90 cfm to	INJ2, ~3%	H2)							
2/5/2008	1015 Test s	start								
2/5/2008	1056	1.2	0	0	0.022		94.0	0.10	10.8	1019
2/5/2008	1200	0.5	0	0	0.46		93.2		11.2	1019
2/5/2008	1407	0.1	0	0	2.7		91.2	0.10	12.7	1018
2/5/2008	1527	0.1	0	0	3.0		56.7		19.4	1019
2/5/2008	1611	0	0	0	3.1		64.9		11.4	1018
Tracer Test #6	30 cfm tot	tal; 10 cfm to	each INJ1	, 2, and 3; ~	8% H2)					
2/7/2008	1500 Test :	start								
2/7/2008	1509	0.0	0	0	0.022		60.7		20.5	1016
2/7/2008	1600	0.0	0	0	0.10		41.8		28.1	1016
2/8/2008	927	0.0	0	0	9.0		88.3		8.7	1017
Tracer Test #7	' (60 cfm tot	al; 20 cfm to	each INJ1	, 2, and 3, ~	-5% H2)					
1/17/2008	900 Test st	art								
1/17/2008	941	13.2	0.24	0	0.86		97.8	0.00	6.0	1015
1/17/2008	1123	1.8	0.16	0	4.7		93.8	0.04	10.1	1015
1/17/2008	1310	1.4	0.24	0	5.3		89.4	0.02	12.2	1013
1/17/2008	1440	1.3	0.18	0	5.6		87.8		13.1	1013
1/17/2008	1602	1.2	0.16	0	5.9		63.0		17.7	10121
1/17/2008	1608	0.6*	Measured of	directly from	piezometer	with no tub	oing.			

Phase II Piez	ometer Moi	nitoring Da	ta	Well ID	P2		Depth	_18		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #8	8 (90 cfm to	tal; 30 cfm e	ach to INJ1	, 2, and 3; -	-4.5% H2)					
2/6/2008	1000 Test	start								
2/6/2008	1008	2.7	0.02	0	0.022		93.8	0.14	10.5	1020
2/6/2008	1112	0.0	0	0	3.9		85.7		12.0	1020
2/6/2008	1215	0.0	0	0	4.2		86.6		13.5	1019
2/6/2008	1405	0.0	0	0	4.8		84.5	0.16	15.5	1017
2/6/2008	1516	0.0	0.00	0	5.6		69.0		17.5	1017
Optimization 7	Test #1 (90 o	cfm to INJ2	for 4 hours	then shut do	own; ~88% I	N2, 10% H2	2, 1% CO2 &	LPG)		
2/20/2008	1151	15.4	0.10	0	0.022		66.7		15.4	1010
2/20/2008	1206 Test	start								
2/20/2008	1523	2.8	0	0.68	7.3		42.1		28.3	1007
2/20/2008	1606 Test	End								
2/20/2008	1646	3.0	0	0.72	6.1		56		21	1008
2/21/2008	941	12.6	0.06	0.06	2.8		74.1		10.5	1005
2/22/2008	1102	15.2	0.12	0.04	0.77		79.2		10.3	1003
Optimization 7	Test #2 (30 o	ofm to INJ2	for 12 hours	then shut o	down; ~88%	N2, 10% H	12, 1% CO2	& LPG)		
2/25/2008	1845 Test	Start								
2/26/2008	653 Test E	nd								
2/26/2008	735	6.8	0.2	0.52	2.2		86.1		4.6	1017
2/27/2008	1605	13.5	0.08	0.04	0.5		32		35.7	1009
2/28/2008	1116	14.4	0.04	0.04	0.046		85.5		16.9	1007

Phase II Piezo	ometer Mor	nitoring Dat	a	Well ID	_P2		Depth	_18		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #3A (1 d	cfm to INJ2;	~88% N2,	10% H2, 1%	6 CO2 & LP	G)				
2/29/2008	1319 Test \$	Start								
2/29/2008	1503	14.6	0.02	0.06	0.005		41.6		30.7	1009
3/3/2008	1109	16.8	0.1	0	0.002		61.5		16.2	1019
3/3/2008	1130 Test I	End								
				1						
Optimization T	est #3B (1 d	cfm to INJ1,	INJ2 & INJ	3; ~88% N2	, 10% H2, 1	% CO2 & I	_PG)			
3/3/2008	1130 Test \$	Start								
3/4/2008	955		0.1	0.02	0.88		64.1		14.3	1013
3/7/2008	1124		0	0.46	2.2		65.5		19.8	
	1306 Test I			0.10			00.0			
3/1/2000	1000 10311	LIIG							1	
Optimization T	est #3C (90	cfm to INJ	1, INJ2 & IN	J3 for 15 mi	inutes then	shut down;	~79% N2, 1	0% H2 & LPG	, 1% CO2)	
3/7/2008	1306 Start	Pulse								
	1321 End F									
3/7/2008	1351	5.1	0	0.6	3		61.7		23.4	1016
3/10/2008	1112	_	0.06		0.01		78.2		17.2	
3/10/2008	1112	14.4	0.00	0.10	0.01		10.2		17.2	1010
Optimization T	est #4 ( 2, 4	15-minutes p	oulses; daily	/ 15-minutes	s pulses w/3	30cfh consta	ant flow)			
3/10/2008	1242		0.12		0.022		67.9		21.1	1016
5, 15, 2000			3.12	3.02	0.022		30			1010
Optimization T	est #5 (20 d	ofm to INJ2	for 125 minu	utes while m	naintaing 30	cfh the res	t of the time:	~80% N2, 10	% H2 & LPG)	
	(200							,,,,,,,,,,,		

Phase II Piezo	ometer Mor	nitoring Dat	ta	Well ID	P2		Depth	_18		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #6 (50 d	ofh to P4-18	& P4-28; ~	80% N2, 10	% H2 & LP(	G)				
3/20/2008	1330 Start	Test								
3/21/2008	957	15.2	0.20	0.30	0.010		72.3		11.6	1020
3/24/2008	1017	10.9	0.20	0.90	0.022					
3/26/2008	1032	10.9	0.16	0.80	0.022		68.9		12.4	1017
3/28/2008	959	9.8	0.16	0.86	0.022		52.8		10.7	1009
3/31/2008	1003	3.6	0.08	4.5	2.5		71.9		10.3	1013
4/2/2008	1108	3.5	0.08	6.0	2.7		66.9		16.4	1008
Optimization T	est #7 (20 d	ofh to P4-18	,28, -38 (	60 cfh total)	; ~80% N2,	10% H2 &	LPG)			
4/2/2008	1233 Start	Test								
4/4/2008	952	2.3	0.02	9.0	2.6		57.6		13.5	1013
4/7/2008	1420	5.9	0.06	6.0	0.94		67.7		19.4	1011
Optimization T	est #7B (30	cfh to P4-1	8, & P4-28	(60 cfh tota	l); ~80% N2	, 10% H2 8	LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1123	8.2	0.00	4.0	0.46		85.2		14.8	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P2\_\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

8/12/2008

1008

0.78

7.5

1.2

51.1

28.3

1002

Phase II Pie	zometer Mor	nitoring Da	ta	Well ID	P2		Depth	_18		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
Optimization	Test #7C (50	) cfh to P4-1	18, & P4-28	(100 cfh tota	al); ~79% N	2, 10% H2	& LPG, 1%	CO2)		
	9 1121 Start				,-			,		
4/11/200	8 1245	11.2	0.02	2.5	0.1		69.3		22.5	1012
4/14/200	8 1016	8.5	0.04	4.0	0.046		73.7		15.6	1007
4/16/200	8 1038	4.2	0.00	6.5	2.4		55.8		16.4	1011
4/22/200	8 1011	4.5	0.10	3.0	0.88		87.1		16.6	1009
4/23/200	8 925	4.1	0.08	3.5	0.67		63.8		13	1010
4/25/200	8 1009	4.4	0.14	4.5	0.010		50.2		23.2	1015
4/29/200	8 1119	1.2	0.10	7.5	1.4		61.5		24.1	1007
5/5/200	8 1322	2.3	0.02	7.0	1.3		48.1		36.9	1001
5/13/200	8 947	0.8	0.08	8.5	0.63		38.1		34.5	1007
5/20/200	8 945	4.2	0.12	5.5	0.10		56.3		24.8	1004
5/23/200	8 1531	10.3	0.18	3.5	0.010		63.7		29.4	990
5/27/200	8 916	4.4	0.22	7.0	0.64		69.8		17.6	1007
6/4/200	8 919	0.3	0.32	9.5	1.8		55.1		24.7	1002
6/12/200	8 1213	5.8	0.40	6.0	0.005		36.3		43.1	1003
6/20/200	8 1042	0.2	0.32	8.0	1.200		38.6		42.2	1005
6/25/200	8 1058	1.5	0.30	7.0	0.82		46.0		34.2	1005
7/2/200	8 1200	0.8	0.4	7.5	1.0		72.6		30.8	1004
7/7/200	8 1148	0.1	0.46	8.5	1.5		52.6		36.5	998
7/18/200	8 1115	0.4	0.58	8	0.94		83.1		26.7	
7/24/200	8 1030	0.5	0.62	7.5	1.100		76.6		26.9	1005
7/31/200	8 1025	0.2	0.74	8.0	1.300		73.0		25.6	1003
8/7/200	8 904	0.1	0.82	8.5	1.3		73.4		20.5	1004
		1								

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #8 (100	cfh of 100%	% Propane t	o P4-18, & I	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1053	7.2	1.32	2.5	0.005					999
9/15/2008	935	5.7	0.58	30	0.005		58.7		27.2	1007
9/29/2008	954	4.1	0.48	30	0.005		68.1		23.3	1006
10/13/2008	1212	13.2	3.22	4.5	0.005		29.9		32.2	1017
10/20/2008	1137	12.1	3.92	3.0	0.005		48.3		26.9	1013
11/5/2008	1327	10.2	5.00*	2.5	0.005		76.7		19.2	1016
11/17/2008	1124	6.9	5.00*	3.5	0.010		69.2		27.2	1014
12/1/2008	1056	7.0	5.00*	3.0	0.002		63.8		20.6	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_28\_\_\_\_

				Waller	Injection G	ac Cample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
	-	, ,	` '				` ′	, ,	` ,	,
12/12/2007	1218	19.9	0.24	0	0.002	50,000	84.9	0.02	12.1	1020
12/12/2007	1539							0.15		
12/13/2007	912	14.7	0	0	0.22		67.1		9.3	1016
12/13/2007	950	14.3	0	0	0.22		73.2		11.2	1016
12/13/2007	1200	Discovered	leak in O2 -	all O2 data	for 12/13/0	7 before 120	00 invalid			
12/13/2007	1319							0.11		
12/13/2007	1334	0.7	0.22	0	7.5		68.9		17.1	1013
12/13/2007	1503	0.5	0.18	0	8.8		87.2		13.2	1013
12/13/2007	1532	0.4	0.18	0.14	6.9		88.2		12.8	1013
12/14/2007	839	0	0.24	0.26	1.8		66.8	0.03	6.7	1016
12/21/2007	1147	18.3	0.48	0	0.46		88.8	0.04	9.5	1013
12/26/2007	1149	19	0.44	0	0.002		86.6	0.01	10.4	1017
12/27/2007	1003	17.6	0.46	0	0.5		74.8	0.04	6.5	1018
12/27/2007	1258	16.9	0.36	0	0.46		82.2		9.5	1016
12/27/2007	1431	16.6	0.36	0	0.77		88.6		8.3	1017
12/27/2007	1547	16.4	0.36	0	0.98		90.1	0.03	7.5	1016
1/2/2008	1021	4.6	0.56	0	0.22		57.5	0.02	17.3	1012
1/21/2008	1000¹	0.6	0.06	0	0.022		90.0		8.6	1007
1/21/2008	1006²	1.4	0.06	0	0.022		80.0		8.4	1007
1/21/2008	1014³	1.3	0.06	0	0.010		90.1		8.0	

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_28\_\_\_

Well or Injection Gas Sample Well Ambient A

				Well or		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)	

Tracer Test #1	(10 cfm to I	NJ2, ~7% H	12)						
1/21/2008	1046 Test s	start							
1/21/2008	1149	1.7	0.08	0	0.022	80.2	0.04	9.6	1008
1/21/2008	1306	1.6	0.06	0	0.046	72.6		9.9	1006
1/21/2008	1500	1.7	0.08	0	0.046	77.7	0.04	10.1	1006
1/21/2008	1620	1.7	0.06	0	0.046	77.5		10.0	1006
1/22/2008	1040	1.4	0.14	0	2.3	80.8	0.06	6.5	1011
1/22/2008	1330	1.2	0.10	0	2.8	86.8		7.9	1009
1/23/2008	1043	1.7	0.14	0	4.3	97.5	0.00	7.6	1008
1/23/2008	1158*	1.0							

Tracer Test #2	2 (20 cfm to I	INJ2, ~8% H	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1151	1.4	0.10	0	0.046	96.7		13.1	1015
1/18/2008	1244	1.3	0.10	0	0.046	95.7	0.01	13.9	1014
1/18/2008	1333	1.5	0.12	0	0.046	91.2		15.2	1014
1/18/2008	1509	1.5	0.12	0	0.010	80.4	0.03	18.0	1014
1/19/2008	933	1.4	0.24	0	7.9	81.5	0.03	9.5	1019
1/19/2008	1114*	0.7	0.20	0	8.7	65.4		19.5	1018

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_28\_\_\_

Well or Injection Gas Sample Well Ambient Air

O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure Temperature Barometric press  Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar)					Well or		Well	Ambient Air
Date Time (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar)			O <sub>2</sub>	Temperature	Barometric pressure			
	Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)	

Tracer Test #3	(30 cfm to I	NJ2, ~4% F	12)						
1/30/2008	1036 Test s	start							
1/30/2008	1139	0.0	0	0	0.10	93.0	0.07	10.1	1020
1/30/2008	1256	0.0	0	0	0.046	94.7		12.1	1019
1/30/2008	1502	0.0	0	0	0.59	84.1	0.09	15.2	1018
1/31/2008	1018	0.0	0	0	4.1	84.5	0.08	9.2	1019
1/31/2008	1154	0	0	0	3.9	85.1		9.5	1018
1/31/2008	1424	0	0	0	3.9	83.7	0.13	8.3	1015
1/31/2008	1435								
1/31/2008	1546	0	0	0	3.8	81.5	0.05	8.2	1014
1/31/2008	1613	0	0	0	3.9	83.1		8.2	1013

Tracer Test #4	(60 cfm to I	NJ2, ~7% H	H2)						
1/28/2008	1236 Test s	start							
1/28/2008	1316	7.9	0.12	0	0.010	97.8		10.3	1010
1/28/2008	1446	4.5	0.12	0	0.75	92.2	0.12	12.9	1011
1/28/2008	1619	1.4	0.10	0	3.7	86.6	0.07	9.5	1012
1/29/2008	848	0	0.06	0	7.2	88.8	0.05	5.6	1017
1/29/2008	Final O2*	0							

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_28\_\_\_\_ Well or Injection Gas Sample Well Ambient Air 02 CO2 **Propane** H<sub>2</sub> He RH Pressure Temperature Barometric pressure Date Time (mbar) (%) (%) (%) (%) (ppm) (%) (in wc) (C<sub>0</sub>) Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1058 0.9 0.022 1019 96.6 0.17 10.8 2/5/2008 1201 0.3 1.1 94.7 11.3 1019 2/5/2008 1408 0 3.2 89.9 0.0 0.18 12.7 1018 2/5/2008 1528 0 3.2 59.0 18.2 0.0 1019 2/5/2008 3.3 1612 0.0 0 63.5 11.3 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 0.022 1510 0.0 0 0 54.3 21.4 1016 2/7/2008 1601 40.5 27.4 1016 0.0 0 0 0.10 2/8/2008 928 0.0 0 9.0 85.4 8.8 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 942 0.28 1/17/2008 0.03 15.8 0.46 98.0 6.2 1015 1/17/2008 1125 4.6 0.18 0 3.9 94.8 0.02 10.1 1015 1/17/2008 1313 1.5 0.3 5.2 92.6 0.01 12.0 1013 1/17/2008 1443 1.2 0.26 0 5.7 89.4 13.0 1012 1/17/2008 1603 0.22 6.0 69.1 16.6 1.1 1012

Phase II Piezo	Phase II Piezometer Monitoring Data Well IDP2 Depth28  Well or Injection Gas Sample Well Ambient Air												
				Well or	Injection G	as Sample			Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			
Tracer Test #8	(90 cfm total	al; 30 cfm ea	ach to INJ1,	2, and 3; ~4	4.5% H2)								
2/6/2008	1000 Test s	start											
2/6/2008	1010	2.5	0.04	0	0.046		94.7	0.26	10.6	1020			
2/6/2008	1113	0.0	0	0	2.0		92.5		12.0	1020			
2/6/2008	1216	0.0	0	0	3.9		91.8		13.54	1019			
2/6/2008	1406	0.0	0	0	4.8		86.3	0.26	15.5	1017			
2/6/2008	1517	0.0	0	0	4.5		72.1		17.4	1017			
2/20/2008	1152 1206 Test s	12.8 start 1.6	0.00 0	nen shut dov		2, 10% H2,	1% CO2 & I 66.4 45.6	_PG)	15.2 27.2	1010			
2/20/2008	1647	2.4	0	0.78	9		56.7		20.9	1008			
2/21/2008	943	4.0	0.00	0.62	5.1		73.9		10.5	1005			
2/22/2008	1103	12	0.00	0.26	1.3		78.2		10.3	1003			
Optimization T	est #2 (30 c	fm to INJ2 f	or 12 hours	then shut de	own; ~88%	N2, 10% H2	2, 1% CO2 &	LPG)					
2/25/2008	1845 Test \$	Start											
2/26/2008	653 Test E	nd											
2/26/2008	737	4.5	0.14	0.54	4.8		84.3		8.7	1017			
2/27/2008	1606	8.8	0	0.28	1.1		33.8		34.2	1009			
2/28/2008	1116	12.4	0	0.18	0.1		81.9		16.7	1007			

Phase II Piezo	meter Mon	itoring Data	a	28						
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #3A (1 c	ofm to INJ2;	~88% N2, 1	0% H2, 1%	CO2 & LPG	<del>3</del> )				
2/29/2008	1319 Test 9	Start								
2/29/2008	1503	13.9	0	0.14	0.022		44.5		29.5	1009
3/3/2008	1110	15.8	0.04	0.04	0.002		58.7		16.2	1019
3/3/2008	1130 Test I	End								
									l .	
Optimization T	oct #3B (1 c	ofm to IN I1		2. 99% NO	100/ 42 10	% CO2 8 1 E	PG)			
•	1130 Test \$		INJZ & INJS	5, ~00 /6 INZ,	10 /6 112, 1	/6 CO2 & LF				
3/4/2008	956		0.06	0.16	0.59		63.3		14.4	1013
3/7/2008			0.00	0.10	0.39		64.7		19.8	1018
	1306 Test F		0	0.14			04.7		19.0	1010
3/1/2008	1300 1681	IIIu								
Optimization T	i i		, INJ2 & INc	J3 for 15 mi	nutes then s	hut down; ~	-79% N2, 10 	% H2 & LPG, 1	1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1352	12.4	0	0.22	1.6		59.5		23.4	1016
3/10/2008	1113	15.9	0.06	0.12	0.1		72.2		17.2	1016
Optimization T	est #4 ( 2, 4	5-minutes p	ulses; daily	15-minutes	pulses w/30	ofh constar	nt flow)			
3/10/2008	1243	16	0.14	0.16	0.046		72.3		21.1	1016
Optimization T	est #5 (20 c	fm to IN.12 f	or 125 minu	tes while m	aintaing 30 g	ofh the rest	of the time:	~80% N2 10%	H2 & LPG)	
Spanii Zadon 1	031 110 (20 0	1111 10 11102 1	5. 125 Hillia	CO WITHOUT	antung 50 t	J.11 1110 1031	or the time,	30 /0 142, 10 /0	1.2 4 21 0)	
<u> </u>							<u> </u>			

88.0

14.8

1009

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_28\_\_\_\_ Well or Injection Gas Sample Well Ambient Air 02 CO2 Propane H<sub>2</sub> He RH Pressure Temperature Barometric pressure (%) Date Time (mbar) (%) (%) (%) (ppm) (%) (in wc) (C<sub>0</sub>) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/21/2008 959 11.7 0.18 1.50 0.046 73.2 1020 11.4 3/24/2008 1018 10.3 0.26 1.32 0.046 61.6 16.0 1012 3/26/2008 1033 0.24 1.40 0.046 7.9 73.5 12.4 1017 3/28/2008 1000 7.8 0.26 1.34 0.046 57.0 10.7 1009 3/31/2008 1004 2.2 0.22 4.0 73.4 1013 9.0 10.3 4/2/2008 1109 1.1 0.2 12.5 3.9 75.5 16.5 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 953 2.1 0.18 2.7 58.3 1013 10.5 13.6 4/7/2008 1421 3.9 0.22 8.5 0.95 67.6 19.4 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test

4/9/2008

1124

7.1

0.14

6.0

0.1

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_28\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure										Barometric pressure
Date Time (%) (%) (%) (ppm) (%) (in wc)									(C <sub>0</sub> )	(mbar)

Optimization T	est #7C (50	cfh to P4-18	3. & P4-28 (	100 cfh tota	l): ~79% N2	2, 10% H2 & LPG, 1% C	O2)	
	1121 Start				,,		- /	
4/11/2008	1246	10.2	0.22	4.0	0.1	63.6	22.4	1012
4/14/2008	1017	7.3	0.24	5.5	0.8	67.7	15.5	1007
4/16/2008	1039	2.6	0.26	9.0	2.6	60.3	16.6	1011
4/22/2008	1012	10.4	0.28	1.4	0.22	78.2	16.7	1009
4/23/2008	926	7.4	0.28	2.5	0.22	61.7	12.9	1010
4/25/2008	1011	3.6	0.36	6.5	0.046	52.7	23.7	1015
4/29/2008	1120	1.0	0.30	8.0	1.2	64.5	24.4	1007
5/5/2008	1324	5.7	0.26	4.5	0.61	45.8	37.0	1001
5/13/2008	948	1.4	0.30	8.5	0.10	37.7	34.7	1007
5/20/2008	946	4.4	0.40	6.0	0.046	55.6	24.0	1004
5/23/2008	1532	17.8	0.48	0.9	0.010	56.8	29.0	990
5/27/2008	918	9.4	0.58	3.5	0.80	70.5	17.8	1007
6/4/2008	920	2.4	0.48	7.5	0.95	57.0	24.6	1002
6/12/2008	1214	7.1	0.62	5.0	0.046	31.5	43.1	1003
6/20/2008	1043	1.0	0.48	8.0	0.870	32.7	42.7	1005
6/25/2008	1059	1.3	0.42	8.0	0.51	45.8	33.3	1005
7/2/2008	1201	1.0	0.42	8.0	0.50	67.2	30.9	1004
7/7/2008	1149	0.7	0.38	8	0.63	46.7	36.5	998
7/18/2008	1116	0.3	0.48	8.5	0.6	71.9	26.7	
7/24/2008	1031	0.6	0.56	8.5	0.540	68.4	27.0	1005
7/31/2008	1027	0.4	0.64	8.5	0.680	60.0	25.7	1003
8/7/2008	905	0.2	0.68	8.5	0.83	72.1	20.6	1004
8/12/2008	1015	0.2	0.68	8.5	0.65	52.5	28.5	1002

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_28\_\_\_

				Well or		Well	Ambient Air			
								Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #8 (100	cfh of 100%	Propane to	P4-18, & P	4-28 (50 cff	to each po	int)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1055	4.4	1.18	5.5	0.005					999
9/15/2008	936	7.5	0.42	30	0.005		58.6		27.3	1007
9/29/2008	955	3.1	0.16	30	0.005		68.9		23.5	1006
10/13/2008	1213	10.7	1.02	30	0.005		32.2		31.0	1017
10/20/2008	1139	8.5	1.00	30	0.005		49.2		27.0	1013
11/5/2008	1329	8.9	1.04	30	0.005		79.3		19.2	1016
11/17/2008	1125	6.7	1.02	30	0.010		70.4		27.0	1014
12/1/2008	1057	6.8	1.08	30	0.002		64.7		20.6	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P2\_\_\_\_ Depth \_\_\_\_38\_\_\_\_

	İ			Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1220	19.4	0.38	0	0.002	70,000	85.8	0.02	12.1	1020
12/12/2007	1538							0.20		
12/13/2007	913	19.8	0.12	0	0.022		62.9		10.4	1016
12/13/2007	953	19.6	0.06	0	0.22		75.1		11.1	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	200 invalid			
12/13/2007	1319							0.12		
12/13/2007	1336	15.1	0.54	0	0.22		69.6		16.8	1013
12/13/2007	1503	12.2	0.54	0	1.6		90.9		13.1	1013
12/13/2007	1533	11.1	0.56	0	2.2		88.6		12.7	1013
12/14/2007	841	5.8	0.62	0.02	2.7		67.3	0.01	7.1	1016
12/21/2007	1149	14.0	0.72	0.04	0.46		89.5	0.03	9.4	1013
12/26/2007	1151	16.2	0.64	0.02	0.022		88.3	0.04	10.3	1017
12/27/2007	1005	16.8	0.64	0	0.22		76.4	0.03	6.3	1018
12/27/2007	1300	17.2	0.46	0	0.22		80.2		9.4	1016
12/27/2007	1433	17.1	0.46	0	0.22		89.5		8.2	1017
12/27/2007	1549	17.2	0.44	0	0.22		90.1	0.01	7.5	1016
1/2/2008	1022	12.3	0.72	0	0.22		61.2	0.02	17.4	1012
1/21/2008	1001¹	1.2	0.38	0	0.10		88.8		8.5	1007
1/21/2008	1007²	1.8	0.36	0	0.22		83.0		8.4	1007
1/21/2008	1016³	1.8	0.36	0	0.046		89.6		8.0	

(%)

(in wc)

(C°)

(mbar)

Phase II Piezometer Mon	itoring Dat	а	Well ID	P2		Depth	_38		
					as Sample			Well	Ambient Air
	Oa	CO	Propage	Η <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure

(ppm)

(%)

Date

Time

(%)

(%)

(%)

Tracer Test #1	(10 cfm to I	INJ2, ~7% I	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1150	2.1	0.34	0	0.046	79.2	0.06	9.6	1007
1/21/2008	1307	2.1	0.38	0	0.046	74.2		9.7	1006
1/21/2008	1501	2.2	0.36	0	0.046	78.8	0.02	10.7	1006
1/21/2008	1622	2.4	0.38	0	0.046	78.8		10.0	1006
1/22/2008	1041	2.3	0.48	0	0.22	79.8	0.06	6.5	1011
1/22/2008	1335	2.1	0.44	0	0.50	85.4		7.6	1009
1/23/2008	1048	2.3	0.48	0	1.3	97.8	0.02	7.4	1008
1/23/2008	1159*	1.7							

Tracer Test #2	2 (20 cfm to	INJ2, ~8% I	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1152	1.6	0.38	0	0.46	96.9		13.1	1015
1/18/2008	1245	1.5	0.42	0	0.57	96.1	0.02	13.9	1014
1/18/2008	1334	1.8	0.42	0	0.66	92.0		15.1	1014
1/18/2008	1510	1.9	0.40	0	0.61	83.4	0.03	17.9	1014
1/19/2008	934	2.4	0.66	0	2.1	73.2	0.01	7.1	1019
1/19/2008	1117*	1.7	0.58	0	2.4	47.0		19.5	1018

88.2

0.08

4.9

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P2\_\_\_\_\_ Depth \_\_\_\_38\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** CO2 **Propane**  $H_2$ He RH Temperature Barometric pressure  $O_2$ Pressure Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1140 0.0 0.34 0.80 91.4 0.09 10.0 1020 1/30/2008 1257 0.32 0.68 95.0 12.1 1019 0.1 0 1503 0.1 1/30/2008 0.32 0 0.75 85.8 0.09 15.1 1018 1/31/2008 1019 0.0 0.38 2.9 82.3 0.11 9.1 1019 1/31/2008 1155 0.40 2.8 81.8 9.4 1018 2.9 1/31/2008 1425 0.40 81.4 0.13 8.3 1015 1435 1/31/2008 1547 0.38 2.9 74.6 0.03 1/31/2008 8.2 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 2.7 1/28/2008 1317 0.52 0 0.046 98.2 10.3 1010 1/28/2008 1447 2.7 0.54 0 0.046 92.8 0.16 12.9 1011 1/28/2008 1620 2.6 0.52 0 0.50 86.2 0.12 9.4 1012

6.3

0.54

0.3

0.3

1/29/2008

1/29/2008 Final O2\*

849

1017

Phase II Piezo	ometer Mon	nitoring Dat	a	Well ID	P2		Depth	_38		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH		Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #5	(90 cfm to	INJ2, ~3% I	H2)							
2/5/2008	1015 Test s	start								
2/5/2008	1059	1.3	0.22	0	0.010		91.1	0.20	10.5	1019
2/5/2008	1202	1.3	0.22	0	0.022		94.9		11.3	1019
2/5/2008	1409	1.3	0.22	0	0.22		89.1	0.21	12.7	1018
2/5/2008	1529	1.2	0.28	0	0.64		60.2		17.5	1019
2/5/2008	1612	1.1	0.26	0	0.77		62.5		11.1	1018
Tracer Test #6	(30 cfm tot	al; 10 cfm to	each INJ1	, 2, and 3; ~	-8% H2)					
2/7/2008	1500 Test s	start								
2/7/2008	1511	0.0	0.18	0	0.046		58.6		11.4	1016
2/7/2008	1602	0.0	0.16	0	0.10		43.8		26.7	1016
2/8/2008	930	0.0	0.16	0	7.5		78.9		9.5	1017
2/8/2008	1044	0.0	0.14	0	7.0		90.4		10.3	1017
Tracer Test #7	Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2)									
1/17/2008	900 Test st	art								
1/17/2008	943	15.1	0.52	0	0.22		97.7	0.04	6.5	1015
1/17/2008	1126	14.7	0.44	0	1.1		95.0	0.04	10.1	1015
1/17/2008	1314	4.4	0.66	0	3.8		93.2		11.9	1014
1/17/2008	1444	2.5	0.66	0	4.8		91.3	0.02	12.9	1012
1/17/2008	1605	1.8	0.62	0	5.4		73.7		15.7	1012

Phase II Piezo	meter Mon	itoring Dat	a	Well ID	P2		Depth	_38		
Well or Injection Gas Sample								Well	Ambient Air	
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #8	(90 cfm tot	al; 30 cfm e	ach to INJ1	, 2, and 3; ~	4.5% H2)					
2/6/2008	1000 Test s	start								
2/6/2008	1011	2.8	0.24	0	0.10		91.8	0.26	10.8	1020
2/6/2008	1115	0.0	0.18	0	0.10		93.3		12.0	1020
2/6/2008	1223	0.0	0.16	0	2.1		86.9		13.2	1019
2/6/2008	1407	0.0	0.16	0	4.0		87.8	0.25	15.5	1017
2/6/2008	1517	0.0	0.12	0	4.0		71.4		17.1	1017
2/6/2008	1608	0.0	0.22	0	3.9		58.0		19.1	1017
Optimization T	est #1 (90 c	fm to INJ2 t	for 4 hours t	hen shut do	wn; ~88% l	N2, 10% H2	, 1% CO2 8	k LPG)		
2/20/2008	1154	4.6	0.22	0	0.046		70.7		15.1	1010
2/20/2008	1206 Test s	start								
2/20/2008	1525	4.2	0.18	0	0.87		47.5		26	1007
2/20/2008	1606 Test I	End								
2/20/2008	1648	4.0	0.16	0.04	2		56.6		20.9	1008
2/21/2008	944	3.5	0.16	0.18	2.4		74.4		10.5	1005
2/22/2008	1104	4.5	0.14	0.1	0.78		77.7		10.3	1003
Optimization T	est #2 (30 c	fm to INJ2 t	for 12 hours	then shut d	lown; ~88%	N2, 10% H	2, 1% CO2	& LPG)		
2/25/2008	1845 Test \$	Start								
2/26/2008	653 Test E	nd								
2/26/2008	738	6.4	0.3	0.22	1		82.7		4.8	1017
2/27/2008	1607	6.4	0.1	0.1	0.1		37.6		32.5	1009
2/28/2008	1118	7.5	0.08	0.08	0.046		84.4		16.7	1007

Phase II Piezo	ometer Mon	itoring Dat	а	Well ID	P2		Depth	_38		
	ĺ			Well or	Well	Ambient Air				
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
Optimization T	est #3A (1 c	fm to INJ2;	~88% N2,	10% H2, 1%	CO2 & LP	G)				
	1319 Test S		•	,		,				
2/29/2008		8.3	0.06	0.1	0.01		46.4		28.6	1009
3/3/2008		10.3	0.12		0.002		59.6		16.2	1019
	1130 Test E		02	0.0.	0.002		00.0			
0/0/2000	1100 1000 1	Ind								
Optimization T	est #3B (1 c	fm to INJ1,	INJ2 & INJ	3; ~88% N2	, 10% H2, 1	% CO2 & I	_PG)			
3/3/2008	1130 Test S	Start								
3/4/2008	958	10.8	0.12	0.06	0.022		65.2		14.4	1013
3/7/2008	1127	12	0.08	0.04	0.022		63.6		19.8	1018
3/7/2008	1306 Test E	End								
									'	
Optimization T	est #3C (90	cfm to INJ1	I, INJ2 & IN	J3 for 15 mi	nutes then	shut down;	~79% N2, 1	0% H2 & LPG	6, 1% CO2)	
3/7/2008	1306 Start I	Pulse								
3/7/2008	1321 End F	ulse								
3/7/2008	1353	11.7	0.08	0.04	0.022		60.5		23.4	1016
3/10/2008	1114	12.3	0.12	0.06	0.022		71.4		17.1	1016
									1	
Optimization T	est #4 ( 2, 4	5-minutes p	oulses; daily	15-minutes	pulses w/3	Ocfh consta	ant flow)			
Optimization T	est #5 (20 c	fm to INJ2 f	or 125 mini	utes while m	aintaing 30	cfh the res	t of the time	; ~80% N2, 10	1% H2 & LPG)	

Phase II Piezo	ometer Mon	nitoring Dat	a	Well ID	P2		Depth	_38		
				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	- - ost #6 (50 c	ofh to D1_18	& D4-28+ .9	20% NO 10	0/. ∐2 & I D/	2)				
	1330 Start		& F 4-20, ~6	30 /6 INZ, 10	/6 112 & LF	3)				
3/21/2008	1001	11.5	0.20	1.38	0.010		75.0		11.6	1020
3/24/2008	1019	12.0	0.24	1.26	0.022		61.2		16.1	1012
3/26/2008	1034	12.1	0.22	1.04	0.010		76.1		12.4	1017
3/28/2008	1001	12.3	0.26	0.82	0.022		58.3		10.6	1009
3/31/2008	1005	6.5	0.14	5.5	1.0		72.8		10.4	1013
4/2/2008	1110	5.2	0.08	7.5	0.22		73.8		16.6	1008
			//				. = 0\			
Optimization T	est #7 (20 c	th to P4-18	,28, -38 (6	60 cfh total):	; ~80% N2,	10% H2 &	LPG)			
4/2/2008	1233 Start	Test								
4/4/2008	953	4.5	0.06	8.0	0.1		58.3		13.6	1013
4/7/2008	1423	4.5	0.18	9.0	0.01		69.2		19.5	1011
0 11 11 11 7			0 0 0 0 0 0 0	/00 fl I	) 000/ NO	400/ 110 0				
Optimization T	est #/B (30	cth to P4-1	8, & P4-28	(60 cth total	); ~80% N2	, 10% H2 8	k LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1126	5.3	0.12	8.5	0.022		90.7		14.7	1009

29.8

30.7

45.8

59.6

44.1

69.6

63.2

58.1

70.2

47.0

Phase II Piezo	meter Mon	itoring Dat	a	Well ID	P2		Depth	_38		
Well or Injection Gas Sample									Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2)										
4/10/2009	1121 Start	Test								
4/11/2008	1247	6.2	0.20	8.0	0.1		65.9		22.4	1012
4/14/2008	1018	4.2	0.16	9.5	0.6		74.7		15.5	1007
4/16/2008	1040	3.5	0.14	10.0	0.1		55.9		16.7	1011
4/22/2008	1013	6.1	0.30	3.5	0.022		84.1		16.7	1009
4/23/2008	927	5.1	0.30	4.0	0.010		61.1		12.9	1010
4/25/2008	1012	2.6	0.32	6.5	0.022		52.4		23.8	1015
4/29/2008	1121	3.1	0.34	6.5	0.22		63.3		24.8	1007
5/5/2008	1325	4.7	0.34	5.5	0.1		47.1		37.3	1001
5/13/2008	949	2.8	0.40	7.0	0.046		38.1		35.1	1007
5/20/2008	947	2.6	0.46	7.5	0.046		58.9		23.5	1004
5/23/2008	1535	4.0	0.44	7.0	0.046		53.9		29.0	990
5/27/2008	919	5.3	0.60	6.5	0.046		71.1		18.0	1007
6/4/2008	921	4.9	0.50	6.0	0.046		58.2		24.9	1002

6/12/2008

6/20/2008

6/25/2008

7/2/2008

7/7/2008

7/18/2008

7/24/2008

7/31/2008

8/7/2008

8/12/2008

1216

1044

1100

1203

1150

1117

1032

1028

906

1010

3.5

3.4

3.1

2.6

2.3

1.3

1.1

0.8

0.5

0.4

0.58

0.60

0.62

0.68

0.66

0.88

0.96

1.14

1.20

1.18

6.5

6.5

6.5

6.5

7.0

7.0

7.0

7.0

7.5

7.5

0.022

0.046

0.046

0.046

0.046

0.046

0.100

0.100

0.50

0.10

1003

1005

1005

1004

998

1005

1003

1004

1002

43.4

42.6

32.7

31.1

36.4

26.7

27.0

25.8

20.6

28.5

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #8 (100	cfh of 100%	6 Propane to	o P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1056	0.4	1.28	12.0	0.005					999
9/15/2008	938	0.6	0.8	30	0.010		57.7		27.3	1007
9/29/2008	956	0.0	0.40	30	0.010		66.9		23.8	1006
10/13/2008	1214	0.8	0.56	30	0.005		36.6		30.2	1017
10/20/2008	1140	0.4	0.64	30	0.005		51.2		26.7	1013
11/5/2008	1330	0.2	0.64	30	0.005		80.1		19.1	1016
11/17/2008	1126	0.1	0.58	30	0.005		73.2		26.7	1014
12/1/2008	1058	0.0	0.60	30	0.002		66.7		20.5	1014

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1222	18.0	0.52	0	0.002	100,000	86.5	0.01	12.0	1020
12/12/2007	1538							0.19		
12/13/2007	916	20.4	0	0	0.022		57.8		11.4	1016
12/13/2007	955	20.1	0	0	0.22		73.7		10.9	1016
12/13/2007	1200	Discovered	leak in O2 -	· all O2 data	for 12/13/0	7 before 120	00 invalid			
12/13/2007	1319							0.13		
12/13/2007	1337	17.7	0.6	0	0.22		67.5		16.5	1013
12/13/2007	1505	17.2	0.6	0	0.22		88.8		13.0	1013
12/13/2007	1535	16.4	0.56	0	0.46		85.6		12.5	1013
12/14/2007	842	16.0	0.60	0	0.50		66.1	0.0	7.2	1016
12/21/2007	1151	16.2	1.38	0	0.22		90.0	0.02	9.5	1013
12/26/2007	1153	16.3	1.32	0	0.022		88.1	0.03	10.5	1017
12/27/2007	1007	16.5	1.48	0	0.22		78.6	0.04	5.8	1018
12/27/2007	1302	16.3	1.26	0	0.022		80.7		9.1	1016
12/27/2007	1435	16.3	1.2	0	0.022		88.5		8.2	1017
12/27/2007	1551	16.5	1.26	0	0.022		90.3	0.03	7.5	1017
1/2/2008	1025	16.5	1.66	0	0.022		55.8	0.03	18.2	1012
1/21/2008	1002¹	16.2	1.18	0	0.010		90.3		8.4	1007
1/21/2008	1008²	16.2	1.20	0	0.02		82.6		8.4	1007
1/21/2008	1019³	16.2	1.22	0	0.02		89.9		8.0	

				Well or	Well	Ambient Air				
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure						Pressure	Temperature	Barometric pressure	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #1	(10 cfm to I	NJ2, ~7% F	<del>l</del> 2)						
1/21/2008	1046 Test s	start							
1/21/2008	1151	15.2	1.18	0	0.022	81.3	0.03	9.6	1007
1/21/2008	1308	15.0	1.16	0	0.010	75.2		9.5	1006
1/21/2008	1502	14.9	1.14	0	0.022	78.9	0.04	10.7	1006
1/21/2008	1623	15.1	1.18	0	0.022	78.1		10.0	1006
1/22/2008	1043	14.8	1.34	0	0.022	80.3	0.02	6.6	1011
1/22/2008	1336	14.4	1.24	0	0.022	86.1		7.7	1009
1/23/2008	1049	14.3	1.18	0	0.10	97.6	0.01	7.3	1008
1/23/2008	1200*	14.3							

Tracer Test #2	2 (20 cfm to I	INJ2, ~8% H	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1153	15.4	1.16	0	0.022	96.6		13.0	1015
1/18/2008	1246	15.3	1.20	0	0.022	96.1	0.02	13.9	1014
1/18/2008	1335	15.6	1.20	0	0.022	91.0		15.0	1014
1/18/2008	1511	15.7	1.20	0	0.046	82.9	0.03	17.8	1014
1/19/2008	936	15.4	1.52	0	0.022	72.1	0.00	11.4	1019
1/19/2008	1118*	15.0	1.44	0	0.022	52.4		19.3	1018

				Well or		Well	Ambient Air			
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure								Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Tracer Test #3	(30 cfm to I	NJ2, ~4% ⊦	l2)						
1/30/2008	1036 Test s	tart							
1/30/2008	1141	13.0	0.42	0	0.010	92.3	0.06	9.8	1020
1/30/2008	1258	13.0	0.40	0	0.022	93.9		12.0	1019
1/30/2008	1504	16.7	0.36	0	0.010	85.4	0.05	15.1	1018
1/31/2008	1021	18.1	0.40	0	0.010	92.4	0.06	9.1	1019
1/31/2008	1156	20.2	0.36	0	0.010	91.1		9.4	1018
1/31/2008	1426	20.9	0.34	0	0.010	89.5	0.08	8.3	1015
1/31/2008	1435								
1/31/2008	1548	20.9	0.30	0	0.010	87.4	0.04	8.2	1014

Tracer Test #4	(60 cfm to I	INJ2, ~7% H	·12)						
1/28/2008	1236 Test s	start							
1/28/2008	1318	20.3	0	0	0.010	96.1		10.3	1010
1/28/2008	1448						0.06		
1/28/2008	1623								
1/29/2008	850	14.4	0.36	0	0.022	91.5	-0.16	5.6	1017
1/29/2008	Final O2*	14.4							

				Well or		Well	Ambient Air			
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure								Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #5	6 (90 cfm to I	NJ2, ~3% H	H2)						
2/5/2008	1015 Test s	tart							
2/5/2008	1104	18.6	0.38	0	0.005	94.0	0.02	10.6	1019
2/5/2008	1203	18.7	0.38	0	0.010	94.2		11.3	1019
2/5/2008	1410	18.6	0.38	0	0.022	91.5	0.04	12.7	1018
2/5/2008	1531	18.8	0.42	0	0.005	70.6		16.4	1019
2/5/2008	1613	18.4	0.40	0	0.010	68.8		18.8	1018

Tracer Test #6	(30 cfm tota	al; 10 cfm to	each INJ1,	2, and 3; ~8	3% H2)				
2/7/2008	1500 Test s	tart							
2/7/2008	1512	15.4	0.54	0	0.005	67.8		21.4	1016
2/7/2008	1603	15.1	0.52	0	0.010	51.4		26.3	1016
2/8/2008	932	13.2	0.56	0	0.010	81.8		10.0	1017
2/8/2008	1045	12.8	0.54	0	0.010	92.6	_	10.4	1017

**Phase II Piezometer Monitoring Data** 

Well ID \_\_\_\_\_P2\_\_\_\_ Depth \_\_\_\_\_48\_\_\_\_\_

				Well or		Well	Ambient Air			
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure									Barometric pressure
Date	Time (%) (%) (%) (ppm) (%) (in wc)									(mbar)

Tracer Test #7	(60 cfm tota	al; 20 cfm to	each INJ1,	2, and 3, ~5	5% H2)				
1/17/2008	900 Test sta	art							
1/17/2008	945	16.4	1.10	0	0.022	97.5	0.02	6.6	1015
1/17/2008	1127	16.3	0.94	0	0.22	95.6	0.02	10.2	1015
1/17/2008	1316	16.7	1.50	0	0.022	96.0	0.01	11.8	1013
1/17/2008	1446	16.7	1.48	0	0.22	91.8		12.8	1012
1/17/2008	1607	16.6	1.48	0	0.22	77.7		14.9	1012

Tracer Test #8	(90 cfm tota	al; 30 cfm ea	ach to INJ1,	2, and 3; ~4	4.5% H2)				
2/6/2008	1000 Test s	start							
2/6/2008	1013	17.3	0.40	0	0.010	93.4	0.06	11.0	1020
2/6/2008	1116	16.6	0.40	0	0.010	92.0		12.0	1020
2/6/2008	1225	16.2	0.38	0	0.002	95.0		13.3	1019
2/6/2008	1409	15.9	0.36	0	0.022	90.7	0.04	15.7	1017
2/6/2008	1519	15.7	0.36	0	0.022	78.1		16.9	1017
2/6/2008	1610	15.8	0.46	0	0.010	65.4		18.4	1017

Well ID \_\_\_\_\_P2\_ **Phase II Piezometer Monitoring Data** Depth 48 Well **Ambient Air Well or Injection Gas Sample** CO<sub>2</sub> Barometric pressure  $O_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Date Time (%) (C°) (%) (%) (%) (ppm) (mbar) (%) (in wc) Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1155 14.8 0.14 0.1 68.8 15 1010 2/20/2008 1206 Test start 2/20/2008 1527 4.5 0.12 0.3 0.022 49.3 25.1 1007 2/20/2008 1606 Test End 2/20/2008 1649 2.8 0.1 0.36 2.9 57.2 21 1008 2/21/2008 949 4.5 0.14 0.1 0.1 85.9 1005 10.6 1105 5.6 0.30 0.022 2/22/2008 0.14 78.6 10.3 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 740 7.9 0.3 0.14 0.005 83.1 4.9 1017 2/27/2008 1608 6.4 0.2 80.0 0.01 40.9 30.8 1009 2/28/2008 0.022 1119 6.5 0.2 0.02 85.8 16.7 1007 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1505 6.2 0.16 0.02 0.005 52.3 27.4 1009 3/3/2008 1112 20.4 0.2 0.001 63.7 16.2 1019 3/3/2008 1130 Test End

**Phase II Piezometer Monitoring Data** Well ID P2 Depth 48 Well Well or Injection Gas Sample **Ambient Air** CO2 Propane RH **Barometric pressure**  $O_2$  $H_2$ He **Pressure** Temperature Date Time (%) (%) (C°) (%) (%) (ppm) (%) (mbar) (in wc) Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 959 20.4 0.22 0 0.005 72.7 14.5 1013 3/7/2008 0 0.022 1128 19.9 0.16 69.5 19.9 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 0 1354 19.5 0.14 0.01 61.8 23.2 1016 3/10/2008 19.9 73.5 1115 0.22 0 0.022 17.2 1016 Optimization Test #4 (2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG)

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P2 Depth 48 Well **Ambient Air** Well or Injection Gas Sample CO2 Propane He RH **Barometric pressure**  $O_2$  $H_2$ **Pressure** Temperature Date Time (%) (C°) (%) (%) (%) (ppm) (%) (in wc) (mbar) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/24/2008 1020 17.4 0.54 0 0.010 16.7 16.1 1012 3/26/2008 1035 17.6 0.50 0 0.010 80.3 12.4 1017 1002 0.52 0 10.6 3/28/2008 18.6 0.005 60.5 1009 3/31/2008 1006 16.9 0.50 0 0.022 73.5 10.5 1013 4/2/2008 1112 9.8 0.70 1.66 0.022 75.3 16.7 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 954 6.7 0.84 3.0 0.022 66.1 13.6 1013 1425 1.24 74.5 19.4 1011 4/7/2008 4.1 3.0 0.1 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test

4/9/2008

4.8

1127

1.26

2.5

0.005

95.2

15.1

1009

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(C <sub>0</sub> )	(mbar)					

0 " ' " T		" · D. ·	0 0 0 0 0 0	400 (1)	I) 700/ NO	400/ 110 0 1 70 40/ 0	20)	
Optimization I	est #/C (50	cth to P4-18	8, & P4-28 (	100 cth tota	I); ~79% N2	, 10% H2 & LPG, 1% C	02)	
4/10/2009	1121 Start	Γest						
4/11/2008	1248	3.4	1.56	3.0	0.046	73.1	22.5	1012
4/14/2008	1020	3.1	1.64	4.5	0.046	74.2	15.4	1007
4/16/2008	1041	0.7	1.64	10.5	0.046	62.6	16.8	1011
4/22/2008	1015	0.0	1.50	2.5	0.046	72.2	16.8	1009
4/23/2008	928	0.0	1.76	3.0	0.046	63.1	12.9	1010
4/25/2008	1013	0.0	1.86	6.0	0.046	61.2	23.9	1015
4/29/2008	1122	0.0	1.78	5.5	0.22	67.8	25.1	1007
5/5/2008	1326	0.0	1.74	5.5	0.046	58.5	37.7	1001
5/13/2008	950	0.0	2.06	6.0	0.046	44.3	35.1	1007
5/20/2008	949	0.0	2.26	6.0	0.046	61.3	23.1	1004
5/23/2008	1536	0.0	2.00	6.0	0.022	55.6	29.0	990
5/27/2008	920	0.0	2.56	6.5	0.046	67.2	18.1	1007
6/4/2008	922	0.0	2.50	6.0	0.046	59.0	25.3	1002
6/12/2008	1217	0.0	2.56	5.5	0.022	30.5	43.2	1003
6/20/2008	1046	0.0	2.46	5.5	0.046	32.0	42.1	1005
6/25/2008	1101	0.0	2.56	5.5	0.046	46.1	32.1	1005
7/2/2008	1204	0.0	2.70	5.5	0.046	58.6	31.4	1004
7/7/2008	1151	0.0	2.5	5.5	0.046	44.4	36.3	998

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1118	0.0	2.78	5.5	0.046		73.7		26.7	
7/24/2008	1033	0.0	2.84	5.5	0.100		69.7		27.1	1005
7/31/2008	1029	0.0	2.94	5.5	0.100		59.0		25.9	1003
8/7/2008	907	0.0	1.48	6.5	0.50		65.2		20.6	1004
8/12/2008	1011	0.0	2.72	6.5	0.10		47.2		28.6	1002
Optimization T	est #8 (100	cfh of 100%	Propane to	P4-18, & P	4-28 (50 cfh	to each po	int)			
9/8/2008	0905 Test S	Start								
9/8/2008	1058	0.0	2.02	20	0.005					999
9/15/2008	939	0.0	1.66	30	0.010		57.6		27.2	1007
9/29/2008	956	0.0	1.52	30	0.010		63.5		24.0	1006
10/13/2008	1215	0.0	1.26	30	0.005		40.9		29.1	1017
10/20/2008	1141	0.0	1.26	30	0.005		56.8		26.7	1013
11/5/2008	1331	0.0	1.16	30	0.005		79.3		19.1	1016
11/17/2008	1127	0.0	1.04	30	0.005		71.6		26.6	1014
12/1/2008	1059	0.0	1.04	30	0.002		66.5		20.6	1014

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1227	19.6	0.00	0	0.002	40,000	78.3	0.03	12.5	1020
12/12/2007	1535							0.17		
12/13/2007	854	15.6	0	0	0.22		84.3		5.7	1016
12/13/2007	942	16.5	0	0	0.22		69.1		11.6	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	for 12/13/0	7 before 12	00 invalid			
12/13/2007	1320							0.14		
12/13/2007	1330	7.7	0	0	4.3		66.4		17.0	1014
12/13/2007	1450	6.0	0	0	5.9		86.0		19.0	1013
12/13/2007	1525	4.7	0	0	5.8		76.3		14.1	1013
12/14/2007	819	4.6	0	0.16	2.1		79.3	0.04	4.2	1016
12/21/2007	1128	10.7	0.16	0.08	0.46		75.7	0.04	11.0	1013
12/26/2007	1200	15	0.24	0.04	0.22		85.5	0	11.3	1017
12/26/2007	1505	15.3	0.14	0.04	0.22		85.7		10.5	1015
12/26/2007	1553	15.6	0.16	0.04	0.22		80.8	0.02	10.6	1015
12/27/2007	943	8.4	0.08	0.04	4.5		80.2	0.05	5.2	1017
12/27/2007	1248	1.8	0.12	0	7.5		74.4		9.2	1017
12/27/2007	1417	1.6	0.1	0	8.1		82.7		8.9	1017
12/27/2007	1538	1.5	0.1	0	8.4		83.9	0.04	7.6	1017
1/2/2008	956	2.2	0.18	0	0.022		48.6	0.04	15.5	1012

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_P3\_\_\_\_\_ Depth \_\_\_18\_\_\_\_

Well or Injection Gas Sample

Well Ambient Air

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Temperature	Barometric pressure				
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1115	2.1	0.06	0	1.3	83.6	0.08	8.2	1008
1/21/2008	1257	1.8	0	0	0.98	77.6		10.6	1006
1/21/2008	1451	1.8	0	0	0.88	78.3	0.08	10.8	1006
1/21/2008	1618	1.8	0	0	0.94	79.9	0.05	10.0	1006
1/22/2008	1045	1.6	0.06	0	4.4	86.2	0.09	6.7	1011
1/22/2008	1337	1.4	0	0	4.6	87.9		7.9	1009
1/23/2008	1050	1.5	0.04	0	5.1	97.7	0.05	7.3	1008
1/23/2008	1202*	1.1							

Tracer Test #2	! (20 cfm to I	INJ2, ~8% I	H2)						
1/18/2008	1120 Test s	tart							
1/18/2008	1137	1.5	0.02	0	0.10	81.0		12.6	1015
1/18/2008	1236	1.7	0.04	0	0.10	73.4	0.03	13.7	1014
1/18/2008	1327	1.7	0	0	0.046	74.2		15.5	1014
1/18/2008	1512	2.0	0	0	0.50	65.6	0.03	17.6	1014
1/19/2008	939	2.3	0.12	0	7.3	68.3	0.01	12.6	1019
1/19/2008	1103*	1.8	0.04	0	7.9	56.4		16.4	1019

Phase II Piezometer Monitoring Data

Well ID \_\_\_P3\_\_\_\_ Depth \_\_18\_\_\_\_

Well or Injection Gas Sample

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Date   Time   (%)   (%)   (%)   (ppm)   (%)   (in wc)									(mbar)

Tracer Test #3	(30 cfm to	INJ2, ~4% I	<del>1</del> 2)						
1/30/2008	1036 Test s	start							
1/30/2008	1145	0.0	0	0	0.10	91.6	0.11	9.8	1020
1/30/2008	1303	0.0	0	0	0.046	94.2		11.9	1019
1/30/2008	1509	0.1	0	0	0.84	81.8	0.10	14.7	1018
1/31/2008	1023	0.1	0	0	3.3	88.6	0.20	9.1	1019
1/31/2008	1157	0.1	0	0	3.2	89.1		9.3	1018
1/31/2008	1418	0	0	0	3.2	84.0	0.19	8.5	1016
1/31/2008	1435								
1/31/2008	1549	0.1	0	0	3.1	86.2	0.07	8.2	1014

Tracer Test #4	(60 cfm to	INJ2, ~7% I	<del>1</del> 2)						
1/28/2008	1236 Test s	start							
1/28/2008	1308	2.3	0.04	0	0.022	95.4		10.7	1010
1/28/2008	1438	0.9	0.08	0	2.7	76.4	0.10	13.0	1011
1/28/2008	1623	0.9	0.04	0	2.9	88.0	0.16	9.3	1012
1/29/2008	838	0.3	0.04	0	6.0	88.1	0.15	5.1	1017
1/29/2008	Final O2*	0.3							

**Phase II Piezometer Monitoring Data** Well ID P3 Depth \_\_\_18\_\_\_\_ Ambient Air Well or Injection Gas Sample Well CO2 Temperature Barometric pressure 02 Propane  $H_2$ He RH Pressure Date Time (%) (%) (%) (%) (mbar) (%) (ppm) (in wc) Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1105 2/5/2008 0.4 0 0.10 95.4 0.19 10.6 1019 2/5/2008 0 1204 0.3 0 0.22 93.3 11.2 1019 2/5/2008 1412 0.2 0 1.5 87.6 0.18 12.6 1018 2/5/2008 1532 0.1 0 1.7 68.4 15.7 1019 0 2/5/2008 1614 0.1 1.9 64.9 16.4 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0.0 2/7/2008 1513 0.02 1.1 56.7 21.4 1016 1604 0.0 0.02 0.80 44.2 2/7/2008 0 25.5 1016 933 0 1017 2/8/2008 0.0 0 8.8 72.2 0.10 10.3 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1008 13.5 0 0 0.22 96.8 0.02 7.7 1015 0.52 1/17/2008 1111 13.0 0 0 96.4 0.05 9.5 1015 0.02 93.2 1/17/2008 1215 6.8 2.9 10.3 1014 1/17/2008 3.4 1321 5.7 0.12 0 96.6 11.8 1013 1/17/2008 5.1 3.9 1448 0.10 87.4 0.03 12.7 1012

				Well or	Injection G	as Sample			Well	Ambient Air
	O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure									Barometric pressure
Date Time (%) (%) (%) (ppm) (%) (in wc)									(C <sub>0</sub> )	(mbar)

Tracer Test #	<sup>‡</sup> 8 (90 cfm tot	al; 30 cfm e	ach to INJ1	, 2, and 3; ~	-4.5% H2)				
2/6/200	8 1000 Test	start							
2/6/200	3 1014	0.1	0	0	0.50	92.6	0.28	11.1	1020
2/6/200	3 1119	0.0	0	0	0.74	86.4		12.0	1020
2/6/200	1226	0.0	0	0	1.4	92.8		13.3	1019
2/6/200	3 1410	0.0	0	0	2.8	80.2	0.28	15.6	1017
2/6/200	3 1520	0.0	0	0	2.9	73.2		16.6	1017
2/6/200	1611	0.0	0	0	3.0	62.7		17.8	1017

Optimization T	est #1 (90 c	fm to INJ2 f	for 4 hours t	hen shut do	wn; ~88% l	N2, 10% H2, 1% CO2 8	k LPG)	
2/20/2008	1156	4.9	0.00	0	0.022	71.4	15	1010
2/20/2008	1206 Test s	start						
2/20/2008	1531	4.1	0.00	0.06	3.8	54.5	23	1007
2/20/2008	1606 Test E	∃nd						
2/20/2008	1653	3.1	0.00	0.26	5.2	54.7	21.2	1008
2/21/2008	950	1.7	0.00	0.46	6.9	83.2	10.6	1005
2/22/2008	1109	2.1	0.00	0.5	4.2	85.4	10.2	1003

Phase II Piezo	ometer Mon	itoring Dat	а	Well ID	P3		Depth1	18		
				Well or	Injection G	as Sample	<b>!</b>		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	-
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
On time in a time. T		f (- IN 10 f	- 40 h	the second state of	J 000/	NO 400/ II	10, 40/, 000	8 L DO)		
Optimization T			or 12 nours	then shut d	iown; ~88%	N2, 10% H	2, 1% 002 6	& LPG)		
	1845 Test S									
2/26/2008	653 Test Er	nd								
2/26/2008	741	3.8	0.1	0.5	3.3		86.2		5.1	1017
2/27/2008	1610	1.2	0	0.42	2.9		46.6		29.2	1009
2/28/2008	1120	1.8	0	0.4	1.4		84.3		16.6	1007
Optimization T	est #3A (1 c	ofm to INJ2;	~88% N2, 1	10% H2, 1%	CO2 & LP	G)				
2/29/2008	1319 Test S	Start								
2/29/2008	1506	3	0	0.38	0.1		51.9		26.5	1009
3/3/2008	1114	2.9	0	0.38	0.84		67.3		16.2	1019
3/3/2008	1130 Test E	End								
Optimization T	est #3B (1 d	ofm to INJ1,	INJ2 & INJ	3; ~88% N2	, 10% H2, 1	% CO2 & L	PG)			
3/3/2008	1130 Test 9	Start								
3/4/2008	1000	2.6	0	0.4	2.9		77.3		14.6	1013
3/7/2008	1130	0.8	0	0.6	4.2		67.4		20	1018
3/7/2008	1306 Test E	∃nd								
Optimization T	est #3C (90	cfm to INJ1	, INJ2 & IN	J3 for 15 mi	nutes then	shut down;	~79% N2, 10	0% H2 & LPG,	1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1354	0.9	0	0.58	3.8		61.4		23	1016
3/10/2008	1117	3.4	0	0.78	0.046		80.5		17.2	1016

Well ID \_\_\_\_P3\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth \_\_\_18\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure 02 CO2 Propane  $H_2$ He RH Pressure Date Time (%) (%) (%) (C°) (mbar) (%) (%) (ppm) (in wc) Optimization Test #4 (2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 1239 3.6 0.08 0.76 68.6 3/10/2008 0.01 20.9 1016 3/10/2008 0.022 1321 3.7 0.08 0.76 1016 3/10/2008 1347 End pulse 3/10/2008 1412 3.8 0.08 0.74 0.1 59.4 22.6 1015 939 68.4 3/11/2008 3.1 0.10 1.24 1.4 15.5 1018 3/12/2008 2.2 1005 0.06 1.58 1.7 8.08 12.9 1014 3/13/2008 919 0.02 14 1.6 1.3 78.2 1011 3/14/2008 1143 1.6 0.04 0.8 80 14.1 1013 3/14/2008 1218 1.6 0.04 0.79 75.8 14.8 1012 3/15/2008 1128 1.6 0.06 2.5 0.46 80.1 11.2 1009 0.22 3/16/2008 1115 2.2 0.00 2.5 71.9 14.1 1009 3/17/2008 927 2.4 0.06 0.022 71.4 9.4 1014 Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 1037 Start Test 3/17/2008 0.0 0.022 3/17/2008 1300 2.1 2.5 73.1 17.7 1014 945 2.5 0.02 0.89 65.9 13.1 3/8/2008 1016 2.5 0.22 3/19/2008 1003 2.8 0.02 73.1 12.3 1013 3/20/2008 948 2.5 0.22 80.3 3.3 0.06 9.8 1016 3/20/2008 ~1100

End Test

Phase II Piezo	ometer Mon	nitoring Dat	a	Well ID	P3		Depth1	8		
					Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #6 (50 c	ofh to P4-18	& P4-28; ~8	30% N2, 10°	% H2 & LP0	G)				
3/20/2008	1330 Start	Test								
3/21/2008	951	0.7	0.06	2.0	3.0		81.1		10.5	1020
3/24/2008	1021	0.0	0.08	2.0	3.2		71.4		16.1	1012
3/26/2008	1037	0.0	0.04	2.0	3.8		84.6		12.3	1017
3/28/2008	1003	0.0	0.04	2.0	2.6		67.5		10.7	1009
3/31/2008	1008	0.0	0.02	10.0	9.0		79.1		10.6	1013
4/2/2008	1113	0.0	0.02	11.5	8.6		75.2		16.7	1008
Optimization T	est #7 (20 c	ofh to P4-18,	,28, -38 (6	60 cfh total);	~80% N2,	10% H2 & L	_PG)			
4/2/2008	1233 Start	Test								
4/4/2008	956	0.1	0.00	11.0	9.8		74.2		13.7	1013
4/7/2008	1426	0.2	0.06	8.5	15.0		72.4		19.4	1011
Optimization T	,		8, & P4-28 (	(60 cth total	); ~80% N2 <sub>:</sub>	, 10% H2 &	LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1130	0.3	0.00	2.5	22		81.3		15.3	1009
Optimization T	est #7C (50	ofh to P4-1	8 & P4-28	(100 cfh tota	al): ~79% N	2 10% H2	& I PG 1% (	:()2)		
	1121 Start		0, 01 120	(100 0111 1011	21), 707014	2, 1070112	1	, (C)		
4/11/2008			0.00	2.0	15.0		72.3		22.6	1012
4/11/2008		1.1	0.20	13.0			80.1		15.3	1012
4/16/2008			0.38	11.0			62.7		17.0	1011
4/22/2008	1001	0.0	0.38	9.5	13		91.6		15.9	1009

	Ī			Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
4/23/2008	919	0.0	0.22	10.0	4.1		76.3		13.4	1010
4/25/2008	1014	0.7	0.22	9.5	0.10		60.2		23.9	1015
4/29/2008	1123	0.0	0.16	9.0	6.1		66.8		25.5	1007
5/5/2008	1328	0.0	0.24	8.5	9.3		39.1		38.2	1001
5/13/2008	952	1.0	0.36	9.0	1.7		40.6		35.2	1007
5/20/2008	950	0.0	0.38	8.0	15		66.5		22.9	1004
5/23/2008	1538	2.2	0.28	7.5	7.3		57.5		29.0	990
5/27/2008	922	0.0	0.56	9.5	7.8		70.0		18.1	1007
6/4/2008	924	0.0	0.36	9.5	5.4		63.4		25.2	1002
6/12/2008	1220	0.9	0.34	8.5	2.6		31.2		42.7	1003
6/20/2008	1048	0.0	0.50	8.5	5.6		33.2		41.3	1005
6/25/2008	1103	0.0	0.44	8.5	11.0		53.6		31.4	1005
7/2/2008	1207	0.0	0.50	9.0	11.0		54.1		33.2	1004
7/7/2008	1153	0	0.4	9.0	6.3		41.5		36.3	998
7/18/2008	1120	0	0.42	9.0	9.2		80.1		26.7	
7/24/2008	1036	0.0	0.36	9.0	11.000		68.7		27.2	1005
7/31/2008	1031	0.0	0.46	9.5	10.000		75.5		26.2	1003
8/7/2008	909	0.0	0.46	9.5	8.7		85.1		20.7	1004
8/12/2008	1013	0.0	0.28	9.0	9.8		52.3		28.7	1002

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #8 (100	cfh of 100%	6 Propane to	D P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1104	8.3	0.48	6.0	0.002					999
9/15/2008	930	4.4	1.9	5.0	0.005		46.6		27.0	1007
9/29/2008	958	9.3	3.30	3.0	0.005		56.8		24.0	1006
10/13/2008	1216	3.8	0.42	30	0.005		46.2		27.8	1017
10/20/2008	1143	2.4	0.48	30	0.005		57.4		27.3	1013
11/5/2008	1333	2.0	0.52	30	0.005		77.9		19.0	1016
11/17/2008	1129	1.6	0.48	30	0.005		62.1		26.4	1014
12/1/2008	1101	1.7	0.52	30	0.002		65.3		20.6	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P3\_\_

Well ID \_\_\_\_\_P3\_\_\_\_ Depth \_\_\_28\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1230	19.8	0.14	0	0.002	100,000	76.3	0.02	12.7	1020
12/12/2007	1536							0.22		
12/13/2007	856	11.3	0	0	7.4		80.4		6.4	1016
12/13/2007	943	14.1	0	0	7.7		68.5		11.4	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	07 before 12	200 invalid			
12/13/2007	1320							0.18		
12/13/2007	1330	0	0	0	8.4		64.2		16.8	1013
12/13/2007	1452	0	0.44	0.52	0.46		73.7		14.3	1013
12/13/2007	1525	0	0.60	0.52	0.22		73.9		13.9	1013
12/14/2007	820	0	0.14	0	0.5		77.0	0.03	4.6	1016
12/21/2007	1131	14.9	0.44	0.02	0.46		80.8	0.02	10.2	1013
12/26/2007	1203	17.7	0.42	0	0.22		76.6	0	12.9	1017
12/26/2007	1508	13.8	0.5	0.02	0.46		86.5		10.4	1015
12/26/2007	1555	6.1	0.52	0.02	2.6		82.5	0.04	10.6	1015
12/27/2007	946	0.2	0.04	0.02	9.4		78	0.02	5.6	1018
12/27/2007	1250	0.2	0	0	9.2		80.4		9	1017
12/27/2007	1419	0.1	0	0	9.4		86.6		8.8	1017
12/27/2007	1540	0.2	0	0	9.6		89.3	0.03	7.6	1017
1/2/2008	1008	0.1	0	0	0.022		49.6	0.02	15.6	1012

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Tracer Test #1	(10 cfm to II	NJ2, ~7% H	l2)						
1/21/2008	1046 Test s	start							
1/21/2008	1117	6.1	0	0	0.10	78.4	0.06	8.4	1008
1/21/2008	1259	5.6	0	0	3.9	76.6		10.5	1006
1/21/2008	1452	5.5	0	0	5.4	74.5	0.06	10.8	1006
1/21/2008	1617	5.6	0	0	5.6	78.3	0.06	9.9	1006
1/22/2008	1049	4.9	0	0	6.8	81.4	0.01	6.7	1011
1/22/2008	1339	4.5	0	0	6.8	86.7		7.7	1009
1/23/2008	1051	4.7	0	0	6.8	98.1	0.04	7.3	1008
1/23/2008	1204*	4.5							

Tracer Test #2	(20 cfm to II	NJ2, ~8% H	12)						
1/18/2008	1120 Test s	start							
1/18/2008	1139	5.0	0	0	0.046	88.4		12.7	1015
1/18/2008	1237	4.9	0	0	5.3	81.4	0.01	13.8	1014
1/18/2008	1328	5.3	0	0	6.6	74.5		15.4	1014
1/18/2008	1513	4.8	0	0	6.8	64.5	0.04	17.5	1014
1/19/2008	940	4.9	0.06	0	8.4	67.1	0.02	13.0	1019
1/19/2008	1105*	4.6	0	0	6.4	56.2		16.8	1018

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			

Tracer Test #3	(30 cfm to II	NJ2, ~4% H	2)						
1/30/2008	1036 Test s	start							
1/30/2008	1146	0.1	0	0	4.0	94.7	0.09	9.8	1020
1/30/2008	1304	0.1	0	0	4.1	95.0	)	11.9	1019
1/30/2008	1510	0.1	0	0	4.2	84.7	0.11	14.8	1018
1/31/2008	1024	0.1	0	0	4.0	89.5	0.14	9.0	1018
1/31/2008	1158	0.1	0	0	3.7	88.8	3	9.3	1018
1/31/2008	1416	0.1	0	0	3.7	85.4	0.14	8.6	1016
1/31/2008	1435								
1/31/2008	1550	0.1	0	0	3.7	85.2	0.05	8.2	1014

Tracer Test #4	(60 cfm to II	NJ2, ~7% H	12)						
1/28/2008	1/28/2008 1236 Test start								
1/28/2008	1309	0.2	0	0	5.6	96.2		10.7	1010
1/28/2008	1439	0.1	0	0	5.9	79.8	0.05	12.9	1011
1/28/2008	1624	0.1	0	0	6.3	88.6	0.11	9.2	1012
1/29/2008	839	0.1	0	0	6.8	89.4	0.22	5.1	1017
1/29/2008	1018*	0.2			6.4				

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 28 Well or Injection Gas Sample Well **Ambient Air** Propane CO2 RH Temperature Barometric pressure  $O_2$  $H_2$ He Pressure Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (mbar) Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1106 2/5/2008 0.1 0 3.0 96.3 0.28 10.6 1019 2/5/2008 1206 0.1 0 0 3.1 94.0 11.1 1019 0 0 2/5/2008 1412 0.1 3.6 88.0 0.28 12.6 1018 0 2/5/2008 1533 0.1 0 3.4 69.1 15.3 1019 0.1 0 0 3.3 16.0 2/5/2008 1615 65.1 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 1515 0.1 0 0.046 2/7/2008 0 55.3 21.4 1016 1606 0.1 44.8 2/7/2008 0 0 2.0 24.8 1016 2/8/2008 948 0.1 0 0 8.9 0.04 66.3 14.7 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1016 16.6 0 0 0.64 96.3 0.01 8.1 1015 1/17/2008 1114 15.7 1.2 94.8 0.03 9.5 1015 1/17/2008 1226 12.8 0 0 2.4 79.6 10.7 1014 11.7 85.7 1/17/2008 1322 12.0 0.08 0 2.6 1013 1/17/2008 3.7 1449 9.9 0.08 0 13.4 0.03 12.8 1012

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 28 **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (mbar) Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 1016 2/6/2008 0.1 0 0 0.50 85.0 0.36 11.5 1020 2/6/2008 1120 0.1 0 0 3.4 86.8 11.9 1020 0 2/6/2008 1227 0.1 0 3.9 89.0 13.3 1019 2/6/2008 1411 0.1 0 0 4.7 80.3 0.39 15.7 1017 0.1 0 0 4.5 16.5 2/6/2008 1521 71.5 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 1157 7.7 2/20/2008 0.00 0.1 71.2 14.9 1010 2/20/2008 1206 Test start 2/20/2008 1532 0.1 0.88 1.02 11 56.9 22.5 1007 2/20/2008 1606 Test End 2/20/2008 1654 0.1 0.72 1.04 9.3 54.9 21.1 1008 2/21/2008 952 2.8 0.58 0.7 6.7 83.6 10.7 1005 2/22/2008 6.8 0.44 0.4 2.1 82.8 10.2 1110 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 742 0.1 2.16 0.48 6.7 86.8 5.1 1017 2 2/27/2008 1611 4.9 1.18 0.32 48.9 28.3 1009

2/28/2008

1121

7.1

1.02

0.26

0.85

82.2

16.6

1007

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 28 **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1508 8.1 0.1 0.82 0.24 53.2 25.7 1009 3/3/2008 1115 7.7 0.74 0.36 1.8 66.5 16.1 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 1001 10.2 0.7 0.22 1.6 78.9 14.7 1013 1133 3/7/2008 10.1 0.4 0.18 1.8 66.7 20 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 1355 3/7/2008 8.8 0.38 0.28 2.8 59.3 22.9 1016 3/10/2008 1118 9.4 0.46 0.4 0.046 80.2 17.3 1016 Optimization Test #4 (2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 1240 9.7 0.56 0.4 0.022 68.2 21 1016 3/10/2008 1322 6.3 0.56 2.5 2.2 1016 3/10/2008 1347 End pulse 3/10/2008 1413 1.7 0.64 6 8.1 60 22.5 1015 940 3.5 0.70 15.5 3/11/2008 4.5 4.1 66.9 1018

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 28 **Well or Injection Gas Sample** Well **Ambient Air** CO2 Temperature Barometric pressure  $O_2$ **Propane**  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) 3/12/2008 79 1006 0.66 2.9 12.9 5.3 1014 919 7.4 0.60 2.5 77 14 3/13/2008 1.8 1011 79.3 3/14/2008 1144 7.8 0.60 14.2 1013 3/14/2008 1219 6.7 0.56 2.9 76.3 14.8 1012 3/15/2008 1129 9.8 0.60 1.74 0.46 79.6 11.2 1009 3/16/2008 1115 9.8 0.44 1.7 0.5 73.6 14.2 1009 3/17/2008 928 9.6 0.56 0.55 70 9.5 1.7 1014 Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 3/17/2008 1037 Start Test 3/17/2008 1301 0.3 0.32 9.5 8.9 76.1 17.7 1014 3.7 3/8/2008 0.44 946 3.6 66.7 13.1 1016 0.42 3/19/2008 1004 6.9 1.7 73.7 12.4 1013 3/20/2008 7.7 78.8 9.8 949 0.44 1.4 1016 **End Test** 3/20/2008 ~1100 Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/21/2008 952 0.2 0.15 2.0 5.1 77.7 10.7 1020 1022 3/24/2008 0.1 0.00 2.5 4.2 68.4 16.1 1012 1037 0.1 2.0 5.0 87.9 3/26/2008 0.00 12.4 1017 3/28/2008 1004 0.1 2.0 2.0 70.3 10.7 1009 3/31/2008 1009 0.0 0.0 17.0 11.0 80.5 10.6 1013 4/2/2008 1114 0.0 0.0 14.5 8.2 72.2 16.7 1008

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 28 **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 957 4/4/2008 0.1 0.00 12.5 7.5 71.6 13.7 1013 73.1 4/7/2008 1427 3.0 0.00 8.5 3.6 19.3 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 1132 4/9/2008 5.7 0.00 6.0 3.2 86.5 15.3 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 4/11/2008 1252 4.6 0.20 2.5 6.1 66.9 22.7 1012 17.5 15.3 4/14/2008 1024 2.8 5.00 6.8 81.0 1007 4/16/2008 1043 0.0 0.54 9.5 8.6 65.9 17.1 1011 4/22/2008 1002 0.3 0.02 11.0 89.6 6.6 16.1 1009 0.046 4/23/2008 920 0.1 0.02 8.5 78.7 13.2 1010 4/25/2008 1016 0.0 0.02 9.0 0.10 59.5 23.7 1015 4/29/2008 1124 0.1 0.08 9.5 7.6 67.4 25.5 1007 5/5/2008 1328 0.1 0.98 9.5 8.1 40.8 38.3 1001 2.2 5/13/2008 953 0.1 1.42 9.5 41.7 35.0 1007 952 0.68 8.5 1.7 70.4 23.0 5/20/2008 0.1 1004 5.8 5/23/2008 1539 0.2 0.78 9.0 65.1 28.9 990 5/27/2008 923 0.1 2.26 10.0 8.4 76.1 18.4 1007

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
6/4/2008	925	0.1	0.04	10.0	6.4		62.6		25.2	1002
6/12/2008	1221	0.1	0.94	10.0	2.5		34.7		42.8	1003
6/20/2008	1050	0.1	0.16	9.5	5.900		31.8		41.3	1005
6/25/2008	1104	0.0	1.06	9.5	10.0		62.2		31.1	1005
7/2/2008	1208	0.1	1.44	10.0	10.0		56.3		34.6	1004
7/7/2008	1154	0.1	0	8.0	3.5		52.5		36.4	998
7/18/2008	1121	0.1	0	10.0	9		90.7		26.9	
7/24/2008	1037	0.1	0.54	9.5	11.000		73.7		27.3	1005
7/31/2008	1032	0.0	1.26	10.0	11.000		69.3		26.1	1003
8/7/2008	910	0.2	0.02	9.0	10		82.6		20.8	1004
8/12/2008	1014	0.1	0.00	10.0	10		55.2		28.6	1002
Optimization Te	est #8 (100 d	ofh of 100%	Propane to	P4-18, & P	4-28 (50 cfl	n to each po	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1106	4.4	1.16	30.0	0.005					999
9/15/2008	932	10.2	1.88	24	0.005		44.3		27.2	1007
9/29/2008	959	7.6	1.75	30	0.005		42.9		23.8	1006
10/13/2008	1218	3.8	0.08	30	0.022		51.4		27.2	1017
10/20/2008	1144	2.9	0.12	30	0.005		57.9		27.4	1013
11/5/2008	1334	3.4	0.16	30	0.005		80.5		19.1	1016
11/17/2008	1130	2.0	0.16	30	0.005		63.4		26.1	1014
12/1/2008	1102	1.9	0.18	30	0.002		65.1		20.6	1014

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1231	19.4	0.00	0	0.002	60,000	80.9	0.01	12.7	1020
12/12/2007	1535							0.22		
12/13/2007	857	8.6	0	0	3.3		82.2		6.9	1016
12/13/2007	943	11.5	0	0	3.6		74.5		11.2	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	for 12/13/0	7 before 120	00 invalid			
12/13/2007	1321							0.21		
12/13/2007	1331	0	0	0	8.3		70.8		16.6	1013
12/13/2007	1454	0	0.06	0.30	4.1		80.0		14.5	1013
12/13/2007	1527	0	0.12	0.38	2.6		80.2		13.5	1013
12/14/2007	822	0	0.02	0.08	0.5		78.7	0.02	4.9	1016
12/21/2007	1133	14.4	0.04	0.04	0.46		82.4	0.01	9.9	1013
12/26/2007	1205	18.6	0		0.22		68.6	0.02	13.4	1017
12/26/2007	1509	16.7	0	0.02	0.22		87.8		10.3	1015
12/26/2007	1557	16.9	0	0.02	0.22		83.1	0.08	10.6	1015
12/27/2007	948	7.8	0	0.04	3.6		80.5	0.02	5.7	1018
12/27/2007	1252	8.1	0	0	4.5		82.8		8.9	1016
12/27/2007	1420	7.6	0	0	5.1		87.6		8.8	1017
12/27/2007	1541	7.1	0	0	5.7		90.3	0.04	7.6	1017
1/2/2008	1009	0.6	0.04	0	0.22		49.6	0.02	15.9	1012

				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Tracer Test #1	(10 cfm to I	NJ2, ~7% ⊢	l2)						
1/21/2008	1046 Test s	start							
1/21/2008	1118	1.9	0.02	0	0.10	77.1	0.06	8.6	1008
1/21/2008	1301	1.7	0	0	0.046	75.3		10.5	1006
1/21/2008	1453	1.7	0	0	0.046	74.6	0.06	10.8	1006
1/21/2008	1616	1.8	0	0	0.79	80.5	0.04	9.9	1006
1/22/2008	1047	1.2	0.06	0	6.1	84.1	0.06	6.7	1011
1/22/2008	1340	1.0	0	0	6.3	87.6		7.8	1009
1/23/2008	1053	1.0	0.06	0	6.7	98.2	0.05	7.3	1008
1/23/2008	1206*	0.8							

Trace	r Test #2	(20 cfm to I	INJ2, ~8% H	H2)						
1/	/18/2008	1120 Test s	start							
1/	/18/2008	1140	1.4	0	0	0.10	87.3		12.7	1015
1/	/18/2008	1239	1.4	0	0	0.10	78.7	0.01	13.7	1014
1/	18/2008	1330	1.6	0	0	0.22	74.3		15.3	1014
1/	18/2008	1514	1.5	0	0	2.6	62.9	0.04	17.0	1014
1/	/19/2008	941	1.3	0.08	0	10.0	65.2	0.01	13.4	1019
1/	/19/2008	1106*	0.8	0.02	0	9.3	54.2		17.3	1018

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P3\_\_\_\_ Depth \_\_\_38\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure CO<sub>2</sub> RH O<sub>2</sub> Propane H<sub>2</sub> He Pressure Date Time (C°) (mbar) (%) (%) (%) (%) (ppm) (%) (in wc)

Tracer Test #3	(30 cfm to I	INJ2, ~4% H	12)						
1/30/2008	1036 Test s	start							
1/30/2008	1149	0.0	0	0	1.0	95.8	0.12	9.9	1020
1/30/2008	1301	0.0	0	0	1.9	94.6		11.9	1019
1/30/2008	1511	0.0	0	0	3.6	87.2	0.11	14.7	1018
1/31/2008	1026	0.0	0	0	4.1	90.0	0.13	9.0	1018
1/31/2008	1159	0	0	0	3.9	88.5		9.3	1018
1/31/2008	1420	0	0.02	0	3.8	85.3	0.11	8.5	1016
1/31/2008	1435								
1/31/2008	1551	0	0	0	3.7	84.8	0.05	8.1	1014

Tracer Test #4	(60 cfm to	INJ2, ~7% H	H2)						
1/28/2008	1/28/2008 1236 Test start								
1/28/2008	1311	2.4	0.04	0	0.2	96.9		10.6	1010
1/28/2008	1441	0.4	0.04	0	4.7	85.7	0.11	12.8	1011
1/28/2008	1625	0.3	0.04	0	5.4	88.3	0.21	9.2	1012
1/29/2008	841	0	0.08	0	7.1	92.8	0.21	5.0	1017
1/29/2008	Final O2*	0							

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air** Propane CO<sub>2</sub> Temperature Barometric pressure  $O_2$  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (Co) (mbar) Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1107 0.7 2/5/2008 1.3 97.3 0.39 10.6 1019 2/5/2008 1207 0.4 0 0 2.5 94.1 11.1 1019 0.2 12.5 2/5/2008 1413 0 0 3.3 89.5 0.32 1018 2/5/2008 1534 0.1 0 0 3.3 71.8 14.8 1019 0.1 1616 0 0 3.3 66.2 15.6 2/5/2008 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 1516 0.0 0.02 0.046 56.7 2/7/2008 21.3 1016 1607 0.0 2/7/2008 0 0 0.10 46.3 23.9 1016 2/8/2008 949 0.0 0 0 8.7 0.00 66.6 15.1 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 8.4 1014 0 2.0 95.9 0.02 8.0 1015 7.8 9.8 1/17/2008 1115 2.8 96.0 0.02 1015 1/17/2008 1231 5.5 0 0 3.8 90.9 10.8 1014 3.4 1/17/2008 1324 0.06 0 4.2 87.4 11.6 1013 1/17/2008 2.7 1452 0.06 0 5.0 80.8 0.02 12.9 1012

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (Co) (mbar) Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 1017 2/6/2008 0.1 0 0.55 84.1 0.32 11.8 1020 12.0 2/6/2008 1121 0.0 0 0 2.1 88.7 1020 2/6/2008 1229 0.0 0 0 2.8 90.8 13.4 1019 2/6/2008 1412 0.0 0 0 4.2 82.2 0.30 15.7 1017 1522 0.0 0 0 4.2 2/6/2008 73.4 16.4 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 1158 7.2 2/20/2008 0.00 0.046 70.6 14.9 1010 2/20/2008 1206 Test start 2/20/2008 1533 0.4 0.00 0.94 11 56.4 21.9 1007 2/20/2008 1606 Test End 2/20/2008 1656 0.2 0.00 0.96 10 54.9 21 1008 2/21/2008 953 1.3 0.02 0.92 6.9 82.2 10.7 1005 2/22/2008 1111 6 0.00 10.2 0.42 1.7 82.6 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 744 0.1 0.16 0.64 6.6 86.4 5.2 1017 3.0 2/27/2008 1612 0.12 0.42 49.8 29.8 1009 1.4 2/28/2008 1122 6.3 0.08 0.28 0.46 82.9 16.7 1007

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air** Pressure Barometric pressure  $O_2$ CO2 Propane H<sub>2</sub> He RH Temperature Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (Co) (mbar) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 7.3 2/29/2008 1509 0.046 1009 0.04 0.26 54.3 24.9 71 3/3/2008 1116 12 0.12 0.08 0.022 1019 16.1 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 1003 12.1 0.14 0.08 0.022 77.6 14.7 1013 12.1 0.022 3/7/2008 1134 0.04 0.08 67.5 20 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 12 1357 3/7/2008 0.02 0.06 0.022 60.6 22.8 1016 3/10/2008 1119 9.9 0.08 0.2 0.046 71.8 17.4 1016 Optimization Test #4 (2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 1241 10.1 0.22 0.022 67.8 0.14 21.1 1016 3/10/2008 1323 10.0 0.14 0.22 0.046 65.7 21.6 1016 1347 End pulse 3/10/2008 3/10/2008 9.9 0.12 0.22 0.046 61.8 22.5 1015 1414 941 7.2 1.3 15.4 3/11/2008 0.14 1.68 67.6 1018

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air Barometric pressure**  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Temperature Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) 3/12/2008 81.2 12.9 1007 7.7 0.10 0.1 1014 921 9.0 0.08 1.8 0.046 76.7 14 3/13/2008 1011 1.36 3/14/2008 1145 10.3 0.10 0.022 78.5 14.3 1013 14.8 3/14/2008 1220 10.2 0.08 1.34 0.022 76.4 1012 3/15/2008 1130 11.6 0.12 0.94 0.022 81.4 11.1 1009 1116 3/16/2008 12.0 0.04 0.84 0.022 74.5 14.2 1009 3/17/2008 930 12.1 0.022 70.3 9.7 0.12 0.98 1014 Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 1037 Start Test 3/17/2008 3/17/2008 1302 11.3 0.04 0.98 0.5 79.7 17.8 1014 3/8/2008 947 7.6 0.08 1.1 67.6 13.2 1016 0.57 3/19/2008 1005 6.3 0.08 4.5 73.9 12.4 1013 3/20/2008 950 6.7 0.22 9.9 1016 0.08 78.4 End Test 3/20/2008 ~1100 Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 6.5 3/21/2008 954 0.12 4.0 0.50 86.7 11.0 1020 1012 3/24/2008 1032 6.8 0.16 2.0 0.10 76.7 16.6 5.7 1038 2.0 0.22 91.5 12.4 1017 3/26/2008 0.12 3/28/2008 1005 5.1 0.14 2.0 0.2 68.0 10.7 1009 3/31/2008 1010 0.0 0.12 13.5 5.6 83.3 10.6 1013 4/2/2008 1115 0.0 0.14 13.0 3.6 72.3 16.7 1008

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air Barometric pressure**  $O_2$ CO2 Propane H<sub>2</sub> He RH Pressure Temperature Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (Co) (mbar) Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 0.0 4/4/2008 958 2.8 75.8 0.12 3.0 13.8 1013 4/7/2008 1429 3.2 0.12 9.5 0.5 76.4 19.1 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 1133 4.5 4/9/2008 0.06 8.5 0.046 86.0 15.3 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 4/11/2008 1244 4.9 0.12 8.0 0.1 67.8 22.7 1012 1025 0.0 81.2 15.2 1007 4/14/2008 4.14 25.0 8.2 4/16/2008 1044 0.5 2.78 11.5 2.8 63.9 17.2 1011 4/22/2008 1004 3.3 1.14 4.0 1.0 78.5 16.3 1009 4/23/2008 922 0.22 0.0 1.10 75.3 13.1 1010 8.5 4/25/2008 1018 0.0 0.86 9.5 0.10 58.3 23.6 1015 4/29/2008 1126 0.0 0.74 1.6 66.1 25.7 1007 8.5 5/5/2008 1330 1.2 0.44 6.5 0.67 39.7 38.5 1001 5/13/2008 954 0.0 0.60 9.5 1.0 41.8 34.9 1007 953 0.0 0.78 8.5 0.10 71.9 23.0 1004 5/20/2008 5/23/2008 1541 4.4 0.62 6.5 0.10 61.5 28.8 990 5/27/2008 924 1.1 0.64 7.5 1.0 74.4 18.6 1007

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P3\_\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

	1			Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
6/4/2008	926	0.0	0.46	8.0	1.1		64.0		25.3	1002
6/12/2008	1223	0.5	0.48	8.5	0.22		31.3		43.1	1003
6/20/2008	1051	0.0	0.44	8.0	1.1		33.2		41.5	1005
6/25/2008	1105	0.0	0.40	8.0	0.10		58.3		30.9	1005
7/2/2008	1209	0.0	0.40	8.0	0.50		48.1		35.6	1004
7/7/2008	1156	0	0.42	7.5	1.3		44		36.4	998
7/18/2008	1123	0	0.54	8.0	0.78		81.4		26.9	
7/24/2008	1030	0.0	0.58	8.0	0.65		69.4		27.4	1005
7/31/2008	1033	0.0	0.64	8.0	1.2		72.8		26.2	1003
8/7/2008	911	0.0	0.68	8.5	1.5		81.8		20.7	1004
8/12/2008	1015	0.0	0.64	8.5	1.2		58		28.7	1002
Optimization T	est #8 (100	cfh of 100%	Propane to	P4-18, & P	4-28 (50 cfh	to each po	int)			
9/8/2008	0905 Test S	Start								
9/8/2008	1108	3.2	2.00	27.0	0.005					999
9/15/2008	933	1.1	1.32	30	0.005		43.5		27.2	1007
9/29/2008	1000	0.2	0.62	30	0.005		42.2		23.5	1006
10/13/2008	1219	0.8	0.30	30	0.010		47.2		27.0	1017
10/20/2008	1146	0.4	0.28	30	0.005		57.8		27.5	1013
11/5/2008	1335	0.4	0.26	30	0.005		78.6		19.5	1016
11/17/2008	1130	0.1	0.20	30	0.010		66.4		26.0	1014
12/1/2008	1102	0.0	0.18	30	0.005		65.7		20.7	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P3\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample		Well	Ambient Air	
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1232	20.7	0.00	0	0.002	100,000	76.3	0.02	12.7	1020
12/12/2007	1535							0.16		
12/13/2007	859	14.0	0	0	1.0		75.6		7.5	1016
12/13/2007	945	17.0	0	0	1.3		71.0		10.9	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	07 before 12	200 invalid			
12/13/2007	1321							0.05		
12/13/2007	1332	0	0.04	0	8.0		63.4		16.6	1013
12/13/2007	1456	0	0.06	0.22	5.7		71.0		14.5	1013
12/13/2007	1528	0	0.04	0.38	3.0		77.0		13.1	1013
12/14/2007	824	0	0.04	0.28	1.7		76.3	0.02	4.9	1016
12/21/2007	1135	20.9	0.08	0	0.22		85.6	0.02	9.6	1012
12/26/2007	1207	20.9	0.02	0	0.022		69.9	0	13.7	1017
12/26/2007	1510	20.9	0.02	0	0.22		87.2		10.3	1015
12/26/2007	1600	20.7	0.02	0	0.22		83.4	0.09	10.5	1015
12/27/2007	950	209	0.04	0.02	0.22		78.7	0.02	5.6	1018
12/27/2007	1254	20.9	0	0	0.22		82.5		8.9	1016
12/27/2007	1423	20.9	0	0	0.22		86.7		8.7	1017
12/27/2007	1543	20.9	0	0	0.22		90.7	0.03	7.5	1017
1/2/2008	1011	20.9	0.08	0	0.22		48.1	0.02	16.5	1012

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P3\_\_\_\_ Depth \_\_\_48\_\_\_\_

1/18/2008

1/19/2008

1/19/2008 1108\*

1515

942

7.1

5.8

5.1

0.02

0.14

0.06

Phase II Piez	ometer Mo	nitoring Da	ta	Well ID	P3		Depth	48		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #	1 (10 cfm to	INJ2, ~7%	H2)							
1/21/2008	1046 Test	start								
1/21/2008	1119	4.8	0.06	0	1.3		90.6	0.07	8.9	1008
1/21/2008	1303	4.8	0.06	0	1.2		77.6		10.4	1006
1/21/2008	1455	13.8	0.06	0	0.22		81.8	0.09	10.8	1006
1/21/2008	1615	18.7	0.04	0	0.046		83.4	0.03	9.9	1006
1/22/2008	1050	20.9	0.10	0	0.022		82.8	0.03	6.8	1011
1/22/2008	1342	20.7	0.04	0	0.022		88.3		7.9	1009
1/23/2008	1055	20.9	0.08	0	0.022		98.4	0.04	7.3	1008
1/23/2008	1207*	20.9								
Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)							
1/18/2008	1120 Test	start								
1/18/2008	1141	5.2	0	0	1.2		91.6		12.8	1015
1/18/2008	1241	5.6	0.02	0	1.2		87.5	0.01	13.8	1014
1/18/2008	1331	6.4	0	0	1.2		73.1		15.2	1014

0

0

0

1.1

3.3

4.1

64.7

62.9

63.6

0.03

0.01

17.1

13.9

17.6

1014

1019

1019

**Phase II Piezometer Monitoring Data** Well ID P3\_ Depth 48

Filase II Flez	Officier Moi	intorning Da	ıa	well ID	1		Deptii	<del></del>		
					Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #3	3 (30 cfm to	INJ2, ~4%	H2)							
1/30/2008	1036 Test s	start								
1/30/2008	1149	1.0	0.10	0	1.1		95.9	0.12	9.8	1020
1/30/2008	1305	0.5	0.16	0	0.97		96.7		12.0	1019
1/30/2008	1512	0.4	0.18	0	1.5		90.3	0.09	14.7	1018
1/31/2008	1027	0.1	0.28	0	2.7		91.5	0.12	8.9	1018
1/31/2008	1200	0.1	0.32	0	3.2		91.9		9.3	1018
1/31/2008	1421	0.1	0.34	0	3.1		90.4	0.12	8.4	1015
1/31/2008	1435									
1/31/2008	1552	0.1	0.32	0	3.1		89.6	0.12	8.2	1014
Tracer Test #4	4 (60 cfm to	INJ2, ~7%	H2)							
1/28/2008	1236 Test s	start								
1/28/2008	1312									
1/28/2008	1442							0.03		
1/28/2008	1627									
1/29/2008	842	1.1	0.82	0	5.4		94.7	0.19	5.0	1017
1/29/2008	Final O2*	1.1								

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 48 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Time Date (%) (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1108 1.1 0.30 0 0.046 97.7 0.26 10.6 1019 1208 1.2 0.22 2/5/2008 0.32 0 93.6 11.1 1019 0.22 2/5/2008 1414 1.1 0.36 0 0.10 94.9 12.6 1018 1535 0.65 69.2 0.44 0 14.6 2/5/2008 1.1 1019 2/5/2008 1617 1.1 0.44 0 0.88 65.9 16.4 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 1517 0.0 0.28 0 0.54 50.9 21.1 1016 1608 0.0 2/7/2008 0.28 0 0.46 44.8 23.5 1016 2/8/2008 950 0.0 0.26 0 5.1 65.7 0.06 15.4 1017 1047 0.1 95.0 10.5 2/8/2008 0.24 0 5.4 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1018 13.6 0 0 0.22 96.3 0.01 8.3 1015 1/17/2008 1118 12.4 0 0 0.22 96.8 0.02 9.9 1015

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P3\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Temperature	Barometric pressure				
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/17/2008	1232	11.8	0	0	0.22		94.5		10.8	1014
1/17/2008	1329	11.1	0.12	0	0.85		95.0		11.6	1013
1/17/2008	1456	10.3	0.12	0	1.6		82.7	0.02	12.9	1012

Tracer Test #	8 (90 cfm to	tal; 30 cfm	each to INJ	1, 2, and 3;	~4.5% H2)				
2/6/2008	1000 Test :	start							
2/6/2008	1019	0.3	0.34	0	0.022	77.7	0.22	12.3	1020
2/6/2008	1122	0.1	0.32	0	0.70	84.8		12.1	1020
2/6/2008	1229	0.1	0.28	0	1.7	83.9		13.4	1019
2/6/2008	1413	0.0	0.26	0	2.8	75.6	0.22	15.7	1017
2/6/2008	1523	0.0	0.24	0	3.0	68.9		16.2	1017
2/6/2008	1612	0.0	0.32	0	3.6				1017

Optimization T	est #1 (90 o	cfm to INJ2	for 4 hours	then shut d	own; ~88%	N2, 10% H2, 1	1% CO2	& LPG)		
2/20/2008	1159	20.9	0.12	0	0.022		72.7		14.7	1010
2/20/2008	1206 Test s	start								
2/20/2008	1535	3.8	0.36	0.02	0.71		58.7		21.8	1007
2/20/2008	1606 Test I	End								
2/20/2008	1657	3.8	0.30	0.04	0.74		55.5		20.8	1008
2/21/2008	955	20.9	0.12	0	0.022		85		10.7	1005
2/22/2008	1112	20.9	0.08	0	0.022		83.5		10.2	1003

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 48 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 0.18 2/26/2008 745 7.0 0.01 87.7 5.2 1017 0.14 7.6 0.022 2/27/2008 1614 0.1 0.06 53.1 27.3 1009 7.2 0.022 2/28/2008 1124 0.06 0.06 83.8 16.7 1007 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1509 6.8 0.02 0.08 0.01 57.2 24.2 1009 1117 3/3/2008 0.1 0.06 0.01 67.9 16.1 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 1004 7.2 0.16 0.06 0.022 78.2 14.8 1013 0.04 1132 19.9 0.005 72.2 20 1018 3/7/2008 3/7/2008 1306 Test End

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 48 Well or Injection Gas Sample Well **Ambient Air**  $O_2$ CO<sub>2</sub> **Propane**  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1357 16.4 0.04 0 0.01 61.9 22.7 1016 1120 19.8 80.7 3/10/2008 0.08 0 0.01 17.4 1017 Optimization Test #4 (2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 1415 15.0 0.02 0.005 3/10/2008 0.12 62.8 22.5 1015 3/12/2008 1008 82.6 0 0.01 20.6 0.10 12.9 1014 3/13/2008 922 20.7 0.06 0 0.01 79.4 14.1 1011 3/14/2008 1146 20.8 0.08 0 0.01 79.4 14.4 1012 3/14/2008 1221 0.02 0.05 0.005 77.9 14.8 1012 19.4 3/15/2008 1131 20.7 0.06 0 0.01 83.7 11.1 1009 3/16/2008 0.01 1118 18.9 0.00 0.02 75.1 14.3 1009 3/17/2008 931 18.6 0.10 0 0.01 71.7 9.7 1014 Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 1037 Start Test 3/17/2008 3/17/2008 1303 12.9 0.06 0.26 0.022 82.1 17.8 1014 0.022 71.9 3/8/2008 948 19.7 0.08 0 13.3 1016

**Phase II Piezometer Monitoring Data** Well ID P3 Depth 48 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ **Propane** He RH **Pressure** Temperature **Barometric pressure**  $H_2$ Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) 3/19/2008 1006 0 0.022 77.9 12.4 1013 19.7 80.0 20.5 0.022 79.8 3/20/2008 951 0.10 0 10 1016 3/20/2008 ~1100 End Test Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/21/2008 956 19.7 0.10 0 0.01 77.9 11.2 1020 3/24/2008 1033\* 12.9 0.78 0.022 16.6 0.24 73.8 1012 0.01 93.8 1040 20.7 0 12.5 3/26/2008 0.14 1017 3/28/2008 1006 18.9 0.18 0.06 0.010 72.6 10.7 1009 3/31/2008 1012 16.1 0.18 0.84 0.022 89.4 10.8 1013 1116 5.4 0.046 16.7 4/2/2008 0.30 7.5 70.4 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 959 3.9 0.046 0.34 7.5 74.4 13.8 1013 9.6 4/7/2008 1430 0.42 5.0 0.046 75.6 19.1 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 8.3 88.0 4/9/2008 1135 0.32 5.0 0.01 15.4 1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P3\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample	!		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Date	Time	(70)	(70)	(70)	(70)	(PPIII)	(70)	(111 110)	(0)	(IIIbai)
Optimization 1	Test #7C (50	) cfh to P4-1	18, & P4-28	(100 cfh to	tal); ~79% N	N2, 10% H2	& LPG, 1%	5 CO2)		
	1121 Start				,,	,	,	,		
4/11/2008	1254	4.4	0.44	7.0	0.046		67.4		22.7	1012
4/14/2008	1027	2.3	0.52	9.0	0.1		81.7		15.3	1007
4/16/2008	1046	1.5	0.64	15.0	0.046		68.8		17.2	1011
4/22/2008	1005	0.2	1.08	8.0	0.046		78.1		16.4	1009
4/23/2008	923	0.1	1.26	9.0	0.10		76.1		13.1	1010
4/25/2008	1019	0.0	1.10	9.5	0.10		60.6		23.6	1015
4/29/2008	1127	0.0	0.98	10.0	0.1		68.2		26.2	1007
5/5/2008	1331	0.0	0.94	10.0	0.1		38.4		38.6	1001
5/13/2008	950	0.0	1.08	9.5	0.046		42.6		34.7	1007
5/20/2008	954	0.0	1.12	9.5	0.046		74.7		23.2	1004
5/23/2008	1542	0.0	1.38	8.0	0.22		60.2		18.7	990
5/27/2008	926	0.0	1.46	8.5	0.046		74.9		18.7	1007
6/4/2008	927	0.0	1.28	8.5	0.10		64.6		25.2	1002
6/12/2008	1224	0.0	1.28	8.5	0.10		20.6		43.2	1003
6/20/2008	1052	0.0	1.20	8.0	0.046		32.0		42.0	1005
6/25/2008	1106	0.0	1.20	8.0	0.10		54.7		30.8	1005
7/2/2008	1210	0.0	1.20	8.0	0.10		44.5		36.8	1004
7/7/2008	1157	0.0	1.08	7.5	0.1		45.1		36.6	998

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P3\_\_\_\_

Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample	<u> </u>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1124	0.0	1.18	7.5	0.046		84.4		26.9	
7/24/2008	1039	0.0	1.18	7.5	0.100		70.0		27.5	1005
7/31/2008	1034	0.0	1.24	7.5	0.100		70.8		26.3	1003
8/7/2008	912	0.0	1.24	7.5	0.22		87.8		20.8	1004
8/12/2008	1016	0.0	1.16	7.5	0.10		52.6		28.6	1002
Optimization 7	Test #8 (100	ofh of 1009	% Propane	to P4-18, &	P4-28 (50 d	fh to each	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1110	0.0	1.12	22.5	0.022					999
9/15/2008	934	0.0	2.52	30	0.005		46.9		27.2	1007
9/29/2008	1001	0.0	1.58	30	0.005		52.6		23.0	1006
10/13/2008	1220	0.0	1.50	30	0.010		52.0		26.6	1017
10/20/2008	1147	0.0	1.60	30	0.005		58.6		27.1	1013
11/5/2008	1337	0.0	1.08	30	0.005		79.8		19.8	1016
11/17/2008	1132	0.0	1.10	30	0.010		67.3		25.9	1014
12/1/2008	1103	0.0	1.16	30	0.005		66.3		20.7	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1240	18.8	0	0	0.002	50,000	84.2	0.02	12.6	1020
12/12/2007	1532							0.16		
12/12/2007	1550							0.18		
12/12/2007	1622	5.60				4x10^3				
12/12/2007	1629	6.20				4x10^3				
12/12/2007	1638	5.4				1x10^2				
12/13/2007	756	9.0	0	0	0.002	2x10^4	90.3		-0.2	1016
12/13/2007	835	5.2	0	0	0.46	7x10^3				1016
12/13/2007	924	12.0	0	0	5.5		65.1		9.9	1016
12/13/2007	1150	12.8	0	0			86.1		13.3	
12/13/2007	1200	Discovered	leak in O2	- all O2 data	for 12/13/0	7 before 120	00 invalid			
12/13/2007	1201	0.3	0	0			87.9		14.5	
12/13/2007	1314							0.16		
12/13/2007	1322	0.2	0	0	7.9		67.8		18.1	1014
12/13/2007	1431	0	0	0.02	8.5		78.6		15.9	1013
12/13/2007	1512	0	0	0.46	2.2		78.4		14.5	1013
12/13/2007	1546	0	0	0.48	1.4		76.4		12.9	1013
12/14/2007	808	0.9	0	0.08	0.81		78.1	0.02	2.5	1016
12/21/2007	1102	13.5	0.06	0.02	0.46		61.8	0.02	NA	1013
12/21/2007	1338	12.6	0	0.02	0.46		64.7		15.9	1012
12/26/2007	1210	13.8	0.04	0	0.022		70	0.07	14.3	1017
12/26/2007	1416	15.3	0	0.02	0.22		77.6		13.8	1015
12/26/2007	1432	15.5	0	0.02	0.22		76		13.1	1015
12/26/2007	1442	15.6	0	0.02	0.22		77.4		13.3	1013
12/26/2007	1455	15.7	0	0.02	0.22		82.3		11.7	1013
12/26/2007	1537	12.5	0	0.02	0.76		82.9		11.3	1015

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/26/2007	1616	11.4	0	0.02	1.1		82.9	0.06	9.9	1015
12/27/2007	931	1.4	0	0	8.3		71	0.04	5.2	1017
12/27/2007	1234	1.2	0	0	8.7		75.1		8.5	1017
12/27/2007	1409	1	0	0	9.1		82.1		9.5	1017
12/27/2007	1529	1	0	0	9.2		83.1	0.01	7.9	1017
1/2/2008	947	0.6	0	0	0.22		59.2	0.04	10.7	1012

Tracer Test #1	(10 cfm to l	NJ2, ~7% H	l2)						
1/21/2008	1046 Test s	start							
1/21/2008	1107	1.7	0	0	0.67	88.8	0.00	7.8	1008
1/21/2008	1125	1.7	0	0	0.67	83.4		9.8	1008
1/21/2008	1156	1.6	0	0	0.64	88.9		9.8	1007
1/21/2008	1242	1.4	0	0	1.0	76.7	0.06	10.1	1006
1/21/2008	1434	1.5	0	0	1.7	80.1	0.08	10.4	1006
1/21/2008	1600	1.3	0	0	2.6	85.2		10.0	1006
1/22/2008	914	1.1	0	0	6.0	80.7	0.04	7.4	1011
1/22/2008	1347	0.9	0	0	6.2	91.1		8.1	1009
1/23/2008	951	1.0	0	0	6.2	78.8	0.10	9.3	1008
1/23/2008	1213*	0.8							

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_\_18\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure 0, CO2 Propane H<sub>2</sub> He RH Pressure Date (%) Time (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 1/18/2008 1127 1.6 0.54 88.7 12.4 1015 1/18/2008 1.5 0 0.52 95.5 12.9 1146 1015 1/18/2008 0.22 1155 1.5 0 97.3 13.1 1015 1/18/2008 0 0.22 88.1 0.03 1209 1.5 13.0 1015 1/18/2008 1220 1.4 0 0 0.22 88.4 13.4 1015 81.2 0 1/18/2008 1320 1.2 1.9 15.8 1014 1/18/2008 1518 1.3 0 4.2 74.7 0.02 17.1 1014 1/19/2008 945 8.0 0.04 0 9.8 62.1 0.05 13.0 1019 1/19/2008 1054\* 8.0 9.4 57.7 16.2 1019 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1053 0.0 0 0.75 88.9 0.04 9.8 1020 1/30/2008 1204 0.0 0 1.8 91.8 10.5 1019 1/30/2008 1409 0.0 0 3.5 83.4 0.17 12.5 1018 1/31/2008 926 0.1 0 0 4.1 89.5 0.12 7.8 1019 1/31/2008 1123 0 0 3.6 83.7 9.6 1018 3.4 84.2 0.20 1/31/2008 1320 8.7 1017 1/31/2008 1435 1/31/2008 1458 0.1 3.4 87.5 0.06 8.2 1014

1/31/2008

1557

0

0

0

3.4

84.3

8.2

1014

Phase II Piezo	meter Mon	itoring Data	a	Well ID	P4	_	Depth			
	Ī			Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #4	(60 cfm to I	NJ2, ~7% F	l2)							
1/28/2008	1236 Test s	start								
1/28/2008	1244	4.7	0.04	0	0.010		96.3		10.5	1010
1/28/2008	1259	2.8	0.02	0	0.046		95.9		10.6	1010
1/28/2008	1339	0.8	0.02	0	3.2		93.0	0.14	12.3	1010
1/28/2008	1450	0.7	0	0	4.4		80.9		12.9	1011
1/28/2008	1536	0.5	0	0	4.7		83.5	0.16	10.2	1011
1/29/2008	745	0	0	0	7.1		80.7	0.15	5.5	1016
1/29/2008	1008*	0			6.4					
Tracer Test #5	(90 cfm to I	NJ2, ~3% F	l2)							
2/5/2008	1015 Test s	start								
2/5/2008	1019	0.4	0	0	0.046		75.8	0.20	8.6	1019
2/5/2008	1118	0.0	0	0	2.3		83.7		10.7	1019
2/5/2008	1327	0.0	0	0	3.6		87.1	0.20	12.3	1019
2/5/2008	1456	0.0	0	0	3.4		80.8		14.3	1019
2/5/2008	1542	0.0	0	0	3.3		66.4		17.0	1018
Tracer Test #6	(30 cfm tota	al; 10 cfm to	each INJ1,	2, and 3; ~8	3% H2)					
2/7/2008	1500 Test s	start								
2/7/2008	1519	0.0	0.02	0	0.59		51.1		21.0	1016
2/7/2008	1610	0.0	0	0	0.54		45.8		22.5	1016
2/8/2008	956	0.0	0	0	8.4		62.2		15.1	1017
2/8/2008	1054	0.0	0	0	8.1		86.4		11.0	1017

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_18\_\_\_

			Well or	Injection G	as Sample			Well	Ambient Air
	Pressure	Temperature	Barometric pressure						
Date Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Tracer Test #7	(60 cfm tota	al; 20 cfm to	each INJ1,	2, and 3, ~5	5% H2)				
1/17/2008	900 Test st	art							
1/17/2008	929	14.2	0	0	0.22	90.8	0.02	4.8	1015
1/17/2008	936	14.3	0	0	0.22	89.4		5.2	1015
1/17/2008	958	14.5	0	0	0.22	85.2		7.3	1015
1/17/2008	1058	13.1	0	0	0.66	87.5	0.02	8.7	1015
1/17/2008	1200	11.2	0	0	2.0	91.6		10.1	1015
1/17/2008	1331	8.1	0	0	3.4	96.6		11.9	1013
1/17/2008	1502	5.8	0	0	4.5	97.1	0.05	13.5	1012

Tracer Test #8	(90 cfm tota	al; 30 cfm ea	ach to INJ1,	2, and 3; ~4	4.5% H2)				
2/6/2008	1000 Test s	start							
2/6/2008	1021	0.0	0	0	0.61	82.1	0.18	12.1	1020
2/6/2008	1127	0.0	0	0	1.0	82.3		12.3	1020
2/6/2008	1234	0.0	0	0	2.2	80.2		13.6	1019
2/6/2008	1417	0.0	0	0	3.7	74.0	0.25	16.0	1017
2/6/2008	1526	0.0	0	0	3.8	68.7		16.3	1017
2/6/2008	1618	0.0	0	0	3.9	66.9		16.9	1017

**Phase II Piezometer Monitoring Data** Well ID P4 Depth \_\_\_\_18\_\_\_\_ Well or Injection Gas Sample Well Ambient Air Temperature Barometric pressure 0, CO2 Propane H<sub>2</sub> He RH Pressure Date Time (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1118 0.04 0.022 70.5 15.9 1010 2/20/2008 1206 Test start 8.0 0.00 33 2/20/2008 1516 0.8 11 29.7 1008 2/20/2008 1606 Test End 9.7 2/20/2008 1610 0.5 0.00 0.9 44.6 23.6 1008 2/21/2008 904 0.2 0.04 0.42 1.9 75.4 11.1 1005 2/22/2008 0.022 81.7 1021 8.0 0.08 0.16 10.4 1003 2/25/2008 1640 2.8 0.12 0.14 0.01 47.2 22.9 1017 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 0.22 6.7 91.2 2/26/2008 656 0.6 0.6 2.7 1017 2/27/2008 1522 0.1 0.36 0.22 53.2 0.1 31.5 1010 2/28/2008 1038 0.06 0.32 0.022 84.2 15.7 1008 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 0.00 0.36 0.046 51.5 2/29/2008 1409 1.4 23 1009 1.9 0.36 0.01 63.5 23.6 2/29/2008 1511 0 1009 3/3/2008 1031 0.6 0.6 3.3 72.4 14.7 1019 3/3/2008 1130 Test End

Phase II Piezo	ometer Mon	itoring Dat	a	Well ID	P4	_	Depth			
				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #3B (1 c	ofm to INJ1,	INJ2 & INJ3	s; ~88% N2,	10% H2, 19	% CO2 & LF	PG)			
3/3/2008	1130 Test 9	Start								
3/4/2008	919	0.4	0.04	0.64	1.8		82.3		10.8	1013
3/7/2008	1042	0.4	0	0.7	2		65.1		19	1018
3/7/2008	1306 Test I	End								
Optimization T	est #3C (90	cfm to INJ1	, INJ2 & IN	J3 for 15 mir	nutes then s	hut down; ~	79% N2, 109	% H2 & LPG, 1	1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1327	1.6	0	0.66	3.9		52.5		23.7	1016
3/7/2008	1400	1.6	0	0.66	3.4		57.9		22.4	1016
3/10/2008	1031	1.2	0.04	0.68	0.22		81.9		15.7	1016
Optimization T	est #4 ( 2, 4	5-minutes p	ulses; daily	15-minutes	pulses w/30	cfh constar	t flow)			
3/10/2008	1236	3.2	0.08	0.68	0.046		65.5		20.7	1016
3/10/2008	1257	5.6	0.08	0.66	0.022					
3/10/2008	1333	6.6	0.14	0.58	0.046		59.4		22.1	1016
3/10/2008	1347	End pulse								
3/10/2008	1402	6.7	0.10	0.6	0.022		53.2		22.6	1015
3/11/2008	904	3.8	0.08	1.12	0.046		60.3		15.6	1017
3/12/2008	952	0.0	0.06	2.5	0.8		84.5		12	1014
3/13/2008	908	0.0	0.04	3.5	1.5		84.1		13.6	1011
3/14/2008	1134	0.8	0.08	2	0.022		92		13.3	1013
3/14/2008	1209	0.4	0.04	3.5	1.8		81		15	1012
3/15/2008	1116	1.6	0.12	1.26	0.022		82.9		11	1009
3/16/2008	1105	2.4	0.04	0.82	0.022		68.2		15	1009
3/17/2008	917	2.7	0.14	0.67	0.022		76.9		8.3	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

			Well or	Injection G	as Sample			Well	Ambient Air
	02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date Time	(%)	(%)	(%)	(C <sub>0</sub> )	(mbar)				

Optimization T	est #5 (20 c	fm to INJ2 f	or 125 minu	tes while ma	aintaing 30 d	of the rest of the	e time; ~	-80% N2, 10%	H2 & LPG)	
3/17/2008	1037	Start Test								
3/17/2008	1247	4.7	0.02	3.5	3.9		74.3		17.6	1014
3/8/2008	936	2.2	0.10	2.5	0.046		80.4		12.4	1016
3/19/2008	952	0.9	0.12	2.5	0.22		88.5		11.7	1013
3/20/2008	936	1.0	0.16	2	0.01		87.1		8.6	1016
3/20/2008	~1100	End Test								

Optimization T	est #6 (50 c	fh to P4-18	& P4-28; ~8	30% N2, 10%	6 H2 & LPG	)				
3/20/2008	1330 Start	Test								
3/28/2008	1034*	0.0	0.0	15.0	12.0	ı	Measured a	at injection poin	t	
3/31/2008	1015	0.4	0	15.5	8.2	ı	Measured v	v/tedlar bag		1013
3/31/2008	1035		0	11	8	ı	Measured v	v/tedlar bag		1013
4/2/2008	1125	0.0	0	14.0	4.2	ı	Measured a	at injection poin	t	1008
4/2/2008	1131	0.0	0	10.0	10.0	I	Measured a	at injection poin	t	1008

Phase II Piezo	ometer Mor	itoring Data	a	Well ID	P4		Depth	18		
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
0 " ' " "		() . D. 10	00 00 (0	20 (1 )	000/ NO 4		20)			
Optimization T	est #7 (20 c	in to P4-18,	28, -38 (6	ou crn total);	~80% N2, 1	0% H2 & LI	(G)			
4/2/2008	1233 Start	Test								
4/4/2008										1013
Optimization T	est #7B (30	cfh to P4-18	3, & P4-28 (	60 cfh total)	; ~80% N2,	10% H2 & L	PG)			
4/7/2008	1458 Start	Test								
Optimization T	est #7C (50	cfh to P4-18	8, & P4-28 (	(100 cfh tota	l); ~79% N2	2, 10% H2 &	LPG, 1% (	CO2)		
4/10/2009	1121 Start	Test								
	1	ļ		1	<u> </u>	1	I .	1	1	
Optimization T	est #8 (100	cfh of 100%	Propane to	P4-18, & P	4-28 (50 cff	to each po	int)			
9/8/2008	0905 Test	Start								
9/8/2008										999

**Phase II Piezometer Monitoring Data** 

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1242	19.4	0.18	0	0.002	50,000	83.0	0.01	12.5	1020
12/12/2007	1532							0.20		
12/12/2007	1551							0.22		
12/12/2007	1622	1.1				1X10^2				
12/12/2007	1630	0.8				1X10^2				
12/12/2007	1639	0.5				3x10^3				
12/13/2007	801	8.4	0.06	0	0.002	2X10^4	89.6		0.3	1016
12/13/2007	833	4.2	0.00	0	1.6	5X10^3	75.3		4.0	1016
12/13/2007	926	10.9	0	0	7.7		67.3		9.6	1016
12/13/2007	1152	11.8	0	0			88.2		13.7	
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1202	0	0	0			85.1		15.0	
12/13/2007	1315							0.20		
12/13/2007	1323	0	0	0	8.3		71.9		17.7	1014
12/13/2007	1428	0.0	0.1	0.24	4.4		78.6		15.7	1013
12/13/2007	1513	0	0.36	0.52	0.54		82.3		14.6	1013
12/13/2007	1547	0	0.46	0.52			78.7		12.8	1013
12/14/2007	809	0	0.1	0	0.5		77.1	0.01	2.8	1016
12/21/2007	1108	14.6	0.46	0.02	0.46		62.5	0.01	11.1	1013
12/21/2007	1342	14.8	0.42	0.02	0.46		69.3		14.9	1012

**Phase II Piezometer Monitoring Data** 

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/26/2007	1220	17.6	0.44	0	0.22		70.6	0.01	14.8	1017
12/26/2007	1412	13.4	0.46	0.02	0.46		76.4		14.2	1015
12/26/2007	1431	9.3	0.42	0.02	0.46		74.7		13.3	1015
12/26/2007	1441	8.1	0.42	0	0.74		77.7		13.3	1015
12/26/2007	1454	6.8	0.42	0	1.9		78.8		12.1	1013
12/26/2007	1540	3.4	0.36	0	5.6		83.9		11.2	1015
12/26/2007	1616	1.9	0.34	0	7		86	0.04	9.7	1015
12/27/2007	934	0.1	0	0	9.1		78.7	0.02	4.8	1017
12/27/2007	1236	0.1	0	0	9		77.8		8.7	1017
12/27/2007	1411	0.1	0	0	9.3		84		9.2	1017
12/27/2007	1532	0.1	0	0	9.6		86.8	0	7.8	1017
1/2/2008	949	0.1	0	0	0.46		62.2	0.03	10.7	1012

Tracer Test #1 (*	10 cfm to IN	J2, ~7% H2	2)						
1/21/2008	1/21/2008 1046 Test start								
1/21/2008	1106	0.9	0	0	0.70	87.6	0.03	7.8	1008
1/21/2008	1124	0.9	0	0	1.7	84.2		9.8	1008
1/21/2008	1155	0.9	0	0	3.6	90.1		9.8	1007
1/21/2008	1243	0.8	0	0	5.0	84.5	0.10	10.1	1006
1/21/2008	1435	0.9	0	0	5.7	81.5	0.10	10.7	1006

**Phase II Piezometer Monitoring Data** 

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/21/2008	1601	0.8	0	0	6.0		86.4		10.0	1006
1/22/2008	915	0.7	0	0	7.0		81.7	0.04	7.4	1011
1/22/2008	1348	0.6	0	0	6.9		91.3		8.4	1009
1/23/2008	952	0.8	0	0	6.7		79.7	0.08	9.4	1008
1/23/2008	1214*	0.8								

Tracer Test #2 (2	20 cfm to IN	J2, ~8% H2	2)						
1/18/2008	1120 Test :	start							
1/18/2008	1128	0.9	0	0	0.10	91.1		12.4	1015
1/18/2008	1145	0.8	0	0	2.4	94.0		12.9	1015
1/18/2008	1156	0.8	0	0	3.7	96.9		13.0	1015
1/18/2008	1210	1.0	0	0	4.9	94.3	0.01	13.2	1015
1/18/2008	1221	0.7	0	0	5.7	92.7		13.4	1015
1/18/2008	1322	0.6	0	0	6.8	86.8		15.8	1014
1/18/2008	1519	0.8	0	0	7.0	78.8	0.01	17.1	1014
1/19/2008	947	0.8	0	0	7.8	65.0	0.03	12.3	1019
1/19/2008	1057*	0.8	0	0	6.4	60.7		15.9	1019

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_28\_\_\_

Phase II Piezo	meter wonit	oring Data		weii iD	P4		Depth	28		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #3	(30 cfm to IN	J2, ~4% H2	2)							
1/30/200	8 1036 Test	start								
1/30/200	8 1052	0.0	0	0	2.2		87.8	0.11	9.8	1020
1/30/200	8 1205	0.0	0	0	4.2		93.3		10.6	1019
1/30/200	8 1611	0.0	0	0	4.7		90.4	0.14	12.5	1018
1/31/200	8 927	0.0	0	0	4.1		93.2	0.15	7.8	1019
1/31/200	8 1123	0	0	0	3.7		87.5		9.6	1018
1/31/200	8 1322	0	0	0	3.5		87.1	0.18	8.9	1017
1/31/200	8 1435									
1/31/200	8 1459	0	0	0	3.7		89.4	0.12	8.2	1014
1/31/200	8 1558	0	0	0	3.8		87.5		8.2	1014
Tracer Test #4	(60 cfm to IN	J2, ~7% H2	2)							
1/28/200	8 1236 Test	start								
1/28/200	8 1246	2.4	0	0	1.2		95.8		10.5	1010
1/28/200	8 1258	1.0	0	0	3.6		94.2		10.5	1010
1/28/200	8 1345	0.0	0	0	5.9		86.9	0.24	11.9	1010
1/28/200	8 1349*	0.0	0	0	5.9					
1/28/200	8 1452	0.0	0	0	6.0		80.9		12.8	1011

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_28\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/28/2008	1539	0.0	0		6.0		86.9	0.26	10.2	1011
1/29/2008	746	0.0	0	0	7.2		82.9	0.22	5.4	1016
1/29/2008	1009*	0.0			6.6					

Tracer Test #5 (9	00 cfm to IN	J2, ~3% H2	2)						
2/5/2008	2/5/2008 1015 Test start								
2/5/2008	1021	0.0	0	0	2.1	79.6	0.27	8.7	1019
2/5/2008	1119	0.0	0	0	3.3	87.3		10.3	1019
2/5/2008	1328	0.0	0	0	4.0	91.6	0.29	12.3	1019
2/5/2008	1457	0.0	0	0	3.7	86.3		14.3	1019
2/5/2008	1543	0.0	0	0	3.5	69.0		17.3	1019

Tracer Test #6 (3	30 cfm total;	; 10 cfm to e	each INJ1, 2	2, and 3; ~8°	% H2)			
2/7/2008	1500 Test	start						
2/7/2008	1520	0.0	0	0	0.046	55.0	21.0	1016
2/7/2008	1611	0.0	0	0	1.9	50.3	22.3	1016
2/8/2008	957	0.0	0	0	8.9	61.0	14.6	1017

**Phase II Piezometer Monitoring Data** 

				Well or	Injection G	as Sample			Well	Ambient Air
O <sub>2</sub> CO <sub>2</sub> Propane H <sub>2</sub> He RH Pressure									Temperature	Barometric pressure
Date	Date Time (%) (%) (%) (ppm) (%) (in wc)									(mbar)

Tracer Test #7 (6	60 cfm total;	20 cfm to e	ach INJ1, 2	2, and 3, ~5°	% H2)				
1/17/2008	900 Test st	art							
1/17/2008	912	16.5	0.30	0	0.22	90.5	0.02	3.1	1015
1/17/2008	927	12.5	0.34	0	0.5	90.8		4.6	1015
1/17/2008	933	8.3	0.34	0	1.2	90.4		5.0	1015
1/17/2008	1000	2.4	0.24	0	3.7	86.8		7.2	1015
1/17/2008	1105	1.3	0.06	0	4.6	93.7	0.04	9.0	1015
1/17/2008	1202	1.2	0	0	4.9	95.0		10.1	1015
1/17/2008	1333	0.8	0.10	0	5.4	98.2		12.1	1013
1/17/2008	1504	0.7	0.06	0	5.8	98.9	0.04	14.0	1012

Tracer Test #8 (9	00 cfm total;	; 30 cfm eac	ch to INJ1, 2	2, and 3; ~4	.5% H2)				
2/6/2008	1000 Test	start							
2/6/2008	1022	0.0	0	0	1.2	80.8	0.24	12.0	1020
2/6/2008	1128	0.0	0	0	4.1	83.7		12.3	1020
2/6/2008	1235	0.0	0	0	4.2	80.6		13.7	1019
2/6/2008	1419	0.0	0	0	4.9	74.9	0.21	16.1	1017
2/6/2008	1527	0.0	0	0	4.7	70.2		16.6	1017

**Phase II Piezometer Monitoring Data** Well ID P4 Depth 28 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1119 72.4 6.6 0.00 0 0.046 15.8 1010 2/20/2008 1206 Test start 2/20/2008 1517 0.0 0.94 1.02 12 37.5 29.6 1008 2/20/2008 1606 Test End 2/20/2008 1611 1008 0.0 0.78 1.06 9.6 48.4 23.3 905 2.0 0.58 7.7 75.9 11 1005 2/21/2008 0.74 2/22/2008 1025 0.48 2.7 84.7 5.8 0.38 10.1 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2.7 2/26/2008 656 0.0 2.24 0.5 7.4 91.6 1017 2/27/2008 1523 4 N 1 34 0.34 26 48 3 31 9 1010

2/21/2000	1323	4.0	1.54	0.54	2.0		40.5	31.9	1010
2/28/2008	1040	6.5	1.1	0.26	1.3		87.9	15.7	1008
Optimization Tes	st #3A (1 cfn	n to INJ2; ~	88% N2, 10	% H2, 1% (	CO2 & LPG	)			
2/29/2008	1319 Test \$	Start							
2/29/2008	1410	6.8	0.80	0.26	0.85		60.2	23.1	1009
2/29/2008	1513	6.2	0.82	0.26	0.85		61.7	23.4	1009

**Phase II Piezometer Monitoring Data** Well ID P4 Depth 28 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** (%) Date Time (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) 3/3/2008 1033 4.3 1019 5.1 0.86 0.36 77.7 14.8 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 920 9.2 0.9 0.28 2.1 85.8 10.1 1013 3/7/2008 1043 8.3 0.48 0.28 2.5 67.4 19 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1330 9.5 0.42 0.2 0.98 55.2 23.5 1016 1401 0.44 9.5 0.2 1.2 3/7/2008 1016 3/10/2008 1032 8.7 0.48 0.3 0.046 84.7 15.7 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 66 3/10/2008 1237 8.9 0.54 0.28 0.022 20.7 1016 9.7 0.046 1256 0.52 0.24 3/10/2008 3/10/2008 1315 6.4 0.64 2.5 3.4 64.6 21.4 1016 2.6 0.84 8.7

3/10/2008

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**Phase II Piezometer Monitoring Data** 

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
3/10/2008	1347	End pulse								
3/10/2008	1403	1.6	0.82	6	9.6		57		22.7	1015
3/11/2008	905	2.2	0.82	4	4.9		64.3		15.3	1018
3/12/2008	953	4.7	0.88	3.5	4.3		88.3		12.2	1014
3/13/2008	909	5.9	0.70	3.5	3.5		87.3		13.6	1011
3/14/2008	1134	6.6	0.64	2	1.7		91.7		13.4	1013
3/14/2008	1208	3.4	0.78	2	7.2					1012
3/14/2008	1229	2.9	0.76	2	8.5					
3/15/2008	1117	10.7	0.68	1.18	0.67		89		11	1009
3/16/2008	1106	11.1	0.46	1.16	0.5		77.2		14.9	1009
3/17/2008	918	9.5	0.60	3	1.7		84		8.5	1014

Optimization Tes	Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG)											
3/17/2008	1037	Start Test										
3/17/2008	1248	0.3	0.20	9.5	9.8	81.8	17.5	1014				
3/8/2008	936	3.6	0.32	10.5	6.7	85.4	12.6	1016				
3/19/2008	954	5.8	0.30	6	3	90.7	11.8	1013				
3/20/2008	938	8.3	0.34	3.5	1.7	90.1	8.8	1016				
3/20/2008	~1100	End Test										

**Phase II Piezometer Monitoring Data** Well ID P4 Depth \_\_\_28\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air**  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/28/2008 1034\* 0.0 12.0 concentrations of injected gasses 0.0 15.0 3/31/2008 1013 4/2/2008 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 1013 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test Optimization Test #8 (100 cfh of 100% Propane to P4-18, & P4-28 (50 cfh to each point) 9/8/2008 0905 Test Start 9/8/2008 999

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1244	19.3	0.36	0	0.002	70,000	85.1	0.02	12.4	1020
12/12/2007	1532							0.44		
12/12/2007	1551							0.42		
12/12/2007	1622	0.5				2x10^4				
12/12/2007	1630	0.4				2x10^4				
12/12/2007	1637	0.3				2x10^4				
12/13/2007	759	8.2	0.16	0	0.002	2x10^4	89.2		0.2	1016
12/13/2007	836	3.8	0.12	0	1.0	2X10^3	75.9		4.0	1016
12/13/2007	927	8.8	0	0	6.7		70.0		9.4	
12/13/2007	1200	Discovered	leak in O2	- all O2 dat	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1203	0	0.14	0						
12/13/2007	1315							0.31		
12/13/2007	1324	0	0.14	0	8.3		75.1		17.3	1014
12/13/2007	1433	0	0.10	0.18	6.2		79.3		16.3	1014
12/13/2007	1514	0	0.18	0.38	2.6		82.6		14.7	1013
12/13/2007	1550	0	0.18	0.38			80.1		12.5	1013
12/14/2007	810	0	0.26	0.12	0.5		73.0	0.02	3.5	1016
12/21/2007	1111	8.9	0.30	0.08	0.51		59.7	0.03	14.2	1013
12/21/2007	1344	9.2	0.24	0.08	0.52		75.4		13.9	1012
12/26/2007	1214	14.2	0.22	0.02	0.22		69.4	0	14.8	1017

Phase II Piezometer Monitoring Data We

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/26/2007	1415	14.1	0.22	0.02	0.22		76.7		14	1015
12/26/2007	1435	13.9	0.22	0.04	0.22		78.9		13.1	1015
12/26/2007	1444	13.4	0.24	0.04	0.22		79.8		13.2	1015
12/26/2007	1542	12	0.26	0.04	0.6		84.9		11	1015
12/26/2007	1620	11.3	0.26	0.04	1.3		88.3	0.04	9.6	1015
12/27/2007	936	1.6	0.24	0.02	8.7		80.3	0.02	4.6	1017
12/27/2007	1238	0.9	0.18	0	8.8		78.1		8.9	1017
12/27/2007	1413	0.8	0.14	0	9.2		85.2		9	1017
12/27/2007	1534	0.7	0.14	0	9.4		88.8	0.03	7.7	1017
1/2/2008	950	0.1	0	0	0.22		67.4	0.04	10.7	1012

Tracer Test #1	I (10 cfm to	INJ2, ~7%	H2)						
1/21/2008	1/21/2008 1046 Test start								
1/21/2008	1108	1.8	0	0	0.55	87.5	0.04	7.9	1008
1/21/2008	1126	1.7	0	0	0.55	82.2		9.9	1008
1/21/2008	1157	1.8	0	0	0.73	89.6		9.8	1007
1/21/2008	1244	1.7	0	0	0.85	82.5	0.07	10.1	1006
1/21/2008	1436	1.8	0	0	2.8	81.2	0.05	10.4	1006
1/21/2008	1602	1.8	0	0	3.7	85.6		10.0	1006
1/22/2008	917	1.1	0	0	6.7	82.5	0.01	7.4	1011

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or	Well	Ambient Air				
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/22/2008	1349	0.7	0	0	6.8		91.2		8.3	1009
1/23/2008	953	0.8	0.02	0	6.8		78.8	0.12	9.3	1007
1/23/2008	1215*	0.7								

Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)						
1/18/2008	3 1120 Test start								
1/18/2008	1129	1.4	0.06	0	0.22	80.4		12.3	1015
1/18/2008	1147	1.4	0.06	0	0.10	84.9		12.8	1015
1/18/2008	1157	1.5	0.08	0	0.62	85.8		12.9	1015
1/18/2008	1322	1.4	0.06	0	2.8	73.2		15.7	1014
1/18/2008	1520	1.5	0.04	0	4.4	69.5	0.04	16.9	1014
1/19/2008	948	0.7	0.12	0	9.8	66.8	0.02	11.8	1019
1/19/2008	1059*	0.7	0.08	0	8.9	59.7		15.7	1019

Tracer Test #3									
1/30/2008	1036 Test s	start							
1/30/2008	1054	0.0	0	0	1.1	87.9	0.14	8.7	1020
1/30/2008	1212	0.0	0	0	2.7	81.9		11.3	1019
1/30/2008	1412	0.0	0	0	3.7	83.1	0.16	12.5	1018
1/31/2008	929	0.0	0	0	4.2	92.6	0.15	7.9	1019

Phase II Piezo	ometer Mor	nitoring Da	ta	Well ID	P4		Depth	38		
				Well or	Injection G	as Sample	<b>;</b>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/31/2008	1124	0	0	0	3.8		86.8		9.6	1018
1/31/2008	1323	0	0	0	3.6		86.4	0.19	8.8	1016
1/31/2008	1435									
1/31/2008	1502	0	0	0	3.7		88.3	0.08	8.2	1014
1/31/2008	1559	0	0	0	3.8		87.0		8.3	1014
Tracer Test #4	(60 cfm to	INJ2, ~7%	H2)							
1/28/2008	1/28/2008 1236 Test start									
1/28/2008	1247	4.7	0.02	0	0.22		96.1		10.4	1010
1/28/2008	1300	4.7	0.02	0	0.22		95.7		10.5	1010
1/28/2008	1346	3.7	0	0	2.7		85.3	0.30	12.0	1010
1/28/2008	1453	2.8	0	0	3.8		81.3		12.8	1011
1/28/2008	1540	2.4	0	0	4.3		86.7	0.31	10.1	1011
1/29/2008	747	0.0	0	0	7.3		84.6	0.30	5.3	1016
1/29/2008	Final O2*	0.0								
Tracer Test #5	(90 cfm to	INJ2, ~3%	H2)							
2/5/2008	1015 Test s	start								
2/5/2008	1022	3.3	0	0	0.10		83.1	0.34	8.9	1019
2/5/2008	1120	2.2	0	0	1.5		90.0		10.7	1019

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/5/2008	1328	0.9	0	0	3.2		92.6	0.30	12.3	1019
2/5/2008	1458	0.4	0	0	3.3		77.3		14.9	1019
2/5/2008	1544	0.3	0	0	3.2		60.6		17.5	1018

Tracer Test #6	(30 cfm tot	al; 10 cfm to	o each INJ1	, 2, and 3;	~8% H2)			
2/7/2008	1500 Test s	start						
2/7/2008	1521	0.0	0	0	0.64	55.7	20.9	1016
2/7/2008	1613	0.0	0	0	0.68	50.5	21.9	1016
2/8/2008	959	0.0	0	0	5.9	59.3	13.8	1017
2/8/2008	1053	0.0	0	0	5.7	84.9	10.9	1017

Tracer Test #7	7 (60 cfm tot	al; 20 cfm to	o each INJ1	, 2, and 3, <i>-</i>	~5% H2)				
1/17/2008	900 Test st	art							
1/17/2008	930	13.0	0.08	0	0.22	90.5	0.03	4.9	1015
1/17/2008	1001	13.1	0.04	0	0.22	86.8		7.2	1015
1/17/2008	1108	12.0	0.04	0	0.46	93.3	0.03	9.1	1015
1/17/2008	1204	10.2	0.04	0	1.1	97.2		10.2	1015
1/17/2008	1334	7.5	0.22	0	2.3	98.8		12.3	1013
1/17/2008	1505	5.1	0.22	0	3.4	97.7	0.04	13.8	1012

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_

Depth \_\_\_38\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date Time (%) (%) (%) (ppm) (%) (in wc)									(C <sub>0</sub> )	(mbar)

Tracer Test #8	3 (90 cfm tot	al; 30 cfm e	each to INJ1	, 2, and 3;	~4.5% H2)				
2/6/2008	1000 Test s	start							
2/6/2008	1023	0.0	0	0	0.71	82.6	0.23	11.9	1020
2/6/2008	1129	0.0	0	0	1.1	82.5		12.3	1020
2/6/2008	1235	0.0	0	0	1.7	80.2		13.7	1019
2/6/2008	1423	0.0	0	0	2.9	69.6	0.20	16.0	1017
2/6/2008	1527	0.0	0	0	3.1	69.3		16.1	1017
2/6/2008	1622	0.0	0	0	3.3	69.4		16.4	1017

Optimization T	est #1 (90 c	ofm to INJ2	for 4 hours	then shut d	own; ~88%	N2, 10% H2, 1% CO2	& LPG)	
2/20/2008	1120	7.8	0.00	0	0.046	72.6	15.4	1010
2/20/2008	1206 Test s	start						
2/20/2008	1518	2.3	0.14	0.68	9.9	33.8	29.8	1008
2/20/2008	1606 Test I	End						
2/20/2008	1612	1.6	0.16	0.78	9.6	48.6	23.2	1008
2/21/2008	907	3.1	0.04	0.72	8.5	76.7	10.8	1005
2/22/2008	1025	6.7	0.06	0.48	4.1	83.8	10	1003

**Phase II Piezometer Monitoring Data** Well ID P4 Depth 38 **Well or Injection Gas Sample Ambient Air** Well CO2  $O_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 658 1.0 1.36 0.62 7 91.6 2.8 1017 3.7 2/27/2008 1525 0.54 0.34 3.7 43.5 31.9 1009 2/28/2008 2 1008 1041 5.0 0.56 0.32 86.6 15.7 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1414 7.3 0.50 0.3 0.98 63.6 23 1009 2/29/2008 1514 7.3 0.5 0.3 0.78 60.8 23.2 1009 3/3/2008 1035 7.6 0.6 0.2 0.046 80.6 1019 14.8 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 921 8.4 0.72 0.22 0.022 84.2 11.2 1013 1045 0.48 0.18 0.046 71 18.7 1018 3/7/2008 3/7/2008 1306 Test End

Phase II Piezo	ometer Mor	nitoring Da	ta	Well ID	P4		Depth	38		
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #3C (90	cfm to INJ	1, INJ2 & IN	IJ3 for 15 m	inutes then	shut down;	~79% N2,	10% H2 & LPG	6, 1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1331	8.9	0.44	0.18	0.022		56.2		23.3	1016
3/10/2008	1041	8.8	0.56	0.42	0.046		82		16.1	1016
Optimization T	est #4 ( 2, 4	45-minutes	pulses; dail	y 15-minute	s pulses w/:	30cfh const	ant flow)			
3/10/2008	1238	8.9	0.64	0.4	0.022		69.7		20.9	1016
3/10/2008	1342	8.0	0.64	0.96	1.4					
3/10/2008	1347	End pulse								
3/10/2008	1404	7.3	0.62	1.32	2.7		58.2		22.7	1015
3/11/2008	906	6.1	0.64	2	1.9		64.8		15.1	1018
3/12/2008	955	6.8	0.58	1.42	0.88		89.2		12.4	1014
3/13/2008	910	7.0	0.50	1.3	0.5		89.7		13.7	1011
3/14/2008	1135	7.2	0.52	1.4	0.5		92.1		13.6	1013
3/14/2008	1210	7.0	0.46	1.4	0.67		81.1		15	1012
3/15/2008	1120	7.9	0.52	1.3	0.5		90.8		111	1009
3/16/2008	1107	7.0	0.38	3	1.5		81		14.7	1009
3/17/2008	919	8.2	0.50	3	0.65		85.8		8.7	1014

**Phase II Piezometer Monitoring Data** Well ID P4 Depth 38 **Well or Injection Gas Sample Ambient Air** Well  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Temperature Barometric pressure Time Date (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 3/17/2008 1037 Start Test 1250 5.7 0.38 3/17/2008 4.2 4.5 84 17.6 1014 3/8/2008 938 4.2 2.7 86.6 12.7 0.46 6 1016 955 3/19/2008 5.1 0.42 1.2 90.6 1013 11.9 3/20/2008 939 5.3 0.44 4.5 0.5 87.5 8.9 1016 3/20/2008 ~1100 **End Test** Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 4/2/2008 1121 0.2 0.3 93.0 11.5 1.8 16.9 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 1013 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 1.3 4/9/2008 1142 0.00 8.5 0.1 93.0 16.2 1009

Phase II Piezometer Monitoring Data Well I

Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_38\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization 7	est #7C (50	ofh to P4-1	8, & P4-28	(100 cfh tot	al); ~79% N	l2, 10% H2	& LPG, 1%	CO2)		
4/10/2009	1121 Start	Test								
4/11/2008	1304	1.2	0.00	9.0	0.1		97.0		23.1	1012
4/16/2008	1201	0.3	2.06	15.0	2.6		55.3		20.2	1011
4/22/2008	1026	0.8	1.14	6.5	0.50		50.3		17.9	1009
4/25/2008	1023	0.3	1.44	8.5	0.10		45.8		23.9	1015
4/29/2008	1129	0.1	1.12	9.0	0.70		43.7		26.6	1007
5/5/2008	1334	0.0	0.8	8.0	0.55		30.7		37.6	1001
5/13/2008	1005	0.0	0.76	9.0	0.10		22.5		35.5	1007
5/20/2008	957	0.0	0.84	9.0	0.10		44.9		23.7	1004
5/23/2008	1545	1.6	0.78	8.5	0.10		33.3		28.6	990
5/27/2008	929	0.6	0.86	8.5	0.046		54.0		18.7	1007
6/4/2008	929	0.0	0.70	8.0	0.70		42.5		24.9	1002
6/12/2008	1227	0.2	0.66	8.4	0.046		18.1		43.2	1003
6/20/2008	1057	0.0	0.58	8.5	0.70		19.7		42.0	1005
6/25/2008	1108	0.0	0.52	8.5	0.10		36.7		30.7	1005
7/2/2008	1213	0.0	0.50	8.0	0.50		25.6		37.9	1004
7/7/2008	1200	0	0.42	8	0.46		21.4		36.8	998
7/18/2008	1126	0	0.48	8	0.1		48.4		27.6	
7/24/2008	1042	0.0	0.50	8.0	0.460		46.3		27.6	1005

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P4\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

	ĺ			Well	Ambient Air					
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/31/2008	1036	0.0	0.52	8.0	0.640		51.0		26.3	1003
8/7/2008	914	0.0	0.88	8.0	0.50		82.9		20.8	1004
8/12/2008	1018	0.0	0.50	8.5	0.69		49.0		28.4	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane t	o P4-18, &	P4-28 (50 c	fh to each p	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1115	1.7	1.86	16.5	0.005					999
9/15/2008	Forgot to m	neasure								1007
9/29/2008	1007	0.5	0.12	30	0.005		68.1		22.1	1006
10/13/2008	1144	0.5	0.08	30	0.005		37.4		31.1	1017
10/20/2008	1148	0.1	0.10	30	0.005		54.8		27.1	1013
11/5/2008	1338	0.0	0.10	30	0.005		74.4		19.9	1016
11/17/2008	1133	0.0	0.06	30	0.005		61.0		26.0	1014
12/1/2008	1105	0.0	0.04	30	0.005		60.8		20.8	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G		Well	Ambient Air		
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1245	18.9	0.44	0	0.002	80,000	87.8	0.02	12.4	1020
12/12/2007	1531							0.58		
12/12/2007	1550							0.54		
12/12/2007	1623	0.3				2X10^4				
12/12/2007	1631	0.2				2X10^4				
12/12/2007	1638	0.1				2X10^4				
12/13/2007	758	8.2	0.00	0	0.002	4X10^4	90.5		0	1016
12/13/2007	838	4.2	0.00	0	0.5	3x10^3	76.0		3.9	1016
12/13/2007	928	9.1	0	0	7.9		69.1		9.5	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 dat	a for 12/13/	'07 before 1	200 invalid			
12/13/2007	1204	0	0	0			83.4		15.4	
12/13/2007	1316							0.32		
12/13/2007	1324	0	0	0	8.3		75.8		17.1	1014
12/13/2007	1435	0	0	0.34	3.7		77.0		16.3	1013
12/13/2007	1516	0	0.02	0.52	0.22		80.3		14.8	1013
12/13/2007	1551	0	0.04	0.50			79.4		12.5	1013
12/14/2007	817	0	0.06	0.02	0.5		69.5	0.03	4.2	1013
12/21/2007	1113	10.2	1.12	0.04	0.46		58.8	0.10	14.3	1013
12/21/2007	1346	10.4	1.02	0.02	0.52		75.6		13.6	1012
12/26/2007	1212	14.1	1.06	0	0.22		70.5	0	14.5	1017
12/26/2007	1418	13.8	0.9	0.02	0.22		78.5		13.7	1015

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or		Well	Ambient Air			
		<b>O</b> <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/26/2007	1435	13.4	0.82	0.02	0.22		79.5		13.1	1015
12/26/2007	1446	12.9	0.76	0.02	0.22		80.7		13.1	1015
12/26/2007	1545	12.3	0.76	0.04	0.22		85.1		10.8	1015
12/26/2007	1622	11.3	0.68	0.06	0.46		87.1	0.04	9.5	1015
12/27/2007	939	11.5	0.88	0.04	0.98		82.1	0.01	4.5	1017
12/27/2007	1240	11	0.8	0.02	1.4		79.6		9.1	1017
12/27/2007	1415	10.8	0.76	0.02	1.8		85.9		9	1017
12/27/2007	1535	10.8	0.76	0.02	2		89.4	0.01	7.7	1016
1/2/2008	953	5.3	0.44	0	0.22		66.8	0.03	11.1	1012

Tracer Test #1	(10 cfm to IN	NJ2, ~7% H	2)						
1/21/2008	1046 Test s	start							
1/21/2008	1109	3.2	0.54	0	0.98	87.0	0.06	8.7	1008
1/21/2008	1127	2.8	0.52	0	0.97	82.3		7.9	1008
1/21/2008	1159	2.8	0.56	0	0.92	84.3		9.9	1007
1/21/2008	1246	2.7	0.54	0	0.89	82.1	0.08	10.3	1006
1/21/2008	1437	3.0	0.52	0	1.0	82.4	0.05	10.6	1006
1/21/2008	1603	2.8	0.50	0	1.3	86.9		10.0	1006
1/22/2008	918	2.8	0.52	0	2.1	82.5	0.02	7.3	1011
1/22/2008	1350	2.5	0.50	0	1.9	91.1		8.4	1009
1/23/2008	954	2.6	0.54	0	2.0	79.8	0.04	9.2	1007
1/23/2008	1216*	3.3							

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Tracer Test #2	(20 cfm to II	NJ2, ~8% H	12)						
1/18/2008	1120 Test s	start							
1/18/2008	1130	4.5	0.50	0	0.22	91.6		12.4	1015
1/18/2008	1158	2.3	0.36	0	0.10	93.6		13.1	1015
1/18/2008	1324	2.1	0.34	0	0.10	88.7	0.02	15.8	1014
1/18/2008	1521	1.7	0.28	0	3.5	63.8	0.04	16.9	1014
1/19/2008	952	1.0	0.36	0	8.6	73.3	0.02	10.8	1019
1/19/2008	1100*	1.1	0.30	0	8.0	68.5		15.6	1019

Tracer Test #3	(30 cfm to II	NJ2, ~4% H	2)						
1/30/2008	1036 Test	start							
1/30/2008	1054	0.1	0.10	0	2.1	88.5	0.19	9.7	1020
1/30/2008	1213	0.0	0.08	0	2.0	89.4		11.3	1019
1/30/2008	1413	0.0	0.06	0	3.5	89.6	0.19	12.5	1018
1/31/2008	931	0.0	0.02	0	4.2	94.3	0.09	8.0	1019
1/31/2008	1125	0	0.02	0	3.8	88.6		9.6	1018

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_48\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2  $H_2$ RH Propane He Pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) 1/31/2008 1325 0 3.6 85.4 0.25 8.8 1016 1435 1/31/2008 1/31/2008 1503 0.02 0 3.6 88.1 0.14 8.2 1014 1/31/2008 1559 0.08 0 3.7 87.4 8.3 1013 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 6.6 1/28/2008 1248 0.48 0 0.046 95.9 10.1 1010 4.2 1347 1.5 0.38 0 94.6 0.26 12.2 1/28/2008 1010 1/28/2008 1454 0.2 0.18 0 5.5 80.3 12.8 1011 0 5.6 88.0 1/28/2008 1541 0.1 0.14 0.14 10.1 1011 1/29/2008 747 0.0 0.04 7.3 87.0 0.25 5.2 1016 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1024 3.6 83.9 0.27 2/5/2008 0.04 0 0.10 8.9 1019 2/5/2008 1122 0.2 0 2.9 89.0 10.7 0 1019 2/5/2008 1330 0 0 3.9 83.4 0.25 12.2 1019 2/5/2008 1459 0 0 0 3.6 69.6 14.3 1019

0

2/5/2008

1545

0

3.5

57.7

17.7

1019

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_\_48\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2  $H_2$ Propane He RH Pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 1523 0.4 0.18 0 0.92 51.2 2/7/2008 21.8 1016 2/7/2008 1613 0.4 0.16 0 0.80 48.7 21.8 1016 2/8/2008 959 0.0 0.34 0 1.5 60.9 13.5 1017 0.32 1.5 82.7 10.8 2/8/2008 1052 0.0 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 931 0.92 0.022 89.7 1/17/2008 13.5 0.02 4.9 1015 1/17/2008 1004 12.8 0.68 0.022 87.7 7.7 1015 0.56 0.22 93.5 1/17/2008 1109 12.0 0 0.03 9.2 1015 0.50 0 96.9 1/17/2008 1210 10.6 0.51 10.1 1015 1335 0.82 0 0.94 98.8 12.5 1013 1/17/2008 9.8 1/17/2008 1507 9.0 0.78 0 1.5 93.9 0.02 14.1 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1025 0.1 0.04 0 1.1 79.6 0.30 11.8 1020 2/6/2008 1131 0.1 0.04 0 0.87 80.1 12.2 1020 2/6/2008 1237 0.1 0.02 0 0.76 76.1 13.7 1019

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1423	0.1	0.04	0	1.1		68.2	0.06	16.0	1017
2/6/2008	1529	0.1	0.02	0	1.3		64.1		17.0	1017
2/6/2008	1623	0.1	0.12	0	1.6		67.4		16.4	1017

Optimization Te	est #1 (90 cf	m to INJ2 fo	or 4 hours th	nen shut dov	wn; ~88% <b>N</b>	N2, 10% H2, 1% CO2 8	& LPG)	
2/20/2008	1121	7.6	0.46	0	0.022	77	15.3	1010
2/20/2008	1206 Test	start						
2/20/2008	1520	0.2	0.14	1	11	32.7	29.5	1008
2/20/2008	1606 Test	End						
2/20/2008	1613	0.1	0.14	1	9.9	47.7	23.1	1008
2/21/2008	907	4.8	0.48	0.1	1.1	81.1	10.7	1005
2/22/2008	1027	5	0.56	0.04	0.62	84.8	9.9	1003

Optimization Te	est #2 (30 cf	m to INJ2 fo	or 12 hours	then shut d	own; ~88%	N2, 10% H	2, 1% CO2	& LPG)		
2/25/2008	1845 Test	Start								
2/26/2008	653 Test E	nd								
2/26/2008	700	1.0	0.5	0.58	5.8		91.4		2.8	1017
2/27/2008	1526	19.0	0.1	0	0.046		43.5		31.8	1009
2/28/2008	1042	20.1	0.08	0	0.022		82.9		15.7	1008

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_\_48\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ Propane  $H_2$ CO2 He RH Pressure Date Time (%) (%) (%) (%) (%) (Co) (mbar) (ppm) (in wc) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 0.022 2/29/2008 1415 18.8 0.00 0.02 59.2 23.1 1009 1515 0.022 60.8 2/29/2008 18.8 0.02 23.1 1009 1036 20.1 0.02 0.01 83.8 3/3/2008 14.9 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 923 85.2 3/4/2008 19.9 0.1 0 0.01 11.7 1013 0.022 3/7/2008 1046 19.3 0 0 66.6 1018 18.5 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 0 0.005 53.2 3/7/2008 1332 16.5 23.2 1016 81.2 1042 0.022 16.2 0.04

3/10/2008

19.3

1016

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Optimization Te	st #4 ( 2, 45	5-minutes p	ulses; daily	15-minutes	pulses w/3	Ocfh constant flow)		
3/10/2008	1347	End pulse						
3/10/2008	1405	12.7	0.10	0.16	0.01	58.4	22.6	1015
3/11/2008	908	20.6	0.06	0	0.01	66.2	14.9	1017
3/12/2008	956	18.7	0.08	0	0.01	88.4	12.5	1014
3/13/2008	911	18.7	0.06	0	0.01	91.2	13.7	1011
3/14/2008	1137	18.6	0.08	0	0.022	91.4	13.7	1013
3/14/2008	1211	16.7	0.06	0.02	0.01	81.4	14.9	1012
3/15/2008	1121	18.6	0.10	0	0.022	89	11.2	1009
3/16/2008	1108	16.1	0.04	0.04	0.022	83.1	14.6	1009
3/17/2008	920	16.4	0.16	0.06	0.01	86.7	8.8	1014

Optimization Te	st #5 (20 cf	m to INJ2 fo	or 125 minu	tes while ma	aintaing 30	cfh the rest of the time	e; ~80% N2, 10% H2 & LPG)	
3/17/2008	1037	Start Test						
3/17/2008	1251	8.5	0.06	3.5	0.5	84.4	17.7	1014
3/8/2008	939	16.7	0.14	0.14	0.022	86.4	12.8	1016
3/19/2008	956	15.2	0.14	0.16	0.022	90.8	11.9	1013
3/20/2008	940	14.6	0.18	0.46	0.01	87.3	9	1016
3/20/2008	~1100	End Test						

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_\_48\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air**  $O_2$  $H_2$ CO2 Propane He RH Pressure Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (Co) (mbar) (ppm) (in wc) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 4/2/2008 1122 1.8 0.24 9.5 0.046 81.3 16.7 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 1002 0.26 0.046 80.5 1.6 10.0 14.1 1013 4/7/2008 1433 5.1 0.52 7.0 0.046 55.5 19.5 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 8.0 4/9/2008 1139 1.8 0.38 0.046 89.8 16.0 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 1303 8.5 0.022 96.9 4/11/2008 1.6 0.48 23.1 1012 4/16/2008 1202 0.2 0.46 14.5 0.220 57.1 20.2 1011 1028 8.2 0.54 5.5 0.010 56.1 17.9 1009 4/22/2008 4/25/2008 1021 0.64 0.010 43.4 23.5 0.8 11.5 1015 1130 0.5 0.66 11.0 0.10 44.3 26.8 1007 4/29/2008 5/5/2008 1332 0.3 8.0 10.0 0.046 34.3 38.4 1001 1007 0.86 9.5 25.4 35.5 5/13/2008 0.1 0.10 1007

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G	as Sample	•		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
5/20/2008	958	0.0	0.86	9.5	0.10		50.7		24.4	1004
5/23/2008	1547	0.0	0.78	9.5	0.10		38.9		28.4	990
5/27/2008	930	0.0	1.00	9.5	0.046		68.3		18.6	1007
6/4/2008	931	0.0	1.08	9.0	0.046		47.7		24.8	1002
6/12/2008	1229	0.0	0.96	8.5	0.10		18.2		43.3	1003
6/20/2008	1058	0.0	0.96	8.5	0.046		19.2		42.6	1005
6/25/2008	1109	0.0	0.72	8.5	0.10		37.9		31.3	1005
7/2/2008	1215	0.0	1.04	8.0	0.10		24.7		38.4	1004
7/7/2008	1159	0.0	1	8.0	0.1		28.4		36.7	998
7/18/2008	1127	0.0	1.12	7.5	0.1		56.4		29	
7/24/2008	1043	0.0	1.12	8.0	0.100		45.5		27.5	1005
7/31/2008	1037	0.0	1.18	7.5	0.100		50.4		26.4	1003
8/7/2008	915	0.0	0.52	8.5	0.78		81.5		20.9	1004
8/12/2008	1019	0.0	1.10	7.5	0.100		57.3		28.4	1002
Optimization Te	est #8 (100 c	ofh of 100%	Propane to	P4-18, & P	4-28 (50 cfl	h to each p	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1117	0.0	0.88	21.0	0.010					999
9/15/2008	Forgot to m	neasure								1007
9/29/2008	1008	0.0	1.46	30	0.005		32.4		22.0	1006
10/13/2008	1146	0.1	1.20	30	0.005		39.1		30.9	1017
10/20/2008	1150	0.1	1.10	30	0.005		56.7		26.9	1013
11/5/2008	1339	0.0	0.96	30	0.005		72.9		19.9	1016

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P4\_\_\_\_ Depth \_\_\_48\_\_\_\_

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
11/17/2008	1134	0.0	0.76	30	0.010		63.7		26.1	1014
12/1/2008	1105	0.0	0.72	30	0.005		61.7		20.7	1014

Phase II Piezometer Monitoring Data Well II

Well ID \_\_\_P5\_\_\_\_ Depth \_\_\_18\_\_\_\_

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1205	19.7	0.20	0	0.002	70,000	78.2	0.02	12.2	1020
12/12/2007	1534							0.20		
12/12/2007	1626	19.3				3x10^4				
12/12/2007	1633	19.1				3x10^4				
12/12/2007	1642	18.6				3x10^4				
12/13/2007	801	15.5	0.12	0	0.002	2X10^4	86.3		0.6	1016
12/13/2007	838	11.6	0.18	0	0.22	2X10^4	72.0		3.9	1016
12/13/2007	934	14.4	0	0	0.22		56.9		10.9	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1205	0.6	0.28	0						
12/13/2007	1315							0.15		
12/13/2007	1325	0.3	0.24	0	7.4		69.5		17.2	1013
12/13/2007	1448	0	0.20	0	8.6		80.6		13.8	1013
12/13/2007	1519	0	0.18	0	8.5		75.1		14.7	1013
12/13/2007	1553	0	0.16	0.16			81.0		12.6	1013
12/14/2007	828	0.5	0.24	0.30	1.3		68.2	0.05	4.6	1016
12/21/2007	1159	8.1	0.30	0.08	0.46		88.6	0.03	10.1	1013
12/26/2007	1223	13.1	0.26	0.06	0.22		79.8	0.03	12.7	1017
12/26/2007	1515	13.2	0.28	0.06	0.22		79.2		12.1	1015
12/26/2007	1609	13.4	0.3	0.06	0.22		81.6	0.04	10.3	1015

Phase II Piezo	ometer Mor	nitoring Da	ta	Well ID	_P5		Depth	18		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/27/2007	1011	3.4	0.32	0	7.4		74.8	0.03	6	1018
12/27/2007	1316	1.6	0.24	0	8.6		82.5		8.6	1016
12/27/2007	1437	1.4	0.24	0	8.7		87.0		8.3	1017
12/27/2007	1554	1.3	0.24	0	9.1		87.4	0.05	7.5	1016
1/2/2008	1031	0.5	0.22	0	0.22		62.0	0.04	17	1012
Tracer Test #1	(10 cfm to	INJ2, ~7%	H2)							
1/21/2008	1046 Test :	start								
1/21/2008	1131	1.9	0.08	0	0.86		80.1	0.11	10.0	1008
1/21/2008	1251	1.3	0.06	0	0.72		80.3	0.01	10.6	1006
1/21/2008	1443	1.2	0.04	0	0.81		77.0	0.08	10.7	1006
1/21/2008	1608	1.1	0.06	0	1.1		96.0	0.04	10.0	1006
1/22/2008	950	0.8	0.06	0	5.3		85.3	0.06	6.8	1011
1/22/2008	1352	0.7	0.04	0	5.9		90.8		8.4	1009
1/23/2008	1012	0.7	0.08	0	6.4		81.7	0.07	9.0	1007
1/23/2008	1110*	0.6			6.5					
Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)							
1/18/2008	1120 Test	start								
1/18/2008	1132	1.7	0.10	0	0.61		83.1		12.4	1015

**Phase II Piezometer Monitoring Data** 

Well ID \_\_\_P5\_\_\_\_ Depth \_\_\_18\_\_\_\_

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/18/2008	1214	1.6	0.10	0	0.57		77.1	0.03	13.4	1015
1/18/2008	1316	1.3	0.10	0	0.53		64.8		15.4	1014
1/18/2008	1348	1.5	0.08	0	0.69		65.3		15.4	1014
1/18/2008	1524	1.5	0.08	0	1.4		57.9	0.04	18.1	1014
1/19/2008	954	0.9	0.16	0	9.9		64.3	0.02	10.4	1019
1/19/2008	1136*	0.6	0.10	0	10.0		61.5		12.8	1018

Tracer Test #3	3 (30 cfm to	INJ2, ~4%	H2)						
1/30/2008	1036 Test s	start							
1/30/2008	1102	0.0	0	0	1.0	84.5	0.09	9.4	1020
1/30/2008	1216	0.0	0	0	0.95	78.3		11.3	1019
1/30/2008	1416	0.0	0	0	2.0	74.7	0.11	12.5	1018
1/31/2008	932	0.0	0	0	4.2	92.2	0.20	8.0	1019
1/31/2008	1126	0	0	0	3.8	85.5		9.6	1018
1/31/2008	1335	0	0	0	3.7	85.9	0.12	8.7	1016
1/31/2008	1435								
1/31/2008	1505	0	0	0	3.7	87.9	0.03	8.2	1014
1/31/2008	1601	0	0	0	3.7	87.3		8.3	1013

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 18 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Time (%) Date (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1251 0.6 0.08 0 0.046 90.1 10.4 1010 1/28/2008 1407 1.0 0.08 0.10 73.0 13.2 1010 0.16 1/28/2008 3.4 1544 0.5 0.02 83.9 0.16 10.1 1011 0.0 7.3 83.5 0.09 5.0 1016 1/29/2008 0 750 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1025 0.10 2/5/2008 0.2 0 77.3 0.20 9.0 1019 0 0.2 0 2/5/2008 1123 0.10 74.9 10.7 1019 2/5/2008 1332 0 0 3.3 77.1 0.20 12.1 1019 2/5/2008 1502 66.3 14.3 0 0 3.5 1019 0 2/5/2008 0 0 3.3 1546 55.4 17.8 1019 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 47.8 2/7/2008 1526 0.0 0.02 0.58 21.3 1016

Phase II Piezometer Monitoring Data Well ID \_\_\_P5\_\_\_\_ Depth \_\_\_18\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/7/2008	1615	0.0	0	0	0.46		45.4		21.5	1016
2/8/2008	1003	0.0	0	0	8.6		60.2		12.5	1017

Tracer Test #7	7 (60 cfm tot	al; 20 cfm t	o each INJ1	l, 2, and 3,	~5% H2)				
1/17/2008	1/17/2008 900 Test start								
1/17/2008	951	12.7	0.06	0	0.022	89.2	0.03	7.1	1015
1/17/2008	1021	12.9	0.04	0	0.22	94.7	0.02	8.3	1015
1/17/2008	1152	11.3	0.02	0	1.4	86.9	0.02	10.0	1015
1/17/2008	1345	6.5	0.20	0	3.6	88.6		12.4	1013
1/17/2008	1509	4.7	0.20	0	4.3	86.3	0.02	14.3	1012

Tracer Test #8	3 (90 cfm tot	tal; 30 cfm e	each to INJ1	I, 2, and 3;	~4.5% H2)				
2/6/2008	1000 Test s	start							
2/6/2008	1027	0.0	0	0	0.92	72.9	0.21	11.6	1020
2/6/2008	1138	0.0	0	0	1.0	69.9		12.4	1020
2/6/2008	1239	0.0	0	0	1.9	67.6		13.8	1019
2/6/2008	1428	0.0	0	0	3.7	61.6	0.23	16.2	1017
2/6/2008	1531	0.0	0	0	3.8	59.4		17.0	1017
2/6/2008	1625	0.0	0	0	4.0	61.9		16.5	1017

**Phase II Piezometer Monitoring Data** Well ID P5 Depth \_\_\_\_18\_\_\_\_\_ Well or Injection Gas Sample **Ambient Air** Well  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1130 4.5 0.00 0.046 70.8 15.1 1010 2/20/2008 1206 Test start 2/20/2008 1537 0.5 0.00 0.94 10 52.1 21.9 1007 2/20/2008 1606 Test End 2/20/2008 1622 0.00 0.4 0.96 9.8 46.7 22.3 1008 909 0.2 0.92 78.6 1005 2/21/2008 0.00 9.4 10.6 2/22/2008 1035 0.06 0.9 6 84.4 9.7 1003 0.88 2/25/2008 48.8 1642 4.8 0.10 0.54 0.5 22.9 1017 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 0/00/0000

2/26/2008	702	0.5	0.48	0.74	6.3		93.4	3.5	1017
2/27/2008	1530	0.2	0.4	0.5	4.8		39.7	32.3	1009
2/28/2008	1050	0.7	0.38	0.46	3		70.6	15.8	1007
Optimization T	est #3A (1	cfm to INJ2;	; ~88% N2,	10% H2, 19	% CO2 & LF	PG)			
2/29/2008	1319 Test	Start							
2/29/2008	1427	2.3	0.40	0.44	1.3		41.9	23.2	1009

Phase II Piez	ometer Moi	nitoring Da	ta	Well ID	_P5		Depth	18		
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/29/2008	1516	2.2	0.42	0.44	0.92		58.3		22.9	1009
3/3/2008	1044	0	0.56	0.78	6.6		65.7		15.1	1019
3/3/2008	1130 Test	End								
Optimization 1	Test #3B (1	cfm to INJ1	, INJ2 & INJ	J3; ~88% N2	2, 10% H2,	1% CO2 &	LPG)			
3/3/2008	1130 Test	Start								
3/4/2008	925	0.5	0.72	0.76	5.6		77.2		12	1013
3/7/2008	1054	0.6	0.5	0.8	5.7		58.4		18.2	1018
3/7/2008	1306 Test	End								
Optimization 1	Test #3C (90	cfm to INJ	1, INJ2 & IN	NJ3 for 15 m	inutes then	shut down	; ~79% N2,	10% H2 & LP0	G, 1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1333	0.6	0.48	0.78	4.9		48.3		22.9	1016
3/10/2008	1049	4.3	0.52	0.94	0.5		66.8		16.4	1016
Optimization 1	Test #4 ( 2, 4	45-minutes	pulses; dail	y 15-minute	s pulses w/	30cfh const	ant flow)			
3/10/2008	1233	4.5	0.64	0.92	0.5		54.8		20.5	1016
3/10/2008	1254	4.6	0.64	0.9	0.22					
3/10/2008	1317	4.9	0.68	0.88	0.22		53.6		21.3	1016
3/10/2008	1347	End nulse								

Phase II Piezometer Monitoring Data	Well IDP5	Depth18	

			Well	Ambient Air						
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Injection G H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
3/10/2008	1407	5.0	0.64	0.68	0.1		49.6		22.6	1015
3/11/2008	911	3.4	0.64	1.7	3.9		68		14.7	1017
3/12/2008	958	0.5	0.64	4.5	7.7		82.5		12.7	1014
3/13/2008	913	0.1	0.60	5.5	8.2		85.8		13.8	1011
3/14/2008	1138	0.1	0.58	6	4.9		83.8		13.7	1013
3/14/2008	1213	0.0	0.56	6	4.9		78.3		14.8	1012
3/15/2008	1122	0.4	0.58	4.5	4.3		82.8		11.2	1009
3/16/2008	1110	1.4	0.40	3.5	3.4		75.9		14.4	1009
3/17/2008	922	2.3	0.52	3	5		81.4		9	1014
Optimization 7	Test #5 (20	cfm to INJ2	for 125 min	utes while n	naintaing 30	ofh the res	st of the time	e; ~80% N2, 10	0% H2 & LPG)	
3/17/2008	1037	Start Test								
3/17/2008	1254	2.5	0.42	4	7.7		67.5		17.8	1014
3/8/2008	940	1.2	0.52	8	7.9		80.1		12.8	1016
3/19/2008	957	0.6	0.48	9	6.4		83.7		11.9	1013
3/20/2008	942	0.4	0.48	9	8		82.6		9.3	1016
3/20/2008	~1100	End Test								
Optimization 7	Test #6 (50	cfh to P4-18	& P4-28; ~	80% N2, 10	% H2 & LP	G)				
3/20/2008	1330 Start	Test								
3/21/2008	1002	0.0	0.36	4.0	5.8		81.8		11.8	1020

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 18 **Well or Injection Gas Sample** Well **Ambient Air**  $O_2$ CO2 **Propane** He RH **Pressure** Temperature **Barometric pressure**  $H_2$ Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) 3/24/2008 0.0 4.2 59.6 1002 0.24 2.0 16.4 1012 3/26/2008 943 0.0 0.18 2.0 4.9 85.0 10.7 1017 3/28/2008 941 0.0 0.14 2.0 2.6 79.7 10.4 1009 3/31/2008 942 0.0 0.10 14.5 11.0 81.3 9.2 1013 4/2/2008 1040 0.0 0.10 13.5 11.0 84.8 13.5 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 924 0.0 0.08 83.5 11.5 16.0 12.0 1013 0.1 4/7/2008 1350 0.02 4.5 26.0 62.4 19.2 1012 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 0.2 1034 0.00 0.8 36.0 80.3 14.2 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 4/11/2008 1219 0.0 0.00 0.2 18.0 60.9 21.2 1013 1.52 7.3 81.5 1007 4/14/2008 1001 0.6 25.5 15.6 4/16/2008 1014 0.0 2.08 9.5 9.6 80.9 14.4 1011 4/22/2008 1031 0.0 0.32 10.0 14 75.9 18.1 1009

**Phase II Piezometer Monitoring Data** 

Well ID \_\_\_P5\_\_\_\_ Depth \_\_\_18\_\_\_\_

	[	Well or Injection Gas Sample							Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
4/23/2008	931	0.0	0.32	9.0	2.5		79.0		12.9	1010
4/25/2008	942	0.0	0.20	9.5	0.10		66.5		19.3	1015
4/29/2008	1053	0.0	0.16	8.5	7.7		60.1		24.9	1007
5/5/2008	1258	0.0	0.78	9.0	11.0		41.6		33.2	1001
5/13/2008	910	0.0	0.86	9.5	2.4		47.3		29.5	1007
5/20/2008	917	0.0	0.64	7.5	19		64.1		24.5	1004
5/23/2008	1502	0.3	0.56	7.5	18		41.0		33.4	990
5/27/2008	848	0.0	1.40	9.5	9.1		78.4		15.8	1007
6/4/2008	850	0.0	0.30	9.5	6.6		69.9		20.9	1002
6/12/2008	1124	0.0	0.60	9.0	4.7		34.0		38.0	1003
6/20/2008	1000	0.0	1.02	8.5	7.1		48.3		32.1	1005
6/25/2008	1028	0.0	0.80	8.5	14.0		56.5		29.3	1005
7/2/2008	1130	0.0	1.00	9.0	14.0		44.0		33.3	1004
7/7/2008	1119	0	0.34	9	7.6		41.4		35	998
7/18/2008	1046	0	0.24	9	11		76.5		24.6	
7/24/2008	1045	0.0	0.38	8.5	13.000		68.2		27.5	1005
7/31/2008	1045	0.0	0.90	9.0	11.000		74.0		26.7	1003
8/7/2008	917	0.0	0.36	8.5	9.5		90.1		21.6	1004
8/12/2008	1022	0.0	0.08	9.0	11.0		63.0		28.8	1002

Well ID \_\_\_P5\_\_\_\_\_ Depth \_\_\_18\_\_\_\_\_ **Phase II Piezometer Monitoring Data** 

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization 7	est #8 (100	cfh of 100%	% Propane t	o P4-18, &	P4-28 (50 c	fh to each p	point)			
9/8/2008	0905 Test	Start								
9/8/2008	1012	9.3	0.80	3.5	0.002					999
9/15/2008	906	4.9	0.64	30	0.002		60.1		25.0	1007
9/29/2008	926	6.0	0.60	30	0.002		60.3		25.1	1006
10/13/2008	1148	6.3	0.46	30	0.005		42.2		30.2	1017
10/20/2008	1115	5.7	0.50	30	0.010		56.2		24.7	1013
11/5/2008	1353	5.6	0.60	30	0.005		76.7		18.7	1016
11/17/2008	1106	4.8	0.60	30	0.010		38.1		31.2	1014
12/1/2008	1107	4.7	0.66	30	0.002		54.9		20.7	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P5\_\_\_\_ Depth \_\_\_\_28\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1207	19.8	0.18	0	0.002	50,000	80.9	0.04	12.2	1020
12/12/2007	1534							0.24		
12/12/2007	1628	0.2				<1x10^2				
12/12/2007	1635	0.1				2x10^3				
12/12/2007	1643	0.1				4x10^3				
12/13/2007	805	10.0	0.00	0	0.002	9X10^3	86.4		1.0	1016
12/13/2007	840	3.9	0.00	0	5.3	7X10^3	73.7		4.1	1016
12/13/2007	935	11.0	0	0	8.1		59.7		11.4	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1316							0.20		
12/13/2007	1326	0	0	0	8.4		64.8		17.3	1014
12/13/2007	1444	0	0.36	0.50	0.51		76.4		14.3	1013
12/13/2007	1520	0	0.52	0.52	0.22		74.1		14.7	1013
12/13/2007	1554	0	0.58	0.52			77.1		12.8	1013
12/14/2007	829	0	0.10	0	0.46		68.9	0.02	4.3	1016
12/21/2007	1201	14.0	0.026	0.04	0.46		88.3	0.04	10.0	1013
12/26/2007	1227	17.0	0.26	0.02	0.22		83.7	0.02	12.2	1016
12/26/2007	1611	6.6	0.3	0.02	2.9		82.2	0.05	10.2	1015
12/27/2007	1014	0.2	0.1	0	9.2		78.3	0.05	6.0	1018
12/27/2007	1318	0.1	0	0	9.2		84.9		8.5	1016

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P5\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				Well	Ambient Air					
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/27/2007	1439	0.1	0	0	9.3		88.3		8.4	1017
12/27/2007	1556	0.1	0	0	9.8		90.2	0.06	7.5	1017
1/2/2008	1034	0.1	0	0	0.22		56.2	0.02	16.9	1012
1/2/2008	1034	0.1	0	0	0.22		56.2	0.02	16.9	1

Tracer Test #1	(10 cfm to I	NJ2, ~7% H	H2)						
1/21/2008	1046 Test start								
1/21/2008	1132	1.2	0	0	1.6	83.5	0.09	9.8	1008
1/21/2008	1253	0.9	0	0	5.1	84.8	0.07	10.7	1006
1/21/2008	1444	0.9	0	0	6.0	81.6	0.08	10.8	1006
1/21/2008	1609	0.9	0	0	6.1	96.4	0.07	10.0	1006
1/22/2008	952	0.8	0	0	6.9	84.9	0.06	6.9	1011
1/22/2008	1353	0.6	0	0	7.0	88.0		8.5	1009
1/23/2008	1020	0.7	0	0	6.8	84.6	0.08	8.6	1007
1/23/2008	1111*	0.7			6.8				

Tracer Test #2									
1/18/2008	1120 Test s	start							
1/18/2008	1133	1.1	0.04	0	0.10	85.1		12.5	1015
1/18/2008	1215	0.7	0	0	5.7	84.1	0.04	13.4	1015
1/18/2008	1317	0.6	0	0	6.7	78.0		15.4	1014

Well ID P5 **Phase II Piezometer Monitoring Data** Depth 28 **Ambient Air** Well or Injection Gas Sample Well  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure (%) (%) Date Time (%) (%) (ppm) (%) (C°) (mbar) (in wc) 1/18/2008 0 0 1349 0.8 6.8 80.6 15.4 1014 0.8 7.2 60.6 20.3 1/18/2008 1526 0 0 0.03 1014 1/19/2008 1004 0.6 0 0 7.0 70.4 0.02 9.4 1019 1/19/2008 1138\* 0.8 12.6 0 0 6.1 67.2 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 9.4 1/30/2008 1103 0.0 0 0 3.5 86.0 0.11 1020 0.0 0 0 4.3 79.1 1/30/2008 1217 11.1 1019 1/30/2008 1417 0.0 0 0 4.7 80.5 12.6 0.13 1018 1/31/2008 0 0 4.2 940 0.0 90.0 0.10 8.3 1019 1/31/2008 1127 0 0 0 3.7 84.7 9.6 1018 3.7 1/31/2008 1337 0 0 0 85.0 0.14 8.7 1016 1/31/2008 1435 1/31/2008 3.8 1507 0 0 87.4 0.04 8.2 0 1014 0 3.9 8.3 1013 1/31/2008 1602 0 0 86.8 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start

1/28/2008

1253

0.2

0

0

4.6

92.6

1010

10.5

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P5\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				Well or	Well	Ambient Air				
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/28/2008	1406	0.0	0	0	6.0		71.6	0.20	13.2	1010
1/28/2008	1547	0.0	0	0	6.3		84.6	0.17	10.1	1011
1/29/2008	752	0.0	0	0	7.3		86.0	0.10	5.0	1016
1/29/2008	Final O2*	0.0								

Tracer Test #5	(90 cfm to I	NJ2, ~3% H	·12)						
2/5/2008	3 1015 Test start								
2/5/2008	1027	0	0	0	3.1	72.0	0.26	9.2	1019
2/5/2008	1125	0	0	0	3.4	75.3		10.7	1019
2/5/2008	1333	0	0	0	4.0	76.0	0.26	12.2	1019
2/5/2008	1503	0	0	0	3.7	69.0		14.4	1019
2/5/2008	1547	0	0	0	3.5	55.4		17.9	1018

Tracer Test #6	(30 cfm tota	al; 10 cfm to	each INJ1	, 2, and 3; ~	8% H2)			
2/7/2008	1500 Test :	start						
2/7/2008	1527	0.0	0	0	0.046	45.4	21.8	1016
2/7/2008	1615	0.0	0	0	1.3	45.0	21.4	1016
2/8/2008	1004	0.0	0	0	8.7	61.3	11.6	1017

Phase II Piezometer Monitoring Data Well ID **P**5 Denth 28

0.0

2/20/2008 1206 Test start

1539

2/20/2008

0.84

1.04

10

48.1

22.5

Phase II Piezo	meter Mon	itoring Data	3	Well ID	P5		Depth	_28		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #7	(60 cfm tota	al; 20 cfm to	each INJ1,	2, and 3, ~	5% H2)					
1/17/2008	900 Test st	tart								
1/17/2008	952	15.6	0	0	0.46		82.6	0.04	7.2	1015
1/17/2008	1022	13.4	0	0	1.1		94.8	0.02	8.3	1015
1/17/2008	1154	6.6	0	0	3.8		86.9	0.03	10.0	1015
1/17/2008	1347	3.5	0.16	0	4.8		89.4		12.5	1013
1/17/2008	1511	2.4	0.18	0	5.2		81.8	0.05	14.8	1012
Tracer Test #8	(90 cfm tota	al; 30 cfm ea	ach to INJ1,	2, and 3; ~	4.5% H2)					
2/6/2008	1000 Test	start								
2/6/2008	1029	0.0	0	0	0.79		73.4	0.19	11.4	1020
2/6/2008	1139	0.0	0	0	3.1		69.9		12.5	1020
2/6/2008	1240	0.0	0	0	3.8		67.6		13.9	1019
2/6/2008	1426	0.0	0	0	4.6		61.4	0.21	16.0	1017
2/6/2008	1532	0.0	0	0	4.5		58.5		17.1	1017
Optimization To	est #1 (90 cf T	fm to INJ2 fo	or 4 hours t	hen shut do	wn; ~88% <b>N</b>	N2, 10% H2	2, 1% CO2 &	LPG)		
2/20/2008	1131	7.1	0.00	0	0.022		70.6		15.1	1010

1007

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P5\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

Phase II Piezo	meter Mon	itoring Data	3	Well ID	P5		Depth	_28		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/20/2008	1606 Test	End								
2/20/2008	1623	0.0	0.72	1.06	9.4		47.2		22.3	1008
2/21/2008	910	1.0	0.56	0.96	9.3		78.2		10.6	1005
2/22/2008	1036	4.9	0.48	0.54	3.8		83.6		9.7	1003
Optimization Te	est #2 (30 cf	m to INJ2 fo	or 12 hours	then shut d	own; ~88%	N2, 10% H	2, 1% CO2	& LPG)		
2/25/2008	1845 Test	Start								
2/26/2008	653 Test E	nd								
2/26/2008	703	0.0	2.12	0.48	7.4		91.8		3	1017
2/27/2008	1531	2.0	1.36	0.44	3.7		37.1		33	1009
2/28/2008	1051	4.7	1.16	0.36	2		71		15.8	1007
Optimization Te	est #3A (1 c	fm to INJ2;	~88% N2, 1	0% H2, 1%	CO2 & LP	G)				
2/29/2008	1319 Test	Start								
2/29/2008	1430	7.2	0.86	0.28	1		48.6		23.5	1009
2/29/2008	1518	7.1	0.88	0.28	0.91		53.1		24	1009
3/3/2008	1045	8.2	0.72	0.32	3		66.5		15.2	1019
3/3/2008	1130 Test	End								

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 28 Well or Injection Gas Sample Well **Ambient Air** CO<sub>2</sub>  $O_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Date Time (%) (%) (%) (%) (ppm) (mbar) (%) (in wc) (Co) Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 926 0.2 1.8 3/4/2008 11 0.74 76.2 12.2 1013 3/7/2008 1055 11.3 0.32 0.14 1.7 58.3 18.2 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1334 10.9 0.3 0.16 48.7 22.8 1016 3/10/2008 1050 8.7 0.4 0.42 0.22 66.5 16.5 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 8.9 0.22 3/10/2008 1234 0.48 0.44 54.9 20.5 1016 0.96 3/10/2008 1253 7.7 0.50 2.6 0.68 5.2 3/10/2008 1318 5 52.8 21.4 1016 8.0 0.68 7 8.6 3/10/2008 1330 1347 End pulse 3/10/2008 0.90 10 22.6 3/10/2008 1408 49.1 1015 0.4 3/11/2008 4.5 913 5.1 0.68 2.5 68.8 14.7 1017

Phase II Piezometer Monitoring Data	Well ID	P5	Depth28
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				Well or	Injection G	as Sample	<u> </u>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure		Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
3/12/2008	1000	7.0	0.64	2.5	3.7		81.6		12.8	1014
3/13/2008	914	7.8	0.52	2	3.2		84.6		13.8	1011
3/14/2008	1139	8.1	0.52	2	1.9		83.4		13.8	1013
3/14/2008	1214	4.0	0.56	2	6.8		78.8		14.8	1012
3/15/2008	1124	9.6	0.52	1.74	1.1		82.2		11.3	1009
3/16/2008	1111	10.7	0.34	1.38	0.78		75.1		14.3	1009
3/17/2008	923	10.2	0.40	1.76	1.5		81.4		9.1	1014
Optimization Te	est #5 (20 cf	fm to INJ2 fo	or 125 minu	tes while m	aintaing 30	cfh the rest	t of the time;	~80% N2, 10	% H2 & LPG)	
3/17/2008	1037	Start Test								
3/17/2008	1255	0.1	0.12	9.5	9.9		65.1		17.7	1014
3/8/2008	941	6.0	0.26	5.5	4		71.3		12.9	1016
3/19/2008	959	8.2	0.26	3.5	2.3		82		12.1	1013
3/20/2008	943	9.1	0.26	2.5	1.4		82.7		9.4	1016
3/20/2008	~1100	End Test								
Optimization Te	est #6 (50 cf	fh to P4-18 8	& P4-28; ~8	0% N2, 10%	% H2 & LPG	5)				
3/20/2008	1330 Start	Test								
3/21/2008	1004	6.5	0.20	2.5	2.5		83.4		12.0	1020
3/21/2008	1028	6.3	0.18	2.5	2.4					
3/24/2008	1003	3.7	0.22	2.5	2.2		63.0		16.3	1012

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 28 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (ppm) (%) (mbar) (in wc) (Co) 3/26/2008 945 3.0 2.5 10.8 1017 0.20 2.4 85.2 942 2.0 1.5 82.7 3/28/2008 1.6 0.2 10.4 1009 3/31/2008 943 0.1 0.12 14.0 9.1 82.5 9.3 1013 4/2/2008 1041 0.0 0.14 13.5 7.4 86.1 13.6 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 925 12.5 7.0 4/4/2008 0.3 0.10 84.6 12.1 1013 1352 3.4 80.0 9.5 4.8 4/7/2008 64.9 19.2 1012 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 1036 6.0 7.0 2.3 78.5 4/9/2008 0.02 14.4 1009 Optimization Test #7C (50 cfh to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2) 4/10/2009 1121 Start Test 4/11/2008 2.4 1220 6.9 0.06 5.5 62.7 21.3 1013 4/14/2008 1003 0.9 0.26 12.5 2.8 82.3 15.6 1007 9.5 6.1 82.3 4/16/2008 1015 0.6 0.48 14.5 1011 3.5 4.0 2.8 4/22/2008 1032 0.26 79.9 18.1 1009 8.5 0.58 932 1010 4/23/2008 0.0 0.22 80.4 12.9

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
4/25/2008	943	0.0	0.08	9.0	0.10		71.3		18.9	1015
4/29/2008	1055	0.0	0.16	8.5	4.4		62.5		24.9	1007
5/5/2008	1259	0.7	0.22	7.5	4.6		46.2		33.4	1001
5/13/2008	915	0.0	0.90	9.5	2.0		47.2		31.6	1007
5/20/2008	918	0.6	0.24	8.0	1.1		68.8		24.0	1004
5/23/2008	1504	0.3	0.58	8.5	2.5		43.5		33.8	990
5/27/2008	849	0.4	0.78	8.5	5.2		84.5		15.9	1007
6/4/2008	851	0.0	0.20	9.0	4.3		68.6		21.9	1002
6/12/2008	1128	0.0	0.56	9.0	2.5		36.7		38.8	1003
6/20/2008	1002	0.0	0.40	8.5	4.1		51.3		33.2	1005
6/25/2008	1030	0.0	0.16	8.0	4.5		62.5		29.6	1005
7/2/2008	1131	0.0	0.16	8.0	4.4		44.8		33.5	1004
7/7/2008	1120	0	0.16	8	3		41.8		35.1	998
7/18/2008	1048	0	0.2	8	4.3		85.2		24.7	
7/24/2008	1046	0.0	0.24	8.0	4.200		73.2		27.5	1005
7/31/2008	1046	0.0	0.32	8.0	4.600		77.7		26.7	1003
8/7/2008	918	0.0	0.30	8.5	4.2		91.6		21.9	1004
8/12/2008	1022	0.0	0.26	8.5	4.1		62.7		28.9	1002

				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Te	est #8 (100 e	cfh of 100%	Propane to	P4-18, & F	24-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test	Start								
9/8/2008	1018	5.3	0.52	6.5	0.005					999
9/15/2008	909	5.8	0.76	30	0.002		58.5		24.9	1007
9/29/2008	938	4.6	0.56	30	0.005		61.3		24.2	1006
10/13/2008	1149	7.2	0.44	30	0.005		43.1		30.3	1017
10/20/2008	1117	5.3	0.46	30	0.005		55.1		24.9	1013
11/5/2008	1354	4.6	0.58	30	0.005		79.4		18.7	1016
11/17/2008	1106	3.6	0.62	30	0.010		42.7		30.8	1014
12/1/2008	1108	3.2	0.68	30	0.005		55.3		20.9	1014

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1210	19.3	0.34	0	0.002	70,000	82.0	0.02	12.1	1020
12/12/2007	1534							0.43		
12/12/2007	1627	0.1				2x10^4				
12/12/2007	1635	0.1				2x10^4				
12/12/2007	1642	0.1				2x10^4				
12/13/2007	803	10.1	0.00	0	0.002	2x10^4	86.8		0.7	1016
12/13/2007	843	3.3	0.00	0	7.0	2x10^3	72.5		4.5	1016
12/13/2007	937	9.2	0	0	8.2		60.2		11.5	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1317							0.31		
12/13/2007	1327	0	0	0	8.4		62.8		17.4	1014
12/13/2007	1442	0	0.14	0.52	0.59		77.1		14.7	1013
12/13/2007	1522	0	0.44	0.52	0.22		75.2		14.8	1013
12/13/2007	1556	0	0.40	0.52			74.1		12.8	1013
12/14/2007	830	0	0.32	0	0.50		70.5	0.03	4.1	1016
12/21/2007	1203	6.8	0.26	0.10	0.46		88.9	0.03	9.9	1012
12/26/2007	1228	11.2	0.22	0.06	0.22		84.2	0.04	12.4	1016
12/26/2007	1612	9.5	0.28	0.06	0.71		82.6	0.02	10.2	1015
12/27/2007	1016	1.3	0.32	0	7.5		78.2	0.03	6	1018
12/27/2007	1320	0.8	0.2	0	8.1		86.9		8.5	1016

Phase II Piez	ometer Mor	nitoring Da	ta	Well ID	P5		Depth	_38		
	Ī			Well or	Injection G	as Sample	<b>;</b>		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/27/2007	1440	0.7	0.18	0	8.3		87.8		8.5	1017
12/27/2007	1558	0.6	0.18	0	8.7		90.9	0.04	7.5	1017
1/2/2007	1035	0.2	0.14	0	0.22		52.6	0.02	16.7	1012
Tracer Test #	1 (10 cfm to	INJ2, ~7%	H2)							
1/21/2008	1046 Test s	start								
1/21/2008	1133	2.7	0.10	0	1.1		84.0	0.06	9.9	1008
1/21/2008	1254	2.5	0.10	0	1.1		85.9	0.07	10.7	1006
1/21/2008	1445	1.9	0.08	0	1.8		84.7	0.09	10.7	1006
1/21/2008	1610	1.7	0.08	0	2.5		89.9	0.06	9.8	1006
1/22/2008	954	1.0	0.08	0	5.7		85.7	0.10	6.8	1011
1/22/2008	1354	0.8	0.04	0	6.1		86.8		6.5	1009
1/23/2008	1021	0.8	0.08	0	6.4		85.1	0.08	8.5	1007
1/23/2008	1113*	0.7								
Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)							
1/18/2008	1120 Test s	start								
					-			·		· · · · · · · · · · · · · · · · · · ·

Tracer Test #2	2 (20 cfm to	INJ2, ~8%	H2)						
1/18/2008	1/18/2008 1120 Test start								
1/18/2008	1135	2.9	0.24	0	0.60	83.8		12.5	1015
1/18/2008	1217	2.3	0.22	0	0.75	80.0	0.03	13.4	1015
1/18/2008	1318	1.6	0.20	0	2.0	68.6		15.6	1014

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 38 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane He RH **Pressure** Temperature Barometric pressure  $H_2$ Time (%) (%) (%) (C°) Date (%) (ppm) (%) (mbar) (in wc) 1/18/2008 1351 1.7 0.20 2.9 73.8 15.4 1014 1528 1.3 0.18 50.8 21.2 1/18/2008 0 4.6 0.03 1014 1/19/2008 1006 0.7 0.14 9.7 72.3 0.00 9.4 1019 1/19/2008 1139\* 8.5 12.5 0.7 0.10 70.0 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1105 0.0 0 1.9 87.6 0.10 9.4 1020 1/30/2008 1218 0.0 0 2.6 80.7 11.0 1019 1/30/2008 1418 0.0 0 4.0 80.3 12.8 0 0.14 1018 1/31/2008 0 4.2 942 0.0 89.8 0.11 8.4 1019 0 1128 0 3.8 84.1 9.6 1/31/2008 1018 1339 0 1/31/2008 0 3.8 85.7 0.16 8.7 1016 1/31/2008 1435 1/31/2008 1509 0 0 3.7 87.7 0.04 8.2 0 1014 1/31/2008 0 0 3.9 8.3 1013 1610 87.6 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start

0.50

94.1

10.5

1/28/2008

1254

7.5

0.04

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P5\_\_\_\_ Depth \_\_\_\_38\_\_\_\_

2/8/2008

1056

0.0

Phase II Piez		morning Du		well ID			Deptn			
				Well or	Injection G				Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	•	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/28/2008	1410	0.2	0.04	0	5.2		77.0	0.24	13.3	1010
1/28/2008	1549	0.0	0	0	6.1		88.1	0.18	10.5	1011
1/29/2008	754	0.0	0	0	7.3		86.6	0.10	4.9	1016
1/29/2008	Final O2*	0.0								
Tracer Test #5	(90 cfm to	INJ2, ~3%	H2)							
2/5/2008	1015 Test s	start								
2/5/2008	1028	1.1	0	0	1.1		73.2	0.28	9.3	1019
2/5/2008	1126	0.0	0	0	3.1		74.9		10.8	1019
2/5/2008	1336	0.0	0	0	4.0		73.7	0.32	12.4	1019
2/5/2008	1504	0.0	0	0	3.7		69.2		14.5	1019
2/5/2008	1548	0.0	0	0	3.5		54.7		18.0	1018
Tracer Test #6	6 (30 cfm tot	al; 10 cfm t	o each INJ1	l, 2, and 3;	~8% H2)					
2/7/2008	1500 Test s	start								
2/7/2008	1528	0.0	0	0	1.1		45		22.0	1016
2/7/2008	1617	0.0	0	0	0.98		44.9		21.3	1016
2/8/2008	1005	0.0	0	0	5.3		62.5		11.3	1017

5.1

76.9

11.0

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 38 **Well or Injection Gas Sample Ambient Air** Well  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Date Time (%) (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 953 11.7 0.08 0.22 81.2 0.00 7.3 1015 0.22 0.02 8.2 1/17/2008 1024 11.7 0.06 93.9 1015 1/17/2008 0 87.7 1155 11.7 0.06 0.22 0.01 10.0 1015 90.8 12.5 1/17/2008 1351 10.4 0.24 1013 1.4 1/17/2008 1513 8.8 0.26 0 2.3 75.5 0.04 15.8 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1030 0.0 0 73.1 11.3 1020 0 1.4 0.18 0.0 0 68.9 12.7 2/6/2008 1141 1.1 1020 2/6/2008 1241 0.0 0 1.3 66.8 14.0 1019 2/6/2008 1430 0 59.3 16.2 0.0 0 2.5 0.18 1017

Optimization 7	Γest #1 (90 d	& LPG)							
2/20/2008	1133	7.8	0.00	0	0.046	71.2		15.1	1010
2/20/2008	1206 Test :	start							

59.1

60.6

17.0

16.9

2.7

2.9

0

2/6/2008

2/6/2008

1533

1626

0.0

0.0

0

0

1017

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/20/2008	1540	0.0	0.80	1.02	11		49.8		22.7	1007
2/20/2008	1606 Test I	End								
2/20/2008	1624	0.0	0.68	1	10		47.4		22.5	1008
2/21/2008	912	4.8	0.46	0.7	7.4		78.3		10.6	1005
2/22/2008	1038	9.2	0.42	0.42	3.5		84.8		9.7	1003
Optimization T	est #2 (30 d	ofm to INJ2 t	or 12 hours	s then shut o	down; ~88%	6 N2, 10% F	12, 1% CO2	! & LPG)		
2/25/2008	1845 Test \$	Start								

Optimization T	est #2 (30 c	ofm to INJ2	for 12 hours	s then shut	down; ~88%	% N2, 10% H2, 1% CO	2 & LPG)	
2/25/2008	1845 Test \$	Start						
2/26/2008	653 Test E	nd						
2/26/2008	704	0.2	2.12	0.56	7	91.2	3.1	1017
2/27/2008	1532	6.0	1.1	0.32	3.2	33.1	33.8	1009
2/28/2008	1052	7.5	0.92	0.34	2.1	69.5	15.8	1008
Optimization T	est #3A (1	cfm to INJ2	; ~88% N2,	10% H2, 19	6 CO2 & LF	PG)		
2/29/2008	1319 Test \$	Start						
2/29/2008	1432	8.8	0.70	0.26	1	51	23.7	1009
2/29/2008	1519	8.8	0.7	0.26	0.87	51.9	24.8	1009
3/3/2008	1046	8.3	0.64	0.24	0.1	66.9	15.3	1019
3/3/2008	1130 Test I	End						

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 38 **Well or Injection Gas Sample** Well **Ambient Air**  $O_2$  $CO_2$ Propane He RH **Pressure** Temperature **Barometric pressure**  $H_2$ Time Date (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 927 8.5 0.72 0.22 75.2 3/4/2008 0.22 12.3 1013 3/7/2008 1056 9.5 0.046 58.7 18.2 1018 0.46 0.16 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1336 9.4 0.44 0.18 0.046 49.3 22.6 1016 3/10/2008 1052 9.6 0.5 0.42 0.022 66.9 16.5 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 1319 9.5 0.60 0.42 0.022 53.5 21.4 1016 1347 End pulse 3/10/2008 3/10/2008 9.0 1409 0.56 0.68 0.77 49.2 22.6 1015 921 7.8 1.42 67.8 15.3 1017 3/11/2008 0.58 82.5 3/12/2008 1001 7.6 0.54 1.5 12.9 1.44 1014 3/13/2008 916 7.7 0.48 1.34 83.9 13.9 1011 0.48 3/14/2008 1140 7.5 1.38 0.63 82.5 13.9 1013

				Well or		Well	Ambient Air			
		O <sub>2</sub>	2					Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
3/14/2008	1215	7.2	0.46	1.42	0.6		78		14.7	1012
3/15/2008	1125	7.8	0.50	1.16	0.5		81.3		11.2	1009
3/16/2008	1112	7.7	0.36	1.68	0.57		75.3		14.3	1009
3/17/2008	924	8.2	0.46	1.74	0.5		81.5		9.2	1014

Optimization T	est #5 (20	cfm to INJ2	for 125 min	utes while r	naintaing 30	) cfh the rest	t of the time	e; ~80% N2, 10	% H2 & LPG)	
3/17/2008	1037	Start Test								
3/17/2008	1254	6.0	0.36	4.5	2.1		61.9		17.7	1014
3/8/2008	943	5.2	0.42	4.5	2.6		78		13.1	1016
3/19/2008	1000	4.7	0.40	4.5	1.4		81.1		12.1	1013
3/20/2008	945	5.0	0.42	4.5	0.5		82.2		9.5	1016
3/20/2008	~1100	End Test								

Optimization T	Test #6 (50 d	ofh to P4-18	3 & P4-28; ~	80% N2, 10	)% H2 & LP	G)			
3/20/2008	1330 Start	Test							
3/21/2008	1010	5.1	0.38	4.0	0.10		82.1	12.4	1020
3/24/2008	1005	5.4	0.46	3.5	0.046		64.8	16.1	1012
3/26/2008	946	5.4	0.48	3.5	0.022		82.8	10.8	1017
3/28/2008	943	5.4	0.5	3.0	0.022		84.3	10.4	1009
3/31/2008	945	2.6	0.42	7.0	1.8		85.4	9.4	1013
4/2/2008	1042	0.9	0.40	10.5	1.8		86.1	13.9	1008

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				Well or	Injection G	as Sample			Well	Ambient Air
		<b>O</b> <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #7 (20 d	ofh to P4-18	,28, -38 (	60 cfh total)	; ~80% N2,	10% H2 &	LPG)			
4/2/2008	1233 Start	Test								
4/4/2008	926	0.4	0.36	10.5	5.8		84.2		12.2	1013
4/7/2008	1353	1.2	0.28	8.5	4.7		66.5		19.2	1012
Optimization T	Test #7B (30	cfh to P4-1	8, & P4-28	(60 cfh tota	I); ~80% N2	2, 10% H2 8	& LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1040	1.5	0.24	9.0	0.1		77.2		14.3	1009
Optimization T	est #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tot	tal); ~79% N	N2, 10% H2	& LPG, 1%	CO2)		
4/10/2009	1121 Start	Test								
4/11/2008	1221	1.7	0.32	9.0	0.1		62.6		21.4	1013
4/14/2008	1005	0.6	0.30	10.0	0.7		82.9		15.7	1007
4/16/2008	1016	0.0	0.30	11.0	0.50		84.3		14.7	1011
4/22/2008	1034	1.1	0.38	6.5	0.10		79.4		18.1	1009
4/23/2008	933	1.2	0.40	7.0	0.22		80.5		12.8	1010
4/25/2008	944	0.5	0.36	8.0	0.10		74.4		18.8	1015
4/29/2008	1056	0.0	0.40	8.5	0.46		63.4		25.0	1007
5/5/2008	1301	0.2	0.40	8.0	0.1		51.8		33.4	1001
5/13/2008	916	0.0	0.46	8.5	0.046		45.4		32.6	1007

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
5/20/2008	920	0.0	0.48	8.5	0.10		68.7		23.5	1004
5/23/2008	1505	0.2	0.40	8.5	0.10		50.8		32.7	990
5/27/2008	850	0.0	0.58	8.5	0.10		84.0		16.1	1007
6/4/2008	853	0.0	0.44	8.0	0.22		67.9		22.8	1002
6/12/2008	1131	0.1	0.46	8.5	0.046		37.7		39.1	1003
6/20/2008	1005	0.0	0.46	8.5	0.540		47.3		34.3	1005
6/25/2008	1032	0.0	0.44	8.5	0.22		56.4		30.3	1005
7/2/2008	1132	0.0	0.42	8.0	0.50		46.6		33.5	1004
7/7/2008	1121	0	0.36	8	0.5		43.6		35.2	998
7/18/2008	1049	0	0.46	8	0.1		75.9		24.9	
7/24/2008	1047	0.0	0.48	8.0	0.220		68.9		27.5	1005
7/31/2008	1042	0.0	0.54	8.0	0.220		70.5		26.5	1003
8/7/2008	919	0.0	0.60	8.0	0.22		90.6		22.0	1004
8/12/2008	1023	6.0	0.60	8.5	0.51		60.5		29.0	1002
Optimization T	est #8 (100	cfh of 100%	% Propane t	o P4-18, &	P4-28 (50 c	fh to each p	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1021	6.2	0.58	6.5	0.005					999
9/15/2008	910	0.9	0.96	30	0.005		59.3		24.9	1007
9/29/2008	929	0.1	0.46	30	0.005		62.8		23.6	1006
10/13/2008	1152	0.6	0.34	30	0.005		42.7		30.4	1017

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
10/20/2008	1118	0.4	0.36	30	0.005		54.3		25.1	1013
11/5/2008	1346	0.1	0.38	30	0.005		65.9		19.0	1016
11/17/2008	1108	0.0	0.34	30	0.010		41.4		30.4	1014
12/1/2008	1109	0.0	0.30	30	0.005		55.6		21.5	1014

				Well or	Injection G	as Sample		Well	Ambient Air	
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1211	19.1	0.00	0	0.002	80,000	82.2	0.02	12.1	1020
12/12/2007	1533							0.33		
12/12/2007	1628	12.0				3x10^4				
12/12/2007	1634	7.7				3x10^4				
12/12/2007	1642	5.1				2x10^4				
12/13/2007	804	13.7	0.00	0	0.002	2x10^4	86.4		0.8	1016
12/13/2007	845	9.0	0.00	0	0.22	2x10^4	71.7		4.7	1016
12/13/2007	938	13.4	0	0	0.46		61.2		11.6	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 1	200 invalid			
12/13/2007	1317							0.18		
12/13/2007	1327	0	0	0	8.0		63.3		17.5	1014
12/13/2007	1446	0	0	0	8.9		79.7		14.0	1013
12/13/2007	1523	0	0	0	8.8		75.4		14.7	1013
12/13/2007	1557	0	0	0.02			76.3		12.8	1013
12/14/2007	831	0	0	0.40	2.3		71.5		4.1	1016
12/21/2007	1204	13.8	0	0	0.57		91.3	0.02	9.8	1012
12/26/2007	1230	14.4	0	0	0.22		84.1	0.01	13.2	1016
12/26/2007	1614	13.4	0	0.02	0.46		82.1	0.04	10.1	1015
12/27/2007	1018	13.5	0	0.02	0.5		80.1	0.04	5.9	1018
12/27/2007	1322	14.8	0	0	0.46		85.8		8.6	1016

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Temperature	Barometric pressure				
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/27/2007	1442	13.7	0	0.02	0.46		87.1		8.7	1017
12/27/2007	1600	13.6	0	0.02	0.63		89.2	0.04	7.4	1017
1/2/2008	1037	11.5	0	0	0.22		54.2	0.03	16.6	1012

Tracer Test #1	(10 cfm to	INJ2, ~7%	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1134	5.7	0	0	2.4	84.8	0.06	9.9	1008
1/21/2008	1255	5.9	0	0	2.1	88.2	0.09	10.7	1006
1/21/2008	1446	6.3	0	0	1.8	85.7	0.09	10.9	1006
1/21/2008	1611	6.5	0	0	1.7	88.4	0.06	9.9	1006
1/22/2008	955	7.7	0	0	0.95	86.3	0.02	6.8	1011
1/22/2008	1356	7.4	0	0	1.1	87.5		8.6	1009
1/23/2008	1024	8.7	0.08	0	0.95	86.4	0.04	8.3	1007
1/23/2008	1114*	8.7							

Tracer Test #2	? (20 cfm to	INJ2, ~8%	H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1136	9.3	0	0	1.0	84.1		12.6	1015
1/18/2008	1218	8.7	0	0	1.2	82.6	0.04	13.4	1015
1/18/2008	1319	8.4	0	0	1.2	69.3		15.7	1014

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 48 Well Well or Injection Gas Sample **Ambient Air**  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure (%) (%) (C°) Date Time (%) (%) (ppm) (%) (mbar) (in wc) 1/18/2008 0 0 1352 8.4 1.3 81.5 1014 15.4 1529 7.9 0 0 1.2 53.7 1/18/2008 0.04 21.9 1014 1/19/2008 1009 7.0 0 0 1.9 75.2 0.01 9.4 1019 1/19/2008 1141\* 0 2.4 6.8 0 77.0 12.5 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1107 0.1 0 0 3.4 88.4 0.08 9.7 1020 1/30/2008 1220 0.1 0 3.2 81.8 11.0 1019 1/30/2008 1419 0.1 0 0 3.3 82.8 13.0 0.11 1018 0 945 0.0 4.0 91.9 0.10 8.5 1019 1/31/2008 1129 0 0 0 3.5 87.1 9.6 1/31/2008 1018 0 1/31/2008 1340 0 3.5 86.0 0.22 8.7 1016 1/31/2008 1435 0 0 88.2 8.2 1/31/2008 1511 0 3.0 0.03 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 9.7 1/28/2008 1256 0 0 0.022 93.4 10.5 1010 1/28/2008 1411 5.0 0 0.10 78.8 0.16 13.3 1010

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Temperature	Barometric pressure				
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/28/2008	1551	4.3	0	0	1.4		87.1	0.10	11.0	1011
1/29/2008	756	0.0	0	0	7.6		86.9	0.13	4.9	1016
1/29/2008	Final O2*	0.0								

Tracer Test #5	(90 cfm to	INJ2, ~3%	H2)						
2/5/2008	1015 Test s	start							
2/5/2008	1030	3.4	0	0	0.10	74.9	0.16	9.2	1019
2/5/2008	1128	4.0	0	0	0.10	76.8		10.8	1019
2/5/2008	1337	1.3	0	0	2.3	71.7	0.22	12.4	1019
2/5/2008	1505	0.5	0	0	3.0	62.1		14.5	1019
2/5/2008	1549	0.3	0	0	3.0	51.4		18.0	1019

Tracer Test #6	(30 cfm tot	al; 10 cfm t	o each INJ1	, 2, and 3;	~8% H2)			
2/7/2008	1500 Test s	start						
2/7/2008	1529	0.2	0.04	0	1.6	41.9	22.1	1016
2/7/2008	1618	0.2	0.04	0	1.5	43.5	21.2	1016
2/8/2008	1006	0.0	0	0	1.3	64.1	11.1	1017
2/8/2008	1057	0.0	0	0	1.3	73.6	11.0	1017

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 48 **Well or Injection Gas Sample Ambient Air** Well  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Time Date (%) (%) (%) (%) (ppm) (%) (C°) (mbar) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 955 14.3 0 0 0.22 80.9 0.02 7.3 1015 1/17/2008 1026 12.5 0 0 0.022 86.3 0.02 8.2 1015 1/17/2008 0 0 1157 11.8 0.22 87.6 0.01 10.1 1015 1353 11.3 0.22 88.6 12.7 0 1013 1/17/2008 1/17/2008 1515 10.9 0 0 0.22 69.2 0.05 17.1 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1032 0.4 0 0 72.9 11.2 1020 1.6 0.14 0 2/6/2008 1143 0.4 0 1.5 68.2 12.7 1020 2/6/2008 1242 0.3 0 0 1.5 65.3 14.1 1019 1437 0 0.4 0 1.7 57.8 0.15 16.0 2/6/2008 1017 1534 1017 0.4 0 0 1.6 57 17.0 2/6/2008 2/6/2008 1627 0.4 0 0 1.6 55.8 17.3 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 0.28 0.046 70.3 2/20/2008 1134 9 0 15.2 1010

2/20/2008 1206 Test start

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/20/2008	1541	2.6	0.00	0.54	5.9		44.9		23.1	1007
2/20/2008	1606 Test E	End								
2/20/2008	1629	3.3	0.04	0.46	4.8		43.2		22.8	1008
2/21/2008	913	8.5	0.48	0	0.5		80.1		10.6	1005
2/22/2008	1039	9.3	0.50	0	0.5		84.1		9.7	1003

Optimization T	est #2 (30 c	ofm to INJ2	for 12 hours	s then shut	down; ~88%	5 N2, 10% H2, 1% CO2	2 & LPG)	
2/25/2008	1845 Test	Start						
2/26/2008	653 Test E	nd						
2/26/2008	706	7.5	0.3	0.4	1.3	90.6	3.2	1017
2/27/2008	1534	10.0	0.46	0	0.046	32.2	34.6	1009
2/28/2008	1053	10.6	0.38	0	0.046	68.1	15.8	1007
Optimization T	est #3A (1	cfm to INJ2;	; ~88% N2,	10% H2, 1%	6 CO2 & LF	PG)		
2/29/2008	1319 Test	Start						
2/29/2008	1433	10.6	0.26	0.02	0.046	54.3	23.8	1009
3/3/2008	1048	10.8	0.28	0	0.022	66.9	15.4	1019
3/3/2008	1130 Test	End						

**Phase II Piezometer Monitoring Data** Well ID P5 Depth 48 **Well or Injection Gas Sample Ambient Air** Well  $O_2$ CO2 Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Time Date (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 928 11.2 0.4 0 75.3 3/4/2008 0.022 12.5 1013 3/7/2008 1058 11.3 0.22 0.02 0.022 58.1 18.2 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 0.18 3/7/2008 1337 11 0.02 0.01 47.2 22.4 1016 3/10/2008 1053 11.8 0.28 0 0.022 67.4 16.5 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 1347 End pulse 3/10/2008 1410 11.7 0.26 0.02 0.01 50.6 22.6 1015 69.3 3/11/2008 923 12.0 0.36 0.06 0.046 15.4 1017 0.40 0 0.022 82.3 12.9 3/12/2008 1003 12.4 1014 0.36 85.6 3/13/2008 917 12.2 0 0.022 13.9 1011 3/14/2008 12.0 0.36 0 1142 0.022 83 14 1013 0.30 3/14/2008 1217 11.8 0.022 79.7 14.7 1012

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date 1	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
3/15/2008	1126	12.0	0.42	0	0.022		82.4		11.2	1009
3/16/2008	1113	11.6	0.26	0.04	0.022		75.7		14.2	1009
3/17/2008	926	12.8	0.32	0.04	0.01		81.7		9.3	1014

Optimization T	% H2 & LPG)								
3/17/2008	1037	Start Test							
3/17/2008	1258	10.8	0.16	0.1	0.022	61.2		17.7	1014
3/8/2008	944	11.4	0.32	0.06	0.022	78.4		13.1	1016
3/19/2008	1001	11.3	0.30	0.06	0.022	82		12.3	1013
3/20/2008	946	10.8	0.26	0.16	0.01	82.6		9.6	1016
3/20/2008	~1100	End Test							

Optimization T	est #6 (50 d	ofh to P4-18	& P4-28; ~	80% N2, 10	G)				
3/20/2008	1330 Start	Test							
3/21/2008	1012	6.9	0.26	0.06	0.68		81.0	12.5	1020
3/24/2008	1006	9.4	0.30	0.78	0.022		66.7	16.0	1012
3/26/2008	948	8.9	0.28	1.36	0.022		82.5	10.9	1017
3/28/2008	945	9.2	0.3	1.26	0.022		86.1	10.5	1009
3/31/2008	946	8.2	0.26	2.0	0.022		85.0	9.6	1013
4/2/2008	1043	6.7	0.22	2.5	0.046		87.1	14.2	1008

					Injection G				Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			
Optimization T	est #7 (20 d	ofh to P4-18	,28, -38 (	60 cfh total)	; ~80% N2,	10% H2 &	LPG)						
4/2/2008	1233 Start	Test											
4/4/2008	927	5.1	0.20	4.5	0.046		86.2		12.3	1013			
4/7/2008	1354	6.1	0.36	4.0	0.046		67.7		19.1	1012			
Optimization T	est #7B (30	cfh to P4-1	8, & P4-28	(60 cfh tota	I); ~80% N2	2, 10% H2 8	& LPG)						
4/7/2008	1458 Start	Test											
4/9/2008	1043	6.9	0.36	3.5	0.005		77.5		14.2	1009			
Optimization T	est #7C (50	ofh to P4-1	8, & P4-28	(100 cfh tot	tal); ~79% N	l2, 10% H2	& LPG, 1%	CO2)					
4/10/2009	1121 Start	Test											
4/11/2008	1222	7.1	0.46	3.5	0.046		61.7		21.5	1013			
4/14/2008	1006	6.1	0.48	4.5	0.022		84.6		15.7	1007			
4/16/2008	1017	4.1	0.42	7.0	0.046		84.2		14.9	1011			
4/22/2008	1035	3.0	0.44	8.5	0.010		78.7		18.7	1009			
4/23/2008	934	3.0	0.42	8.5	0.046		81.4		12.7	1010			
4/25/2008	945	1.9	0.28	8.5	0.046		73.9		18.8	1015			
4/29/2008	1057	1.6	0.36	9.0	0.10		26.2		25.2	1007			
5/5/2008	1303	1.6	0.42	8.5	0.1		33.1		39.1	1001			
5/13/2008	919	1.0	0.46	8.5	0.046		38.7		33.1	1007			

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
5/20/2008	921	0.9	0.42	8.5	0.10		68.1		23.4	1004
5/23/2008	1507	0.4	0.44	8.5	0.10		42.6		32.1	990
5/27/2008	852	0.4	0.66	9.0	0.10		84.9		16.3	1007
6/4/2008	854	0.6	0.66	8.0	0.10		67.0		23.4	1002
6/12/2008	1134	0.2	0.66	8.0	0.046		32.5		39.4	1003
6/20/2008	1007	0.3	0.76	8.0	0.046		40.2		35.5	1005
6/25/2008	1033	0.3	0.80	7.5	0.10		53.5		30.8	1005
7/2/2008	1133	0.3	0.84	7.5	0.10		48.1		33.0	1004
7/7/2008	1123	0.2	0.78	7.5	0.046		44		35.3	998
7/18/2008	1050	0.1	0.96	7.5	0.1		82.4		25	
7/24/2008	1048	0.0	0.98	7.0	0.100		70.7		27.7	1005
7/31/2008	1044	0.0	1.04	7.0	0.100		77.3		26.6	1003
8/7/2008	921	0.0	1.10	7.5	0.046		89.0		22.3	1004
8/12/2008	1026	0.0	1.04	7.5	0.100		64.1		28.8	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane t	o P4-18, &	P4-28 (50 c	fh to each p	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1025	6.2	0.64	6.54	0.005					999
9/15/2008	911	0.5	1.16	30	0.005		58.8		24.8	1007
9/29/2008	930	0.0	1.28	30	0.005		61.4		23.0	1006
10/13/2008	1153	0.2	1.02	30	0.005		42.7		30.3	1017

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
10/20/2008	1119	0.1	1.04	30	0.010		53.4		25.3	1013
11/5/2008	1349	0.0	0.52	30	0.005		63.3		18.9	1016
11/17/2008	1109	0.0	0.70	30	0.010		46.8		29.6	1014
12/1/2008	1110	0.0	0.66	30	0.005		54.1		21.8	1014

Phase II Piezometer Monitoring Data	Well IDP6	Depth18
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				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1153	20.1	0.06	0	0.002	40,000	87.3	0.04	11.5	1020
12/12/2007	1537							0.15		
12/13/2007	903	10.6	0	0	1.5		77.2		7.2	1016
12/13/2007	957	12.0	0	0	6.4		69.8		11.7	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1342	0	0.04	0	8.5		77.9		16.8	1013
12/13/2007	1506	0	0	0.24	5.3		90.0		13.5	1013
12/13/2007	1538	0	0.02	0.48	1.5		85.3		12.8	1013
12/14/2007	847	0	0.16	0.10	0.77		65.5	0.04	7.3	1016
12/21/2007	1209	10.2	0.12	0.08	0.46		88.9	0.02	9.9	1012
12/26/2007	1235	15.2	0.14	0.04	0.022		76	0.02	14.2	1016
12/27/2007	1023	0.4	0.2	0	9.1		75.3	0.04	6	1018
12/27/2007	1325	0.3	0.1	0	9.2		80.9		8.9	1016
12/27/2007	1445	0.2	0.1	0	9.5		85.6		8.6	1017
12/27/2007	1607	0.2	0.1	0	9.6		83.4	0.04	7.4	1017
1/2/2008	1040	0.2	0.1	0	0.22		65	0.02	16.1	1012
Tracer Test #1	(10 cfm to II	NJ2, ~7% H	2)							
1/21/2008	1046 Test :	start								
1/21/2008	1211	1.3	0	0	0.046		82.6	0.05	10.0	1007

Phase II Piezor	meter Moni	itoring Data	ì	Well ID	P6		Depth	_18		
	į			Well or	Injection G	as Sample	e		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/21/2008	1312	1.2	0	0	0.46		80.6		9.5	1006
1/21/2008	1508	1.2	0	0	2.4		81.1		11.1	1006
1/22/2008	1000	1.0	0.02	0	6.5		85.4	0.08	6.8	1011
1/22/2008	1403	0.9	0	0	6.5		83.3		8.7	1009
1/23/2008	1025	1.1	0	0	6.8		86.6	0.07	8.2	1007
1/23/2008	1118*	0.6								
Tracer Test #2	(20 cfm to II	NJ2, ~8% H	2)							
1/18/2008	1120 Test s	start								
1/18/2008	1201	1.0	0.04	0	0.046		74.7		13.2	1015
1/18/2008	1304	0.9	0.02	0	1.2		67.1		14.7	1014
1/18/2008	1353	1.1	0.02	0	3.1		70.9		15.5	1014
1/18/2008	1532	0.9	0	0	4.6		50.7	0.04	22.9	1014
1/19/2008	1010	0.9	0.06	0	11.0		67.1	0.02	9.4	1019
1/19/2008	1145*	0.7	0.02	0	9.6		68.6		12.7	1018
Tracer Test #3	(30 cfm to II	NJ2, ~4% H	2)							
1/30/2008	1036 Test s	start								
1/30/2008	1110	0.0	0	0	0.10		88.2	0.09	9.8	1020
1/30/2008	1221	0.0	0	0	1.9		82.4		11.1	1019

Depth 18 **Phase II Piezometer Monitoring Data** Well ID P6 Well **Ambient Air** Well or Injection Gas Sample  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure (%) (%) Date Time (%) (%) (ppm) (%) (in wc) (C°) (mbar) 1/30/2008 0 0 1422 0.0 3.8 77.9 0.10 1018 13.1 0 4.2 1/31/2008 949 0.0 0 86.4 0.16 8.6 1019 1/31/2008 1130 0 0 0 3.8 85.1 9.6 1018 1/31/2008 1344 0 0 0 3.8 79.8 0.13 8.8 1016 1/31/2008 1435 0 0 3.8 1/31/2008 1514 0 86.9 0.04 8.2 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1302 2.2 0 0.022 0 90.1 10.4 1010 0 0 4.1 1412 0.4 13.3 1/28/2008 79.4 0.14 1011 1553 5.9 1/28/2008 0 0 0.18 0.0 87.6 11.7 1011 1/29/2008 756 0.0 0 0 7.4 87.5 0.08 4.8 1016 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1032 0.3 0 0 0.10 72.8 0.18 9.2 1019 2/5/2008 1129 0 0 0 2.6 77.7 10.9 1019 2/5/2008 1338 0 0 0 3.9 82.5 0.20 12.5 1019

Depth 18 **Phase II Piezometer Monitoring Data** Well ID P6 Well **Ambient Air** Well or Injection Gas Sample  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure (%) (%) Date Time (%) (%) (ppm) (%) (in wc) (C°) (mbar) 2/5/2008 0 0 1506 0 3.7 79.5 14.7 1019 3.5 1550 0 63.2 2/5/2008 0 0 18.6 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0 2/7/2008 1531 0.0 0 0.046 57.6 22.2 1016 2/7/2008 1619 0 0 1.4 56.1 21.1 0.0 1016 2/8/2008 1008 0.0 0 0 8.8 64.5 10.8 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1028 1/17/2008 10.7 0 0 0.99 0.04 76 8.2 1015 1/17/2008 1141 5.0 0 0 3.6 77.7 9.8 1015 1/17/2008 1356 1.7 0.16 0 5.2 70.6 13.2 1013 1517 0 5.7 1012 1/17/2008 1.2 0.16 60.9 18.3 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1033 0.0 0 0 0.52 79.1 0.20 11.2 1020

2/6/2008

1146

0.0

0

0

3.0

79.1

1020

12.8

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1243	0.0	0	0	3.8		76.6		14.2	1019
2/6/2008	1439	0.0	0	0	4.7		80.2	0.20	16.0	1017
2/6/2008	1535	0.0	0	0	4.6		68.8		17.4	1017

Optimization Te	st #1 (90 cf	& LPG)						
2/20/2008	1135	6	0.00	0	0.046	73.8	15.1	1010
2/20/2008	1206 Test s	start						
2/20/2008	1543	0.0	0.62	1.02	11	53.7	23.7	1007
2/20/2008	1606 Test I	End						
2/20/2008	1630	0.0	0.54	1.02	11	52.8	3 22.8	1008
2/21/2008	915	0.0	0.38	1.04	9.9	78.4	10.8	1005
2/22/2008	1041	2.6	0.32	0.72	4.8	83.8	9.7	1003

Optimization Te	est #2 (30 cfi								
2/25/2008	1845 Test \$	Start							
2/26/2008	653 Test E	nd							
2/26/2008	707	0.0	2.18	0.62	7.1	90.7		3.3	1017
2/27/2008	1535	0.6	1.14	0.42	4.3	39.4		35.6	1009
2/28/2008	1100	2.3	0.92	0.4	2.3	75.8		16.3	1007

Depth 18 **Phase II Piezometer Monitoring Data** Well ID P6 Well Well or Injection Gas Sample **Ambient Air**  $O_2$ CO<sub>2</sub> Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (mbar) (in wc) (Co) (ppm) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1435 4.4 0.36 0.72 0.66 55.7 24.1 1009 3/3/2008 1049 1.2 0.92 0.58 65.3 15.4 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 930 2.3 3/4/2008 0.68 3.7 69.9 12.7 1.02 1013 3/7/2008 1107 2.8 0.62 0.68 4.1 62.8 18.4 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1338 4.4 0.52 3.4 57 22.2 0.6 1016 1055 3/10/2008 7.9 0.54 0.64 0.22 71 16.6 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 0.59 63.5 1324 8.5 0.64 0.86 21.7 1016

Depth 18 **Phase II Piezometer Monitoring Data** Well ID P6 Well Well or Injection Gas Sample **Ambient Air**  $O_2$ CO<sub>2</sub> Propane  $H_2$ He RH **Pressure** Temperature Barometric pressure Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 5.0 3/21/2008 1014 0.0 0.26 2.0 77.2 12.5 1020 3/24/2008 1008 0.0 0.12 2.0 3.9 69.5 15.9 1012 3/26/2008 950 0.06 2.0 4.6 0.0 82.6 11.0 1017 0.04 2.0 2.6 3/28/2008 946 0.0 77.7 10.4 1009 948 0.0 15.0 10.0 80.9 3/31/2008 0.06 9.6 1013 1045 14.5 11.0 4/2/2008 0.0 0.06 78.6 14.5 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 929 4/4/2008 0.0 0.02 11.5 15.0 80.4 12.3 1013 15.0 4/7/2008 1356 1.1 0.00 5.5 68.5 18.8 1012 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 1046 2.0 0.00 2.0 22.0 80.5 14.4 1009

				Well or	Well	Ambient Air				
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Optimization Te	est #7C (50 o	cfh to P4-18	3, & P4-28 (	100 cfh tota	l); ~79% N2	2, 10% H2 & LPG, 1% (	CO2)	
	1121 Start						,	
4/11/2008	1224	0.2	0.00	0.2	14.0	65.2	21.6	1013
4/14/2008	1008	2.9	0.00	9.0	1.8	81.8	15.7	1007
4/16/2008	1019	0.0	0.84	9.0	9.5	76.8	15.0	1011
4/22/2008	1041	0.0	0.04	12.0	10.0	84.6	19.5	1009
4/23/2008	936	0.1	0.00	9.0	3.4	83.1	12.7	1010
4/25/2008	947	1.4	0.00	8.5	0.10	73.7	18.8	1015
4/29/2008	1059	0.0	0.08	9.0	7.3	57.7	25.5	1007
5/5/2008	1304	0.0	0.96	9.0	10.0	53.6	33.0	1001
5/13/2008	921	0.0	0.92	9.5	2.2	42.9	32.9	1007
5/20/2008	923	0.0	0.58	7.5	10.0	72.9	23.6	1004
5/23/2008	1508	0.0	0.72	7.0	22	56.4	31.6	990
5/27/2008	853	0.0	1.94	9.5	8.8	76.6	16.4	1007
6/4/2008	856	0.0	0.18	9.5	6.3	59.3	24.1	1002
6/12/2008	1138	0.0	0.66	9.5	3.9	39.0	39.4	1003
6/20/2008	1009	0.0	0.72	8.5	6.600	49.5	36.5	1006
6/25/2008	1035	0.0	1.02	9.0	13.0	56.7	31.2	1005
7/2/2008	1135	0.0	1.36	9.5	13.0	54.0	32.6	1004
7/7/2008	1125	0	0.16	9	7.1	48.6	35.5	998

Phase II Piezometer Monitoring Data Well

Well ID \_\_\_\_\_P6\_\_\_\_\_ Depth \_\_\_\_18\_\_\_\_

		Well or Injection Gas Sample							Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1052	0	0.08	9.5	10		76.6		24.9	
7/24/2008	1050	0.0	0.46	9.0	12.000		57.2		27.9	1005
7/31/2008	1048	0.0	1.12	9.5	11.000		61.3		26.7	1003
8/7/2008	923	0.0	0.16	9.0	9.4		70.5		24.2	1004
8/12/2008	1025	0.0	0.00	9.5	10.0		53.2		28.8	1002
Optimization Te	est #8 (100 c	ofh of 100%	Propane to	P4-18, & P	4-28 (50 cfl	n to each po	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1029	10.5	0.6	2.5	0.002					999
9/15/2008	913	11.0	0.66	2.5	0.005		57.8		24.7	1007
9/29/2008	932	12.7	0.96	2.5	0.005		57.8		22.1	1006
10/13/2008	1155	17.6	0.98	3.0	0.005		35.8		30.7	1017
10/20/2008	1122	16.0	1.36	2.0	0.005		50.8		25.8	1013
11/5/2008	1358	15.7	1.98	1.38	0.005		78.3		18.8	1016
11/17/2008	1111	13.4	2.36	2.0	0.005		49.1		28.7	1014
12/1/2008	1112	12.7	3.02	2.0	0.002		57.2		22.3	1014

Phase II Piezometer Monitoring Data	Well IDP6	Depth28
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				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1156	20.0	0.02	0	0.002	60,000	87.7	0.02	11.6	1020
12/12/2007	1537							0.22		
12/13/2007	903	9.8	0	0	7.8		77.2		7.1	1016
12/13/2007	959	11.3	0	0	8.3		68.8		12.2	1016
12/13/2007	1200	Discovered	l leak in O2	- all O2 data	for 12/13/0	7 before 12	00 invalid			
12/13/2007	1343	0	0	0	8.6		81.1		16.4	1013
12/13/2007	1507	0	0.48	0.52	0.46		87.4		13.9	1013
12/13/2007	1539	0	0.56	0.52	0.22		85.1		12.9	1013
12/14/2007	847	0	0.06	0	0.46		63.3	0.0	7.3	1016
12/21/2007	1211	15.3	0.12	0.02	0.46		91.7	0.04	10.3	1012
12/26/2007	1236	17.6	0.12	0	0.22		75.2	0.03	13.8	1016
12/27/2007	1025	0.1	0.04	0	9.5		80.2	0.04	6.1	1018
12/27/2007	1326	0.1	0	0	9.2		82.9		8.9	1016
12/27/2007	1447	0.1	0	0	9.5		86.1		8.5	1017
12/27/2007	1609	0.1	0	0	9.9		87.7	0.04	7.4	1017
1/2/2008	1042	0.1	0	0	0.022		66.3	0.02	16.1	1012
Tracer Test #1	Tracer Test #1 (10 cfm to INJ2, ~7% H2)									
1/21/2008	1046 Test	start								
1/21/2008	1212	1.3	0	0	2.7		82.1	0.05	10.1	1007

Phase II Piezometer Monitoring Data				Well ID	P6		Depth2	28		
				Well or	Injection G	as Sample	<del>)</del>		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	<b>Temperature</b>	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/21/2008	1313	1.2	0	0	4.6		81.9		9.6	1006
1/21/2008	1509	1.2	0	0	5.7		82.1		11.1	1006
1/22/2008	1002	1.1	0	0	7.0		84.0	0.09	6.8	1011
1/22/2008	1405	0.8	0	0	7.0		83.7		8.8	1009
1/23/2008	1026	1.0	0	0	6.9		86.5	0.08	8.1	1008
1/23/2008	1119*	0.6								
	!						<del>'</del>			
Tracer Test #2	2 (20 cfm to	INJ2, ~8% H	H2)							
1/18/2008	1120 Test s	start								
1/18/2008	1202	1.2	0	0	3.9		73.6		13.0	1015
1/18/2008	1305	0.8	0	0	6.2		67.0		14.8	1014
1/18/2008	1354	1.3	0	0	6.7		67.8		15.7	1014
1/18/2008	1533	0.9	0	0	7.2		48.1	0.03	23.2	1014
1/19/2008	1012	0.8	0	0	7.3		65.4	0.02	9.4	1019
1/19/2008	1146*	0.6	0	0	6.2		71.5		12.7	1018
Tracer Test #3	3 (30 cfm to	INJ2, ~4% l	H2)							
1/30/2008	1036 Test s	start								
1/30/2008	1112	0.0	0	0	3.3		88.6	0.10	9.8	1020
1/30/2008	1222	0.0	0	0	4.2		81.1		11.2	1019

Depth 28 **Phase II Piezometer Monitoring Data** Well ID P6 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Time (%) (%) (%) Date (%) (ppm) (%) (in wc) (C°) (mbar) 1/30/2008 0 0 13.3 1422 0.0 4.7 79.1 0.11 1018 1/31/2008 951 0 0.17 8.7 0.0 0 4.1 87.8 1019 1/31/2008 1131 0 0 0 3.8 84.6 9.5 1018 1/31/2008 0 1347 0 0 3.8 81.7 0.12 8.8 1016 1/31/2008 1435 1/31/2008 0 0 1515 0 3.9 85.5 0.04 8.2 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1303 0.2 0 0 5.1 91.6 10.5 1010 1/28/2008 0 0 13.2 0.0 6.0 79.9 0.20 1414 1011 1/28/2008 0 0.0 0 6.5 83.1 0.21 12.2 1011 1555 87.3 1/29/2008 800 0.0 0 7.3 0.11 4.8 1016 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1033 68.2 0 0 3.1 0 0.23 9.3 1019 2/5/2008 1131 0 0 0 3.4 72.0 11.0 1019

2/5/2008

1341

0

0

0

4.0

75.0

0.26

12.6

1019

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 28 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature (%) (%) (%) Date Time (%) (ppm) (%) (in wc) (C°) (mbar) 2/5/2008 15.2 1507 0 0 0 3.7 1019 77.4 0 1551 3.5 57.3 2/5/2008 0 0 18.9 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0 0.0 2/7/2008 1532 0 0.046 48.5 22.1 1016 1621 0.0 2/7/2008 0 0 2.3 50.7 20.9 1016 2/8/2008 1009 0.0 0 0 2.6 63.1 20.7 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1030 7.8 0 0 2.1 72.8 0.02 1015 8.3 5.3 0 1/17/2008 1143 0 3.6 77.0 9.9 1015 1/17/2008 1358 3.9 0.08 0 4.7 68.5 13.6 1013 2.7 0.08 0 1012 1/17/2008 1519 5.1 57.3 18.9 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1035 0.0 0 0 2.8 77.2 0.19 11.1 1020

2/6/2008

1147

0.0

0

0

3.8

74.6

1020

12.8

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P6\_\_\_\_ Depth \_\_\_28\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Pressure	Temperature	Barometric pressure		
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1244	0.0	0	0	4.0		71.2		14.3	1019
2/6/2008	1440	0.0	0	0	4.7		70.3	0.20	16.0	1017
2/6/2008	1536	0.0	0	0	4.6		62.8		17.6	1017

Optimization T	est #1 (90 c	fm to INJ2 t	for 4 hours t	hen shut do	wn; ~88% l	N2, 10% H2, 1% CO2 8	LPG)	
2/20/2008	1136	6.9	0.00	0	0.046	74.6	15.3	1010
2/20/2008	1206 Test s	start						
2/20/2008	1544	0.0	0.80	1.04	10	52.9	23.9	1007
2/20/2008	1606 Test I	∃nd						
2/20/2008	1631	0.0	0.68	1.06	9.6	52.7	22.7	1008
2/21/2008	917	1.5	0.28	0.88	9.1	76.2	10.8	1005
2/22/2008	1042	7	0.14	0.34	3.7	83	9.7	1003

Optimization T	est #2 (30 c	& LPG)							
2/25/2008	1845 Test S	Start							
2/26/2008	653 Test Er	nd							
2/26/2008	708	0.0	2	0.48	7.3	89.5		3.3	1017
2/27/2008	1537	6.3	0.6	0.28	3.2	36.3		36.4	1009
2/28/2008	1101	8.6	0.44	0.2	1.8	75.1		16.3	1007

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 28 **Well or Injection Gas Sample** Well **Ambient Air**  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure**  $O_2$ Date Time (%) (%) (%) (%) (mbar) (%) (in wc) (C<sub>0</sub>) (ppm) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 1436 8.6 0.30 0.22 0.98 1009 2/29/2008 64.6 24.4 3/3/2008 1051 9 0.32 0.28 2.3 66.8 15.6 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 931 3/4/2008 11.6 0.36 0.16 1.3 73.4 12.8 1013 3/7/2008 1108 11.7 0.18 0.14 1.1 63.8 18.4 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1339 9.4 0.2 1.02 2.1 60 22.2 1016 1056 0.18 3/10/2008 11.7 0.1 0.1 69.1 16.6 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) 3/10/2008 6.5 1326 1.4 0.72 7.3

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 28 Well **Well or Injection Gas Sample Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/21/2008 1015 7.5 0.10 2.5 1.4 78.7 12.5 1020 3/24/2008 1009 5.2 0.06 2.5 1.1 68.7 15.8 1012 2.5 3/26/2008 950 0.02 1.3 11.0 4.0 79.4 1017 947 3.8 0.02 2.0 0.98 76.2 3/28/2008 10.5 1009 3/31/2008 949 0.9 0.00 12.0 6.8 83.5 9.7 1013 1046 0.02 13.0 77.3 4/2/2008 0.4 6.1 14.7 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 930 12.0 4/4/2008 0.6 0.04 5.5 77.2 12.5 1013 1357 9.0 3.8 68.9 1012 4/7/2008 4.0 0.10 18.8 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 1049 6.2 0.04 7.0 1.6 79.0 14.5 1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P6\_\_\_\_ Depth \_\_\_28\_\_\_\_

				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

uic	Time	(70)	(70)	(70)	(70)	(ppiii)	(70)	(111 110)	(0)	(IIIbai)
ptimization T	est #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tota	al); ~79% N	2, 10% H2 8	LPG, 1% (	CO2)		
	1121 Start		·			·	·			
4/11/2008	1226	8.2	0.06	4.5	1.4		65.4		21.6	101
4/14/2008	1009	2.3	0.02	10.0	1.4		82.5		15.8	100
4/16/2008	1020	1.4	0.02	9.5	4.1		69.1		15.1	101
4/22/2008	1042	4.1	0.06	4.5	1.7		84.2		19.6	100
4/23/2008	937	2.2	0.00	6.5	0.60		83.2		12.6	101
4/25/2008	950	0.0	0.00	9.5	0.10		73.0		18.9	101
4/29/2008	1100	0.5	0.00	8.5	2.3		58.8		25.4	100
5/5/2008	1305	2.0	0.00	7.0	2.1		53.1		33.1	100
5/13/2008	924	0.0	0.00	10.0	1.3		41.4		33.3	100
5/20/2008	925	2.5	0.10	7.5	0.69		74.9		23.8	100
5/23/2008	1509	1.5	0.00	8.5	1.2		49.6		31.2	99
5/27/2008	855	1.4	0.16	8.0	2.9		75.9		16.4	100
6/4/2008	858	0.0	0.04	9.0	2.4		58.8		24.3	100
6/12/2008	1139	0.4	0.02	9.0	4.1		32.7		39.5	100
6/20/2008	1011	0.0	0.06	8.5	2.200		39.0		37.4	100
6/25/2008	1036	0.1	0.16	8.0	2.0		50.3		31.0	100
7/2/2008	1136	0.0	0.26	8.0	2.2		51.0		32.3	100
7/7/2008	1126	0	0.12	8.5	2		43.7		35.3	99

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P6\_\_\_\_ Depth \_\_\_28\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1053	0	0.38	8.5	2.2		80.8		25	
7/24/2008	1051	0.0	0.46	8.5	2.100		59.1		28.0	1005
7/31/2008	1149	0.0	0.42	8.5	2.500		59.6		26.7	1003
8/7/2008	924	0.0	0.40	8.5	2.3		70.1		25.1	1004
8/12/2008	1027	0.0	0.44	8.5	2.0		60.0		28.7	1002
Optimization T	6 Propane to	o P4-18, & F	P4-28 (50 cf	h to each p	oint)					
9/8/2008	0905 Test S	Start								
9/8/2008	1030	4.4	0.2	7	0.005					999
9/15/2008	915	4.2	0.2	30	0.005		58.2		24.9	1007
9/29/2008	933	4.6	0.10	30	0.005		59.3		22.2	1006
10/13/2008	1156	8.0	0.10	30	0.005		34.3		31.2	1017
10/20/2008	1123	5.8	0.12	30	0.005		45.9		26.1	1013
11/5/2008	1359	5.0	0.16	30	0.005		78.4		18.8	1016
11/17/2008	1112	4.2	0.18	30	0.005		49.7		28.6	1014
12/1/2008	1113	3.7	0.22	30	0.002		56.2		22.7	1014

Phase II Piezometer Monitoring Data	Well IDP6	Depth38
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				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1158	19.4	0.48	0	0.002	60,000	87.0	0.00	11.8	1020
12/12/2007	1536							0.24		
12/13/2007	906	10.8	0.08	0	0.46		79.4		7.2	1016
12/13/2007	1000	11.7	0	0	5.7		70.6		12.7	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	for 12/13/0	7 before 12	00 invalid			
12/13/2007	1344	0	0.12	0	8.6		76.1		16.2	1013
12/13/2007	1509	0	0.10	0.16	6.6		86.4		13.8	1013
12/13/2007	1540	0	0.08	0.38	2.6		84.3		13.1	1013
12/14/2007	849	0	0.02	0.16	0.87		65.9	0.06	7.5	1017
12/21/2007	1214	8.1	0.52	0.08	0.59		90.7	0.02	10.8	1012
12/26/2007	1238	13.3	0.56	0.04	0.22		76.1	0.03	13.3	1016
12/27/2007	1027	10.5	0.58	0.04	2.5		80.1	0.04	6.1	1018
12/27/2007	1329	9.7	0.46	0.04	3.2		84		9	1016
12/27/2007	1448	9.3	0.46	0.04	3.7		87.7		8.4	1017
12/27/2007	1611	8.9	0.48	0.04	4.1		88.1	0.02	7.3	1017
1/2/2008	1045	1.1	0.42	0	0.22		62.2	0.02	16.5	1012
Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)							
1/21/2008	1046 Test	start								
1/21/2008	1214	2.1	0.26	0	0.74		82.4	0.06	10.3	1007

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 38 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Time (%) (%) Date (%) (%) (ppm) (%) (in wc) (C°) (mbar) 1/21/2008 0 1314 2.1 0.30 0.79 82.9 9.7 1006 1510 2.1 0.28 0 81.3 1/21/2008 0.83 11.1 1006 1/22/2008 1003 1.9 0.28 0 4.0 82.1 0.07 6.7 1011 1/22/2008 0 1009 1406 1.7 0.24 4.4 83.8 8.7 1.7 0.28 1/23/2008 1027 0 5.2 85.8 8.1 1008 0.06 1/23/2008 1120\* 1.1 Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 1/18/2008 1205 1.9 0.34 0 12.9 0.85 71.5 1015 1/18/2008 0.30 0 65.2 1307 1.7 0.81 14.8 1014 1/18/2008 15.2 2.1 0.30 0 0.90 1356 67.1 1014 0.28 0 1/18/2008 1534 1.9 1.6 48.2 0.04 23.5 1014 1/19/2008 1014 1.4 0.34 0 9.2 62.3 0.01 9.4 1019 1/19/2008 1148\* 0.32 0 9.2 12.7 1018 8.0 71.8 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1114 0.0 0.04 0 1.8 90.5 0.10 9.7 1020 1/30/2008 1224 0.0 0.02 0 1.6 81.8 11.2 1019

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 38 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Time (%) (%) (%) Date (%) (ppm) (%) (in wc) (C°) (mbar) 1/30/2008 0 13.5 1423 0.0 0.02 2.6 76.2 0.10 1018 1/31/2008 0 4.3 86.0 8.7 952 0.0 0 0.11 1019 1/31/2008 1132 0 0 0 3.9 83.3 9.5 1018 1/31/2008 0 1348 0 0 3.8 79.4 0.11 8.8 1016 1/31/2008 1435 1/31/2008 0 1516 0 0.02 3.8 83.6 0.05 8.2 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1304 4.1 0.28 0 0.22 90.8 10.5 1010 1/28/2008 0.26 0 1.6 0.26 12.9 1415 4.4 81.1 1011 1/28/2008 0 12.3 0.16 4.8 81.5 1556 1.0 0.18 1011 1/29/2008 801 0.0 0.06 7.4 85.4 0.07 7.8 1016 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1035 3.3 0 0 0.10 68.0 0.20 9.4 1019 2/5/2008 1132 1.8 0 0 1.2 70.0 11.0 1019 2/5/2008 1342 0.1 0 0 3.7 75.5 0.22 12.6 1019

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 38 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature Time (%) (%) (%) Date (%) (ppm) (%) (in wc) (C°) (mbar) 2/5/2008 1508 0 0 0 3.6 16.3 1019 75.4 0 2/5/2008 1552 3.5 59.5 19.0 0 0 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0 0.0 2/7/2008 1533 0.04 0.046 51.2 22.0 1016 1621 0.04 0 2/7/2008 0.46 51.7 20.9 1016 0.0 2/8/2008 1015 0.0 0.02 0 6.5 66.8 10.1 1017 0.0 0 0 6.3 2/8/2008 1059 76.2 11.1 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1031 0 1/17/2008 14.2 0.30 0.22 72.4 0.02 8.4 1015 1/17/2008 1144 12.6 0.28 0 0.22 75.1 9.9 1015 1/17/2008 0.46 0 1359 7.7 3.0 68.2 13.7 1013 1/17/2008 1521 0 1012 4.5 0.48 4.2 55.7 19.2 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start

2/6/2008

1037

0.0

0

0

0.86

0.18

11.1

77.4

1020

Phase II Piezometer Monitoring Data	Well IDP6	Depth38
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	Thase in reconnecter informering Data Well is Depth												
					Injection G				Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			
2/6/2008	1148	0.0	0	0	0.77		74.3		12.8	1020			
2/6/2008	1246	0.0	0	0	1.8		72.3		14.4	1019			
2/6/2008	1442	0.0	0	0	3.8		74.4	0.16	16.2	1017			
2/6/2008	1538	0.0	0	0	3.9		62.2		17.5	1017			
2/6/2008	1627	0.0	0.02	0	4.0		62.6		17.9	1017			
Optimization T	est #1 (90 c	fm to INJ2 f	or 4 hours t	hen shut do	wn; ~88% N	N2, 10% H2	, 1% CO2 &	LPG)					
2/20/2008	1137	6.5	0.12	0	0.046		73.8		15.3	1010			
2/20/2008	1206 Test s	start											
2/20/2008	1545	0.5	0.04	0.94	11		52.3		24.4	1008			
2/20/2008	1606 Test E	nd											
2/20/2008	1632	0.4	0.02	0.96	11		51.8		22.7	1008			
2/21/2008	918	3.0	0.08	0.44	6		74.3		10.9	1004			
2/22/2008	1044	4.2	0.10	0.26	3.2		82.7		9.9	1003			
Optimization T	est #2 (30 c	fm to INJ2 f	or 12 hours	then shut d	own; ~88%	N2, 10% H	2, 1% CO2	& LPG)					
2/25/2008	1845 Test S	Start											
2/26/2008	653 Test Er	nd											
2/26/2008	710	1.0	0.32	0.7	6.2		88.7		3.4	1017			
2/27/2008	1538	4.7	0.16	0.28	2.5		36.9		37.1	1009			
2/28/2008	1102	5.5	0.12	0.24	1.6		74.9		16.4	1007			

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 38 Well **Well or Injection Gas Sample Ambient Air**  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure**  $O_2$ Date Time (%) (%) (%) (%) (%) (C°) (mbar) (in wc) (ppm) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1437 6.4 0.06 0.24 0.82 1009 71.8 24.7 3/3/2008 1052 8.1 0.14 0.046 63.8 0.14 15.6 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 933 3/4/2008 8.7 0.22 0.12 0.022 71.9 12.9 1013 3/7/2008 1109 10.1 0.12 0.1 0.022 65.9 18.5 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1341 10 0.1 0.022 64.2 22.3 0.1 1016 1057 0.22 0.08 3/10/2008 10.8 0.022 68.9 16.6 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow)

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 38 Well **Well or Injection Gas Sample Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure** Date Time (%) (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 3/21/2008 1017 9.4 0.24 1.0 0.022 81.1 12.6 1020 3/24/2008 1010 8.7 0.34 1.78 0.022 69.5 15.8 1012 2.0 3/26/2008 952 8.2 0.34 0.022 80.3 11.0 1017 948 8.1 0.36 2.0 0.022 74.0 3/28/2008 10.5 1009 3/31/2008 950 6.5 0.30 2.5 1.2 84.7 9.8 1013 1047 0.30 3.5 1.3 4/2/2008 6.2 76.5 14.9 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 932 8.0 4/4/2008 4.1 0.32 1.2 80.2 12.6 1013 1358 9.0 0.72 1011 4/7/2008 3.1 0.34 68.9 18.7 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 1051 3.1 0.28 8.5 0.1 84.7 14.6 1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P6\_\_\_\_ Depth \_\_\_\_38\_\_\_

				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
-										

timization T	est #7C (50	cfh to P4-1	8 & P4-28 (	100 cfh tota	al)· ~79% N	2, 10% H2 & LPG, 1%	CO2)	
	1121 Start		0, 41 120 (	TOO OIII TOTA	707014	2, 1070112 & 21 3, 170		
4/11/2008	1227	2.8	0.36	9.0	0.1	68.6	21.6	10
4/14/2008	1011	3.2	0.38	8.0	0.046	79.8	15.7	10
4/16/2008	1021	3.1	0.38	7.5	0.1	67.6	15.2	10
4/22/2008	1044	2.6	0.42	6.5	0.022	81.4	19.9	10
4/23/2008	938	2.6	0.42	6.5	0.010	85.6	12.6	10
4/25/2008	951	2.2	0.34	6.5	0.10	78.3	19.5	1
4/29/2008	1102	2.1	0.42	7.0	0.046	63.5	25.2	1
5/5/2008	1306	1.5	0.44	7.0	0.1	64.8	33.1	1
5/13/2008	925	1.3	0.52	7.0	0.046	40.6	33.7	1
5/20/2008	926	0.8	0.60	7.5	0.046	69.0	23.3	1
5/23/2008	1511	0.7	0.44	7.5	0.10	51.0	31.0	!
5/27/2008	856	0.8	0.68	8.0	0.022	70.3	16.4	1
6/4/2008	859	1.1	0.64	7.5	0.046	53.8	24.2	1
6/12/2008	1140	0.5	0.60	8.0	0.046	28.5	39.4	1
6/20/2008	1012	0.0	0.58	8.0	0.10	33.2	38.0	1
6/25/2008	1037	0.0	0.56	8.0	0.10	46.2	31.1	1
7/2/2008	1137	0.0	0.56	8.0	0.10	48.1	32.0	1
7/7/2008	1127	0	0.5	8	0.1	43	35.3	9

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P6\_\_\_\_ Depth \_\_\_\_38\_\_\_

				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1054	0	0.6	8	0.1		80.4		25.3	
7/24/2008	1052	0.0	0.60	8.0	0.100		59.9		28.2	1005
7/31/2008	1050	0.0	0.64	8.0	0.100		60.4		26.7	1003
8/7/2008	926	0.0	0.62	8.0	0.10		60.6		26.4	1004
8/12/2008	1028	0.0	0.64	8.0	0.10		56.6		28.6	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane to	o P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test S	Start								
9/8/2008	1032	0.7	0.7	10.5	0.022					999
9/15/2008	916	1.6	1.1	30	0.022		50.9		25.0	1007
9/29/2008	934	0.4	0.60	30	0.022		55.4		22.6	1006
10/13/2008	1157	1.0	0.44	30	0.022		31.4		31.4	1017
10/20/2008	1124	0.6	0.46	30	0.022		47.4		26.1	1013
11/5/2008	1400	0.4	0.48	30	0.022		77.9		18.7	1016
11/17/2008	1113	0.3	0.46	30	0.046		52.1		28.3	1014
12/1/2008	1114	0.1	0.44	30	0.022		53.5		23.2	1014

Phase II Piezometer Monitoring Data	Well ID	P6	Depth	_48
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				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	$H_2$	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1200	20.8	0.00	0	0.002	80,000		0.02	11.9	1020
12/12/2007	1536							0.10		
12/13/2007	907	20.7	0	0	0.22		75.0		7.4	1016
12/13/2007	1002	19.1	0	0	0.22		63.6		13.2	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	7 before 12	00 invalid			
12/13/2007	1345	9.4	0.62	0	1.4		69.2		16.0	1013
12/13/2007	1510	6.7	0.64	0	2.8		78.9		13.9	1013
12/13/2007	1542	5.8	0.66	0	3.4		78.4		13.2	1013
12/14/2007	850	20.7	0.04	0	0.5		61.0	0.04	7.6	1017
12/21/2007	1216	20.9	0	0	0.22		87.7	0.02	11.3	1012
12/26/2007	1240	20.9	0	0	0.22		72.3	0.02	13.2	1016
12/27/2007	1030	20.9	0	0	0.22		79.2	0.03	6	1018
12/27/2007	1331	20.9	0	0	0.22		82.5		9.1	1016
12/27/2007	1450	20.9	0	0	0.22		88.7		8.3	1017
12/27/2007	1614	20.9	0	0	0.22		88.8	0.03	7.3	1017
1/2/2008	1047	20.9	0.02	0	0.22		50.7	0.03	16.5	1012
Tracer Test #1	(10 cfm to	INJ2, ~7% I	H2)							
1/21/2008	1046 Test s	start								
1/21/2008	1215	9.9	0.52	0	0.81		79.0	0.06	10.3	1007

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 48 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Time (%) (%) Date (%) (%) (ppm) (%) (C°) (mbar) (in wc) 1/21/2008 0 1316 9.7 0.50 0.81 83.4 10.6 1006 1511 0.52 0 0.74 1/21/2008 9.7 80.0 11.1 1006 1/22/2008 1005 20.9 0.04 0 0.022 84.0 0.06 6.7 1011 1/22/2008 0 0 1009 1410 20.9 0.022 84.2 8.8 0 1/23/2008 1029 20.9 0.04 0.022 85.2 0.03 8.0 1008 1/23/2008 1127\* 20.9 Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 1/18/2008 1206 9.9 0.54 0 0.92 12.9 74.7 1015 1/18/2008 0 67.3 14.9 1308 9.5 0.54 0.98 1014 1/18/2008 15.8 9.5 0.54 0 1.0 1358 68.6 1014 0 46.1 1/18/2008 1535 9.1 0.54 1.1 0.04 23.7 1014 20.7\*\* 1/19/2008 1015 0.08 0 0.022 70.5 0.01 9.7 1019 1/19/2008 1149\* 20.2 0.08 0 72.2 0.046 12.6 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1115 5.3 0.42 0 2.0 91.1 0.03 9.7 1020 1/30/2008 1225 4.3 0.48 0 2.0 82.3 11.2 1019

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 48 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ **Propane**  $H_2$ He RH **Pressure** Temperature Time (%) (%) Date (%) (%) (ppm) (%) (in wc) (C°) (mbar) 1/30/2008 0 13.7 1426 3.4 0.56 2.2 71.6 0.06 1018 0.80 0 86.7 8.9 1/31/2008 954 0.9 1.9 0.05 1019 1/31/2008 1133 8.0 0.82 0 1.7 85.0 9.6 1018 1/31/2008 1345 0.7 0.80 0 1.7 80.2 0.06 8.8 1016 1/31/2008 1435 1/31/2008 0.82 0 1517 4.1 0.88 84.2 0.03 8.3 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1306 16.0 0.26 0 0.022 91.3 10.6 1010 1/28/2008 1417 0 12.6 0.50 0.022 81.1 12.7 0.15 1011 1/28/2008 0.56 0 0.022 77.8 0.07 12.1 1559 10.3 1011 3.2 0.94 1/29/2008 803 0.02 3.4 86.3 0.04 4.9 1016 1/29/2008 1014\* 2.8 0.98 3.6 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1037 0 14.6 0.10 0.010 68.2 0.06 9.6 1019

0

0

0.022

0.022

72.7

78.0

0.10

2/5/2008

2/5/2008

1133

1343

9.2

5.2

0.20

0.36

1019

1019

11.0

12.7

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 48 Well **Ambient Air Well or Injection Gas Sample Barometric pressure**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature (%) Date Time (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) 2/5/2008 0 1509 0.046 62.1 18.3 1019 4.3 0.46 0 1553 18.9 2/5/2008 3.8 0.48 0.046 57.4 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0 2/7/2008 1534 1.1 0.54 1.0 53.3 22.0 1016 1621 0.52 0 0.90 52.6 20.7 1016 2/7/2008 1.1 2/8/2008 1016 17.5 0.40 0 0.022 67.1 10.1 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1034 17.1 0.08 0 0.022 69.9 0.02 8.4 1016 0 1/17/2008 1146 15.9 0.20 0.22 75.0 9.9 1015 1/17/2008 1401 15.1 0.50 0 0.22 69.0 13.6 1013 0.60 0 0.22 1/17/2008 1523 14.5 52.0 19.8 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1039 3.5 0.40 0 0.10 78.3 0.06 11.1 1020

2/6/2008

1150

2.7

0.42

0

0.10

75.7

1020

12.9

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P6\_\_\_\_ Depth \_\_\_\_48\_\_\_

2/28/2008

1103

20.6

0

0

0.022

76.4

16.4

				Well or	<b>Injection G</b>	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1247	2.3	0.44	0	0.046		73		14.4	1019
2/6/2008	1443	1.6	0.44	0	0.22		71.1	0.08	16.3	1017
2/6/2008	1539	1.4	0.44	0	0.61		60.8		18.8	1017
2/6/2008	1630	1.2	0.56	0	0.78		59.6		18.3	1017
Optimization T	est #1 (90 c	fm to INJ2 f	or 4 hours t	hen shut do	wn; ~88% <b>N</b>	N2, 10% H2	, 1% CO2 &	LPG)		
2/20/2008	1139	20.9	0.04	0	0.022		75.8		15.3	1010
2/20/2008	1206 Test s	tart								
2/20/2008	1547	8.7	0.36	0	0.01		49.2		24.6	1008
2/20/2008	1606 Test E	nd								
2/20/2008	1634	9.9	0.32	0	0.022		50.4		22.7	1008
2/21/2008	919	20.9	0.00	0	0.01		73.2		10.9	1005
2/22/2008	1045	20.9	0.00	0	0.022		82		10	1003
Optimization T	est #2 (30 c	fm to INJ2 f	or 12 hours	then shut d	own; ~88%	N2, 10% H	2, 1% CO2	& LPG)		
2/25/2008	1845 Test S	Start								
2/26/2008	653 Test Er	nd								
2/26/2008	711	11.6	0.48	0.1	0.01		88		3.4	1017
2/27/2008	1539	19.6	0.04	0	0.022		35.2		37.7	1009

1007

Phase II Piezo	ometer Mon	itoring Dat	ta	Well ID	P6		Depth	48		
				Well or	Injection G	as Sample	<b>;</b>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
									_	
Optimization 1	est #3A (1 d	ofm to INJ2;	~88% N2,	10% H2, 1%	CO2 & LP	G)				
2/29/2008	1319 Test \$	Start								
2/29/2008	1439	18.9	0.00	0	0.022		71.3		25.3	1009
3/3/2008	1053	20.7	0	0	0.022		64.4		15.7	1019
3/3/2008	1130 Test I	End								
	!		!			!				
Optimization T	est #3B (1 d	ofm to INJ1,	INJ2 & INJ	3; ~88% N2	, 10% H2, 1	% CO2 & L	PG)			
3/3/2008	1130 Test \$	Start								
3/4/2008	934	20.9	0	0	0.01		71.1		13	1013
3/7/2008	1110	20.1	0	0	0.005		64.6		18.5	1018
3/7/2008	1306 Test I	End								
Optimization 1	est #3C (90	cfm to INJ	1, INJ2 & IN	J3 for 15 mi	nutes then	shut down;	~79% N2, 10	0% H2 & LPG	, 1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/10/2008	1059	20.2	0	0	0.005		68		16.7	1016
Optimization T	est #4 ( 2, 4	5-minutes	oulses; daily	15-minutes	pulses w/3	Ocfh consta	ant flow)			

**Phase II Piezometer Monitoring Data** Well ID P6 Depth 48 Well **Well or Injection Gas Sample Ambient Air**  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure**  $O_2$ Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 0.022 3/24/2008 1011 14.2 0.40 0.06 68.1 15.8 1012 3/26/2008 953 12.2 0.50 0.16 0.010 82.2 11.0 1017 3/28/2008 949 0.46 14.7 0.1 0.01 72.1 10.5 1009 3/31/2008 951 0.54 0.46 0.022 84.6 9.9 11.9 1013 4/2/2008 1049 10.0 0.60 1.02 0.022 78.5 15.2 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 9.3 1.30 934 0.62 0.022 72.7 12.7 1013 1359 9.2 2.0 0.74 73.5 4/7/2008 0.022 18.6 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 1053 6.9 0.72 5.0 0.022 82.0 14.8 1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P6\_\_\_\_ Depth \_\_\_\_48\_\_\_

				Well or	Well	Ambient Air				
		O <sub>2</sub>	Pressure	Temperature	Barometric pressure					
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
		•								
0.0	T+ 1170 /F/	200)								

			. ,	. ,				
Optimization T	est #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tota	al); ~79% N	2, 10% H2 & LPG, 1%	CO2)	
4/10/2009	1121 Start <sup>-</sup>	Test						
4/11/2008	1228	5.3	0.88	6.5	0.1	70.2	21.7	1013
4/14/2008	1013	5.7	0.92	6.5	0.046	77.0	15.8	1007
4/16/2008	1023	5.8	0.96	5.5	0.046	71.4	15.3	1011
4/22/2008	1045	6.6	0.92	5.0	0.046	81.9	19.9	1009
4/23/2008	940	5.0	0.98	6.5	0.010	88.7	12.6	1010
4/25/2008	952	3.9	0.82	7.5	0.046	69.9	20.5	1015
4/29/2008	1103	3.7	0.94	7.5	0.046	60.9	25.1	1007
5/5/2008	1307	3.5	0.98	7.0	0.046	57.4	. 33.2	1001
5/13/2008	926	2.8	1.04	7.5	0.046	35.0	34.0	1007
5/20/2008	927	2.7	1.24	7.0	0.046	71.3	23.1	1004
5/23/2008	1512	2.6	1.02	7.0	0.046	47.6	30.8	990
5/27/2008	859	1.8	1.32	7.5	0.046	71.0	16.6	1007
6/4/2008	900	1.7	1.30	7.5	0.046	57.2	24.2	1002
6/12/2008	1144	1.5	1.16	7.0	0.022	30.9	39.5	1003
6/20/2008	1014	1.0	1.20	7.0	0.022	37.4	38.6	1006
6/25/2008	1038	0.9	1.22	7.0	0.10	46.7	31.2	1005
7/2/2008	1139	0.7	1.26	7.0	0.10	55.2	31.9	1004
7/7/2008	1129	0.5	1.16	7	0.046	46.7	35.7	998

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P6\_\_\_\_ Depth \_\_\_\_\_48\_\_\_

				Well or	Injection G	as Sample	!		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1056	0.2	1.32	7	0.046		89.8		25.4	
7/24/2008	1053	0.2	1.30	7.0	0.100		60.0		28.2	1005
7/31/2008	1052	0.1	1.36	7.0	0.046		68.4		26.7	1003
8/7/2008	927	0.0	1.38	7.0	0.10		60.1		27.1	1004
8/12/2008	1029	0.0	1.30	7.0	0.10		57.1		28.5	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane to	P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test S	Start								
9/8/2008	1034	0.0	1.12	16.5	0.022					999
9/15/2008	917	0.8	1.3	30	0.022		49.1		25.2	1007
9/29/2008	936	0.1	1.18	30	0.022		52.8		23.2	1006
10/13/2008	1158	0.2	1.04	30	0.022		32.6		31.5	1017
10/20/2008	1126	0.2	1.08	30	0.010		50.6		25.8	1013
11/5/2008	1401	0.0	1.00	30	0.022		77.9		18.6	1016
11/17/2008	1114	0.0	0.88	30	0.022		54.2		28.1	1014
12/1/2008	1114	0.0	0.82	30	0.010		52.3		23.5	1014

Phase II Piezometer Monitoring Data	Well IDP7	Depth28
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				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1109	20.5	0.00	0	0.002	<100	81.7	0.01	10.2	1021
12/12/2007	1540							0.11		
12/13/2007	1025	13.3	0	0	7.9		65.5		12.7	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 1	200 invalid			
12/13/2007	1348	0	0	0	8.6		72.7		15.9	1013
12/14/2007	854	0	0	0.04	0.5		65.6	0.02	7.0	1017
12/21/2007	1228	18.0	0.02	0	0.46		80.3	0.04	10.7	1012
12/26/2007	1243	18.6	0	0	0.022		76.4	0.04	12	1016
12/27/2007	1043	5.7	0.06	0	6.5		80.8	0.04	5.5	1018
12/27/2007	1333	4.6	0	0	7		78.7		9.2	1016
12/27/2007	1454	3.7	0	0	7.5		84.6	0.04	8.4	1017
1/2/2008	1050	0.2	0	0	0.22		53.1	0.04	16.4	10.2

Tracer Test #1 (	10 cfm to IN	IJ2, ~7% H2	2)						
1/21/2008	1046 Test :	start							
1/21/2008	1219	2.6	0	0	0.046	73.8	0.04	10.4	1007
1/21/2008	1318	2.6	0	0	1.3	80.2		10.4	1006
1/21/2008	1517	2.4	0	0	4.5	75.8		10.9	1006
1/22/2008	1022	2.2	0	0	6.9	83.8	0.06	6.2	1011
1/22/2008	1416	1.8	0	0	7.0	82.8		8.6	1009

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P7\_\_\_\_ Depth 28 Well or Injection Gas Sample **Ambient Air** Well  $O_2$ CO2 Propane  $H_2$ He RH **Pressure Temperature Barometric pressure** (%) (%) Date Time (%) (%) (%) (C°) (mbar) (in wc) (ppm) 1/23/2008 0 1008 1031 2.1 0 6.9 86.4 0.06 7.9 1/23/2008 1128\* 0.7 Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 2.3 1/18/2008 1212 0 0.046 69.0 13.2 1015 1257 2.1 14.2 1/18/2008 0 2.1 63.4 1014 1/18/2008 1359 2.5 0 0 3.9 66.2 15.8 1014 1537 2.1 0 6.4 0.02 23.9 1/18/2008 45.8 1014 1/18/2008 1626 2.3 0 6.9 0 63.8 16.4 1014 1/18/2008 1633\* 8.0 0 7.1 65.4 15.9 1014 1/18/2008 1639\*\* 2.3 0 0 7.1 15.0 72.4 1014 2.0 9.4 1/19/2008 1023 0 0 67.3 0.01 9.7 1019 1/19/2008 1153\* 0.6 0 7.9 96.0 14.1 1017 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start

0

0

0

0

0.57

2.4

4.4

89.2

81.5

75.5

0.0

0.0

0.0

1118

1227

1428

1/30/2008

1/30/2008

1/30/2008

1018	

9.7

11.1

13.8

0.06

0.09

1020

1019

Well ID \_\_\_\_P7\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth 28 Well or Injection Gas Sample **Ambient Air** Well  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure Temperature Barometric pressure** Time (%) (%) Date (%) (%) (%) (C°) (mbar) (in wc) (ppm) 1/31/2008 955 0.0 0 4.2 85.3 0.10 8.9 1019 9.5 1134 0 1/31/2008 0 0 3.8 83.2 1018 1/31/2008 1353 0 0 3.7 82.9 0.08 8.8 1016 1/31/2008 1435 1/31/2008 1519 0 0 0 3.7 85.0 0.03 8.3 1014 0 8.2 0 0 3.8 83.7 1/31/2008 1614 1013 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1322 2.4 0 2.6 91.1 10.3 1010 1/28/2008 1419 0.5 0.13 0 5.0 82.8 12.5 1011 1601 0.1 0 0 6.1 0.11 11.6 1/28/2008 76.8 1012 0.0 4.9 1/29/2008 805 0 7.3 84.0 0.05 1016 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1039 1.2 9.8 2/5/2008 63.2 1019 0 1.0 0.11 11.0 2/5/2008 1135 0.1 0 0 2.6 68.4 1019 2/5/2008 1345 0 0 3.8 77.4 0.12 12.6 1018

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P7\_\_\_\_ Depth 28 Well or Injection Gas Sample Well **Ambient Air**  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Temperature **Barometric pressure** (%) (%) (%) Date Time (%) (%) (C°) (mbar) (in wc) (ppm) 2/5/2008 1511 0 0 3.6 1019 64.3 19.3 1554 2/5/2008 0 0 0 3.4 60.8 19.0 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0.0 2/7/2008 1536 0 0.046 58.8 21.8 1016 1624 0.0 20.6 2/7/2008 0 0.10 56.6 1016 2/8/2008 1018 0.0 0 0 8.4 69.1 10.0 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1038 11.3 0 0 1.5 67.8 0.02 8.5 1/17/2008 1015 4.0 1/17/2008 1404 0 0 4.9 63.8 13.7 1013 1/17/2008 1535 3.2 0 5.5 48.5 18.8 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 1041 0.0 2/6/2008 0 0 0.61 76.9 0.15 11.1 1020 2/6/2008 1152 0.0 0 0 3.0 73.1 13.0 1020 2/6/2008 1249 0.0 0 3.8 72.7 14.5 1019

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				Well or	Well	Ambient Air				
		02	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1445	0.0	0	0	4.4		72.6	0.06	16.3	1017
2/6/2008	1541	0.0	0	0	4.4		62.6		19.5	1017

Optimization Tes	st #1 (90 cfr	n to INJ2 fo	r 4 hours the	en shut dow	/n; ~88% N	2, 10% H2, 1% CO2 &	LPG)	
2/20/2008	1140	9.5	0.00	0	0.046	75.7	15.3	1010
2/20/2008	1206 Test :	start						
2/20/2008	1552	0.0	0.20	1.02	11	50.2	24.4	1007
2/20/2008	1606 Test	End						
2/20/2008	1635	0.0	0.12	1.02	10	52.8	22.3	1008
2/21/2008	929	7.4	0.08	0.4	3.9	74.6	10.4	1005
2/22/2008	1046	10.2	0.00	0.18	1.5	83.2	10.1	1003

Optimization Tes	st #2 (30 cfr								
2/25/2008	1845 Test	Start							
2/26/2008	653 Test E	nd							
2/26/2008	713	0.1	0.76	0.62	7.2	89.2		3.6	1017
2/27/2008	1541	9.3	0.2	0.18	1	35.9		38.2	1009
2/28/2008	1105	10.5	0.02	0.14	0.1	73.5		16.4	1007

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P7\_\_\_\_ Depth 28 Well or Injection Gas Sample Well **Ambient Air** CO<sub>2</sub>  $O_2$ Propane H<sub>2</sub> He RH **Pressure** Temperature **Barometric pressure** Time Date (%) (%) (%) (%) (C°) (mbar) (%) (in wc) (ppm) Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 1440 11 0.046 69.3 26.2 2/29/2008 0.00 0.14 1009 3/3/2008 1055 11.3 0.046 60.7 0.04 0.18 15.7 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 935 12.3 65.6 0.022 0.04 0.16 13.1 1013 0.022 3/7/2008 1112 11.4 0.18 66.3 18.5 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1342 11.1 0.18 0.01 66.4 22.3 1016 1101 11.7 3/10/2008 0.06 0.2 0.022 71.3 16.8 1016 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow)

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_P7\_\_\_\_ Depth 28 Well or Injection Gas Sample Well **Ambient Air**  $O_2$  $CO_2$ Propane  $H_2$ He RH **Pressure** Temperature **Barometric pressure** Date Time (%) (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 7.2 3/21/2008 1018 0.00 3.0 0.046 80.9 12.7 1020 3/24/2008 1013 6.7 0.00 2.5 0.046 70.4 15.8 1012 5.9 954 2.0 0.022 11.0 1017 3/26/2008 0.00 80.1 10.5 951 6.6 2.0 0.022 68.9 3/28/2008 0.04 1009 10.0 952 0.3 13.5 6.7 79.6 3/31/2008 0.00 1013 1051 0.1 6.0 4/2/2008 0.00 14.0 73.6 15.4 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 936 0.2 4/4/2008 0.00 13.0 5.7 72.7 12.8 1013 7.5 2.0 4/7/2008 1405 0.06 6.5 89.0 18.7 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 8.9 4/9/2008 1057 0.00 4.5 1.0 83.6 15.0 1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

7/24/2008

1055

0.0

0.46

8.5

1.400

56.8

		•					•			
				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Te	st #7C (50 c	fh to P4-18	, & P4-28 (1	00 cfh total	); ~79% N2	, 10% H2 &	LPG, 1% C	O2)		
4/10/2009	1121 Start	Test								
4/11/2008	1230	10.9	0.02	3.0	0.1		70.7		21.8	1013
4/16/2008	1024	2.3	0.00	8.5	2.3		60.3		15.4	1011
4/22/2008	1047	4.3	0.06	4.0	0.10		87.9		20.1	1009
4/25/2008	955	1.8	0.02	7.5	0.046		66.2		21.3	1015
4/29/2008	1105	0.9	0.00	8.0	1.0		63.6		24.6	1007
5/5/2008	1309	1.5	0.02	7.5	0.82		56.5		33.2	1001
5/13/2008	928	0.1	0.08	9.0	0.83		32.3		34.3	1007
5/20/2008	928	5.8	0.14	5.0	0.046		58.1		22.8	1004
5/23/2008	1514	4.0	0.10	7.0	0.046		41.6		30.7	990
5/27/2008	900	1.1	0.20	8.5	1.4		56.0		16.5	1007
6/4/2008	902	0.1	0.16	9.5	1.5		45.0		24.7	1002
6/12/2008	1147	1.1	0.24	8.5	0.22		44.6		40.0	1003
6/20/2008	1017	0.2	0.26	8.5	0.96		32.9		39.2	1006
6/25/2008	1040	0.4	0.26	8.5	1.1		42.1		30.9	1005
7/2/2008	1140	0.3	0.40	8.5	1.2		51.1		31.4	1004
7/7/2008	1130	0.1	0.36	8.5	0.8		50.3		35.8	998
7/18/2008	1057	0	0.44	8.5	1.2		89.8		25.5	

1005

28.3

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

	Ī			Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/31/2008	1053	0.0	0.46	8.5	1.500		61.0		26.7	1003
8/7/2008	929	0.0	0.44	9.0	1.4		50.2		26.4	1004
8/12/2008	1031	0.0	0.46	9.0	1.2		55.1		28.4	1002
Optimization Tes	st #8 (100 cf	fh of 100% I	Propane to	P4-18, & P4	1-28 (50 cfh	to each po	int)			
9/8/2008	9/8/2008 0905 Test Start									
9/8/2008	1038	5.6	0.78	4.5	0.005					999
9/15/2008	919	3.2	0.94	9.5	0.010		36.2		25.6	1007
9/29/2008	938	5.1	1.70	19.5	0.005		42.3		23.9	1006
10/13/2008	1200	8.8	2.18	16.0	0.010		25.3		31.8	1017
10/20/2008	1127	6.2	3.00	21.5	0.010		46.6		25.6	1013
11/5/2008	1403	5.9	4.82	20.5	0.010		75.9		18.7	1016
11/17/2008	1116	5.0	5.00	25.5	0.010		54.1		28.2	1014
12/1/2008	1116	4.3	5.00	24.5	0.005		52.7		23.9	1014

Phase II Piezometer Monitoring Data	Well IDP7	Depth38
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				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1117	20.6	0.22	0	0.002	3,000	86.8	0.02	10.2	1020
12/12/2007	1540							0.11		
12/13/2007	1021	13.3		0	8.2		62.7		12.7	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 dat	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1349	0	0	0	8.6		73.9		15.6	1013
12/14/2007	855	0	0.22	0	0.50		67.4	0.01	6.9	1016
12/21/2007	1229	18.6	0.34	0	0.46		83.8	0.04	10.5	1012
12/26/2007	1246	19	0.34	0	0.022		83.3	0.02	11.6	1016
12/27/2007	1044	12.4	0.44	0	3.6		82.8	0.04	5.7	1018
12/27/2007	1335	9.9	0.32	0	4.6		81.9		9.1	1016
12/27/2007	1456	9.2	0.32	0	4.9		86.1	0.03	8.4	1017
1/2/2008	1058	0.3	0.04	0	0.22		57.9	0.04	15	1012

Tracer Test #	±1 (10 cfm to	o INJ2, ~7%	H2)						
1/21/2008	08 1046 Test start								
1/21/2008	1220	2.5	0	0	0.10	72.4	0.04	10.4	1007
1/21/2008	1321	2.5	0.02	0	1.7	78.3		10.7	1006
1/21/2008	1519	2.4	0	0	4.0	73.1		10.8	1006
1/22/2008	1023	2.2	0.04	0	6.3	79.1	0.06	6.2	1011
1/22/2008	1417	1.9	0	0	6.4	79.4		8.6	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Temperature	Barometric pressure				
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/23/2008	1033	2.2	0.04	0	6.4		85.5	0.08	7.8	1008
1/23/2008	1129*	0.8								

Tracer Test #	<sup>‡</sup> 2 (20 cfm to	NJ2, ~8%	5 H2)						
1/18/2008	1120 Test s	start							
1/18/2008	1213	2.2	0.04	0	0.46	65.8		13.3	1015
1/18/2008	1258	2.0	0.06	0	2.8	62.4		14.3	1014
1/18/2008	1400	2.3	0.02	0	5.0	63.2		15.7	1014
1/18/2008	1539	1.9	0.02	0	6.5	43.8	0.04	24.0	1014
1/18/2008	1628	2.2	0	0	6.8	60.8		16.3	1014
1/18/2008	1632*	0.8	0	0	6.8	62.9		16.0	1014
1/18/2008	1641**	2.3	0	0	7.0	69.2		14.7	1014
1/19/2008	1024	2.0	0.08	0	8.9	62.8	0.02	9.8	1019
1/19/2008	1154	0.6	0.06	0	7.5	97.4		14.3	1017

Tracer Test #	Tracer Test #3 (30 cfm to INJ2, ~4% H2)								
1/30/2008	/2008 1036 Test start								
1/30/2008	1119	0.0	0	0	1.0	89.6	0.08	9.8	1020
1/30/2008	1229	0.0	0	0	3.3	80.7		11.3	1019
1/30/2008	1431	0.0	0	0	4.5	70.2	0.08	14.2	1018

Well ID \_\_\_\_P7\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth 38 Well or Injection Gas Sample **Ambient Air** Well  $O_2$  $CO_2$ **Propane** H<sub>2</sub> He RH **Pressure** Temperature **Barometric pressure** (%) Date Time (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) 1/31/2008 0 0 4.2 957 0.0 84.3 0.08 8.9 1019 3.8 1/31/2008 1135 0 0 0 83.1 9.5 1018 1/31/2008 1354 0 0 3.7 81.8 0.10 8.7 1016 1435 1/31/2008 1/31/2008 1520 0 0 3.7 0.05 1014 83.3 8.3 0 0 3.9 82.5 8.1 1/31/2008 1615 1013 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1336 0.04 92.2 8.0 4.6 10.6 1010 1/28/2008 6.1 1423 0.0 0.02 84.1 12.2 0.14 1011 1/28/2008 1603 0 0 6.4 0.12 11.3 0.0 77.8 1012 1/29/2008 807 0.0 0 7.3 84.0 0.04 5.0 1017 1/29/2008 Final O2\* 0.0 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1042 0 2.4 0.1 61.4 0.10 9.9 1019 2/5/2008 1141 0 0 0 3.4 70.3 11.0 1019 2/5/2008 1346 0 0 3.9 76.7 0.13 12.6 1018

Well ID \_\_\_\_P7\_\_\_\_ **Phase II Piezometer Monitoring Data** Depth 38 **Well or Injection Gas Sample Ambient Air** Well  $O_2$  $CO_2$ **Propane** H<sub>2</sub> He RH **Pressure** Temperature **Barometric pressure** (%) Date Time (%) (%) (%) (%) (in wc) (C°) (mbar) (ppm) 2/5/2008 1512 1019 0 0 3.6 63.6 19.8 3.5 2/5/2008 1556 0 0 0 60.7 19.1 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 0 0 21.7 2/7/2008 1537 0.0 0.046 59.7 1016 1.0 2/7/2008 1625 0 58.4 20.5 0.0 1016 2/8/2008 1019 0.0 0 8.5 68.8 8.9 1017 Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 65.2 1/17/2008 1039 9.3 0.02 0 1.9 0.03 8.6 1015 4.8 1/17/2008 1406 4.1 0.12 63.3 13.7 1013 1/17/2008 1537 3.5 0.12 5.4 47.6 19.0 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 0 2.1 1020 1044 0.0 78.0 0.12 11.0 2/6/2008 1153 0.0 0 0 3.6 73.0 13.2 1020 2/6/2008 1250 0.0 0 3.9 73.5 14.5

1019

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	Pressure	Temperature	Barometric pressure			
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/6/2008	1446	0.0	0	0	4.6		73.9	0.12	16.4	1017
2/6/2008	1542	0.0	0	0	4.5		61.6		19.6	1017

Optimization	Test #1 (90	cfm to INJ2	2 for 4 hours	then shut	down; ~88%	% N2, 10% H2, 1%	6 CO2 & LPC	9)	
2/20/2008	1142	10.2	0.00	0	0.046		76.2	15.3	1010
2/20/2008	1206 Test :	start							
2/20/2008	1553	0.0	0.56	1.02	10		52.9	24.4	1008
2/20/2008	1606 Test	End							
2/20/2008	1637	0.0	0.46	1.04	10		54.2	22	1007
2/21/2008	930	9.1	0.20	0.22	2.8		74.8	10.4	1005
2/22/2008	1048	11.1	0.14	0.1	1		80.8	10.2	1003

Optimization	Test #2 (30	cfm to INJ2	for 12 hou	rs then shu	t down; ~88	% N2, 10%	H2, 1% CC	)2 & LPG)		
2/25/2008	2/25/2008 1845 Test Start									
2/26/2008	653 Test E	nd								
2/26/2008	714	0.0	1.86	0.54	7.2		89.1		3.7	1017
2/27/2008	1543	10.1	0.6	0.12	0.65		34.9		38.6	1009
2/28/2008	2/28/2008 1106 11.3 0.48 0.1 0.046 72.6									1007

Phase II Pie	zometer Mo	onitoring D	ata	Well ID	P7		Depth	38		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #3A (1	cfm to INJ	2; ~88% N2	, 10% H2, 1	% CO2 & L	.PG)				
2/29/2008	1319 Test	Start								
2/29/2008	1445	11.8	0.40	0.12	0.022		56		29.1	1009
3/3/2008	1056	12.2	0.32	0.16	0.022		58.4		15.8	1019
3/3/2008	1130 Test	End								
Optimization	Test #3B (1	cfm to INJ	1, INJ2 & IN	IJ3; ~88% N	N2, 10% H2	, 1% CO2 8	& LPG)			
3/3/2008	1130 Test	Start								
3/4/2008	936	13	0.36	0.16	0.022		64.1		13.2	1013
3/7/2008	1113	12.2	0.2	0.16	0.022		70.9		18.7	1018
3/7/2008	1306 Test	End								
Optimization	Test #3C (9	00 cfm to IN	J1, INJ2 & I	NJ3 for 15	minutes the	n shut dow	n; ~79% N2, T	, 10% H2 & LF	PG, 1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1343	11.6	0.18	0.16	0.046		67.3		22.4	1016
3/10/2008	1102	12.2	0.24	0.16	0.022		67.1		16.8	1016
Optimization	Test #4 (2,	45-minutes	pulses; da	ily 15-minut	es pulses w	//30cfh con	stant flow)			

Phase II Piez	zometer Mo	onitoring Da	ata	Well ID	P7		Depth	38		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization	Test #5 (20	cfm to INJ2	2 for 125 mi	nutes while	maintaing 3	30 cfh the re	est of the tim	ne; ~80% N2, ′	10% H2 & LPG	
Optimization	Test #6 (50	cfh to P4-1	8 & P4-28;	~80% N2, 1	0% H2 & L	PG)				
3/20/2008	1330 Start	Test								
3/24/2008	1014	7.8	0.22	2.5	0.046		70.4		15.8	1012
3/26/2008	955	7.2	0.20	2.5	0.022		80.6		11.0	1017
3/28/2008	952	8.1	0.20	2.0	0.022		68.5		10.5	1009
3/31/2008	954	0.2	0.08	13.5	6.2		82.6		10.1	1013
4/2/2008	1052	0.1	0.10	14.0	5.3		76.6		15.5	1008
Optimization	Test #7 (20	cfh to P4-1	8,28, -38	(60 cfh tota	I); ~80% N2	2, 10% H2 8	& LPG)			
4/2/2008	1233 Start	Test								
4/4/2008	937	0.1	0.08	13.5	4.9		69.3		12.8	1013
4/7/2008	1406	5.8	0.06	8.0	1.3		81.2		18.6	1011
Optimization	Test #7B (3	0 cfh to P4-	18, & P4-28	3 (60 cfh tot	al); ~80% N	12, 10% H2	& LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1059	6.4	0.00	6.5	0.72		79.8		145.2	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

				Well or	as Sample			Well	Ambient Air	
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date Time	)	(%)	(%)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)			

Optimization	Test #7C (5	50 cfh to P4-	-18, & P4-2	8 (100 cfh to	otal); ~79%	N2, 10% H2 & LPG, 19	% CO2)	
4/10/2009	1121 Start	Test		·	·			
4/11/2008	1231	9.4	0.06	4.0	0.1	71.3	21.9	1013
4/16/2008	1026	2.7	0.08	8.0	1.7	61.9	15.6	1011
4/22/2008	1048	5.0	0.16	3.5	0.10	87.9	20.3	1009
4/25/2008	956	0.8	0.14	8.5	0.046	61.6	21.6	1015
4/29/2008	1106	1.1	0.06	8.0	0.22	65.6	24.5	1007
5/5/2008	1311	1.9	0.06	7.0	0.1	55.9	33.6	1001
5/13/2008	929	0.1	0.16	9.0	0.10	34.4	34.3	1007
5/20/2008	930	5.2	0.28	6.0	0.022	61.0	22.8	1004
5/23/2008	1515	4.8	0.26	7.0	0.046	41.8	30.7	990
5/27/2008	901	2.4	0.34	8.0	0.86	58.5	16.5	1007
6/4/2008	904	0.1	0.32	9.5	0.74	45.9	25.0	1002
6/12/2008	1151	1.6	0.34	8.0	0.046	48.5	40.9	1003
6/20/2008	1019	0.1	0.34	8.5	0.10	35.6	39.3	1006
6/25/2008	1041	0.2	0.44	8.5	0.10	44.3	30.9	1005
7/2/2008	1143	0.0	0.58	8.0	0.50	63.7	31.1	1004
7/7/2008	1132	0	0.58	8.5	0.1	54.2	35.9	998
7/18/2008	1058	0	0.68	8.5	0.77	93.8	25.6	
7/24/2008	1056	0.0	0.68	8.5	0.920	55.8	28.4	1005

Phase II Piezometer Monitoring Data Well ID \_\_\_\_P7\_\_\_\_ Depth \_\_\_38\_\_\_\_\_

	ĺ			Well or	Injection G	as Sample	<u> </u>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/31/2008	1054	0.0	0.66	8.5	1.000		63.9		26.8	1003
8/7/2008	930	0.0	0.68	9.0	1.0		53.8		25.8	1004
8/12/2008	1032	0.0	0.64	8.5	0.82		54.4		28.4	1002
Optimization	Test #8 (10	0 cfh of 100	% Propane	to P4-18, 8	k P4-28 (50	cfh to each	point)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1036	4.9	0.98	5.5	0.005					999
9/15/2008	920	2.3	1.38	16.5	0.010		38.8		25.7	1007
9/29/2008	940	3.9	2.12	30	0.010		39.1		24.2	1006
10/13/2008	1201	7.6	2.58	30	0.010		23.7		32.2	1017
10/20/2008	1129	4.9	3.18	30	0.010		47.7		25.5	1013
11/5/2008	1405	4.0	4.56	30	0.010		79.6		18.7	1016
11/17/2008	1117	3.7	4.90	30	0.010		54.5		28.1	1014
12/1/2008	1117	3.3	5.00	30	0.005		54.9		24.3	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_P7\_\_\_\_\_ Depth \_\_\_48\_\_\_\_\_

				Well or	Well	Ambient Air				
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1120	18.8	0.68	0	0.002	40,000	84.0	0.04	10.4	1020
12/12/2007	1540							0.09		
12/13/2007	1019	19.8	0	0	0.022		55.1		13.0	1016
12/13/2007	1200	Discovered	l leak in O2	- all O2 dat	a for 12/13/	07 before 1	200 invalid			
12/13/2007	1350	18.0	0.82	0	0.22		80.1		15.2	1013
12/14/2007	855	18.4	0.84	0	0.22		71.3	0.0	6.8	1017
12/21/2007	1232	18.4	1.22	0	0.22		88.5	0.02	10.1	1012
12/26/2007	1248	17.7	1.36	0	0.22		84.2	0.02	12.3	
12/27/2007	1046	17.9	1.42	0	0.22		81.2	0.03	6.1	1018
12/27/2008	1337	17.6	1.2	0	0.22		82.2		9.1	1016
12/27/2008	1457	17.6	1.18	0	0.22		86.4	0.02	8.3	1017
1/2/2008	1101	17.3	1.58	0	0.22		61.7	0.04	14.6	1012

Tracer Test #1	(10 cfm to II	NJ2, ~7% H	H2)						
1/21/2008	1046 Test s	start							
1/21/2008	1222	17.5	1.44	0	0.022	71.9	0.04	10.4	1007
1/21/2008	1322	17.4	1.50	0	0.046	76.4		10.8	1006
1/21/2008	1551	17.8	1.42	0	0.010	79.9		10.0	1006
1/22/2008	1025	18.0	1.46	0	0.022	78.4	0.04	6.2	1011
1/22/2008	1419	17.7	1.36	0	0.022	79.5		8.6	1009
1/23/2008	1035	17.9	1.62	0	0.022	84.8	0.04	7.8	1008
1/23/2008	1130*	17.6							

68.2

61.3

80.6

0.01

14.8

9.8

14.3

1014

1019

1017

Depth \_\_\_48\_\_\_\_ **Ambient Air** Well or Injection Gas Sample Well  $O_2$ CO<sub>2</sub> Propane  $H_2$ He RH Pressure Temperature Barometric pressure Date Time (%) (%) (%) (ppm) (%) (in wc) (C°) (mbar) Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 1259 1/18/2008 17.7 1.16 14.5 0.010 62.1 1014 1/18/2008 1402 17.7 1.16 0.022 62.0 15.7 1014 1540 1.12 0.022 42.4 0.03 24.0 1014 1/18/2008 17.5 0.022 1/18/2008 1630 17.7 1.12 59.7 16.2 1014 1/18/2008 1635\* 17.5 1.26 0.022 64.5 15.7 1014 1/18/2008 1642\*\* 0.022

Well ID \_\_\_P7\_\_\_\_

**Phase II Piezometer Monitoring Data** 

1/19/2008

1/19/2008 1157\*

17.7

17.9

17.6

1026

1.16

1.34

1.48

						•				
Tracer Test #3	(30 cfm to I	NJ2, ~4% F	H2)							
1/30/2008	1036 Test	start								
1/30/2008	1120	16.9	1.60	0	0.010		88.2	0.03	9.9	1020
1/30/2008	1230	16.9	1.58	0	0.010		80.0		11.2	1019
1/30/2008	1432	16.8	1.56	0	0.010		70.5	0.05	14.4	1018
1/31/2008	958	16.9	1.56	0	0.010		85.8	0.04	9.0	1019

0.022

0.022

Phase II Piezo	meter Moni	toring Data	a	Well ID	P7		Depth4	18		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/31/2008	1136	16.9	1.60	0	0.010		83.9		9.6	1018
1/31/2008	1358	17.0	1.62	0	0.010		80.1	0.08	8.7	1016
1/31/2008	1435									
1/31/2008	1521	16.9	1.62	0	0.010		82.8	0.03	8.3	1014
1/31/2008	1617	16.6	1.62	0	0.010		82.2		8.1	1013
Tracer Test #4	(60 cfm to II	NJ2, ~7% ⊢	l2)							
1/28/2008	1236 Test s	start								
1/28/2008	1328	17.1	1.70	0	0.010		93.5		10.9	1010
1/28/2008	1425	16.9	1.78	0	0.005		82.0	0.05	12.1	1011
1/28/2008	1604	16.8	1.62	0	0.010		76.3	0.05	11.1	1011
1/29/2008	808	16.9	1.70	0.02	0.010		82.9	0.03	5.0	1017
1/29/2008	Final O2*	16.9								
		·								
Tracer Test #5	(90 cfm to II	NJ2, ~3% H	l2)							
2/5/2008	1015 Test s	start								
2/5/2008	1043	15.5	1.12	0	0.010		62.8	0.04	10.1	1019
2/5/2008	1142	15.5	1.08	0	0.010		69.1		11.1	1019
2/5/2008	1347	15.3	1.06	0	0.022		75.0	0.08	12.6	1018
2/5/2008	1513	15.7	1.18	0	0.010		58.6		20.3	1019
2/5/2008	1556	15.6	1.14	0	0.010		58.6	-	19.3	1018

Phase II Piezo	meter Moni	toring Data	а	Well ID	_P7		Depth4	48		
				Well or	Injection G	as Sample	•		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #6	(30 cfm tota	ıl; 10 cfm to	each INJ1,	2, and 3; ~	8% H2)					
2/7/2008	1500 Test :	start								
2/7/2008	1538	15.9	1.30	0	0.005		61.1		21.5	1016
2/7/2008	1627	15.9	1.28	0	0.010		57.8		20.4	1016
2/8/2008	1020	15.7	1.22	0	0.022		69.1		10.0	1017
Tracer Test #7	(60 cfm tota	al; 20 cfm to	each INJ1,	2, and 3, ~	5% H2)					
1/17/2008	900 Test st	art								
1/17/2008	1042	17.8	0.96	0	0.022		65.7	0.02	8.6	1015
1/17/2008	1406	18.0	1.40	0	0.22		61.8		13.5	1013
1/17/2008	1540	17.9	1.44	0	0.022		48.9		18.8	1012
Tracer Test #8	(90 cfm tota	al; 30 cfm ea	ach to INJ1,	2, and 3; ~	4.5% H2)					
2/6/2008	1000 Test :	start								
2/6/2008	1046	15.5	1.06	0	0.005		79.9	0.07	10.9	1020
2/6/2008	1155	15.5	1.06	0	0.005		76.5		13.2	1020
2/6/2008	1252	15.4	1.04	0	0.010		75		14.5	1019
2/6/2008	1446	15.3	1.02	0	0.022		76.4	0.07	16.3	1017
2/6/2008	1543	15.3	1.02	0	0.022		63.5		19.7	1017
2/6/2008	1632	15.9	1.24	0	0.005		60.0		19.0	1017

Phase II Piezo	meter Moni	toring Data	a	Well ID	_P7		Depth	48		
	[			Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure		Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Te	est #1 (90 cf	m to INJ2 fo	or 4 hours t	hen shut do	wn; ~88% I	N2, 10% H2	2, 1% CO2 8	& LPG)		
2/20/2008	1143	15.1	1.52	0	0.022		75.2		15.3	1010
2/20/2008	1206 Test s	start								
2/20/2008	1554	14.7	1.36	0	0.022		53.2		24	1008
2/20/2008	1606 Test I	∃nd								
2/20/2008	1638	14.7	1.32	0	0.022		55.4		21.9	1008
2/21/2008	932	15.5	1.62	0	0.022		74.8		10.4	1005
2/22/2008	1054	15.3	1.62	0	0.005		84.5		10.4	1003
			40.1			NO 400/ I	10 404 000	0.1.00)		
Optimization Te	Ì		or 12 hours	then shut o	lown; ~88%	N2, 10% F	12, 1% CO2	& LPG)		
	1845 Test \$									
2/26/2008	653 Test E	na							+	
2/26/2008	716	14.9	1.76	0.08	0.01		89.2		3.7	1017
2/27/2008	1544	14.6	1.4	0	0.022		35		38.8	1009
2/28/2008	1108	15.2	1.32	0	0.022		71.8		16.6	1007
Optimization Te	est #3A (1 cl	m to INJ2;	~88% N2, 1	10% H2, 1%	CO2 & LP	G)				
2/29/2008	1319 Test \$	Start								
2/29/2008	1446	14.5	1.08	0	0.005		58.3		29.3	1009
3/3/2008	1057	14.5	1.12	0	0.022		58.7		15.8	1019
3/3/2008	1130 Test I	≣nd								

Phase II Piezo	meter Moni	itoring Data	a	Well ID	_P7		Depth	48		
					Injection G	as Sample			Well	Ambient Air
D-1-	T:	O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	•
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Te	est #3B (1 cf	fm to INJ1,	INJ2 & INJ	3; ~88% N2	, 10% H2, 1	1% CO2 & L	PG)			
3/3/2008	1130 Test \$	Start								
3/4/2008	937	14.9	1.36	0	0.01		65.7		13.3	1013
3/7/2008	1114	14.5	1.02	0	0.022		70		18.8	1018
3/7/2008	1306 Test I	End								
Optimization Te	est #3C (90	cfm to INJ1	, INJ2 & IN	J3 for 15 mi	nutes then	shut down;	~79% N2, 1	10% H2 & LPG	6, 1% CO2)	
3/7/2008	1306 Start	Pulse								
3/7/2008	1321 End F	Pulse								
3/7/2008	1344	14.3	1	0	0.022		66.6		22.5	1016
3/10/2008	1103	14.7	1.14	0	0.022		66.4		16.8	1016
Optimization Te	est #4 ( 2, 45	5-minutes p	ulses; daily	15-minutes	s pulses w/3	30cfh consta	ant flow)			
Optimization Te	est #5 (20 cf	m to IN.12 f	or 125 mini	ıtes while m	aintaing 30	cfh the res	t of the time	· ~80% N2 10	1% H2 & I PG)	
Optimization 16	(20 0)	111 10 11 102 1	01 120 1111110	NOO WINO II	annan ig oo			, 0070112, 10	770112 (3 21 3)	
<u> </u>										
Optimization Te	est #6 (50 cf	h to P4-18	& P4-28; ~8	30% N2, 10	% H2 & LP	G)				
3/20/2008	1330 Start	Test								
3/26/2008	956*	6.0	0.02	2.0	0.046		85.3		11.1	1017
3/28/2008	953	15.1	1.52	0.00	0.010		72.4		10.6	1009
3/31/2008	956	14.7	1.28	0.04	0.022		82.8		10.1	1013
4/2/2008	1053	15.0	1.40	0.02	0.022		75.8		15.5	1008
On timination T		% t- D4 40	00 00 (0	20 - 41- 1-1-1	000/ NO	400/ 110 0	DO)			
Optimization Te	,		28, -38 (6	ou cin total);	~80% N2,	10% H2 & I	LPG)			
4/2/2008	1233 Start	rest								

Phase II Piezo	meter Moni	toring Data	a	Well ID	_P7		Depth	48		
	[			Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure		Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
4/4/2008	938	14.5	1.30	0.08	0.022		71.6		12.9	1013
4/7/2008	1407	13.5	1.38	0.52	0.022		79.7		18.7	1011
Optimization Te	est #7B (30	cfh to P4-18	3, & P4-28 (	60 cfh total	); ~80% N2	, 10% H2 &	LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1100	12.9	1.24	0.8	0.022		78.4		15.3	1009
Ontimization To		ofh to D4 44	2 8 D4 20 /	(400 of b to t	-I). 700/ N	2 40% 112	8 L DC 40/	CO2)		
Optimization Te			o, & P4-20 (	100 cm tota	ai), ~19% in	2, 10% П2	& LPG, 1%	CO2)		
	1121 Start									
4/11/2008	1232	11.3	1.32	2.0	0.1		72.8		21.9	1013
4/16/2008	1027	10.4	1.34	2.5	0.0		62.2		15.6	1011
4/22/2008	1050	10.1	1.42	3.0	0.046		88.3		20.5	1009
4/25/2008	957	8.4	1.18	3.5	0.046		58.1		21.8	1015
4/29/2008	1108	10.0	1.34	3.0	0.046		64.5		24.7	1007
5/5/2008	1312	10.3	1.36	2.5	0.022		55.4		33.9	1001
5/13/2008	931	8.2	1.34	4.0	0.022		32.2		34.4	1007
5/20/2008	932	9.0	1.48	3.5	0.046		58.3		23.0	1004
5/23/2008	1516	11.5	1.44	1.6	0.010		41.0		30.3	990
5/27/2008	903	7.7	1.62	4.0	0.022		60.0		16.6	1007
6/4/2008	905	9.0	1.50	3.0	0.022		49.7		24.9	1002
6/12/2008	1154	6.8	1.40	3.5	0.010		46.6		41.4	1003
6/20/2008	1020	6.0	1.40	4.0	0.022		34.7		39.5	1006
6/25/2008	1042	5.6	1.44	4.0	0.046		43.5		31.1	1005
7/2/2008	1144	5.4	1.48	4.0	0.022		63.2		30.9	1004
7/7/2008	1133	6.5	1.44	3	0.022		52.3		36	998
7/18/2008	1059	4	1.64	4.5	0.046		93.3		25.5	

Phase II Piezometer Monitoring Data Well ID \_\_\_P7\_\_\_\_\_ Depth \_\_\_48\_\_\_\_\_

				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/24/2008	1058	3.6	1.64	4.5	0.046		57.7		28.4	1005
7/31/2008	1055	3.2	1.74	4.5	0.046		66.8		26.9	1003
8/7/2008	931	2.5	1.44	5.5	0.046		54.6		25.2	1004
8/12/2008	1033	3.0	1.78	4.5	0.046		63.8		28.3	1002
Optimization Te	est #8 (100 o	cfh of 100%	Propane to	P4-18, & F	P4-28 (50 cf	h to each p	oint)			
9/8/2008	0905 Test	Start								
9/8/2008	1040	2.4	1.98	6.5	0.010					999
9/15/2008	922	1.1	2.06	30	0.010		35.6		25.6	1007
9/29/2008	941	0.1	2.08	30	0.010		37.1		24.3	1006
10/13/2008	1202	0.0	1.78	30	0.010		21.9		32.2	1017
10/20/2008	1131	0.1	1.84	30	0.005		49.4		26.2	1013
11/5/2008	1406	0.0	1.80	30	0.005		80.4		18.8	1016
11/17/2008	1118	0.0	1.64	30	0.005		55.3		27.8	1014
12/1/2008	1118	0.0	1.62	30	0.005		54.9		24.4	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_\_ Depth \_\_\_18\_\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1134	20.8	0.10	0	0.002	30,000	76.5	0.04	10.4	1020
12/12/2007	1542							0.05		
12/13/2007	1029	13.2	0	0	8.0		64.5		12.6	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/0	07 before 12	200 invalid			
12/13/2007	1351	0	0	0	8.7		68.4		14.6	1013
12/14/2007	858	0.2	0.32	0.04	0.55		72.1	0.01	6.6	1017
12/21/2007	1236	18.4	0.28	0	0.22		82.4	0.04	10.3	1012
12/26/2007	1250	19.3	0.2	0	0.22		74.3	0.02	12.2	1016
12/27/2007	1050	12.4	0.42	0	2.7		76.2	0.04	6.3	1018
12/27/2007	1339	11.2	0.32	0	3.3		78.5		8.9	1016
12/27/2007	1501	10.7	0.34	0	3.7		84.5	0.06	8.5	1017
1/2/2008	1104	2.5	0.16	0	0.22		61.8	0.04	13.6	1012

Tracer Test #1 (1)	0 cfm to INJ	2, ~7% H2)							
1/21/2008	1046 Test	start							
1/21/2008	1223	3.7	0.10	0	0.046	72.8	0.05	10.4	1007
1/21/2008	1323	3.6	0.10	0	0.10	76.8		10.9	1006
1/21/2008	1553	3.6	0.04	0	2.6	74.7	0.07	10.0	1006
1/22/2008	1027	3.8	0.12	0	5.0	79.2	0.05	6.2	1011
1/22/2008	1420	3.3	0.06	0	5.3	79.8		8.5	1009

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_18\_\_\_\_

				Well or	Injection G		Well	Ambient Air		
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/23/2	2008 1	36	3.7 0.10	0	5.7		84.9	0.04	7.9	1008
1/23/	2008 1138*	1	.3							

Tracer Test #2 (2)	0 cfm to INJ	l2, ~8% H2)							
1/18/2008	1120 Test :	start							
1/18/2008	1249	3.0	0.08	0	0.10	67.2		13.9	1014
1/18/2008	1403	3.4	0.04	0	3.8	63.7		15.7	1014
1/18/2008	1541	2.9	0.02	0	5.4	42.9	0.03	24.3	1014
1/19/2008	1032	3.0	0.08	0	9.0	60.2	0.01	10.0	1019
1/19/2008	1200*	0.7	0.10	0	7.6	61.4		14.6	1018

Tracer Test #3 (3	0 cfm to INJ	2, ~4% H2)							
1/30/2008	1036 Test	start							
1/30/2008	1123	0.1	0	0	0.46	91.2	0.07	9.9	1020
1/30/2008	1232	0.1	0	0	2.4	82.9		11.2	1019
1/30/2008	1435	0.1	0	0	4.2	74.0	0.09	14.7	1018
1/31/2008	1000	0.1	0	0	4.1	85.9	0.08	9.1	1019
1/31/2008	1138	0.1	0	0	3.7	83.2		9.6	1018
1/31/2008	1400	0.1	0	0	3.7	80.6	0.08	8.7	1016
1/31/2008	1435								
1/31/2008	1523	0.1	0	0	3.6	82.2	0.06	8.3	1014

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_18\_\_\_\_ Well or Injection Gas Sample **Ambient Air** Well Temperature Barometric pressure Propane Pressure  $O_2$ CO2  $H_2$ He RH Date Time (%) (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1330 3.4 0.16 2.5 88.0 11.4 1010 1/28/2008 1429 0.3 0.10 0 5.6 82.4 0.04 12.3 1011 1/28/2008 1606 0.1 0.02 6.1 77.0 0.10 10.8 1012 7.2 1/29/2008 811 0.0 0.02 84.2 0.03 5.1 1017 6.5 1/29/2008 1012\* 0.1 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1044 1.4 0.84 65.4 0.08 10.2 1019 2/5/2008 1144 0.1 0 3.1 0 73.8 11.1 1019 0 2/5/2008 1348 0.0 0 3.8 79.5 0.10 12.6 1018 1514 0 2/5/2008 0.0 0 3.5 51.1 20.9 1019 2/5/2008 1558 0.0 0 0 3.4 62.2 19.2 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 0.1 63 1540 0 0.046 21.5 1016 2/7/2008 1629 0.0 0 20.1 1016 0 0.10 59.1 2/8/2008 0.0 0 8.5 1022 69.3 10.0 1017

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_18\_\_\_\_\_ Well or Injection Gas Sample Well Ambient Air Temperature Barometric pressure Propane  $O_2$ CO2  $H_2$ He RH Pressure Time Date (%) (%) (C°) (mbar) (%) (%) (ppm) (%) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1045 10.8 0.06 0 1.8 64.4 0.03 8.6 1015 1/17/2008 1410 4.8 0.22 0 4.8 62.4 13.3 1013 0.22 1/17/2008 1542 3.4 0 5.6 47.3 0.01 18.6 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1048 0.1 0.22 82.6 1020 0.11 10.9 0.0 0 2/6/2008 1158 0 3.2 79.7 13.2 1020 0 2/6/2008 1253 0.1 0 3.7 78.0 14.4 1019 2/6/2008 0.0 0 1448 0 4.3 80.4 0.11 16.4 1017 0 2/6/2008 1544 0.0 0 4.3 63.6 19.7 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 1144 2/20/2008 11.4 0.02 0.022 74.7 15.4 1010 2/20/2008 1206 Test start 2/20/2008 1556 0.1 0.76 55 23.8 1008 11 2/20/2008 1606 Test End 1640 0.72 2/20/2008 0.1 1.02 9.9 57.3 21.6 1008 4.2 75.8 2/21/2008 934 7.6 0.46 0.44 10.4 1005 2/22/2008 1055 10.1 0.34 0.26 1.6 82.7 10.4 1003

**Phase II Piezometer Monitoring Data** Well ID P8\_\_\_\_\_ Depth \_\_\_\_18\_\_\_\_\_ Well or Injection Gas Sample Well Ambient Air  $O_2$ CO2 Propane  $H_2$ He RH Pressure Temperature Barometric pressure Date Time (%) (C°) (mbar) (%) (%) (%) (ppm) (%) (in wc) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2.36 0.56 2/26/2008 718 0.1 7 89.3 3.8 1017 2/27/2008 1546 8.7 0.96 0.24 1.5 35.3 39.2 1009 9.7 0.78 0.61 2/28/2008 1110 0.22 71.3 16.7 1007 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1448 10.2 0.60 0.22 0.046 58.1 29.6 1009 3/3/2008 1102 11.3 0.42 0.18 0.022 75.3 16 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 944 10.8 0.44 0.22 0.022 78.5 13.8 1013 3/7/2008 1116 10.1 0.22 0.26 0.005 66.5 19 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1345 11.1 0.18 0.22 0.01 68.6 22.6 1016 3/10/2008 1104 11 0.24 0.24 0.005 66.8 16.8 1016

Phase II Piezome	eter Monito	ring Data		Well ID	P8		Depth	18		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Test	#4 ( 2, 45-r	ninutes puls	ses; daily 15	i-minutes p	ulses w/30c	fh constant	flow)			
Optimization Test	#5 (20 ctm	to INJ2 for	125 minutes	s while mair	ntaing 30 cff	the rest of	the time; ~	80% N2, 10%	H2 & LPG)	
Optimization Test	#6 (50 cfh t	to P4-18 & I	P4-28; ~80%	% N2, 10%	H2 & LPG)					
	1330 Start				Í					
3/21/2008			0	0	0.01		76.6		12.7	1020
3/26/2008	958	20.9	0	0	0.01		83.3		11.1	1017
3/28/2008	955	20.9	0	0	0.005		73.5		10.6	1009
3/31/2008	958	20.9	0	0	0.005		75.8		15.6	1013
4/2/2008		6.5	0.16	6.5			85.2		18.5	1008
*Tubing to P8-18	was disconi	nected; all d	lata from 3/2	21/08 - 4/2/	08 @1054 ir	nvalid				
Optimization Test	#7 (20 cfh t	to P4-182	2838 (60 (	ofh total): ~8	30% N2. 10°	% H2 & LP(	G)			
	1233 Start			,,	,					
4/4/2008	939	6.6	0.20	6.0	2.5		70.8		12.9	1013
4/7/2008	1409	7.8	0.28	6.5	2.7		79.8		18.6	1011
		. =								
Optimization Test			k P4-28 (60	cth total); ~	-80% N2, 10	)% H2 & LF	<b>'</b> G)			
	1458 Start									
4/9/2008	1103	11.9	0.22	3.0	1.4		79.3		15.4	1009

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_18\_\_\_\_

1038

8/12/2008

0.0

0.56

9.0

1.5

		•								
					Injection G				Well	Ambient Air
D /	I <del></del> -	O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	<u> </u>
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Tes	t #7C (50 cff	n to P4-18,	& P4-28 (10	00 cfh total);	~79% N2,	10% H2 & L	_PG, 1% CO	2)		
4/10/2009	1121 Start	Test								
4/11/2008	1234	12.9	0.32	2.0	0.7		70.9		21.9	1013
4/16/2008	1029	10.8	0.20	3.5	0.8		59.3		15.7	1011
4/22/2008	1051	4.8	0.32	4.5	1.4		86.4		20.1	1009
4/25/2008	959	7.8	0.18	4.0	0.10		52.5		22.1	1015
4/29/2008	1109	2.3	0.26	7.5	1.7		66.3		24.3	1007
5/5/2008	1314	3.5	0.28	6.5	1.9		58.9		34.6	1001
5/13/2008	934	2.2	0.26	8.0	0.96		23.8		34.2	1007
5/20/2008	933	10.3	0.54	3.5	0.86		51.1		22.7	1004
5/23/2008	1519	9.0	0.28	4.0	0.10		24.4		30.0	990
5/27/2008	905	6.3	0.60	6.5	1.8		47.5		16.7	1007
6/4/2008	907	1.4	0.58	9.0	2.1		41.5		25.2	1002
6/12/2008	1156	3.6	0.42	7.5	0.93		26.5		42.0	1003
6/20/2008	1023	1.0	0.52	8.5	1.7		32.1		40.4	1006
6/25/2008	1048	1.1	0.6	8.0	2.5		47.7		32.6	1005
7/2/2008	1146	1.1	0.64	8.0	2.1		61.6		30.7	1004
7/7/2008	1136	0.5	0.58	8.5	1.4		51.4		36.1	998
7/18/2008	1101	0.2	0.64	8.5	1.8		95.2		25.6	
7/24/2008	1059	0.4	0.54	8.5	1.900		57.1		28.4	1005
7/31/2008	1058	0.0	0.56	9.0	1.900		67.7		27.2	1003
8/7/2008	933	0.0	0.60	9.0	1.8		49.7		24.7	1004
								•		

64.2

28.2

1002

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_18\_\_\_\_

				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Test	:#8 (100 cfh	of 100% P	ropane to P	4-18, & P4-	28 (50 cfh t	o each poin	nt)			
9/8/2008	0905 Test	Start								
9/8/2008	1045	10.2	0.82	2.5	0.005					999
9/15/2008	926	9.1	1.02	3.5	0.005		36.7		26.3	1007
9/29/2008	950	12.0	1.12	2.5	0.002		62.4		22.3	1006
10/13/2008	1205	16.2	1.08	0.90	0.010		22.6		31.5	1017
10/20/2008	1133	14.8	1.36	1.76	0.005		48.1		26.6	1013
11/5/2008	1408	17.1	1.46	0.84	0.005		76.1		18.8	1016
11/17/2008	1120	15.7	1.46	1.62	0.005		62.9		27.2	1014
12/1/2008	1120	16.4	1.42	1.32	0.005		56.2		24.7	1014

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				Well or	Iniection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1140	20.7	0.04	0	0.002	50,000	77.7	0.02	10.7	1020
12/12/2007	1541							0.06		
12/13/2007	1031	14.1	0	0	7.0		61.8		12.8	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 dat	a for 12/13/	07 before 1	200 invalid			
12/13/2007	1353	0.2	0.1	0	8.4		71.8		14.3	1013
12/14/2007	859	0.8	0.28	0.14	0.88		69.6	0.0	6.5	1017
12/21/2007	1238	19.0	0.18	0	0.22		86.2	0.03	10.4	1012
12/26/2007	1253	20	0.14	0	0.022		78.2	0.01	11.6	1016
12/27/2007	1053	13.5	0.18	0	2.5		79.9	0.02	6.3	1018
12/27/2007	1341	12.4	0.1	0	3		82.2		9	1016
12/27/2007	1504	11.8	0.1	0	3.5		85.4	0.02	8.5	1017
1/2/2008	1107	3.3	0.18	0	0.22		62.6	0.03	13.4	1012
Tracer Test #1	(10 cfm to	INJ2, ~7%	H2)							
1/21/2008	1046 Test s	start								
1/21/2008	1225	4.6	0.12	0	0.046		76.5	0.02	10.4	1007
1/21/2008	1325	4.5	0.10	0	0.046		80.9		11.1	1006
1/21/2008	1554	4.0	0.10	0	0.79		79.4	0.05	10.0	1006
1/22/2008	1028	3.4	0.08	0	4.6		80.5	0.04	6.3	1011
1/22/2008	1422	2.9	0.02	0	4.9		82.7		8.6	1009

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_ Well or Injection Gas Sample Well **Ambient Air** Propane Temperature Barometric pressure  $O_2$ CO2  $H_2$ RH He Pressure Date Time (%) (%) (%) (%) (C°) (%) (mbar) (ppm) (in wc) 1/23/2008 85.8 0.02 1038 0 3.2 0.06 5.4 7.6 1008 1/23/2008 1132\* 1.2 Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 3.7 1/18/2008 1251 0.16 0 0.10 68.2 14.8 1014 1405 3.8 0.12 0 64.7 1/18/2008 1.0 15.8 1014 1/18/2008 0 1543 2.9 0.12 3.8 45.0 0.02 24.7 1014 1/19/2008 0 9.5 59.2 0.01 1033 2.9 0.08 10.1 1019 1/19/2008 1201\* 0.8 0.10 0 8.6 69.2 14.8 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 0.2 0 0.93 1124 0.04 90.4 0.08 10.0 1020 1233 1/30/2008 0.1 0.02 0 0.87 84.2 11.1 1019 1/30/2008 1436 0.0 0.02 0 3.2 73.5 0.08 15.0 1018 1001 86.0 9.2 1/31/2008 0.0 0 4.1 0.07 1019 1/31/2008 1138 0 0 3.7 83.5 0 9.6 1018 1/31/2008 1401 0 0 3.6 80.8 0.10 8.7 1016 1/31/2008 1435

0

3.6

82.2

0.08

8.3

0

1/31/2008

1524

0.1

1014

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $O_2$  $H_2$ RH CO2 Propane He Pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1331 0.06 0 0.046 89.6 11.1 11.6 1010 1/28/2008 1431 2.7 0.08 0 3.9 83.7 0.07 12.6 1011 1/28/2008 1607 0.5 0.04 0 5.3 78.3 0.11 10.7 1012 0.03 1/29/2008 813 0.1 0.04 0 7.1 83.6 5.1 1017 1/29/2008 1013\* 0.2 6.4 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 2/5/2008 1046 5.6 0 0.022 63.5 0.06 10.3 1019 1145 72.5 2/5/2008 1.4 1.8 11.1 1019 2/5/2008 1349 0.5 3.2 80.1 0.08 12.6 1018 2/5/2008 1515 0.3 0 3.0 55.6 21.2 1019 0 2/5/2008 1559 0.2 3.0 64.1 19.1 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 2/7/2008 1541 0.0 0.06 0 0.10 63.2 21.6 1016 2/7/2008 1630 0.0 0.04 0 0.10 59.7 20.1 1016 2/8/2008 1023 0.0 0 8.3 68.3 10.0 1017

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $H_2$ RH  $O_2$ CO2 **Propane** He Pressure Date Time (%) (%) (%) (%) (%) (C°) (mbar) (ppm) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1051 18.0 0 0.22 0.02 1/17/2008 65.5 8.7 1015 1/17/2008 1412 6.1 0.16 0 4.4 66.2 13.3 1013 1/17/2008 1544 4.8 0.18 5.0 48.9 0.02 19.0 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1049 0.2 0.64 81.2 0.09 10.9 1020 0.0 2/6/2008 1159 1.3 78.4 13.2 1020 2/6/2008 1255 0.0 2.4 79.8 14.5 1019 16.2 2/6/2008 1448 0.0 3.8 80.9 0.11 1017 2/6/2008 65.7 1546 0.0 3.9 19.7 1017 2/6/2008 1635 0.0 3.9 60.2 19.4 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1145 0.00 0.022 74.4 11.3 15.4 1010 2/20/2008 1206 Test start 1557 0.6 0.32 0.96 55.4 2/20/2008 10 23.7 1008 2/20/2008 1606 Test End 1641 0.5 2/20/2008 0.30 0.96 10 58.5 21.3 1008

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				well of	mjection G	as Sample	<del>2</del>		well	Allibielit Ali
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
2/21/2008	935	4.2	0.28	0.72	4.9		75.3		10.8	1005
2/22/2008	1056	8.3	0.20	0.38	1.8		82.3		10.4	1003
										_

Optimization T	est #2 (30 d	ofm to INJ2	for 12 hours	s then shut	down; ~88%	% N2, 10% I	H2, 1% CO	2 & LPG)		
2/25/2008	1845 Test	Start								
2/26/2008	653 Test E	nd								
2/26/2008	719	0.2	1.3	0.62	6.6		87.7		3.9	1017
2/27/2008	1547	5.6	0.76	0.34	1.5		34.9		39.2	1009
2/28/2008	1111	7.9	0.62	0.3	0.69		70.3		16.7	1007
Optimization T	est #3A (1	ofm to INJ2;	~88% N2,	10% H2, 19	% CO2 & LF	PG)				
2/29/2008	1319 Test	Start								
2/29/2008	1449	8.8	0.46	0.28	0.046		58.8		29.7	1009
3/3/2008	1103	11	0.24	0.18	0.022		63.5		16	1019
3/3/2008	1130 Test	End								

0	ptimization T	est #3B (1 o	cfm to INJ1	, INJ2 & INJ	l3; ~88% N	2, 10% H2,	1% CO2 &	LPG)		
	3/3/2008	1130 Test	Start							
	3/4/2008	945	10	0.26	0.24	0.022		67.9	13.8	1013
	3/7/2008	1118	9.1	0.12	0.28	0.01		66.1	19.4	1018
	3/7/2008	1306 Test	End							

**Phase II Piezometer Monitoring Data** Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_ **Well or Injection Gas Sample** Well **Ambient Air** Temperature Barometric pressure  $H_2$  $O_2$ CO2 Propane He RH Pressure Date (%) (%) Time (%) (%) (%) (Co) (mbar) (ppm) (in wc) Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1347 9.1 0.1 0.28 0.01 73 22.9 1016 3/10/2008 1105 9.9 0.16 0.32 0.005 65.5 1016 16.8 Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) Optimization Test #6 (50 cfh to P4-18 & P4-28; ~80% N2, 10% H2 & LPG) 3/20/2008 1330 Start Test 959 3/26/2008 7.8 0.24 1.74 0.010 79.6 11.2 1017 3/28/2008 956 8.3 0.26 0.005 70.8 10.7 1009 1.3 959 0.22 1.58 3/31/2008 10.0 0.005 81.4 10.2 1013 4/2/2008 1055 8.0 0.18 3.5 1.8 74.5 15.7 1008 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 4/4/2008 940 7.9 0.12 3.5 1.1 69.3 13.0 1013 80.6 4/7/2008 1410 7.3 0.18 6.5 2.7 18.7 1011

WALLID

Phase II Piezo	meter Mon	nitoring Dat	a	Well ID	P8		Depth	_28		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization T	est #7B (30	cfh to P4-1	8, & P4-28	(60 cfh tota	I); ~80% N2	2, 10% H2 8	& LPG)			
4/7/2008	1458 Start	Test								
4/9/2008	1105	12.3	0.10	2.5	1.4		80.0		15.4	1009
Optimization T	est #7C (50	cfh to P4-1	8, & P4-28	(100 cfh tot	al); ~79% N	N2, 10% H2	& LPG, 1%	CO2)		
4/10/2009	1121 Start	Test								
4/11/2008	1235	12.7	0.20	2.0	0.8		72.8		22	1013
4/16/2008	1030	12.9	0.22	2.0	0.1		59.1		15.8	1011
4/22/2008	1052	4.6	0.22	4.5	1.8		86.5		19.8	1009
4/25/2008		7.5	0.14	4.0	0.10		49.9		22.3	1015
4/29/2008	1111	2.0	0.20	7.5	1.7		67.1		24.1	1007
	1315		0.16	7.0	1.9		55.1		35.0	1001
5/5/2008										
5/13/2008	935		0.18	7.0	0.10		25.3		34.2	1007
5/20/2008	936	9.0	0.34	4.0	1.2		56.5		24.0	1004
5/23/2008	1521	10.2	0.28	3.5	0.10		35.2		30.0	990
5/27/2008	907	5.5	0.44	7.0	2.0		47.5		16.9	1007
6/4/2008	909	1.3	0.38	9.0	2.0		41.4		25.6	1002
6/12/2008	1158	9.2	0.34	4.0	0.1		31.4		41.3	1003
6/20/2008	1025	0.5	0.34	8.5	1.8		32.5		40.8	1006
6/25/2008			0.36	8.5	2.7		44.8		32.7	1005
7/2/2008	1147	0.7	0.48	8.5	2.6		72.4		30.4	1004
7/7/2008			0.38	9.0	1.8		58.6		36.2	998

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_28\_\_\_\_

				Well or		Well	Ambient Air			
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
7/18/2008	1102	0.1	0.46	8.5	2.3		94.6		25.6	
7/24/2008	1101	0.4	0.40	8.5	2.300		62.0		28.5	1005
7/31/2008	1059	0.0	0.38	9.0	2.300		68.5		27.3	1003
8/7/2008	934	0.0	0.36	9.0	2.2		49.5		24.4	1004
8/12/2008	1036	0.0	0.40	9.0	1.9		64.8		28.3	1002
Optimization T	est #8 (100	cfh of 100%	6 Propane t	to P4-18, &	P4-28 (50 c	fh to each	point)			
9/8/2008	0905 Test	Start								
9/8/2008	1047	11.9	0.56	2.0	0.005					999
9/15/2008	927	11.0	0.64	2.5	0.005		34.7		26.5	1007
9/29/2008	951	1.2	1.76	30	0.005		44.3		22.5	1006
10/13/2008	1206	17.7	0.76	0.38	0.005		22.9		32.0	1017
10/20/2008	1134	16.1	0.84	1.06	0.005		47.2		26.8	1013
11/5/2008	1409	18.2	0.90	0.46	0.005		76.5		18.8	1016
11/17/2008	1121	17.0	0.86	0.70	0.005		66.3		27.0	1014
12/1/2008	1121	17.7	0.82	0.58	0.005		55.9		24.8	1013

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_\_ Depth \_\_\_\_38\_\_\_\_

				Well or		Well	Ambient Air			
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1143	19.2	0.56	0	0.002	100,000	76.4	0.02	10.9	1020
12/12/2007	1541							0.04		
12/13/2007	1033	20.2	0	0	0.22		62.3		12.9	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/	07 before 12	200 invalid			
12/13/2007	1354	19.0	0.62	0	0.022		74.8		13.9	1013
12/14/2007	900	18.7	0.6	0	0.46		70.8	0.02	6.5	1017
12/21/2007	1240	18.9	1.04	0	0.22		86.1	0.05	10.6	1012
12/26/2006	1254	18.7	1.04	0	0.022		80.1	0	11.2	1016
12/27/2007	1055	18.9	1.2	0	0.22		81.4	0.03	6.5	1018
12/27/2007	1343	18.7	0.98	0	0.22		80.9		9	1016
12/27/2007	1507	18.8	1	0	0.22		85.9	0.04	8.5	1017
1/2/2008	1108	18.9	1.14	0	0.22		63.7	0.02	13.3	1012

Tracer Test #1	(10 cfm to II	NJ2, ~7% H	12)						
1/21/2008	1046 Test s	start							
1/21/2008	1226	18.9	0.92	0	0.005	72.7	0.01	10.4	1007
1/21/2008	1326	18.8	0.90	0	0.022	77.6		11.2	1006
1/21/2008	1556	18.8	0.88	0	0.022	74.4	0.04	10.0	1006
1/22/2008	1030	18.9	1.02	0	0.022	77.6	0.03	6.3	1011
1/22/2008	1423	18.7	0.88	0	0.022	79.7		8.5	1009

**Phase II Piezometer Monitoring Data** Well ID P8\_\_\_\_ Depth 38 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH Pressure (C°) Date Time (%) (%) (%) (%) (%) (in wc) (mbar) (ppm) 1/23/2008 1039 18.9 1.02 0 0.10 84.8 0.01 7.6 1008 1/23/2008 1133\* 18.7 Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 1/18/2008 1252 18.6 0.76 0 0.022 65.7 14.1 1014 1/18/2008 1406 18.7 0.84 0 0.010 64.8 15.9 1014 1544 0.84 0 0.022 0.03 1014 1/18/2008 18.5 41.9 24.8 0.022 59.9 1/19/2008 1035 18.8 1.02 0 0.01 10.1 1019 1/19/2008 1203\* 18.5 1.16 0 0.022 62.7 15.6 1018 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1126 16.5 1.18 0 0.046 90.7 0.06 9.9 1020 11.0 1/30/2008 1235 16.4 1.20 0 0.046 83.8 1019 1/30/2008 1443 16.3 1.16 0 0.10 77.0 0.04 15.0 1018 0 85.3 9.3 1/31/2008 1003 15.9 1.18 0.10 0.05 1019 1/31/2008 1140 15.9 1.22 0 0.10 83.6 9.6 1018 1/31/2008 1402 15.8 1.22 0 0.10 80.9 0.05 8.7 1016 1/31/2008 1435

1/31/2008

1525

1.24

15.8

0

0.10

82.5

0.05

8.4

1014

**Phase II Piezometer Monitoring Data** Well ID P8\_\_\_\_\_ Depth 38 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH Pressure Date Time (%) (%) (%) (%) (mbar) (%) (ppm) (in wc) Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1333 17.2 1.34 0 0.046 89.0 11.8 1010 1/28/2008 1433 17.1 1.38 0 0.005 82.6 0.04 12.7 1011 1/28/2008 1609 17.2 1.32 0 0.010 78.3 0.05 10.5 1012 0.022 1/29/2008 814 16.9 1.38 0 83.0 0.02 5.1 1017 1/29/2008 Final O2\* 16.9 Tracer Test #5 (90 cfm to INJ2, ~3% H2) 2/5/2008 1015 Test start 1047 2/5/2008 14.2 0.82 0 0.010 62.3 0.04 1019 10.5 1147 14.2 0.80 0 2/5/2008 0.010 73.9 11.1 1019 2/5/2008 1354 14.1 0.78 0 0.002 79.3 0.04 12.7 1018 2/5/2008 1517 14.4 0.88 0 0.022 55.2 21.4 1019 2/5/2008 1601 14.3 0.86 0 0.022 62.6 19.3 1018 Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2) 2/7/2008 1500 Test start 1543 13.7 2/7/2008 0.96 0 0.010 63.7 21.8 1016 0.94 0.022 2/7/2008 1631 13.6 0 59.6 20.0 1016 2/8/2008 1024 0 0.022 13.3 0.88 69.5 10.0 1017

**Phase II Piezometer Monitoring Data** Well ID P8\_\_\_\_\_ Depth 38 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Time Date (%) (%) (mbar) (%) (%) (%) (ppm) (in wc) Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2) 1/17/2008 900 Test start 1/17/2008 1054 18.6 0.56 0 0.22 65.7 0.02 8.8 1015 1.00 1/17/2008 1414 19.1 0 0.022 65.8 13.5 1013 1/17/2008 1546 18.9 0.96 0 0.22 45.4 0.03 19.3 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1051 13.9 0.84 0 0.010 83.1 0.05 11.0 1020 2/6/2008 1201 13.8 0.76 0 0.010 80.0 13.2 1020 0 2/6/2008 1256 0.72 0.010 80.2 13.8 14.4 1019 1450 0.022 2/6/2008 13.7 0.76 0 81.1 0.06 16.1 1017 2/6/2008 1547 13.6 0.74 0 0.022 66.2 19.5 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1146 13.9 1.04 0.022 74.9 15.5 1010 2/20/2008 1206 Test start 2/20/2008 1558 13.6 0.92 0 0.022 56.4 23.6 1008 2/20/2008 1606 Test End 1642 0.022 2/20/2008 13.4 0.90 0 58.8 21.2 1008 75.6 2/21/2008 936 13.9 1.02 0 0.022 10.4 1005 2/22/2008 1057 14.1 1.02 0 0.022 82.6 10.4 1003

**Phase II Piezometer Monitoring Data** Well ID P8\_\_\_\_\_ Depth 38 Well or Injection Gas Sample Well **Ambient Air** Temperature Barometric pressure  $O_2$ CO2 **Propane**  $H_2$ He RH **Pressure** Date Time (%) (%) (mbar) (%) (%) (ppm) (in wc) Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/25/2008 1845 Test Start 2/26/2008 653 Test End 2/26/2008 720 14.7 1.08 0.08 0.01 87.5 1017 2/27/2008 1549 13.8 0.92 0 0.005 34.3 39.1 1009 0 2/28/2008 1112 14.2 0.72 0.022 69.3 16.9 1007 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1450 14.2 0.72 0 0.005 58.7 30.2 1009 3/3/2008 1104 14.5 0.82 0.005 62.1 16 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 946 14.5 0.9 0 0.01 65.7 13.8 1013 3/7/2008 1120 14.3 0.74 0 0.005 68.7 19.6 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1348 14.2 0.66 0 0.005 71.9 23 1016 3/10/2008 1107 14.5 0.8 0.005 67.8 16.9 1016

Phase II Piezor	meter Moni	toring Data	ı	Well ID	P8		Depth	_38		
	ĺ			Well or	Injection G	as Sample	)		Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
Optimization Te	est #4 ( 2, 45	5-minutes p	ulses; daily	15-minutes	pulses w/3	Ocfh consta	ant flow)			
Optimization Te	est #5 (20 cf	m to INJ2 fo	or 125 minu	tes while m	aintaing 30	cfh the rest	t of the time;	~80% N2, 10	% H2 & LPG)	
Optimization Te	est #6 (50 cf	h to P4-18 8	% P4-28; ~8	0% N2, 10%	% H2 & LPG	G)				
3/20/2008	1330 Start	Test								
3/26/2008	1000	13.8	0.92	0.24	0.010		77.9		11.2	1017
3/31/2008	1000	13.3	0.88	0.46	0.010		79.9		10.2	1013
4/2/2008	1057	13.2	0.90	0.52	0.046		77.8		15.8	1008
Optimization Te	est #7 (20 cf	h to P4-18,	28, -38 (6	0 cfh total);	~80% N2,	10% H2 & L	_PG)			
4/2/2008	1233 Start	Test								
4/4/2008	942	11.8	0.86	0.94	0.046		65.9		13.0	1013
4/7/2008	1411	10.3	0.88	2.0	0.22		81.1		18.8	1011
Optimization Te	set #7B (30 )	ofh to P/L-18	2 & P/L-28 (	60 ofh total)	· ~80% N2	10% H2 &	I PG)			
	1458 Start		5, & 1 <del>4</del> -20 (	oo ciri totai)	, ~00 /0 INZ,	10 /0 112 &	Li 0)			
4/9/2008	1107	9.5	0.82	9.4	0.022		81.2		15.4	1009
Ontimization To	ot #70 (50	ofh to D4 10	0 0 04 00 /	100 ofb tota	J). 700/ N/	2 400/ 112	0 LDC 40/ (	202)		
Optimization Te	1121 Start		5, & P4-26 (	100 cm tota	II); ~79% INZ	2, 10% 円2	& LPG, 1% (	502)		
4/10/2009	1031	8.8	0.92	3.5	0.046		57.1		15.9	1011
4/10/2008	1051	9.2	0.92	3.5	0.046		88.2		19.9	1009
4/25/2008	1002	9.2	0.80	3.0	0.046		48.5		22.6	1015
4/29/2008	1112	9.2	0.90	3.5	0.046		65.1		23.8	1007

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_\_ Depth \_\_\_\_38\_\_\_\_

				Well or	Injection G	as Sample	<b>!</b>		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	Не	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
5/5/2008	1316	8.2	0.90	3.5	0.022		54.9		35.4	1001
5/13/2008	937	7.5	0.94	4.0	0.022		24.6		34.2	1007
5/20/2008	937	6.7	0.98	4.5	0.046		52.1		25.6	1004
5/23/2008	1522	6.4	0.60	4.0	0.046		26.4		29.9	990
5/27/2008	908	6.8	1.16	4.5	0.046		46.3		17.0	1007
6/4/2008	910	6.2	0.66	4.5	0.046		41.1		25.8	1002
6/12/2008	1202	6.0	1.02	4.5	0.010		29.3		42.0	1003
6/20/2008	1025	4.9	1.02	5.0	0.005		32.4		42.0	1005
6/25/2008	1050	4.5	1.02	5.0	0.046		45.3		32.8	1005
7/2/2008	1152	4.1	1.04	5.0	0.010		73.4		30.3	1004
7/7/2008	1138	3.8	0.94	5.0	0.022		58.5		36.1	998
7/18/2008	1103	3	1.12	5.5	0.046		93.6		25.6	
7/24/2008	1102	2.6	1.10	5.5	0.010		71.5		28.6	1005
7/31/2008	1100	2.2	1.18	5.5	0.046		63.9		27.3	1003
8/7/2008	935	1.9	1.22	6.5	0.046		47.6		24.2	1004
8/12/2008	1038	1.7	1.18	6.0	0.046		61.8		28.3	1002
Optimization Te	est #8 (100 d	ofh of 100%	Propane to	P4-18, & P	4-28 (50 cfl	h to each po	oint)			
9/8/2008	0905 Test \$	Start								
9/8/2008	1049	1.3	1.26	6.5	0.010					999
9/15/2008	928	1.3	1.44	13.0	0.022		34.5		26.8	1007
9/29/2008	Did not me	asure								1006
10/13/2008	1208	0.8	1.82	30	0.010		20.6		32.5	1017
10/20/2008	1135	0.9	1.94	30	0.005		45.2		26.8	1013

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_\_ Depth \_\_\_\_38\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	pm) (%) (in wc)		(C <sub>0</sub> )	(mbar)
11/5/2008	1411	0.9	2.18	30	0.005		75.1		18.9	1016
11/17/2008	1122	0.5	2.16	30	0.010		70.9		27.0	1014
12/1/2008	1122	1.0	2.16	30	0.002		54.8		24.8	1013

Phase II Piezometer Monitoring Data Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_48\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
12/12/2007	1145	18.9	0.00	0	0.002	90,000	83.0	-0.05	11.0	1020
12/12/2007	1541							0.04		
12/13/2007	1035	20.1	0	0	0.22		67.4		12.5	1016
12/13/2007	1200	Discovered	leak in O2	- all O2 data	a for 12/13/(	7 before 12	200 invalid			
12/13/2007	1356	18.7	0	0	0.022		88.2		19.7	1013
12/14/2007	901	18.6	0.04	0	0.46		75.6	0.0	6.5	1017
12/21/2007	1245	18.4	0.20	0	0.22		87.5	0.03	11.3	1012
12/26/2007	1257	18.3	0.18	0	0.022		87	0	11	1016
12/27/2007	1057	18.3	0.2	0	0.22		80.8	0.04	6.5	1018
12/27/2007	1344	18.1	0	0	0.022		81.4		9	1016
12/27/2007	1509	18.5	0.1	0	0.022		86.2	0.02	8.5	1017
1/2/2008	1110	18.1	0.22	0	0.22		79.9	0.02	13.4	1012

Tracer Test #1 (10	cfm to INJ2	, ~7% H2)							
1/21/2008	1046 Test s	tart							
1/21/2008	1229	18.2	0.28	0	0.022	73.0	0.01	10.3	1007
1/21/2008	1328	18.4	0.28	0	0.022	75.0		11.3	1006
1/21/2008	1557	18.4	0.26	0	0.022	73.8	0.02	10.0	1006
1/22/2008	1031	18.2	0.40	0	0.022	77.3	0.03	6.3	1011
1/22/2008	1424	18.1	0.36	0	0.022	78.6		8.5	1009
1/23/2008	1040	17.7	0.36	0	0.10	84.3	0.02	7.5	1008
1/23/2008	1134*								

**Phase II Piezometer Monitoring Data** Well ID P8 Depth 48 Well or Injection Gas Sample Well Ambient Air CO2 Propane H<sub>2</sub> Barometric pressure  $O_2$ He RH Pressure Temperature Date (%) (%) (%) Time (%) (%) (ppm) (in wc) (Co) (mbar) Tracer Test #2 (20 cfm to INJ2, ~8% H2) 1/18/2008 1120 Test start 18.2 1/18/2008 1254 0 0.022 64.6 14.0 0 1014 1/18/2008 1408 18.7 15.9 0.26 0 0.046 63.0 1014 1/18/2008 0.30 0 25.0 1546 18.6 0.046 41.1 0.04 1014 1/19/2008 1036 18.6 0.40 0 0.046 58.8 0.02 10.1 1019 1/19/2008 1204\* 0 18.4 0.24 0.046 68.3 16.5 1017 Tracer Test #3 (30 cfm to INJ2, ~4% H2) 1/30/2008 1036 Test start 1/30/2008 1127 12.3 0.07 0.44 0 0.77 90.7 9.9 1020 1237 12.3 0 1/30/2008 0.50 0.94 84.1 11.0 1019 1/30/2008 1445 12.0 0.48 0 0.94 79.7 0.05 15.0 1018 0.50 83.7 1142 0 0.10 0.06 9.6 1/31/2008 10.4 1018 1/31/2008 0.52 0 8.7 1403 10.3 0.10 81.2 0.06 1016 1/31/2008 1435 0 1/31/2008 1526 10.3 0.48 0.10 82.8 0.06 8.4 1014 Tracer Test #4 (60 cfm to INJ2, ~7% H2) 1/28/2008 1236 Test start 1/28/2008 1336 14.9 0.66 0.005 86.4 12.1 1010

Phase II Piezom	eter Monitor	ing Data		Well ID	P8		Depth	_48		
				Well or	Injection G	as Sample	)		Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
1/28/200	8 1434	14.8	0.54	0	0.002		82.5	0.06	12.8	101
1/28/200	8 1613	15.1	0.70	0	0.002		78.4	0.04	10.1	101
1/29/200	8 816	14.5	0.66	0	0.046		83.9	0.01	5.1	101
1/29/200	8 1016*	14.8			0.50					
Tracer Test #5 (9	0 cfm to INJ2	2, ~3% H2)								
2/5/200	8 1015 Test s	start								
2/5/200	8 1050	10.8	0.46	0	0.005		62.8	0.06	10.6	101
2/5/200	8 1148	10.8	0.42	0	0.002		71.2		11.2	101
2/5/200	8 1355	10.7	0.44	0	0.002		79.4	0.06	12.7	101
2/5/200	8 1518	10.9	0.42	0	0.002		54.8		21.8	101
2/5/200	8 1601	10.9	0.36	0	0.005		63.9		19.5	101
Tracer Test #6 (3	0 cfm total; 1	0 cfm to ea	ch INJ1, 2,	and 3; ~8%	H2)					
2/7/200	8 1500 Test s	start								
2/7/200	8 1544	9.3	0.46	0	0.022		62.5		22.0	101
2/7/200	8 1632	9.4	0.44	0	0.005		59.3		20.1	101
2/8/200	8 1025	8.7	0.42	0	0.022		69.6		10.0	101
Tracer Test #7 (6	0 cfm total; 2	0 cfm to ea	ch INJ1, 2,	and 3, ~5%	H2)					
1/17/200	8 900 Test st	art								
1/17/200	8 1057	18 4	0.12	0	0.22		64.3	0.02	8.7	101

**Phase II Piezometer Monitoring Data** Well ID P8 Depth 48 **Well or Injection Gas Sample** Well **Ambient Air** Propane Barometric pressure  $O_2$ CO2  $H_2$ He RH Pressure **Temperature** (%) (%) (%) (%) Date Time (%) (ppm) (in wc) (Co) (mbar) 13.8 1/17/2008 1419 19.2 0 0.40 0.002 64.9 1013 0 1/17/2008 1551 19.2 0.42 0.002 45.2 0.01 19.9 1012 Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2) 2/6/2008 1000 Test start 2/6/2008 1052 0 82.0 10.4 0.46 0.005 0.06 11.0 1020 2/6/2008 1202 10.4 0.46 0 0.005 79.3 13.3 1020 0 2/6/2008 1257 10.4 0.44 0.005 77.9 14.4 1019 2/6/2008 10.3 0.40 0 0.005 80.6 0.09 16.0 1017 1451 2/6/2008 1548 10.2 0.38 0 0.005 66.6 19.3 1017 Optimization Test #1 (90 cfm to INJ2 for 4 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG) 2/20/2008 1148 12.8 0.64 0 0.022 75.1 15.5 1010 2/20/2008 1206 Test start 2/20/2008 1559 12.5 0.54 0 0.01 54.9 23.5 1008 2/20/2008 1606 Test End 0 0.022 2/20/2008 1643 12.5 0.52 58.1 21.1 1008 2/21/2008 938 12.8 0.62 0 0.022 74.9 10.5 1005 2/22/2008 13 1059 0.62 0.022 82.4 10.4 1003 Optimization Test #2 (30 cfm to INJ2 for 12 hours then shut down; ~88% N2, 10% H2, 1% CO2 & LPG)

2/25/2008 1845 Test Start

**Phase II Piezometer Monitoring Data** Well ID P8 Depth 48 **Well or Injection Gas Sample** Well **Ambient Air** Barometric pressure Propane H<sub>2</sub>  $O_2$ CO2 He RH Pressure **Temperature** (%) (%) (%) (%) Date Time (%) (ppm) (in wc) (Co) (mbar) 2/26/2008 653 Test End 2/26/2008 722 13.6 0.86 0.1 0.022 86.7 1017 0 2/27/2008 1551 13.0 0.56 0.022 33.1 39.2 1009 2/28/2008 1126 13.2 0.26 0 73.8 16.8 1007 0.01 Optimization Test #3A (1 cfm to INJ2; ~88% N2, 10% H2, 1% CO2 & LPG) 2/29/2008 1319 Test Start 2/29/2008 1452 13.4 0.40 0.02 0.005 58.3 30.5 1009 3/3/2008 1106 13.6 0.42 0 0.005 60.8 16 1019 3/3/2008 1130 Test End Optimization Test #3B (1 cfm to INJ1, INJ2 & INJ3; ~88% N2, 10% H2, 1% CO2 & LPG) 3/3/2008 1130 Test Start 3/4/2008 947 13.9 0.44 0 0.005 63.7 13.9 1013 3/7/2008 1121 13.5 0.32 0.02 0.005 63.8 19.7 1018 3/7/2008 1306 Test End Optimization Test #3C (90 cfm to INJ1, INJ2 & INJ3 for 15 minutes then shut down; ~79% N2, 10% H2 & LPG, 1% CO2) 3/7/2008 1306 Start Pulse 3/7/2008 1321 End Pulse 3/7/2008 1348 13.7 67.5 0.4 0 0.005 23.1 1016 3/10/2008 0 66 1108 13.7 0.46 0.005 16.9 1016

**Phase II Piezometer Monitoring Data** Well ID P8 Depth 48 **Well or Injection Gas Sample** Well **Ambient Air** CO2 H<sub>2</sub> Barometric pressure  $O_2$ Propane He RH Pressure Temperature (%) (%) (%) (%) (C°) Date Time (%) (ppm) (in wc) (mbar) Optimization Test #4 ( 2, 45-minutes pulses; daily 15-minutes pulses w/30cfh constant flow) Optimization Test #5 (20 cfm to INJ2 for 125 minutes while maintaing 30 cfh the rest of the time; ~80% N2, 10% H2 & LPG) 3/26/2008 1002 Could not sample; insufficient flow 1013 Optimization Test #7 (20 cfh to P4-18, --28, -38 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/2/2008 1233 Start Test 943 Could not sample; insufficient flow 4/4/2008 1013 4/7/2008 1412 Could not sample; insufficient flow 1011 Optimization Test #7B (30 cfh to P4-18, & P4-28 (60 cfh total); ~80% N2, 10% H2 & LPG) 4/7/2008 1458 Start Test 4/9/2008 Could not sample; insufficient flow 1009

**Phase II Piezometer Monitoring Data** 

Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_48\_\_\_\_

				Well or	Injection G	as Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)

Optimization Test	#7C (50 cfh	to P4-18, & P4-28 (100 cfh total); ~79% N2, 10% H2 & LPG, 1% CO2)	
4/10/2009	1121 Start	Test	
4/16/2008	1032	Could not sample; insufficient flow	1011
4/22/2008	1058	Could not sample; insufficient flow	
4/25/2008	1003	Could not sample; insufficient flow	
4/29/2008	1113	Could not sample; insufficient flow	1007
5/5/2008	1318	Could not sample; insufficient flow	1001
5/13/2008	938	Could not sample; insufficient flow	1007
5/20/2008	938	Could not sample; insufficient flow	1004
5/23/2008	1523	Could not sample; insufficient flow	990
5/27/2008	910	Could not sample; insufficient flow	1007
6/4/2008	911	Could not sample; insufficient flow	1002
6/12/2008	1203	Could not sample; insufficient flow	1003
6/20/2008	1028	Could not sample; insufficient flow	1005
6/25/2008	1051	Could not sample; insufficient flow	1005
7/2/2008	1153	Could not sample; insufficient flow	1004
7/7/2008	1139	Could not sample; insufficient flow	998
7/18/2008	1105	Could not sample; insufficient flow	
7/24/2008	1105	Could not sample; insufficient flow	1005
7/31/2008	1102	Could not sample; insufficient flow	1003
8/7/2008	937	Could not sample; insufficient flow	1004

Phase II Piezometer Monitoring Data

Well ID \_\_\_\_\_P8\_\_\_\_ Depth \_\_\_\_48\_\_\_\_

				Well or	Injection (	Gas Sample			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Optimization Test	#8 (100 cfh	of 100% Pr	opane to P	4-18, & P4-2	8 (50 cfh to	each point	)			
9/8/2008	0905 Test	Start								
9/8/2008	1051	Could not s	sample; ins	ufficient flow				999		
9/15/2008	929	Could not s	sample; insu	ufficient flow				1007		
9/29/2008	929	Could not s	sample; inst	ufficient flow						1006
10/13/2008	1209	Could not s	sample; inst	ufficient flow						1017
10/20/2008	1136	Could not s	sample; inst	ufficient flow						1013
11/5/2008	1412	Could not s	sample; inst	ufficient flow						1016
11/17/2008	1123	Could not s	sample; inst	ufficient flow		1014				
12/1/2008	1123	Could not s	sample; insi	ufficient flow						1013

		Nitrogen		Hydi	rogen			LPG		CO <sub>2</sub>		Heliu	m	С	DM-INJ1		С	DM-INJ2		(	CDM-INJ3	
Date	Time	Pressure Rotameter (psig) (cfm)	Flow (scfm)	Pressure Rotar (psig) (cf			Pressure (psig)	Rotameter (cfh)	Flow (scfm)	Pressure Rotamet (psig) (cfh)	er Flow (scfm)	Pressure Rotam (psig) (cfm		ressure R (psig)		Flow (scfm)	Pressure R			Pressure F (psig)		Flow (scfm)
12/12/2007	1559	34 48	89	, <u>, , , , , , , , , , , , , , , , , , </u>	0	0.0	34	, ,	0.00	34	0 0.00		0 0.0	34	0	0	Δ	50	57.5	34	0	0
12/12/2007	1605		76		0	0.0	29		0.00	29	0 0.00		1.4 6.5	29	0	0		50	65.0	29	0	0
12/12/2007	1611		87		0	0.0	32		0.00	32	0 0.00		0 0.0	32	0	0	4	50	57.5	32	0	
12/12/2007	1645	3 10	11		0	0.0	32	0	0.00	32	0 0.00		0 0.0	32	0	0	2	9.5	10.6	32		
12/13/2007		5 10			0		27	0		27				27	0	0	3	50	57.5	27		0
	845		76		4.0	0.0	27		0.00	27	0.00		0 0.0	27	0	0	4			27	- 0	0
12/13/2007	826		68		1.2	7.6	26		0.00	26	0.00		0 0.0	26	0	0	4	50	73.4	26	- 0	0
12/13/2007	1416		90		0	0.0	34.5				0.74		0 0.0	34.5	0	0	4	50	57.3	34.5	0	0
12/13/2007	1600	35 52	98		0	0.0	35	28		35 3	0.79		0 0.0	35	0	0	5	50	58.9	35	0	0
12/13/2007	1605		10		0	0.0	0	0	0.00	0	0.00		0.0		0	0			0.0		0	0
12/14/2007	930		22		0	0.0	52	0	0.00	52	0.00		0 0.0	52	0	0	1	8	8.4	52	0	0
12/26/2007	1347	44 5	10	44	0.25	1.9	44	0	0.00	44	0.00	44	0.0	0	0	0	0	10	14.6	0	0	0
12/26/2007	1347	Start test; Target = 9 cfm N2, 1 cfm	n H2																			
12/26/2007	1425	48 5	11	48	0.3	2.4	48	0	0.00	48	0.00	48	0.0	0	0	0	0	10	15.3	0	0	0
12/26/2007	1425	Increase H2 flow, Re-adjust to 0.25	5 on rotameter																			
12/27/2007	921	44 5	10	44	0.3	2.3	44	0	0.00	44	0.00	44	0.0	0	0	0	1.5	8	12.9	0	0	0
12/27/2007	922	44 5	10	44	0.3	2.3	44	0	0.00	44	0.00	44	0.0	0	0	0	1.5	10	16.1	0	0	0
12/27/2007	1635	Pat decides to shut off H2, decreas	se nitrogen to 5cfm o	ver the weekend																		
12/27/2007	1645	57 5	11	57	0	0.0	57	0	0.00	57	0.00	57	0.0	0	0	0	2	5	5.4	3	0	0
1/2/2008	928	56 5	11	56	0	0.0	56	0	0.00	56	0.00	56	0.0	1	0	0	1	5.5	5.8	0	0	0
1/2/2008	929	Nitrogen Tank=12 inches H2O																				
1/2/2008	1148	53 5	11	53	0	0.0	53	0	0.00	53	0.00	53	0.0	0	0	0	0	4.5	4.6	0	0	0
1/2/2008	1256	0 0	0	0	0	0.0	0	0	0.00	0	0.00	0	0.0	0	0	#DIV/0!	0	0 #D	DIV/0!	0	0	#DIV/0!
Tracer Test #1 (10 cfm	to INJ2, ~7	H2)																				
1/21/2008	729 (N2 Flush)	8 82	104	8.0	0	0.0	8	0	0.00	8	0 0.00	8	0 0.0	2	39	42.4	1.5	40	42.8	0.5	40	41.5
1/21/2008	1046 (test start)	2 8	8.7		0.2	0.81	2	0	0.00	2	0 0.00	2	0 0.0	3	0	0	1	10	13.0	0	0	0
1/21/2008		2 8	8.7		0.2	0.81	2	0	0.00	2	0 0.00		0 0.0	2	0	0	1.5	10.5	13.9	0	0	0
1/22/2008			8.8		0.2	0.82	2.5	0	0.00	2.5	0 0.00		0 0.0	3	0	n	2	10	13.4	0	0	
1/23/2008			8.8		0.2	0.82	2.5		0.00	2.5	0 0.00		0 0.0	2.5	0	0	1.5	10	13.2	0	0	
1/23/2008	1229 (test	0 0	0.0		0.2	0.0	۸.	0	0.00	0	0 0.00		0 0.0	0	0	#DIV/0!	1.0	0 #D		0		#DIV/0!
1/25/2000	Jonu)	<u> </u>	0.0	<u>⊓ Ч</u>	<u> </u>	0.0	0	1 0	0.00	<u> </u>	U <sub>1</sub> 0.00	71 YI	<b>υ</b> Ι υ.υ	<u> </u>	- V	#DIV/0:	<u> </u>	Ο <sub> </sub> #Δ	٧/٥:	<u> </u>		"DIV/U:
Tracer Test #2 (20 cfm		% H2)																				
1/18/2008	1120 (test start)	50.5 8	17	50.5	0.3	2.4	50.5	0	0.00	50.5	0.00	50.5	0.0	0	0	0	0	20	27.3	0	0	0
1/18/2008	1655	52 8	17	52	0.2	1.6	52	0	0.00	52	0.00	52	0.0	0.5	0	0	0.5	18.5	23.7	0	0	0
1/19/2008	838	52 8	17	52	0.2	1.6	52	0	0.00	52	0.00	52	0.0	2	0	0	1	17	22.1	0	0	0
1/19/2008		Notice pressure in 2nd H2 18-pack	x = 0 psi; open valve	to 3rd H2 18-pack (cl	lose valve	to 2nd 18-pack	k); adjust H	2 rotameter to 7.	9% H2 at INJ2 (@	1050 am H2 = 5.8%	at INJ2)											
	•								,		,	. ,	•		·			ı				

			Nitr	rogen		Hydrogen			LPG			CO <sub>2</sub>			Helium			CDM-INJ1			CDM-INJ2			CDM-INJ3	
Date	Time	Pressure	Rotameter	Flow		Rotameter	Flow	Pressure	Rotameter		Pressure Ro	otameter		Pressure F			Pressure				Rotameter			Rotameter	
	1215 (test	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
1/19/2008	end)	0	8	8	0	0	0.0	0	0	0.00	0	0	0.00	0	0	0.0	0	0	0	C	0	0.0	0	0	0
1/19/2008	1216 (N2	6.5	82	2 100	6.5	0	0.0	6.5	0	0.00	6.5	0	0.00	6.5	0	0.0	0	39	39.8	,	40	40.8	0	40	40.8
	1230 (end		02	100	0.0			0.0			0.0	J		0.0			J	- 00						10	
1/19/2008	N2 flush)	0	C	0	0	0	0.0	0	0	0.00	0	0	0.00	0	0	0.0	0	0	#DIV/0!	C	0	#DIV/0!	0	0	#DIV/0!
Tracer Test #3 (30 cfm	to INJ2, ~4	1%H2)																							1
1/30/2008	854 (begin	1 8	82	2 104	. 8	0.00	0.0	8	0	0.00	8	0	0.00	8	0	0.0	3	39	43.7	1.5	40	42.8	0.5	40	41.48826
			!	•		0.00	0.0			0.00		J	0.00	J		0.0			10.7	1.0	10	12.0	0.0	10	11.10020
1/30/2008	Nitrogen ta	ank = 36" Hyd 	drogen 18-pack	ks = 700, 200, 850 psi																					
1/30/2008	N2 flush)	1.0	C	0	1	0.00	0.0	1	0	0.00	1	0	0.00	1	0	0.0	2	0	#DIV/0!	0.5	0	#DIV/0!	0	0	#DIV/0!
1/30/2008	1013 (no s	start test - NC	(GO)																						1
1/30/2008	1020 (Can	't aet hydroa	en to flow: Calle	ed pat and Praxair to reset p	ressure on N2 t	tank)																			1
	1036(test																								
1/30/2008	start)	16.0	17	7 25	16	0.30	1.7	16	0	0.00	16	0	0.00	16	0	0.0	2	0	0.0	0.5	30	36.4	0	0	0
1/30/2008	1402	16.0	17	7 25	16	0.30	1.7	16	0	0.00	16	0	0.00	16	0	0.0	0	0	0.0	С	30	35.8	0	0	0
1/30/2008	1528	16.0	17	7 25	16	0.30	1.7	16	0	0.00	16	0	0.00	16	0	0.0	0	0	0.0	c	30	35.8	0	0	0
1/30/2008	Nitrogen to	ank – :Hydro	gen 18-nacke -	= 650, 100, 900 psi																					1
1/31/2008	844	19.0	17	7 26	19	0.20	1.2	19	0	0.00	19	0	0.00	19	0	0.0	2.5	0	0.0	2	30	36.4	0	0	0
1/31/2008	Nitrogen ta	ank = 23";H	ydrogen 18-pac	cks = 0, 0, 850 psi																					
1/31/2008		12.0	20	27	12	0.30	1.5	12	0	0.00	12	0	0.00	12	0	0.0	3	0	0.0	2	30	37.3	0.5	0	0
1/31/2008	1435 (test	2.0		0	2	0.00	0.0	2	0	0.00	2	0	0.00	2	0	0.0	2.5	0	#DIV/0!	1.5	. 0	#DIV/0!	0.5	0	#DIV/0!
,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	, , , , , , , , , , , , , , , , , , , ,			-					-									-							
Tracer Test #4 (60 cfm	to INJ2)																								
1/28/2008		Nitrogen tar	nk = 35.5"	Hydrogen 18-pack = 2300 p	osi																				
1/28/2008	1236 (test start)	46	28	58	46	0.70	5.4	46	0	0.00	46	0	0.00	46	0	0.0	0.5	0	0.0	0.5	58*	#VALUE!	0	0	0
1/28/2008	1402	2 47	27	7 56	47	0.65	5.1	47	0	0.00	47	0	0.00	47	0	0.0	0	0	0.0	0.5	58*	#VALUE!	0	0	
			l.		1	0.03	3.1		0	0.00	47		0.00	47	0	0.0	0	0	0.0	0.0	30	#VALUE:		0	
1/28/2008	1630	Nitrogen tar	nk = 30.0"	Hydrogen 18-pack = 1700 p	osi																				
1/29/2008	730 1019 (end	54	27	7 60	54	0.65	5.4	54	0	0.00	54	0	0.00	54	0	0.0	2	0	0.0	2.5	58*	#VALUE!	0.5	0	0
1/29/2008	test)	Nitrogen tar	nk = 9.0"	Hydrogen 18-packs = 700,	200, 850 psi			Note - did not r	ecord final read	ings on control par	nel, just noted	gas levels	3												İ
1/29/2008	1020 (begin N2	8	85	5 108	. 8	0	0.0	8	0	0.00	8	0	0.00	8	0	0.0	3.5	40	45.4	2.5	40	44.1	1.0	40	42.2
	1246 (end		00	100			0.0			0.00		J	0.00	J		0.0	0.0	10	10.1	2.0	10		1.0	10	12.2
1/29/2008	N2 flush)																								
Tracer Test #5 (90 cfm	to INJ2, Ta	arget ~3% H2	2)																						
2/5/2008	953	Nitrogen tar	nk = 54 psi. 36"	Hydrogen =59 psi; 2200, 59	& 2200. 60. 22	250																			1
							2.7	24	0	0.00	24	0	0.00	24	0	0.0	0	0	0.0	2.5	- FO	#\/^    =	0	0	0
2/5/2008		24				1		24	0	0.00	24	U	0.00	24	U	0.0	0	0	0.0	2.5	>50	#VALUE!	0	0	0
2/5/2008	1015 (test	4	70	Not sure if N2 flow is right;	call Pat, restart	; Test N2 to	all 3 INJs														-				
2/5/2008	start)	22	50	81	22	0.65	3.9	22	0	0.00	22	0	0.00	22	0	0.0	0	0	0.0	2	>50	#VALUE!	0	0	0
2/5/2008	1618	3 22	48	3 77	. 22	0.65	3.9	22	0	0.00	22	0	0.00	22	0	0.0	0.5	0	0.0	3	>50	#VALUE!	0	0	0
				; Hydrogen = 55 & 2000, 55		L				1.50					-	2.3	5.5								
	1	printingen tar	in = 00 psi, 2/	, riyuruyeri = 55 & 2000, 55 (	u 1300, 33 & Z	200	1		l											l	1				

				Nitrogen			Hydrogen			LPG			CO <sub>2</sub>			Helium			CDM-INJ1			CDM-INJ2			CDM-INJ3	
Date 1	Time	Pressure	Rotame	ter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter		Pressure	Rotameter		Pressure	Rotameter	Flow	Pressure	Rotameter		Pressure F	Rotameter	Flow
	1635 (test	(psig)	(cfm)		(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
2/5/2008 6	end)	2		0	C	0 2	0	0.0	2	. 0	0.00	2	0	0.00	2	0	0.0	0.5	0	#DIV/0!	1.5	0	#DIV/0!	0	0	#DIV/0!
	1636 (N2	0		00	404	4		0.0			0.00	0	0	0.00	0	0	0.0	0	20	40.4	0	40	40.5	0.5	40	
2/5/2008 f	1730 (end	8		82	104	4 8	0	0.0	<u>8</u>	0	0.00	8	U	0.00	8	0	0.0		39	42.4		40	43.5	0.5	40	41.5
2/5/2008		0		0	C	0 0	0	0.0	C	0	0.00	0	0	0.00	0	0	0.0	0	0	#DIV/0!	0	0	#DIV/0!	0	0	#DIV/0!
Tracor Tost #6 (30 cfm to	otal 10 of	m each to IN	11 2 and	2+. 90/. U2\																						
Tracer Test #6 (30 cfm to	otai, 10 cr	m each to in	J1, 2, and	3;~6% ⊓2 <u>)</u>																						
2/7/2008	839	Begin N2 flus	sh; N2 trai	ler = 6"																						
2/7/2008	1016	End N2 flush	; N2 traile	r = 1", will re	sume flushing after	Praxair refills to	ank																			
2/7/2008	1150	Resume N2 f	flush: at 1	455 still have	e N2 at 1.5 - 1.8% at	t some points:	decdide to st	tart test and ru	n H2 at 7-8%																	
1	1500 Test		,								0.00	07	0	0.00	07	0	0.0		4.0	40.0		40	40.0		40.0	40.0
2/7/2008 s	start	27		15	26	6 27	0.50	3.2	27	0	0.00	27	0	0.00	27	0	0.0	0	10	13.3	0	10	13.3	0	10.0	13.3
2/8/2008	836	30		14	25	5 30	0.55	3.7	30	0	0.00	30	0	0.00	30	0	0.0	2	10	14.7	1	10	14.2	0	9.0	12.4
	1103	26		15	25	5 26	0.55	3.5	26	0	0.00	26	0	0.00	26	0	0.0	0	10	13.6	0	10	13.6	0	10.0	13.6
	1104 End test	0		0		0	0.00	0.0		0	0.00	0	0	0.00	0	0	0.0	0	0	#DIV/0!	0	0	#DIV/0!	0	0.0	#DIV/0!
		U U		<u> </u>		<u> </u>					0.00	U	U	0.00	U	0	0.0	0	0	#DIV/0:	0	U	#DIV/U:		0.0	#DIV/0:
	1105	N2 trailer = 2	1" ; H2 18	s-packs = 65	0, 50, 2250 psi (~22	250 psi = full 18	-pack, 3600	cfm per 18-pag	ck)										<u> </u>							
Tracer Test #7 (60 cfm to	otal: 20 cf	m to each IN	.l1 2 and	13 ~5% H2)																						
			5 1, <u>2</u> , and	70 112)																					$\overline{}$	
1/17/2008	859 900 (test	0		0	С	0 0	0	0.0	C	0	0.00	0	0	0.00	0	0	0.0	3	0	#DIV/0!	1	0	#DIV/0!	0	0	#DIV/0!
1/17/2008 s		3		50	56	6 3	0.85	3.6	3	0	0.00	3	0	0.00	3	0	0.0	3	22	28.6	1	20	24.5	0	22	26.1
1/17/2008	1210	2.5		50	55	5 2.5	0.82	3.4	2.5	0	0.00	2.5	0	0.00	2.5	0	0.0	1	22	26.9	0.5	20	24.0	. 0	22	26.0
				50								-	-		0	-		0.5								
1/17/2008	1554 1650 (end			50	56	0 3	0.84	3.5	3	0	0.00	3	0	0.00	3	0	0.0	0.5	22	26.5	0.5	20	24.1	0	22	26.1
1/17/2008 t		3		50	56	6 3	0	0.0	3	0	0.00	3	0	0.00	3	0	0.0	0.5	22	22.8	0.5	20	20.7	0	22	22.4
1/17/2008 f	1651 (N2 flush)	8		80	101	1 8	0	0.0	8	0	0.00	8	0	0.00	8	0	0.0	2	36	39.1	1.5	38	40.7	0.5	38	39.4
1/17/2008 f	1750 (N2	60		0		0		0.0			0.00	0	0	0.00	0	0	0.0	0	0	0.0	0	0	0.0	0	0	0.0
	817 (N2	60		U		0	, 0	0.0		0	0.00	U	U	0.00	U	U	0.0	- 0	Ť		0	U	0.0			0.0
1/18/2008 f	flush) 1051(begi	8		80	101	1 8	0	0.0	8	0	0.00	8	0	0.00	8	0	0.0	4	36	41.4	2.5	38	41.9	1.5	38	40.7
1/18/2008 r		50		8	17	7 50	0	0.0	50	0	0.00	50	0	0.00	50	0	0.0	0	0	0	0	20	20.4	0	0	0.0
Tracer Test #8 (90 cfm to	otal; 30 cf	m each to IN	J1, 2, and	l 3; ~4.5% H	2)																					
2/6/2008	806	Begin N2 flus	sh																							
2/6/2008	959	End N2 flush																								
	1000 Test	38		40	77	7 38	0.7	E 4	38	_	0.00	38		0.00	38		0.0	_	20	20.4	0.5	20	36.3		30	25.7
				40					38	0	0.00		U		38	0			30					- 0		
2/6/2008	1705 1706 Test			40	79	9 41	0.75	5.6	41	0	0.00	41	0	0.00	41	0	0.0	2	30	38.5	0.5	30	36.7	0	30	36.1
2/6/2008 E		2		0	0	0 2	2 0	0.0	2	0	0.00	2	0	0.00	2	0	0.0	1.5	0	#DIV/0!	1	0	#DIV/0!	0	0	#DIV/0!
				<del></del>				· <u> </u>							<del></del>											
Optimization Test #1 (90	0 cfm to IN 1206 Test		rs, then s	hut down; 8	88% N2, 10% H2, 1%	% CO2, 1% LP	G)																			
2/20/2008 \$		23		44	72	2 23	2.3	14.0	23	66	1.41	23	68	1.47	23	0	0.0	1.5	0	0.0	3.5	>50 #	VALUE!	0	0	0.0
2/20/2008	1602	22		45	73	3 22	1.75	10.5	22	68	1.43	22	35	0.75	22	0	0.0	0	0	0.0	2.5	>50 #	VALUE!	0	0	0.0
1	1606 Test			0									20						Ť							
2/20/2008 E	⊨na	48		U	C	0 48	sj 0	0.0	48	0	0.00	48	0	0.00	48	0	0.0	0	0	#DIV/0!	0	U	#DIV/0!	0	0	#DIV/0!

			Nitro	ogen		Hydrogen			LPG			CO <sub>2</sub>			Helium		(	CDM-INJ1			CDM-INJ2			CDM-INJ3	
Date Tin	ne		Rotameter	Flow		Rotameter	Flow	Pressure	Rotameter			Rotameter	Flow		Rotameter		Pressure I				Rotameter			Rotameter	
		(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
															•							_			
Optimization Test #2 (30 c	fm to INJ	2 for 12 hours	s, then shut	down; 88% N2, 10% H2, 1	% CO2, 1% LP	G)																			
2/25/2008 sta	45 Test ert	5.5	23	28	5.5	0.6	2.7	5.5	22	0.34	5.5	22	0.35	5.5	0	0.0	2	0	0.0	2	30	40.2	0	0	0.0
2/26/2008	643	6	21	25	6	0.6	2.7	6	10	0.16	6	27	0.43	6	0	0.0	4	0	0.0	3	29	40.7	0.5	0	0.0
2/26/2008 En	3 Test d	54	0	0	54	0	0.0	54	0	0.00	54	0	0.00	54	0	0.0	4	0	#DIV/0!	2	0	#DIV/0!	0	0	#DIV/0!
Optimization Test #3A (1 c	fm to INJ	2; ~88% N2, 1	0% H2, 1%	CO2 & LPG)																					
2/29/2008 sta	19 Test rt T	otal Flow = 60	ofh (N2 = 53	3, H2 = 6, CO2 & LPG = 0.6	cfh)																				
3/3/2008		otal Flow = 57																							
	30 Test		-																						
0/0/2000   2.11	<u> </u>				<u> </u>	I		1		L						<u> </u>	ı					L	ı		
Optimization Test #3B (1 c	fm to IN I	1. IN.I2. & IN	l3. ~0.33 cfh	n per well:~88% N2 10% H	2. 1% CO2 & I	PG)																			
	30Test			INJ2 & INJ3 (approx. 0.33																					
3/4/2008		otal Flow = 56		11402 & 11400 (approx. 0.00 t	Jilli per well)																				
3/7/2008		otal Flow = 30																							
130	06 Test		CITI																						
3/7/2008 En	u [1	otal Flow = 0									l														
Optimization Test #3C (90	06	J1, INJ2 & IN			% N2, 10% H2																				
3/7/2008 Sta	21	4	60	69	4	2.4	10.3	4	240	3.61	4	67	1.02	4	0	0.0	0	29	39.2	0	30	40.5	0	30	40.5
3/7/2008 En	dPulse	60	0	0	60	0	0.0	60	0	0.00	60	0	0.00	60	0	0.0	2	0	#DIV/0!	2	0	#DIV/0!	0	0	#DIV/0!
Optimization Test #4 (30 c	fm to INJ	1, INJ2 & INJ3	3 (10 cfm ea	ch) for 45 minutes, then 3	0 cfm to INJ2 f	or 45 minute	s;~79% N2,	10% H2 & LPG	, 1% CO2)																
12		ollowed by 1	5 minutes da	aily pulses at 30 cfm to IN	J2 while maint	aing~30 cfh	the rest of th	ne time																	
3/10/2008 Sta		0.5	21	22	0.5	0.85	3.3	0.5	>100	#VALUE!	0.5	22	0.30	0.5	0	0.0	0	10	#VALUE!	0	10	#VALUE!	0	10	#VALUE!
3/10/2008	1302 47	3	19	21	3	0.85	3.6	3	>100	#VALUE!	3	22	0.33	3	0	0.0	2	0	#VALUE!	2	30	#VALUE!	0	0	#VALUE!
3/10/2008 En		otal flow = 30	cfm																						
		otal flow = 48	cfm																						
950 3/11/2008 Sta	artpules	18	13	20	18	0.85	4.8	18	>100	#VALUE!	18	24	0.48	18	0	0.0	0	0	#VALUE!	0	30	#VALUE!	0	0	#VALUE!
3/11/2008 En	05 dpulse T	otal flow = 30	cfm																						
3/12/2008		otal flow = 28	cfm																						
3/12/2008 Sta		22	13	21	22	0.8	4.8	22	>100	#VALUE!	22	22	0.47	22	0	0.0	0.5	0	#VALUE!	0.5	30	#VALUE!	0	0	#VALUE!
3/12/2008 En	32 dpulse T	otal flow = 30	cfm																						
3/13/2008	900 T	otal flow = 23	cfm																						
3/13/2008 Sta		6	13	16	6	0.8	3.6	6	>100	#VALUE!	6	22	0.35	6	0	0.0	1	0	#VALUE!	1	30	#VALUE!	0	0	#VALUE!
3/13/2008 En	0	otal flow = 30	cfm																						
3/14/2008																									
5, : 1,2550					1			ı	1					1	1	<u> </u>			I.			1	Į.		

ĺ		Nitro	ogen		Hydrogen			LPG			CO <sub>2</sub>			Helium			CDM-INJ1		CDM-INJ2		CDM	-INJ3
Date Time	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter			Rotameter	Flow	Pressure	Rotameter Flow	Pressure R	Rotameter		Pressure Rotar	meter Flow
1154 3/14/2008 Startpules	(psig)	(cfm) 40	(scfm)	(psig)	(cfm) 7 2.3	(scfm) 12.9	(psig)	(cfh) >100	(scfm) #VALUE!	(psig)	(cfh)	(scfm) 0.99	(psig) 17	(cfm)	(scfm)	(psig) 0.5	(cfm) (scfm) 0 #VALUE!		(cfm) -50	(scfm) #VALUE!	(psig) (cf	m) (scfm) 0 #VALUE!
3/14/2008 Endpulse				30 11	2.0	12.0	.,	<i>-</i> 100	"THEOL.			0.00		Ů	0.0	0.0	o nvitot.		-00	WVYLOL.	Ŭ	o nvilor.
3/15/2008 1105	Total flow = :	52 cfm																				
3/15/2008 Startpules	17	40		60 17	7 2.35	13.1	17	>100	#VALUE!	17	66	1.31	17	0	0.0	0	0 #VALUE!	1.5 >	·50	#VALUE!	0	0 #VALUE!
1204 3/15/2008 Endpulse	Total flow = 3	30 cfm																				
	Total flow = :	22 cfm																				
3/16/2008 Startpules	4	15		17 4	4 2.3	9.9	4	>100	#VALUE!	4	66	1.00	4	0	0.0	0	0 #VALUE!	0	30	#VALUE!	0	0 #VALUE!
3/16/2008 Endpulse	Total flow = 3	30 cfm																				
3/17/2008 907	Total flow =	14 cfm																				
Optimization Test #5 (20 cfm to IN	J2 for 125 m	ninutes while n	naintaing 30 cfh the	rest of the time;~80	0% N2, 10%	H2 & LPG)																
3/17/2008 StartPulse 1242	5	11		13 5	5 0.6	2.6	5	>100	#VALUE!	5	0	0.00	5	0	0.0	0	0 #VALUE!	0	20	#VALUE!	0	0 #VALUE!
3/17/2008 Endpulse	Total flow = 3	30 cfm																				
3/18/2008 930	Total flow = 8	8 cfm																				
3/18/2008 931	Total flow = 3	36 cfm																				
3/19/2008 943	Total flow = 2	22 cfm																				
3/20/2008 927	Total flow =	19 cfm																				
Optimization Test #6 (50 cfh to P4	-18 & P4-28;	~80% N2, 10%	6 H2 & LPG)																			
	Total flow =	50 cfh																				
3/21/2008 945	Total flow =	50 cfh																				
3/24/2008 935	Total flow =	49 cfh																				
3/26/2008 910	Total flow =	50 cfh																				
3/26/2008 1055	Total flow =	57 cfh																				
3/28/2008 920	Total flow =	57 cfh																				
3/31/2008 1030	Total flow =	57 cfh																				
4/2/2008 920 1233	Total flow =	57 cfh																				
4/2/2008 (Test 7)	P4-18, -28, -	38 = 20 cfh eac	ch (60cfh total)		Control Pa	nel = 33 cfh, 34	l psi															
Optimization Test #7A (60 cfh to P	4-18, -28, -3	8 (20 cfh each)	), 10% H2 & LPG)																			
4/2/2008 (StartTest)	P4-18, -28, -	38 = 20 cfh eac	ch (60cfh total)		Control Pa	nel = 33 cfh, 34	l psi															
4/4/2008 913	P4-18 = 24 c	ofh, P4-28 = 23	cfh, P4-38 = 21 cfh			Control Panel	= 39 cfh, 34 psi															
4/4/2008 1005	O2 = 0.0% H	12 = 6.9% LPG	= 13.5%																			
4/4/2008 1006	Reset: P4-18	8, -28, -38 = 20	cfh each		H2 = 8.0%	LPG = 10.5%																
4/7/2008 1343	P4-18 = 20 c	ofh, P4-28 = 19	cfh, P4-38 = 20 cfh			Control Panel	= 33 cfh, 34 psi															
4/7/2008 1456	Control Pane	el = 57 cfh, 32 p	osi P4-18, -28, -38, -48	8 = 25, 25, 24, 24 cfl	h (98 cfh tota	al)																

	Nitrogen		Hydrogen			LPG			CO <sub>2</sub>			Helium			CDM-INJ1			CDM-INJ2		(	CDM-INJ3	
Date Time	Pressure Rotameter Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter			Rotameter		Pressure	Rotameter		Pressure	Rotameter	Flow	Pressure F	Rotameter	Flow
1458 start	(psig) (cfm) (scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
4/7/2008 test 7B	Set P4-18 & P4-28 = 30 cfh each (60 cfh total)																					
Optimization Test #7B (60 cfh to I	P4-18, & P4-28, (30 cfh each), 10% H2 & LPG)																					
1458 start 4/7/2008 test 7B	Set P4-18 & P4-28 = 30 cfh each (60 cfh total)																					
4/9/2008 1016	Control Panel = 37 cfh, 34 psi	P4-18 = 33 cf	h; P4-28 = 3	3 cfh																		
4/9/2008 1154	H2 = 1.8%; LPG = 1.74%; O2 = 0.0%																					
4/9/2008 1242	H2 = 8.4%; LPG = 9.5%; 02 = 0.0%; P4-18 = 30 cfh; P	P4-28 = 30 cfh																				
	Control Panel = 35 cfh, 28 psi	P4-18 = 29 cf	h· P4-28 = 2	9 cfh																		
	Open up P4-18 & P4-28 all the way to >40 cfh each	1 1 10 200	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,																			
4/10/2000 1121	Open up F4-10 & F4-20 all the way to >40 till each							<u> </u>						l					l			
Optimization Test #7C (100 cfh to	P4-18, & P4-28, (50 cfh each), 10% H2 & LPG, 1% C	(02)																				
4/10/2008 test	Control Panel = 55 cfh, 33 psi	P4-18 = >40 (	ofh; P4-28 =	>40 cfh																		
4/11/2008 1205	Control Panel = 54 cfh, 32 psi	P4-18 = >40 (	ofh; P4-28 =	>40 cfh																		
4/11/2008 1205	32.0 54 98.	<mark>.2</mark>																				
4/11/2008 1422	Propane tank filled, tank volume = 80%, 38 psi																					
4/11/2008 1515	P4-18 = >40 cfh; P4-28 = >40 cfh, H2 = 8.5%, LPG = 1	11.0%																				
4/11/2008 1516	Control Panel = 50 cfh, 26 psi																					
4/14/2008 940	Control Panel = 34 cfh, 11 psi	P4-18 = 20 cf	h; P4-28 = 2	0 cfh	H2 = 15%, LPC	G = 26%		Propane ta	nk = 63%, 3	38 psi												
4/14/2008 1154	Control Panel = 58 cfh, 35 psi	P4-18 = >40 (	ofh; P4-28 =	>40 cfh		H2 = 9.7%, LPG	i = 10.5%, CO2 =	1.10%														
4/16/2008 1005	Control Panel = 57 cfh, 35 psi	P4-18 = >40 d	ofh; P4-28 =	>40 cfh																		
4/16/2008 1050	H2 = 8.0%, LPG = 10.0%, CO2 = 0.36%		Readjust ra	ites to: H2 = 9.	0%, LPG = 10.5	5%, CO2 = 0.86%	,															
4/16/2008 1115	Connect "T" fittings at P4	P4-18 = 25 +	25 = 50 cfh;	P4-28 = 25 +	24 = 49 cfh																	
	Propane tank = 54%, 38 psi	H2 18-packs :	= 0, 0, 900 p	si (~2300 psi =	full 18-pack)																	
4/17/2008 1000	Control Panel = 57 cfh, 35 psi	P4-18 = 50 cf	h: P4-28 = 4	9 cfh																		
4/17/2008 1001	Begin Nitrogen flush in preparation for drilling																					
4/17/2008	3 60 6	7 3	0	0.0	3	0	0.00	3	0	0.00	3	0	0.0		26	26.5		27	27.5		27	27.5
	Stop Flushing		Ü	0.0	3	· ·	0.00			0.00			0.0		20	20.0		21	21.0		21	27.0
	Propane Tank = 50% full, 38 psi, H2 = 800 psi, N2 = 3	7 nei																				
	CO2 leaking at 16 pack, will call Praxair	psi																				
		D4 40 40 6	D4.00 4	0 "																		
4/18/2008	Control Panel = 58 cfh, 34 psi	P4-18 = 48 cf	n; P4-28 = 4	8 cm																		
	Injected %s> CO2 = 0%, LPG = 10%, H2 = 8%, O2 =																					
	Control Panel = 58 cfh, 34 psi; propane = 31% volume																					
4/22/2008 930	P4-18 = 48 cfh; P4-28 = 48 cfh; H2 = 0 psi (empty); N2	2 = 10"																				
4/22/2008 1056	Injected %s> O2 = 0%, CO2 = 0%, LPG = 12.5%, H	2 =0.91%																				
	Note - out of H2; call praxair for refill; adjust LPG to 10	0.5%																				
4/22/2008 1105	Open up "empty" H2 18-packs, injecting 1.0% H2										1											

6/4/2008

833 Control Panel = 57 cfh, 35 psi

propane = 50% volume, 38 psi

	Nitro	ogen		Hydrogen	ı		LPG			CO <sub>2</sub>			Helium			CDM-INJ1			CDM-INJ2		C	DM-INJ3	
Date Tin	me Pressure Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	-	Rotameter	Flow		Rotameter			Rotameter	Flow	Pressure	Rotameter		Pressure R		Flow
	(psig) (cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
4/23/2008	914 Injected %s> O2 = 0%, C																						
4/23/2008	916 P4-18 = 49 cfh; P4-28 = 48	· · · · · · · · · · · · · · · · · · ·	35 psi																				
4/23/2008	Propane = 26% volume, 38	•	<u> </u>																				
4/25/2008	900 Control Panel = 57 cfh; prop	•		0/ 00 00/																			-
4/25/2008 4/25/2008	938 Control Panel = 58 cfh, 34 p 938 P4-18 = 48 cfh, P4-28 = 47			%, O2 = 0%																			
4/25/2008	H2, N2, LPG = 37 psi, CO2	· · · · · · · · · · · · · · · · · · ·																					
4/25/2008	1030 Readjust to H2 = 10%, LPG																						
4/29/2008	1047 P4-18 = 48 cfh, P4-28 = 47			ıme 37 nei				H2 18-packs = 2	300/38 pei:	1800/38 ps	i: 2300/39 n	l vei											-
4/29/2008	1048 Control Panel = 58 cfh, 34 p							CO2 = 740/46  ps		1000/30 ps	i, 2300/39 p	751											-
4/29/2008	1145 Readjust to H2 = 10%, LPG	· · · · · · · · · · · · · · · · · · ·	,	70, 02 = 070	,			CO2 = 140/40 ps	31														
5/5/2008	1336 P4-18 = 47 cfh. P4-28 = 47	· · · · · · · · · · · · · · · · · · ·		-> O2 = 0%	CO2 = 0.92%	, LPG = 10.0%,																	
5/5/2008	1340 Control Panel = 57 cfh, 33 p		propane = 80			1		00/38 psi; 2400/38	l nsi		CO2 = 840	1/58 nsi											
5/5/2008	1344 N2 = 12", 36 psi	201	ргорано – оо	To volumo,	00 poi	112 10 paono –	2 100/00 poi, 00	70,00 poi, 2 100,00	7 501		002 - 010	5/00 poi											
5/5/2008	1350 Readjust to H2 = 9.5%, LPG	3 = 9.5% CO2 = 0.84% O2	? = 0%			P4-18 = 48 cfh	P4-28 = 47 cfh	1															
5/13/2008	837 Control Panel = 57 cfh, 34 p	· · · · · · · · · · · · · · · · · · ·	propane = 50	1% volume :	38 psi		20																
5/13/2008	841 H2 18 packs = 2300/36psi;			10.0	1																		
5/13/2008	843 N2 = 22", 36 psi																						
5/13/2008	856 P4-18 & 28 = 47 cfh;		Injected %s -	-> O2 = 0%	. CO2 = 1.72%	, LPG = 11.0%,	H2 =1.2%																
5/13/2008	1010 Change CO2 tank source: C	CO2 = 900/62 psi																					
5/13/2008	1040 Readjust to H2 = 10%, LPG	G = 9.5%, CO2 = 1.00%, O2	= 0%			P4-18 & 28 = 4	7 cfh																
5/20/2008	853 Control Panel = 57 cfh, 35 p	osi	propane = 60	% volume,	38 psi																		
5/20/2008	855 H2 18 packs = 2300/36psi;	0/35 psi; 0/36 psi; CO2 = 66	60/58 psi																				
5/20/2008	858 N2 = 35", 37 psi																						
5/20/2008	909 P4-18 & 28 = 47 cfh;		Injected %s -	-> O2 = 0%	CO2 = 1.00%	, LPG = 9.5%, H	2 =4.2%																
5/20/2008	1052 Readjust to H2 = 10%, LPG	G = 9.5%, CO2 = 0.94%, O2	= 0%			P4-18 & 28 = 4	7 cfh																
5/23/2008	842 Control Panel = 56 cfh, 35 p	osi	propane = 50	% volume,	38 psi																		
5/23/2008	844 H2 18 packs = 2200/39psi;	0/38 psi; 0/38 psi; CO2 = 66	60/58 psi																				
5/23/2008	846 N2 = 30", 37 psi																						
5/23/2008	918 P4-18 & 28 = 47 cfh;		Injected %s -	-> O2 = 0%	, CO2 = 1.02%	, LPG = 10%, H	2 =4.2%																
5/23/2008	948 hooked up H2 6 pack to line	e: 1950/36 psi																					
5/23/2008	1032 readjust injection %'s: H2 =	9.8%, LPG = 9.5%, CO2 =	1.06%, O2 = 0	0.0%																			
5/23/2008	1336 readjust injection %'s: H2 =	10%, LPG = 9.5%, CO2 = 1	1.06%, O2 = 0.	.0%																			
5/23/2008	1450 Check injection %'s: H2 = 1	0%, LPG = 9.5%, CO2 = 1.0	02%, O2 = 0.0	%																			
5/23/2008	1550 Check injection %'s: H2 = 9.	.4%, LPG = 9.0%, CO2 = 1.	.14%, O2 = 0.0	)%			P4-18 & 28 = 4	7 cfh	1	1	ļ												
5/27/2008	826 Control Panel = 57 cfh, 35 p	osi	propane = 30	% volume,	37 psi				1	1	ļ												
5/27/2008	828 H2 18 packs = 1500/40psi;	H2 6 pack: 1800/40 psi; CO	2 = 380/64 psi	i					1		<u> </u>												
5/27/2008	830 N2 = 22", 38 psi								4														
5/27/2008	844 P4-18 & 28 = 47 cfh;		Injected %s -	-> O2 = 0%	, CO2 = 2.48%	, LPG = 11%, H	2 =9.5%		4														
5/27/2008	935 readjust injection %'s: H2 =	9.8%, LPG = 10%, CO2 = 0	0.98%, O2 = 0.	.0%		1			4														
5/28/2008	900 Hook up 2 H2 18 packs: 230	00/40 psi; 2300/40psi							4														
5/28/2008	905 Check injection %'s: H2 = 9	.9%, LPG = 10.5%, CO2 = 1	1.20%, O2 = 0	.0%	]				4														

	Nitro	ogen		Hydrogen			LPG			CO <sub>2</sub>			Helium		C	DM-INJ1			DM-INJ2			CDM-INJ3	
Date Tim		Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure Rot		Flow	Pressure I		Flow	Pressure R		Flow	Pressure F	otameter	Flow		Rotameter	Flow
	(psig) (cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig)	(cfh) (:	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)		(cfm)	(scfm)	(psig)	(cfm)	(scfm)
6/4/2008	835 H2 18 packs = 600/40psi; 23	300/40 psi; 2300/40 psi; CC	02 = 20/46 psi						-														
6/4/2008	837 N2 = 37", 37 psi																						
6/4/2008	846 P4-18 & 28 = 47 cfh;		Injected %s -	-> O2 = 0%	, CO2 = 0%, LI	PG = 11%, H2 =	7.6%																
6/4/2008	939 Change CO2 tank source: C	•		<u> </u>																			
6/4/2008	955 readjust injection %'s: H2 =								-														
6/10/2008	841 Control Panel = 57 cfh, 34 p		P4-18 & 28 =	48, 47 cfh;																			
6/10/2008	842 Stop test to drill confirmation								-														
6/10/2008	,	P4-18 & 28 = 48, 47 cfh;																					
6/10/2008	1652 Injected %s> O2 = 0%, C0								-														
6/12/2008	1231 P4-18 & 28 = 48, 46 cfh;		<i>'</i>		,	, LPG = 10.5%,																	
6/12/2008	1232 Control Panel = 56 cfh, 33 p		propane = 20	% volume, 3	37 psi	N2 = 21", 36 p	Si		-														
6/12/2008	1232 H2 18 packs = 0/34psi; 2200		= 920/56 psi																				
6/12/2008	1305 Readjust Hydrogen 18-pack	•							-														
6/12/2008	1305 Injected %s> O2 = 0%, C0					P4-18 & 28 = 4																	
6/20/2008	1103 P4-18 & 28 = 47, 47 cfh;					, LPG = 10.0%,			-														
6/20/2008	1103 Control Panel = 57 cfh, 32 p		propane = 50	% volume, :	37.5 psi	N2 = 30", 35 p	Si																
6/20/2008	1103 H2 18 packs = 0/30psi; 1100																						
6/20/2008	1120 Open new CO2 cylinder. Ac					D. 10.000																	
6/20/2008	1220 Injected %s> O2 = 0.0%,	·				P4-18 & 28 = 4	/ cht																
6/25/2008	1010 Control Panel = 57 cfh, 34 p		propane = 80	% volume, 3	38 psi	N2 = 28"																	
6/25/2008	1010 H2 18 packs = 0/28psi; 1050			22 22/	222 4 222	100 1000																	
6/25/2008	1110 P4-18 & 28 = 48, 47 cfh;					, LPG = 10.0%,	H2 = 10%																
7/2/2008	1054 Control Panel = 56 cfh, 34 p		propane = 50	% volume, 3	38 psi	N2 = 35"																	
7/2/2008	1054 H2 18 packs = 0/24psi; 1050	0/41 psi; 0/40 psi; CO2 = 52	20/56 psi																				
7/2/2008	1054 P4-18 & 28 = 47, 47 cfh;	00 1000/100 100																					
7/2/2008	1221 Injected %s> O2 = 0%, C0	O2 = 1.62%, LPG = 10.5%,	H2 = 10%																				
7/2/2008	1235 Turned CO2 down to 53 psi	00 4000 100 40 50																					
7/2/2008	1235 Injected %s> O2 = 0%, C0	O2 = 1.08%, LPG = 10.5%,	H2 = 10%																				
7/2/2008	1235 P4-18 & 28 = 47, 47 cfh;	D4 00 47 #																					
7/7/2008	1033 P4-18= 47 cfh 1044 Three New H2 18-packs del	P4-28= 47 cfh																					
7/7/2008 7/7/2008	1044 Injected %s> O2 = 0.0%,								1														
		•	0%, ⊓Z = 1Z%						1														
7/7/2008	1044 Control Panel = 57 cfh, 33 p 1044 propane = 30% volume, 37								1														
7/7/2008																							
7/7/2008	1044 H2 18 packs = off; off; 2400	/41 psi																					
7/7/2008	1044 CO2 = >1000/52 psi																						
7/7/2008	1044 N2 = 26" / 36 psi	d = di																					
7/7/2008	1114 Turned all new H2 tanks and																						
7/7/2008	1114 propane = 30% volume, 37	•																					
7/7/2008	1114 H2 18 packs = 2400/41 psi;	2400/41 psi; 2400/41 psi							1														
7/7/2008	1114 CO2 = >1000/53 psi 1114 N2 = 26" / 36 psi					1			†														
7/7/2008	·	Propago = 109/ CO2 109	NOZ HO = 440Z						1														
7/7/2008	1114 Injected %s> O2 = 0.0%,	Propane = 10%, CO2 = 1.00	∪%, HZ = 11%	) <u> </u>		1	l	l	J														

Nitrogen Hydrogen LPG CO2 Helium CDM-INJ1 CDM-INJ Date Time Pressure Rotameter Flow Pressure Rotameter	er Flow Pressure Rotameter Flow
(psig)         (cfm)         (psig)         (cfm)         (psig)         (cfh)         (scfm)         (psig)         (cfh)         (scfm)         (psig)         (cfm)         (	(scfm) (psig) (cfm) (scfm)
	(50)
7/11/2008 1051 Confirmation borings drilled yesterday	
7/11/2008 1051 P4-18= 47 cfh P4-28= 49 cfh	
7/11/2008 1051 Injected %s> O2 = 0.0%, Propane = 10%, CO2 = 1.42%, H2 = 13%	
7/11/2008 1053 Control Panel = 58 cfh, 34 psi	
7/11/2008 1053 propane = 16% volume, 37 psi	
7/11/2008 1053 CO2 = 840/54 psi	
7/11/2008 1053 N2 = 18" / 36 psi	
7/11/2008 1109 Adjusted tank pressures	
7/11/2008 1109 propane = 16% volume, 37 psi	
7/11/2008 1109 H2 18 packs = 2300/40 psi; 1650/40 psi; 2300/40 psi	
7/11/2008 1109 CO2 = 840/52 psi	
7/11/2008 1109 N2 = 18" / 36 psi	
7/11/2008 1109 Injected %s> O2 = 0.0%, Propane = 10%, CO2 = 1.16%, H2 = 11%	
7/11/2008 1109 P4-18= 47 cfh P4-28= 49 cfh	
7/18/2008 946 Control Panel = 56 cfh, 34 psi	
7/18/2008 946 propane = 48% volume, 38 psi	
7/18/2008 946 H2 18 packs = 1100/39 psi; 1600/40 psi; 2400/40 psi	
7/18/2008 946 CO2 = 40/45 psi 7/18/2008 946 N2 = 30" / 36 psi	
7/18/2008 946 P4-18= 46 cfh P4-28= 49 cfh	
7/18/2008 946 Injected %s> O2 = 0.0%, Propane = 11%, CO2 = 0.00%, H2 = 10%	
7/18/2008 1129 Hooked up new CO2 tank and adjusted tank pressures 7/18/2008 1129 propane = 48% volume, 38 psi	
7/18/2008 1129 H2 18 packs = 1100/39 psi; 1600/40 psi; 2400/40 psi	
7/18/2008 1129 CO2 = 900/53 psi	
7/18/2008 1129 N2 = 30" / 36 psi	
7/18/2008 1129 Injected %s> O2 = 0.0%, Propane = 10.5%, CO2 = 0.98%, H2 = 11%	
7/24/2008 1000 Control Panel = 56 cfh, 34 psi	
7/24/2008 1000   H2 18 packs = 40/40 psi; 1650/41 psi; 2400/42 psi	
7/24/2008 1000 CO2 = 820/50 psi	
7/24/2008 1000 N2 = 18" / 36 psi	
7/24/2008 1000 Injected %s> O2 = 0.0%, Propane = 10%, CO2 = 0.66%, H2 = 13%	
7/24/2008 1020 Adjusted tank pressures 7/24/2008 1020 propane = 70% volume, 38 psi	
7/24/2008 1020 H2 18 packs = 40/40 psi; 1650/40 psi; 2400/40 psi	
7/24/2008 1020 CO2 = 820/53 psi	
7/24/2008 1020 N2 = 18" / 36 psi	
7/24/2008 1106 Injected %s> O2 = 0.0%, Propane = 10%, CO2 = 1.06%, H2 = 10%	
7/31/2008 1004 Control Panel = 56 cfh, 34 psi	
7/31/2008 1004   H2 18 packs = 0/40 psi; 700/40 psi; 2100/40 psi	
7/31/2008 1004 CO2 = 800/53 psi	
7/31/2008 1004 N2 = 32" / 36 psi	
7/31/2008 1018 Injected %s> O2 = 0.0%, Propane = 10.5%, CO2 = 1.26%, H2 = 11%	
7/31/2008 1103 Injected %s> O2 = 0.0%, Propane = 10.5%, CO2 = 1.14%, H2 = 10%  8/7/2008 840 Control Panel = 56 cfh, 36 psi	
8/7/2008 840 Control Panel = 56 cm, 36 psi 8/7/2008 840 propane = 75% volume, 38 psi	
8/7/2008 840 H2 18 packs = 0/40 psi; 0/40 psi; 1600/40 psi	
8/7/2008 840 CO2 = 40/44 psi 8/7/2008 840 N2 = 19" / 37 psi	
8/7/2008 840 P4-18= 46 cfh P4-28= 48 cfh P4-28= 48 cfh	
8/7/2008 840 Injected %s> O2 = 0.0%, Propane = 10.5%, CO2 = 0.00%, H2 = 11%	

				Nit	trogen		Hydrogen			LPG			CO <sub>2</sub>		Helium			CDM-INJ1			CDM-INJ2		CI	DM-INJ3	
Date	Tir	me	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure Rot	ameter	Flow	Pressure Rotamete	Flow	Pressure	Rotameter	Flow	Pressure	Rotameter	Flow	Pressure Ro	tameter	Flow
			(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfh)	(scfm)	(psig) (	cfh)	(scfm)	(psig) (cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)	(psig)	(cfm)	(scfm)
	8/7/2008	94	6 Replace CC	O2 source - 860	0/46psi																				
	8/7/2008	100	5 Injected %s	s> O2 = 0.0%	5, Propane = 10%, CO2 = 1.0	2%, H2 = 10%	Ó																		
	8/12/2008	92	8 Control Pan	nel = 56 cfh, 34	psi																				
	8/12/2008	92	8 propane = 5	50% volume, 38	8 psi																				
	8/12/2008	92	8 H2 18 pack	s = 0/39  psi; 0/4	/40 psi; 700/40 psi																				
	8/12/2008	92	8 CO2 = 880/	/46 psi																					
	8/12/2008	92	8 N2 = 10" / 3	36 psi																					
	8/12/2008	92	8 P4-18= 45 (	cfh	P4-28= 49 cfh																				
	8/12/2008	92	8 Injected %s	s> O2 = 0.0%	5, Propane = 10.5%, CO2 = 0	0.00%, H2 = 10	)%																		
	8/12/2008	104	9 Adjusted ta	ink pressures																					
	8/12/2008	104	9 Injected %s	s> O2 = 0.0%	6, Propane = 11%, CO2 = 0.9	92%, H2 = 5%																			

		System	LPG	Panel Sampling Port	Propane	Tank	P4	-18	P4	l-28
Date	Time	Pressure	Rotameter	Rotameter	Pressure	Volume	Rotameter 1	Rotameter 2	Rotameter 1	Rotameter 2
		(psig)	(cfh)	(cfm)	(psig)	(%)	(cfh)	(cfh)	(cfh)	(cfh)
9/8/2008	905	34.5	63	60	38	35	25	25	25	25
9/15/2008	901	33.5	67	60	38	60	25	25	25	25
9/15/2008	948	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
9/29/2008	915	33	75	60	38	60	25	25	25	24
9/29/2008	1010	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
9/30/2008	949	33	75	60	38	47	25	25	25	24
9/30/2008	957	33	74	58			36	36	12	12
9/30/2008	1005	33	74	58			37	36	12	11
10/13/2008	1134	33	77	58	38	85	36	36	12	12
10/13/2008	1222	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
10/20/2008	1105	33	76	58	38	60	35	36	12	12
10/20/2008	1152	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
11/5/2008	1300	34	76	59	38	85	35	36	13	12
11/5/2008	1415	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
11/17/2008	1052	32	76	58	37.5	60	35	37	12	11
11/17/2008	1143	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						
12/1/2008	1035	33	76	59	38	85	34	36	14	12
12/1/2008	1125	Injected %s	> LPG = 30 %	(O2 = 0.0%, CO2 = 0.00%)						

CDM-INJ1

Helium

CDM-INJ2

CDM-INJ3

Source file: Test 8 - 6 Feb 2008.xls

**Phase II Tracer Test Injection Data** 

Well ID \_\_\_\_INJ1\_\_\_\_

				Well or In	jection Ga	s Sample			Well	Ambient Ai
		02	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	emperatur	metric pres
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
12/12/2007	1527							0.18		
12/21/2007	1258	16.2	0.60	0.02	0.22		84.9	0.0	11.4	1012
12/27/2007	1304	9.6	0.58	0	2.4		78.9		9	1016
Tracer Test #			H2)							
	1046 Test s									
1/21/2008		1.8	0	0	0.022		58.8	0.03	9.9	1008
1/23/2008	1210*	1.4								
_										
Tracer Test #	•		H2)							
	1120 Test s									
1/18/2008		1.5		0	0.046		57.6		13.4	1015
1/18/2008		0.9		0	2.8		53.4	0.04		1014
1/19/2008	1110*	1.3	0.08	0	7.0		76.9		18.6	1018
Tracer Test #			H2)							
	1036 Test s									
1/30/2008		0.0	0	0	0.10		91.0	0.10		1020
1/30/2008		0.0	0	0	1.2		94.0		12.0	1019
1/30/2008		0.0	0	0	2.9		81.7	0.10		1018
1/31/2008		0.0	0	0	3.9		79.8	0.10		1019
1/31/2008		0	0	0	3.5		76.8		9.6	1018
1/31/2008		0.0	0	0	3.4		74.9	0.16	8.7	1016
1/31/2008										
1/31/2008	1543	0	0	0	3.4		77.5	0.07	8.4	1014
									•	
Tracer Test #	. `		H2)							
	1236 Test s									
1/28/2008		0.6	0.04	0	4.2		76.4	0.17	10.2	1011
1/29/2008		0	0.04	0	6.6		76.3	-0.04	5.2	1017
1/29/2008	Final O2*	0								

Source file: Test 8 - 6 Feb 2008.xls

**Phase II Tracer Test Injection Data** 

Well ID \_\_\_\_INJ1\_\_\_\_

				Well or In	jection Gas	s Sample			Well	Ambient Ai
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	emperatur	metric pres
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
					, , ,					
Tracer Test #	5 (90 cfm to	INJ2, ~3%	H2)							
2/5/2008	1015 Test s	start								
2/5/2008	1055	0.2	0	0	0.71		90.4	0.22	10.9	1019
2/5/2008	1158	0.3	0	0	2.1		89.8		11.3	1019
2/5/2008	1405	0.1	0	0	3.3		82.6	0.22	12.8	1018
2/5/2008	1526	0.1	0	0	3.2		55.5		21.2	1019
2/5/2008	1610	0.1	0	0	3.2		69.0		11.7	1018
Tracer Test #	46 (30 cfm to	tal; 10 cfm	to each INJ	1, 2, and 3;	~8% H2)					
2/7/2008	1500 Test s	start								
2/7/2008	1507	0.0	0	0	7.8		33.1		21.4	1016
2/7/2008	1509	0.0	0	0	7.2		32.3		28.2	1016
2/8/2008	925	0.0	0	0	8.8		59.6	0.16	8.3	1017
2/8/2008	1043	0.0	0	0	8.2		77.8		10.2	1017
				H2ave =	8.000					
Tracer Test #	<sup>‡</sup> 7 (60 cfm to	tal; 20 cfm	each to INJ	1, 2, and 3;	~5% H2)					
1/17/2008	900 Test st	art								
1/17/2008	1257	0.1	0	0	5.1		8.4	0.10	11.9	1013
				H2ave =	5.100					
Tracer Test #	48 (90 cfm to	tal; 30 cfm	each to INJ	1, 2, and 3;	~4.5% H2)					
2/6/2008	1000 Test s	start								
2/6/2008	1006	0.0	0	0	4.6		90.4	0.54	10.2	1020
2/6/2008	1111	0.0	0	0	4.5		39.0		11.8	1020
2/6/2008	1213	0.0	0	0	4.3		52.6		13.4	1019
2/6/2008	1403	0.0	0	0	5.1		41.1	0.58	15.4	1017
2/6/2008	1515	0.0	0	0	4.7		43.2		17.6	1017

H2ave = 4.640

	1			Well o	or Injection Gas Sa	ımple			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure		Barometric pressure
Date Time		(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C°)	(mbar)
12/12/2007	1522	(1.9)	(,,,	(7-)	(,,,	(FF)	(,,,	9.9	(-)	()
12/13/2007	840	0	0	0	8.1	10^5	11.3	4.3	5.1	1016
12/13/2007	1328	0	0	0	8.5		10.9		17.1	1014
12/13/2007	1424	0	0.70	0.54	0.22		6.2		15.2	1013
12/13/2007	1554	0	0.70	0.52	0.022		13.9		13.0	1013
12/14/2007	834	0	0	0	0.22			0.11	5.4	1016
12/21/2007	1122	10.3	0.90	0.08	0.22		60.8	0.01	13.2	1013
12/26/2007	1355	0.2	0	0	0.57		12.3	0.1	11.9	1015
12/26/2007	1425	0.1	0	0	8.4					
12/27/2007	925	0.1	0	0	9.1		6.6	0.06	5.3	1017
12/27/2007	1244	0.1	0	0	9		6.9		9.3	1017
12/27/2007	1525	0.2	0	0	9.6		7.2	0.08	7.9	1017
1/2/2008	933	0.1	0	0	0.22		4.5	0.04	9.5	1012
Troppy Took #4 (40 of	to IN IO 70	( 110)								
Tracer Test #1 (10 cfr 1/21/2008 1046 7	Toot stort	% H∠)								
1/21/2008 1048	1049	0.9	0	0	6.4		46.5		7.8	1007
1/21/2008	1121	0.9	0	0	6.4		43.8		9.1	1007
1/21/2008	1241	0.8	0	0	6.2		34.5	0.21	9.9	1007
1/21/2008	1439	0.8	0	0	6.3		15.6	0.21	10.1	1007
1/21/2008	1624	0.9	0	0	6.3		13.0	0.22	10.1	1000
1/22/2008	908	0.8	0	0	7.1		23.3	0.20	7.5	1011
1/22/2008 1200*	300	0.1	0	0	6.8		20.0	0.20	1.5	1011
1/23/2008	946	0.7	0	0	6.6		59.2	0.20	9.0	1008
1/23/2008 1104*	340	0.3	O .	Ŭ.	6.8		00.2	0.20	5.0	1000
1/20/2000 1101		0.0		H2ave =	6.544		l	I		
Tracer Test #2 (20 cfr	m to INJ2, ~8%	6 H2)								
1/18/2008 1120 7		,								
1/18/2008	1123	0.5	0	0	8.8		54.5	0.06	12.3	1015
1/18/2008	1143	0.5	0	0	7.4					
1/18/2008	1300	0.5	0	0	6.9					
1/18/2008 1552*		0.1	0	0	7.8		4.2	0.12	22.3	1014
1/19/2008	848	0.5	0	0	7.9		15.3		7.4	1018
1/19/2008 1015*		0.1	0	0	5.8		8.9	0.14	13.6	1019
				H2ave =	7.433					
Tracer Test #3 (30 cfr		6 H2)								
1/30/2008 1036 7										
1/30/2008	1043	0.0	0	0	4.6		26.1	0.50	9.2	1020
1/30/2008	1153	0.0	0	0	4.4		24.7		10.1	1019
1/30/2008	1406	0.0	0	0	4.7		37.0	0.50	12.3	1018
1/31/2008	920	0.0	0	0	4.1		39.8	0.50	7.9	1019
1/31/2008	1121	0	0	0	3.6		42.8	0.70	9.4	1018
1/31/2008	1318	0	0	0	3.4		43.3	0.53	8.5	1017
1/31/2008	1342	0	0	0	3.9		28.2		8.7	1016
1/31/2008	1435	2.0					40.0	0.00	7.0	4045
1/31/2008	1453	0.0	0	0	3.6		43.9 48.0	0.08	7.9	1015
1/31/2008	1555	0.0	0	0 H2ave =	4.100		48.0		8.0	1014

H2ave = 4.100

				Well	or Injection Gas Sa	mple			Well	Ambient Air
		O <sub>2</sub>	CO <sub>2</sub>	Propane	H <sub>2</sub>	He	RH	Pressure	Temperature	Barometric pressure
Date	Time	(%)	(%)	(%)	(%)	(ppm)	(%)	(in wc)	(C <sub>0</sub> )	(mbar)
Tracer Test #4	4 (60 cfm to INJ2, ~7%	6 H2)								
1/28/2008	8 1236 Test start	·								
1/28/2008	1239	0	0	0	6.4		76.4	1.95	10.4	1010
1/28/2008	1337	0	0	0	5.7					
1/28/2008	8 1340*	0	0	0	6.2					
1/28/2008		0	0	0	6.0		70.8	1.90	10.3	1011
1/29/2008	741	0	0	0	7.1		43.5	1.70	5.9	1016
1/29/2008	8 1010*	0			6.6					
				H2ave =	6.333					
Tracer Test #5	5 (90 cfm to INJ2, ~3%	6 H2)								
2/5/2008	8 1015 Test start									
2/5/2008	8 1016	0	0	0	3.5		11.0	2.4	8.3	1019
2/5/2008	1051	0	0	0	3.3					1019
2/5/2008	1117	0	0	0	3.5		13.2		10.5	1019
2/5/2008		0	0	0	4.0		23.2	2.40	12.0	
2/5/2008	8 1435	0	0	0	3.7				14.8	1018
2/5/2008	1541	0	0	0	3.5		23.9		16.8	1019
				H2ave =	3.583					
	6 (30 cfm total; 10 cfm	to each INJ1, 2, and	d 3; ~8% H2)							
	8 1500 Test start									
2/7/2008		0.0	0	0	. 10		13.8		21.1	
2/7/2008		0.0	0	0			25.7		22.9	
2/8/2008		0.0	0	0	0.0		37.2		13.0	
2/8/2008	1051	0.0	0	0	0.0		45.3		10.6	1017
				H2ave =	8.100					
	7 (60 cfm total; 20 cfm	to each INJ1, 2, and	d 3, ~5% H2)							
	8 900 Test start									
1/17/2008				0			69.5	0.06	2.5	
1/17/2008		0.4	0	0	4.9		55		10.0	1015
1/17/2008	8 1302*	0.1								
				H2ave =	4.800					
	8 (90 cfm total; 30 cfm	each to INJ1, 2, and	d 3; ~4.5% H2)							
	8 1000 Test start									
2/6/2008		0.0	0	0			22.4	0.64	9.8	
2/6/2008		0.0	0	0			32.1		12.1	
2/6/2008		0.0	0	0			27.5		13.4	
2/6/2008		0.0	0	0	V.V.		29.8	0.65	15.8	
2/6/2008	1524	0.0	0	0	4.7		36.0		16.1	1017

H2ave = 4.600

7.0

81.7

0.14

5.1

1017

1/29/2008

1/29/2008 Final O2\*

819

0.1

0.1

0.04

	ent Air
Date         Time         (%)         (%)         (%)         (ppm)         (%)         (in wc)         (C°)         (m           Tracer Test #5 (90 cfm to INJ2, ~3% H2)         2/5/2008 1015 Test start         2/5/2008 1015 Test start         11.1         75.1         0.11         11.3           2/5/2008 1357 0.2         0         0         2.7         79.7         0.14         12.8           2/5/2008 1519 0.1         0         0         2.9         45.8         22.0           2/5/2008 1603 0.1         0         0         2.9         55.5         19.6	
Tracer Test #5 (90 cfm to INJ2, ~3% H2)         2/5/2008 1015 Test start       2/5/2008 1150 0.3 0 0 1.1 75.1 0.11 11.3         2/5/2008 1357 0.2 0 0 2.7 79.7 0.14 12.8         2/5/2008 1519 0.1 0 0 2.9 45.8 22.0         2/5/2008 1603 0.1 0 0 2.9 55.5 19.6	ic pressure
2/5/2008 1015 Test start       2/5/2008 1150 0.3 0 0 1.1 75.1 0.11 11.3       2/5/2008 1357 0.2 0 0 2.7 79.7 0.14 12.8       2/5/2008 1519 0.1 0 0 2.9 45.8 22.0       2/5/2008 1603 0.1 0 0 2.9 55.5 19.6	bar)
2/5/2008     1015 Test start       2/5/2008     1150     0.3     0     0     1.1     75.1     0.11     11.3       2/5/2008     1357     0.2     0     0     2.7     79.7     0.14     12.8       2/5/2008     1519     0.1     0     0     2.9     45.8     22.0       2/5/2008     1603     0.1     0     0     2.9     55.5     19.6	
2/5/2008     1150     0.3     0     0     1.1     75.1     0.11     11.3       2/5/2008     1357     0.2     0     0     2.7     79.7     0.14     12.8       2/5/2008     1519     0.1     0     0     2.9     45.8     22.0       2/5/2008     1603     0.1     0     0     2.9     55.5     19.6	
2/5/2008     1357     0.2     0     0     2.7     79.7     0.14     12.8       2/5/2008     1519     0.1     0     0     2.9     45.8     22.0       2/5/2008     1603     0.1     0     0     2.9     55.5     19.6	
2/5/2008     1519     0.1     0     0     2.9     45.8     22.0       2/5/2008     1603     0.1     0     0     2.9     55.5     19.6	1019
2/5/2008 1603 0.1 0 0 2.9 55.5 19.6	1018
	1019
Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2)	1018
Tracer Test #6 (30 cfm total; 10 cfm to each INJ1, 2, and 3; ~8% H2)	
2/7/2008 1500 Test start	
2/7/2008     1505     0.0     0     0     7.7     44.9     21.3	1016
2/7/2008     1558     0.0     0     0     7.2     25.2     28.0	1016
2/8/2008     1033     0.0     0     0     8.5     34.8     10.0	1017
H2ave = 7.800	
Tracer Test #7 (60 cfm total; 20 cfm to each INJ1, 2, and 3, ~5% H2)	
1/17/2008 900 Test start	1011
1/17/2008         1255         0.2         0         0         5.1         52.0         0.27         11.9	1014
H2ave = 5.100	
Tracer Test #8 (90 cfm total; 30 cfm each to INJ1, 2, and 3; ~4.5% H2)	
2/6/2008 1000 Test start	1020
2/6/2008 1204 0.0 0 0 4.8 65.8 1.05 10.0 10.0 10.0 10.0 10.0 10.0 10.0	1020
2/6/2008 1259 0.0 0 0 4.1 71.8 14.5	1020
2/6/2008 1452 0.0 0 0 4.1 71.8 14.5 16.0	1019
2/6/2008 1452 0.0 0 0 4.8 62.5 1.05 16.0 2/6/2008 1550 0.0 0 0 4.6 44.7 19.1	1017
$\frac{27672008}{1550} \frac{1550}{0.01} \frac{0.01}{01} \frac{01}{01} \frac{4.81}{4.80} \frac{44.71}{19.11} \frac{19.11}{19.11}$	1017

Table Soil Analytical Data

Sample	PID	USCS D Soil Perchlorate		e.	Nitrate		Moisture	
Gampic	(ppm)	Type	μg/kg (dry)		mg-N/kg (dry)	flag	worstare %	
P4-10-102907	0.1	CL	14667	<u>-</u>	4.4		25	
P4-15-102907	0.0	CL	25000		6.4		36	
P4-15-D	NA	NA	17647		5.7		32	
P4-20-102907	0.0	CL	21875		8.0		36	
P4-30-102907	0.0	SP	28125		8.6		36	
P4-40-102907	0.1	CL	19403		6.9		33	
P4-40-D	NA	NA	18667		7.1		25	
P4-50-102907	0.0	SW	1116		2.0		14	
P3-10-102307	0.1	CL/SP	75342		5.6		27	
P3-20-102307	0.0	CL/SW	75362		7.8		31	
P3-30-102307	0.5	GC/CL	68657		7.0		33	
P3-40-102307	0.0	CL	33333		4.5		22	
P3-50-102307	1.2	GW	2907		3.1		14	
CDM-INJ2-10-102607	0.0	CL/ML	4324		5.0		26	
CDM-INJ2-20-102607	0.0	CL	8806		6.4		33	
CDM-INJ2-25-102607	0.0	CL	5921		5.0		24	
CDM-INJ2-25-D	NA	NA	4459		3.9		26	
CDM-INJ2-30-102607	0.0	SM	4524		3.6		16	
CDM-INJ2-40-102607	0.0	GC	2556		3.0		10	
CDM-INJ2-50-102607	0.0	SP-SM	282		3.6		15	
P5-10-102407	0.0	CL	7206		5.3		32	
P5-20-102407	0.0	CL	3944		5.6		29	
P5-30-102407	0.2	CL/SW	3433		6.4		33	
P5-40-102407	0.0	CL/SC	4571		7.0		30	
P5-50-102407	0.0	SP	1798		3.5		11	
CDM-INJ1-US-073106-15	NA	ML	41000		5.2		19.9	
CDM-INJ1-US-073106-20	NA	CL/GC	73000		10.0		34.6	
CDM-INJ1-US-073106-35	NA	SM	17000		2.3		13.7	
CDM-INJ1-US-073106-50	NA	SM	7700		2.2		13.2	
CDM-INJ1-US-073106-70		SM	5700		1.6		7.8	
CDM-INJ3-10-101807	0.0	GC	333333		37.7		31	
CDM-INJ3-20-101807	0.0	GC	36111		3.8		28	
CDM-INJ3-30-101807	0.0	SM	22222		4.3		19	
CDM-INJ3-40-101807	0.0	ML/SP	9302	_	2.9		14	
CDM-INJ3-50-101807		SW	3444		2.8		10	
P6-10-102207		CL/GC	1068	_	3.9		26	
P6-20-102207		CL/GW	13415		4.4		18	
P6-30-102207		SP/CL	1957		2.6		8	
P6-40-102207		GM/SW	5435	_	2.7		8	
P6-50-102207		SW	11023		3.1		12	
P2-05-102507	0.3	CL	597222		5.8		28	
P2-05-D		NA	463768		15.9		31	
P2-10-102507		CL	231884		27.5		31	
P2-20-102507	0.2	GW	242857		15.7		30	

		USCS					
Sample	PID	Soil	Perchlorate		Nitrate		Moisture
	(ppm)	Туре	μg/kg (dry)	flag	mg-N/kg (dry)	flag	%
P2-20-D	NA	NA	388889		16.7		28
P2-30-102507	0.5	GW	47561		8.5		18
P2-40-102507	0.0	SP/CL	12088		4.2		9
P2-50-102507	0.0	CL	51724		5.3		13
P7-10-101607	162.0	ML	14030		4.5		33
P7-20-101607	63.0	GM	13187		3.7		9
P7-30-101607	86.0	CL/SP	21429		3.0		16
P7-40-101607	28	SP	6047		3.6		14
CDM-P1-US-072706-15	NA	ML	11	J	3.2		10.1
CDM-P1-US-072706-25	NA	GC	1300		4.0		12.6
CDM-P1-US-072706-35	NA	SP/GC	5000		1.8		6.9
CDM-P1-US-072706-45	NA	GC/SM	8500		2.2		10.8
CDM-P1-US-072706-70	NA	SM	12000		1.3		16.7
P8-10-101107		CL/GW	75000		8.5		40
P8-30-101107		GC/GP	4048		3.1		16
P8-40-101207			89		3.0		17
P8-50-101207	184.0	GW	18	J	2.6		16
CDM-CB-1-041808-10		CL	4598		0.6	_	30.4
CDM-CB-1-041808-20		GC	4454		0.8		30.4
CDM-CB-1-041808-30		GW/CL	7018		0.6		31.6
CDM-CB-1-041808-30D		NA	2479		0.2		15.3
CDM-CB-1-041808-40		GW	1487		0.4		12.6
CDM-CB-1-041808-50		GW ML (OL	869		0.2		14.8
CDM-CB-2-041808-10		ML/CL	8905		0.4		31.5
CDM-CB-2-041808-20 CDM-CB-2-041808-30		SW GW	657 2576		0.3 0.2	U	7.14 37.9
CDM-CB-2-041808-30D		GW-GM	5196		0.2	U	13.4
CDM-CB-2-041808-40		GW-GW	12277		0.5		10.4
CDM-CB-2-041808-50		GW	2700		0.3		11.1
CDM-CB3-10-061008		CL	21277		0.6		29.5
CDM-CB3-20-061008		GP	7859		0.4		9.66
CDM-CB3-30-061008		GM	3869		0.1	U	9.53
CDM-CB3-30D-061008	NA	NA	5875		0.7		14.9
CDM-CB3-40-061008	NA	GP	1582		0.6		11.5
CDM-CB3-50-061008	NA	GP	1076		0.1		7.97
CDM-CB4-10-061008		CL	191458		14.4		32.1
CDM-CB4-20-061008		GC/CL	12065		2.6		8.83
CDM-CB4-30-061008		GC/ML	12135		0.8		9.35
CDM-CB4-30D-061008		NA OD OM	14192		1.0		8.4
CDM-CB4-40-061008		GP-GM	22379		0.9		15.1
CDM-CB4-50-061008		GM MLCI	5297		0.1	U	9.38
CDM-CB5-10-071008		MLCL	310		0.2		29.3
CDM-CB5-25-071008		SM SM	2200 3200		0.5		34.6
CDM-CB5-25-071008 CDM-CB5-30D-071008		NA	3200		0.5 0.1		36.9 9.6
CDM-CB5-30D-071008		SM	1400		0.1		15.6
CDM-CB5-50-071008		SM	1600		0.4		10.4
CDM-CB6-10-071008		CL/ML	51000		0.1		28
CDM-CB6-20-071008		CL/SM	4000		0.2		31
CDM-CB6-25-071008		SM	1700		0.2		15.8
CDM-CB6-30-071008		SM	1200		0.1		19.1
CDM-CB6-40-071008		GM/SM	2500		0.1		11.8
CDM-CB6-50-071008	0	SM	4400		0.1		10.1
CDM-CB7-10-090208	NA	CL	16000		0.2		29.5
CDM-CB7-20-090208		CL	3800		1.1		32.9
CDM-CB7-30-090208	NA	CL	8000		0.9		31.5

		USCS					
Sample	PID	Soil	Perchlorate	9	Nitrate		Moisture
	(ppm)	Туре	μg/kg (dry)		mg-N/kg (dry)	flag	%
CDM-CB7-30D-090208	NÁ	NA.	8800		0.9	Ŭ	33
CDM-CB7-40-090208	NA	GM	210		0.1		11.3
CDM-CB7-50-090208		GM	1400		0.1		17.7
CDM-CB8-10-090208	NA	CL	560000		13.0		36
CDM-CB8-20-090208		GC	37000		5.3		11
CDM-CB8-30-090208		GW	16000		0.2		4.4
CDM-CB8-30D-090208	NA	NA	27000		0.2		6.8
CDM-CB8-40-090208	NA	GM	56000		0.1		19.9
CDM-CB8-50-090208	NA	GM	1800		0.2		23
CDM-CB9-10-120208	NA	GW	120		0.4		19.5
CDM-CB9-20-120208	NA	CL	960		0.2		22.1
CDM-CB9-30-120208	NA	CL	150		0.3		11.3
CDM-CB9-30D-120208	NA	NA	140		0.2		9.4
CDM-CB9-40-120208	NA	GM	350		0.3		12.1
CDM-CB9-50-120208	NA	SW	1500		0.5		9.3
CDM-CB10-10-120208	NA	GW	26000		0.1		10.5
CDM-CB10-20-120208	NA	CL	11000		0.1		16.3
CDM-CB10-30-120208	NA	GW	270		0.2		10.3
CDM-CB10-30D-120208	NA	NA	130		0.2		9.5
CDM-CB10-40-120208	NA	GW/GM	8800		0.2		10.1
CDM-CB10-50-120208	NA	GW	210		0.3		13.5
CDM-CB11-10-120308	NA	GW/GM	47000		0.4		9.4
CDM-CB11-20-120308	NA	GM	14000		1.5		16.7
CDM-CB11-30-120308		GC	23000		0.1		16.9
CDM-CB11-30D-120308		NA	18000		0.1		14.9
CDM-CB11-40-120308		ML	26000		0.5		13.3
CDM-CB11-50-120308		GW	11000		0.9		8.4
CDM-CB12-10-120308		CL	7500		0.5		31.1
CDM-CB12-20-120308		GM	7600		3.4		27.9
CDM-CB12-30-120308		GW	1400		0.1	U	9.3
CDM-CB12-30D-120308		NA	780		0.1	U	9.8
CDM-CB12-40-120308		GW/GM	25000		0.1		7.2
CDM-CB12-50-120308		GW	9400		0.4		8.3
CDM-CB13-10-120308		CL	110000		2.7		30.2
CDM-CB13-20-120308		GM	140000		1.0		29.3
CDM-CB13-30-120308		GM	15000		0.1	U	11.4
CDM-CB13-30D-120308		NA OM	15000		0.1		10.7
CDM-CB13-40-120308		GM	6900		0.1		8.2
CDM-CB13-50-120308		GW	4300		0.3		7.2
CDM-CB14-10-120308		CL	14	U	0.1		27.8
CDM-CB14-20-120308		CL	24	ļ	0.2	.,	31
CDM-CB14-30-120308		GM	1400		0.1	U	6.8
CDM-CB14-30D-120308		NA CM	2900		0.1		7.8
CDM-CB14-40-120308		GM CM	1600		0.4		15.4
CDM-CB14-50-120308 CDM-CB15-10-120308		GM CL	2700 15	U	0.3 0.2		9.1 31.6
CDM-CB15-10-120308		CL	35		0.2		31.8
CDM-CB15-20-120308		GW	1200		0.1		9.1
CDM-CB15-30D-120308		NA	3200		0.1		9.1
CDM-CB15-30D-120308		GC	390		0.1		14.7
CDM-CB15-40-120308		GW	2300		0.1		9.1
CDM-CB16-10-120308		CL	15	U	0.2		32.4
CDM-CB16-20-120308		CL	15	Ü	0.1		35.5
CDM-CB16-30-120308		GW	13	U	0.1		25.6
CDM-CB16-30D-120308		NA	13		0.1		23.4
CDM-CB16-40-120308		GM	440		0.1		13.5
CDM-CB16-50-120308		GM	3100		0.24		9.1

Sample	PID	USCS Soil	Perchlorate	)	Nitrate		Moisture
·	(ppm)	Туре	μg/kg (dry)	flag	mg-N/kg (dry)	flag	%
CDM-CB17-10-120308	NA	CL	660		0.15		32.00
CDM-CB17-20-120308	NA	CL	4900		2.9		30.80
CDM-CB17-30-120308	NA	GM	8800		0.1	J	11.60
CDM-CB17-30D-120308	NA	NA	6800		0.1		9.50
CDM-CB17-40-120308	NA	CL	3800		1.1		25.10
CDM-CB17-50-120308	NA	GW	700		0.3		6.10
CDM-CB18-10-120308	NA	CL	48000		0.1		18.20
CDM-CB18-20-120308	NA	CL	3000		0.1		31.40
CDM-CB18-30-120308	NA	GC	7400		0.1		19.40
CDM-CB18-30D-120308	NA	NA	9900		0.2		16.70
CDM-CB18-40-120308	NA	GM	1900		0.1		11.60
CDM-CB18-50-120308	NA	GM	2900		0.1		7.10
CDM-CB19-10-120308	NA	CL	160000		8.0		32.30
CDM-CB19-20-120308	NA	GW	59000		4.2		19.30
CDM-CB19-30-120308	NA	GW-GM	13000		0.1		7.50
CDM-CB19-30D-120308	NA	NA	8400		0.1		7.70
CDM-CB19-40-120308	NA	GW-GM	25000		0.4		10.30
CDM-CB19-50-120308	NA	GW-GM	4900		0.8		8.30

Notes

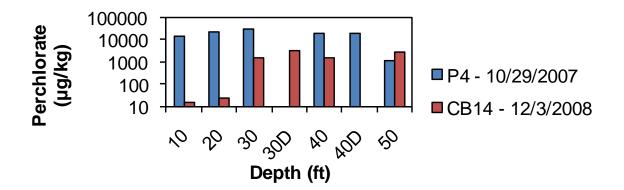
PID - Photoionization detector

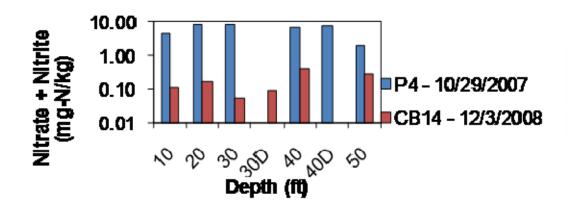
USCS - Unified Soil Classification System

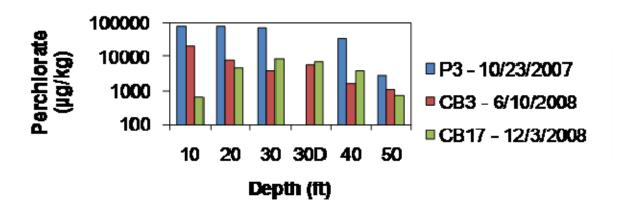
µg/kg - Micrograms per kilogram mg-N/kg - Milligrams nitrogen per kilogram

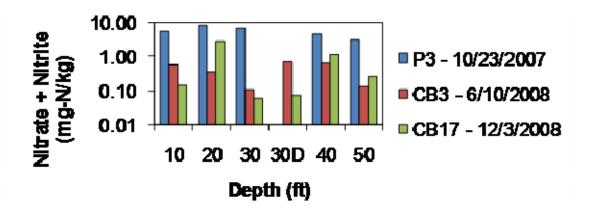
ppm - parts per million U - Not detected

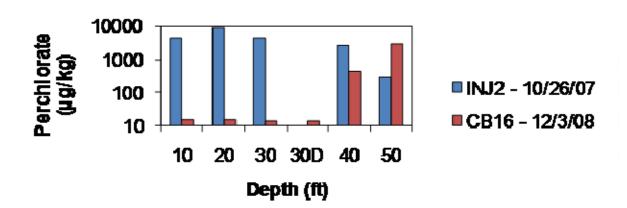
NA - Not analyzed

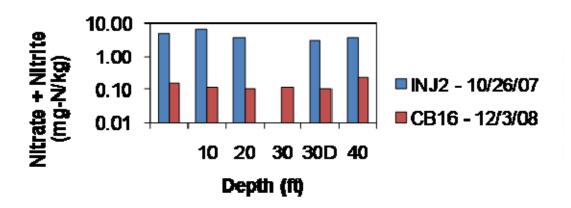


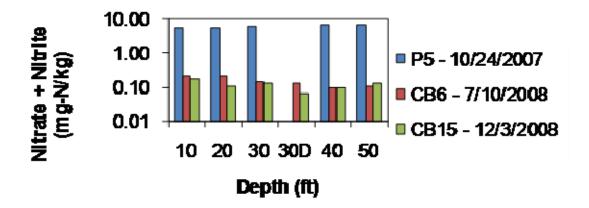


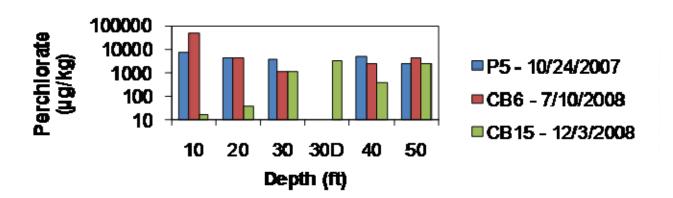


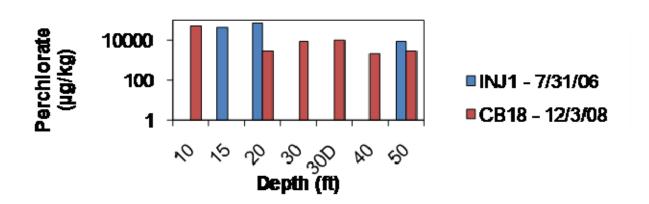


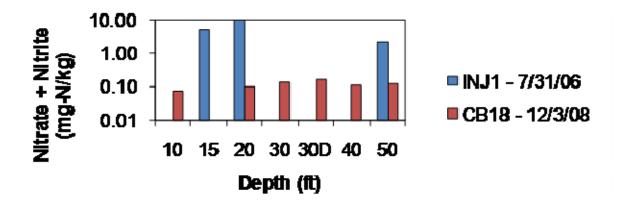


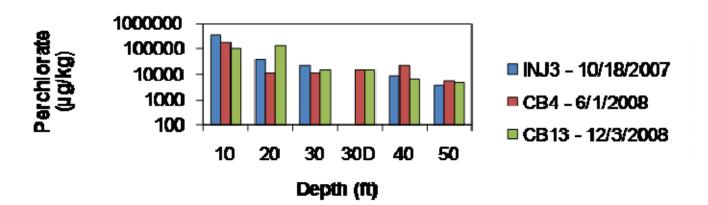


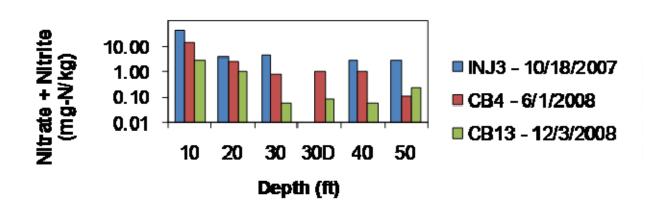


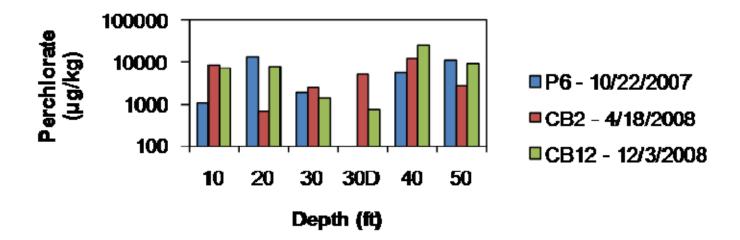


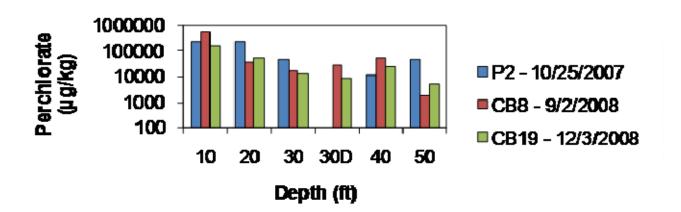


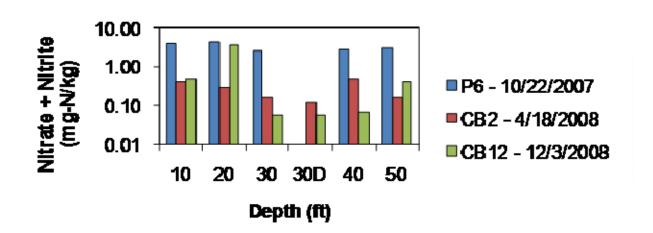


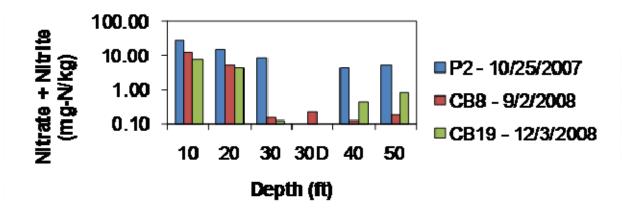












## **Appendix D: Treatability Test Report**

## Appendix A

## **Treatability Test Report**

# In Situ Bioremediation of Perchlorate in Vadose Zone Using Gaseous Electron Donors.

ESTCP Project ER-0511
Propellant Burn Area
Inactive Rancho Cordova Test Site
Rancho Cordova, California



September 2007

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### Acronyms

ASTM American Society for Testing and Materials

atm-m<sup>3</sup>/mol atmosphere, meter cubed, per mole

bgs Below ground surface

C Concentration °C Degrees Celsius

CDM Camp Dresser & McKee cfm Cubic feet per minute

ClO<sub>4</sub> Perchlorate

CMT Continuous multi-chamber tubing

CO<sub>2</sub> Carbon dioxide

d Days

EPA U. S. Environmental Protection Agency

ESTCP Environmental Security Technology Certification Program

FID Flame ionization detector Ft amsl Feet above mean sea level

g Gram

GC Gas chromatograph

GEDIT Gaseous electron donor injection technology

h Hours H<sub>2</sub> Hydrogen Hg Mercury

IRCTS Boeing Interactive Rancho Cordova Test Site

k Average permeability

LAAP Longhorn Army Ammunition Plant

LPG Liquified petroleum gas

m<sup>3</sup> Cubic meters

m<sup>3</sup>/day Cubic meters per day

m/day Meters per day

mg/kg Milligrams per kilogram

mL Milliliters mm Millimeters

mM Millimoles per liter

mmol Millimoles mol/L Moles per liter msl Mean sea level

N<sub>2</sub> Nitrogen

N/kg Nitrogen per kilogram

NAWQA National Water Quality Assessment

NO<sub>2</sub> Nitrite NO<sub>3</sub> Nitrate O<sub>2</sub> Oxygen

PBA Propellant burn area
PID Photo-ionization detector

ppb Parts per billion ppm Parts per million

P<sub>sat</sub> Saturation vapor pressure psi Pounds per square inch

PSU The Pennsylvania State University

PVC Polyvinyl chloride

Q Flow rate

TCD Thermal conductivity detector

TOC Total organic carbon

TVS Total volatile solids in the sediments/soils

USA Underground Service Alert

USCS Unified Soil Classification System
USEPA U. S. Environmental Protection Agency

 $\begin{array}{ll} \mu M & \text{Micrometers} \\ V & \text{Volume} \end{array}$ 

VOC Volatile organic compound WDC Water Development Corporation

### 1.0 Introduction

The Department of Defense Environmental Security Technology Certification Program (ESTCP) is funding CDM to conduct a demonstration of gaseous electron donor injection technology (GEDIT) for *in situ* bioremediation of perchlorate in soil. CDM and ESTCP have selected the Aerojet Inactive Rancho Cordova Test Site Propellant Burn Area (IRCTS-PBA) as a suitable site for this demonstration. A treatability study was conducted using soil collected from the site to determine engineering design parameters for the demonstration. The treatability study was conducted in accordance the February 14, 2006 Workplan and the September 1, 2006 memorandum Response to Treatability Study Workplan Comments (ER-0511). This treatability study involved the following tasks:

- Completion of two soil borings
- Collection and analysis of soil samples
- Installation of one injection well and one piezometer
- Completion of a perchlorate biodegradation study comprised of microcosm and column tests by The Pennsylvania State University
- Completion of an air injection test

This report presents the methods, results, and conclusions from this treatability study.

## 2.0 Soil Borings, Lithology, Sample Collection, Sample Analysis Results, and Well Installation

This section presents the methods and procedures that were utilized to drill and install one air injection well (CDM-INJ1) and one multi-level air monitoring well (CDM-P1). The location of the wells is presented on **Figure 2-1**.

### 2.1 Pre-Field Activities

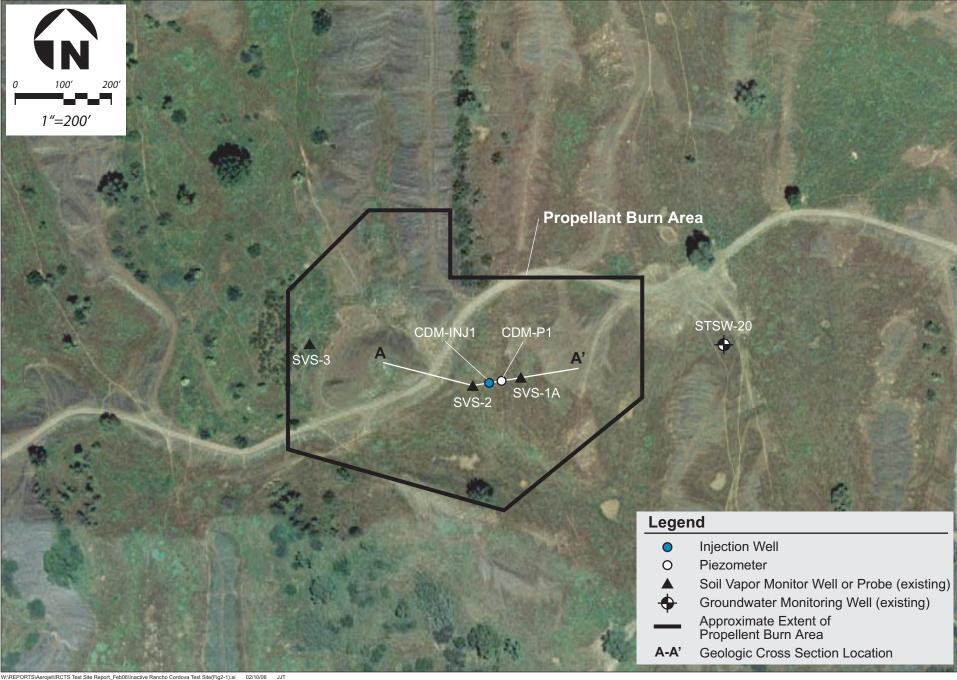
Drilling and well construction permits were obtained from the County of Sacramento Environmental Management Department prior to drilling. The approved drilling permits are included in **Appendix A-1**. Underground Service Alert (USA) and Aerojet utilities were notified 72 hours prior to drilling to determine the locations of any subsurface utilities.

### 2.2 Drilling

From July 27, to August 2, 2006, two boreholes were advanced by the Water Development Corporation (WDC) of Woodland, California. Both boreholes were drilled utilizing the sonic drilling method. The injection well (CDM-INJ1) was advanced to a total depth of 70.5 feet below ground surface (bgs) using a 6-inch diameter core barrel and a 10-inch diameter washover casing. The monitoring well (CDM-P1) was advanced to a total depth of 72 feet bgs using a 4-inch diameter core barrel and a 6-inch diameter wash-over casing.

The boreholes were continuously cored to total depth by advancing the core barrel in 10-foot increments. As the core barrel was advanced, a continuous core sample was simultaneously collected inside the core barrel. After each 10-foot increment, the temporary wash-over casing was advanced to depth and the core barrel was tripped from the borehole. The core sample was removed from the core barrel and placed in a plastic core bag. This process was repeated until the borehole was advanced to total depth.

The continuous core was logged using the Unified Soil Classification System in accordance to ASTM Standard D2488: Standard Practice for Description and Identification of Soils (Visual-Manual Procedure). The core was logged by a CDM field geologist under the supervision of a State of California, Professional Geologist. The log included a description of the materials encountered during drilling and noting zones impacted of visual contamination. Additionally, the core was screened for volatile organic compounds using a photo-ionization detector (PID) by placing a portion of the core in a zip-lock sealed bag. After approximately five to 10 minutes, the zip-lock bag was punctured with a small hole and the tip of the PID was inserted into the bag to assess the head space in the bag for volatile organic compounds. The measurements were recorded on the boring log. The boring logs are presented in **Appendix A-2**. Soil samples were collected from the continuous core and placed in sample containers. As required, some of the samples were placed on ice. Samples were submitted to the CDM laboratory in Bellevue, Washington; Laucks Testing Labs (Laucks) in Seattle, Washington; and The Pennsylvania State University (PSU) in University Park, Pennsylvania under chain-of-custody protocol.



**CDM** 

Figure 2-1

Soil samples were collected and submitted to the laboratory for analysis from the core of each boring at 5-foot intervals from the 5-foot to 70-foot depth. The samples submitted to the CDM laboratory were analyzed for perchlorate using a perchlorate ion-selective probe following extraction with an equal weight of water in accordance with the Workplan, and moisture by ASTM Method D2216. The samples submitted to Laucks were analyzed for perchlorate by EPA Method 314.1, nitrate and nitrite as nitrogen by EPA Method 353.2, total organic carbon (TOC) by EPA Method 415.1 modified for soil, moisture by ASTM Method D2216, pH by Standard Method number 9045-C, and grain size by ASTM D422. The samples submitted to the Pennsylvania State University (PSU) were used for a perchlorate bioremediation study as described in Section 3.

### 2.3 Well Construction

Upon reaching total depth of the borehole, an air injection well was installed in CDM-INJ1 and a multi-level air monitoring well was installed in CDM-P1. CDM-INJ1 was installed as an air injection location. CDM-P1 was installed as a monitoring point to assess the extent of influence of the injection air. The as-built construction details of the wells are shown on **Figure 2-2 and 2-3**.

The injection well CDM-INJ1 was constructed with a 6-inch diameter schedule 40 PVC well casing with flush-threaded joints (**Figure 2-2**). The well screen consisted of a 6-inch diameter schedule 40 PVC machine slotted pipe with a total of 60 feet of 0.020-inch slotted screen. The screen was installed between 10 and 70 feet bgs. The filter pack consisted of Number 3 sand sealed with a bentonite pellet seal. The annular space above the bentonite pellet seal was sealed with a cement bentonite grout. The well was completed in an above grade monument.

The monitoring well CDM-P1 was constructed with four nested wells completed at different depths. Each well was constructed with a 0.25-inch diameter polyurethane tubing (**Figure 2-3**). Each well was completed with a 0.25-inch diameter, 6-inch long stainless steel vapor probe. The vapor probes were installed at depths of 18, 33, 48, and 68 feet bgs. The filter pack placed in the annular space around each probe consisted of Number 3 Monterey sand. The annular space above and below the filter pack was sealed with a benonite chip seal. The annular space above the uppermost bentonite seal was sealed with a cement bentonite grout. The multi-port well was completed in an above grade monument.

The wells were not developed because water was not used during drilling and groundwater was not encountered during drilling.

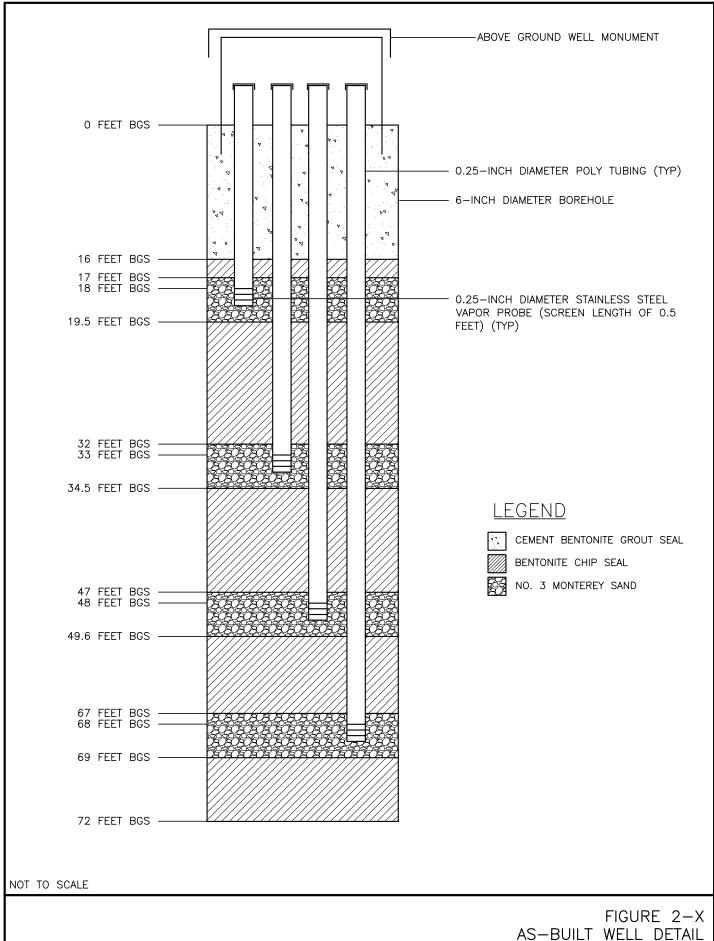
### 2.4 Decontamination

All field equipment including the drill rig and downhole tools were cleaned and decontaminated prior to being introduced into the drilling and sampling environment. The equipment and downhole tools were decontaminated by steam cleaning or washing in a solution of non-phosphate detergent followed by a double rinse of clean water.

## LEGEND CEMENT BENTONITE GROUT SEAL BENTONITE CHIP SEAL - ABOVE GROUND WELL MONUMENT NO. 3 MONTEREY SAND 0 FEET BGS -- 10-INCH DIAMETER BOREHOLE 6-INCH DIAMETER SCH 40 PVC WELL CASING 6 FEET BGS — 8 FEET BGS -10 FEET BGS -6-INCH DIAMETER SCH 40 PVC 0.020-INCH SLOTTED SCREEN (SCREEN LENGTH IS 60 FEET) - CLOSED SHOE 70 FEET BGS — 70.5 FEET BGS — NOT TO SCALE FIGURE 2-X

CDM

FIGURE 2-X AS-BUILT WELL DETAIL CDM-INJI GEDIT-AEROJET



AS-BUILT WELL DETAIL
CDM-PI
GEDIT-AEROJET

CDM

### 2.5 Lithology

The lithology encountered during drilling ranged from silt and clay to silty sand and clayey gravel to cobbles. No soil discoloration or odors were observed in the drill cuttings from either boring. All of the PID readings were non-detect. No groundwater was encountered in any formations during drilling. A detailed description of the soils encountered in each borehole is presented on the boring logs (**Appendix A-2**). **Table 2-1** and **Figures 2-4** and **2-5** show the grain size distribution for soils encountered during boring completion and **Figure 2-6** shows a lithologic cross-section based on these data and existing data (Aerojet, 2000). These data indicate that soil is generally coarse-grained and supportive of gas injection with the exception of shallow soil (i.e., 15 ft bgs) in boring CDM-INJ1.

**Table 2-1 Soil Grain Size Analysis Results** 

			Sample	Sieve Slot Size	Weight Retained	Cumulative Retained
Well	Date	Depth	Type	(mm)	(grams)	(%)
CDM-INJ1	7/31/2006	15	Sample	< 0.075	77	77
CDM-INJ1	7/31/2006	15	Sample	0.075	18	95
CDM-INJ1	7/31/2006	15	Sample	0.106	4.4	99.4
CDM-INJ1	7/31/2006	15	Sample	0.25	0.4	99.8
CDM-INJ1	7/31/2006	15	Sample	0.425	0.1	99.9
CDM-INJ1	7/31/2006	15	Sample	0.85	0.2	100.1
CDM-INJ1	7/31/2006	15	Sample	2	0	100.1
CDM-INJ1	7/31/2006	15	Sample	4.75	0	100.1
CDM-INJ1	7/31/2006	15	Sample	9.5	0	100.1
CDM-INJ1	7/31/2006	15	Sample	19	0	100.1
CDM-INJ1	7/31/2006	15	Sample	25	0	100.1
CDM-INJ1	7/31/2006	15	Sample	37.5	0	100.1
CDM-INJ1	7/31/2006	15	Sample	50	0	100.1
CDM-INJ1	7/31/2006	20	Sample	< 0.075	30	30
CDM-INJ1	7/31/2006	20	Sample	0.075	9	39
CDM-INJ1	7/31/2006	20	Sample	0.106	31	70
CDM-INJ1	7/31/2006	20	Sample	0.25	14	84
CDM-INJ1	7/31/2006	20	Sample	0.425	16	100
CDM-INJ1	7/31/2006	20	Sample	0.85	0	100
CDM-INJ1	7/31/2006	20	Sample	2	0	100
CDM-INJ1	7/31/2006	20	Sample	4.75	0	100
CDM-INJ1	7/31/2006	20	Sample	9.5	0	100
CDM-INJ1	7/31/2006	20	Sample	19	0	100
CDM-INJ1	7/31/2006	20	Sample	25	0	100
CDM-INJ1	7/31/2006	20	Sample	37.5	0	100
CDM-INJ1	7/31/2006	20	Sample	50	0	100
CDM-INJ1	7/31/2006	35	Sample	< 0.075	5.2	5.2
CDM-INJ1	7/31/2006	35	Sample	0.075	2.1	7.3
CDM-INJ1	7/31/2006	35	Sample	0.106	11	18.3
CDM-INJ1	7/31/2006	35	Sample	0.25	4.9	23.2
CDM-INJ1	7/31/2006	35	Sample	0.425	6.5	29.7
CDM-INJ1	7/31/2006	35	Sample	0.85	7.5	37.2
CDM-INJ1	7/31/2006	35	Sample	2	13	50.2
CDM-INJ1	7/31/2006	35	Sample	4.75	15	65.2
CDM-INJ1	7/31/2006	35	Sample	9.5	30	95.2
CDM-INJ1	7/31/2006	35	Sample	19	6	101.2
CDM-INJ1	7/31/2006	35	Sample	25	0	101.2

**Table 2-1 Soil Grain Size Analysis Results (cont.)** 

			Sample Sieve Slot Size Weight Retained		Cumulative Retained	
Well	Date	Depth	Туре	(mm)	(grams)	(%)
CDM-INJ1	7/31/2006	35	Sample	37.5	0	101.2
CDM-INJ1	7/31/2006	35	Sample	50	0	101.2
CDM-INJ1	7/31/2006	50	Sample	< 0.075	14	14
CDM-INJ1	7/31/2006	50	Sample	0.075	8.1	22.1
CDM-INJ1	7/31/2006	50	Sample	0.106	22	44.1
CDM-INJ1	7/31/2006	50	Sample	0.25	13	57.1
CDM-INJ1	7/31/2006	50	Sample	0.425	18	75.1
CDM-INJ1	7/31/2006	50	Sample	0.85	9.7	84.8
CDM-INJ1	7/31/2006	50	Sample	2	7.8	92.6
CDM-INJ1	7/31/2006	50	Sample	4.75	7.9	100.5
CDM-INJ1	7/31/2006	50	Sample	9.5	0	100.5
CDM-INJ1	7/31/2006	50	Sample	19	0	100.5
CDM-INJ1	7/31/2006	50	Sample	25	0	100.5
CDM-INJ1	7/31/2006	50	Sample	37.5	0	100.5
CDM-INJ1	7/31/2006	50	Sample	50	0	100.5
CDM-INJ1	7/31/2006	70	Sample	< 0.075	5.6	5.6
CDM-INJ1	7/31/2006	70	Sample	0.075	3.4	9
CDM-INJ1	7/31/2006	70	Sample	0.106	9.1	18.1
CDM-INJ1	7/31/2006	70	Sample	0.25	5.5	23.6
CDM-INJ1	7/31/2006	70	Sample	0.425	9.7	33.3
CDM-INJ1	7/31/2006	70	Sample	0.85	7.4	40.7
CDM-INJ1	7/31/2006	70	Sample	2	11	51.7
CDM-INJ1	7/31/2006	70	Sample	4.75	13	64.7
CDM-INJ1	7/31/2006	70	Sample	9.5	15	79.7
CDM-INJ1	7/31/2006	70 70	Sample	9.5 19	20	99.7
CDM-INJ1	7/31/2006	70	Sample	25	0	99.7
CDM-INJ1	7/31/2006	70 70	Sample	37.5	0	99.7
CDM-INJ1	7/31/2006	70 70	Sample	50	0	99.7
CDM-INJ1	7/31/2006	70 70	Duplicate	< 0.075	7	99.7 7
CDM-INJ1		70 70	•	0.075	6	13
	7/31/2006	70 70	Duplicate			
CDM-INJ1	7/31/2006		Duplicate	0.106	9.5	22.5
CDM-INJ1	7/31/2006	70	Duplicate	0.25	5.7	28.2
CDM-INJ1	7/31/2006	70	Duplicate	0.425	13	41.2
CDM-INJ1	7/31/2006	70	Duplicate	0.85	14	55.2
CDM-INJ1	7/31/2006	70	Duplicate	2	15	70.2
CDM-INJ1	7/31/2006	70	Duplicate	4.75	6	76.2
CDM-INJ1	7/31/2006	70	Duplicate	9.5	30	106.2
CDM-INJ1	7/31/2006	70 70	Duplicate	19	0	106.2
CDM-INJ1	7/31/2006	70	Duplicate	25	0	106.2
CDM-INJ1	7/31/2006	70	Duplicate	37.5	0	106.2
CDM-INJ1	7/31/2006	70	Duplicate	50	0	106.2
CDM-P1	7/27/2006	15	Sample	< 0.075	8	8
CDM-P1	7/27/2006	15	Sample	0.075	3.8	11.8
CDM-P1	7/27/2006	15	Sample	0.106	14	25.8
CDM-P1	7/27/2006	15	Sample	0.25	6.7	32.5
CDM-P1	7/27/2006	15	Sample	0.425	10	42.5
CDM-P1	7/27/2006	15	Sample	0.85	14	56.5
CDM-P1	7/27/2006	15	Sample	2	25	81.5
CDM-P1	7/27/2006	15	Sample	4.75	19	100.5

**Table 2-1 Soil Grain Size Analysis Results (cont.)** 

			Sample	Sample Sieve Slot Size Weight Retained Co		Cumulative Retained
Well	Date	Depth	Type	(mm)	(grams)	(%)
CDM-P1	7/27/2006	15	Sample	9.5	0	100.5
CDM-P1	7/27/2006	15	Sample	19	0	100.5
CDM-P1	7/27/2006	15	Sample	25	0	100.5
CDM-P1	7/27/2006	15	Sample	37.5	0	100.5
CDM-P1	7/27/2006	15	Sample	50	0	100.5
CDM-P1	7/27/2006	25	Sample	< 0.075	3.3	3.3
CDM-P1	7/27/2006	25	Sample	0.075	1.4	4.7
CDM-P1	7/27/2006	25	Sample	0.106	4.7	9.4
CDM-P1	7/27/2006	25	Sample	0.25	2.4	11.8
CDM-P1	7/27/2006	25	Sample	0.425	3.8	15.6
CDM-P1	7/27/2006	25	Sample	0.85	11	26.6
CDM-P1	7/27/2006	25	Sample	2	22	48.6
CDM-P1	7/27/2006	25	Sample	4.75	15	63.6
CDM-P1	7/27/2006	25	Sample	9.5	31	94.6
CDM-P1	7/27/2006	25	Sample	19	5.5	100.1
CDM-P1	7/27/2006	25	Sample	25	0	100.1
CDM-P1	7/27/2006	25	Sample	37.5	0	100.1
CDM-P1	7/27/2006	25	Sample	50	0	100.1
CDM-P1	7/27/2006	25 25	Sample	< 0.075	10	100.1
CDM-P1	7/27/2006	35	•	0.075	5.3	15.3
		35 35	Sample Sample	0.106	5.5 16	31.3
CDM-P1	7/27/2006		•			
CDM-P1	7/27/2006	35	Sample	0.25	5.6	36.9
CDM-P1	7/27/2006	35	Sample	0.425	8	44.9
CDM-P1	7/27/2006	35	Sample	0.85	15	59.9
CDM-P1	7/27/2006	35	Sample	2	18	77.9
CDM-P1	7/27/2006	35	Sample	4.75	15	92.9
CDM-P1	7/27/2006	35	Sample	9.5	8.1	101
CDM-P1	7/27/2006	35	Sample	19	0	101
CDM-P1	7/27/2006	35	Sample	25	0	101
CDM-P1	7/27/2006	35	Sample	37.5	0	101
CDM-P1	7/27/2006	35	Sample	50	0	101
CDM-P1	7/27/2006	45	Sample	< 0.075	7	7
CDM-P1	7/27/2006	45	Sample	0.075	4.1	11.1
CDM-P1	7/27/2006	45	Sample	0.106	14	25.1
CDM-P1	7/27/2006	45	Sample	0.25	15	40.1
CDM-P1	7/27/2006	45	Sample	0.425	38	78.1
CDM-P1	7/27/2006	45	Sample	0.85	21	99.1
CDM-P1	7/27/2006	45	Sample	2	1.8	100.9
CDM-P1	7/27/2006	45	Sample	4.75	0	100.9
CDM-P1	7/27/2006	45	Sample	9.5	0	100.9
CDM-P1	7/27/2006	45	Sample	19	0	100.9
CDM-P1	7/27/2006	45	Sample	25	0	100.9
CDM-P1	7/27/2006	45	Sample	37.5	0	100.9
CDM-P1	7/27/2006	45	Sample	50	0	100.9
CDM-P1	7/27/2006	70	Sample	< 0.075	9.4	9.4
CDM-P1	7/27/2006	70	Sample	0.075	4.6	14
CDM-P1	7/27/2006	70	Sample	0.106	13	27
CDM-P1	7/27/2006	70	Sample	0.25	9.6	36.6
CDM-P1	7/27/2006	70	Sample	0.425	17	53.6

**Table 2-1 Soil Grain Size Analysis Results (cont.)** 

			Sample	Sieve Slot Size	Weight Retained	Cumulative Retained
Well	Date	Depth	Туре	(mm)	(grams)	(%)
CDM-P1	7/27/2006	70	Sample	0.85	8.2	61.8
CDM-P1	7/27/2006	70	Sample	2	2.8	64.6
CDM-P1	7/27/2006	70	Sample	4.75	2.1	66.7
CDM-P1	7/27/2006	70	Sample	9.5	20	86.7
CDM-P1	7/27/2006	70	Sample	19	14	100.7
CDM-P1	7/27/2006	70	Sample	25	0	100.7
CDM-P1	7/27/2006	70	Sample	37.5	0	100.7
CDM-P1	7/27/2006	70	Sample	50	0	100.7

Notes:

bgs = below ground surface

mm = millimeters

Figure 2-4 CDM-INJ1 Grain Size Distribution

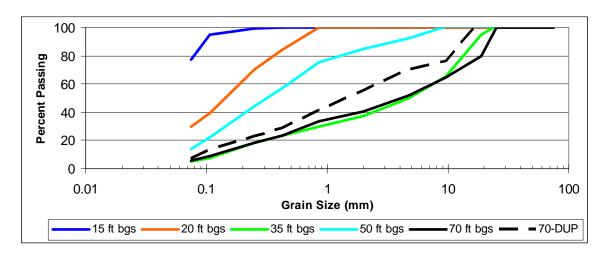
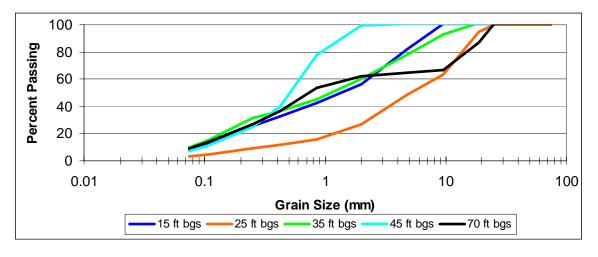
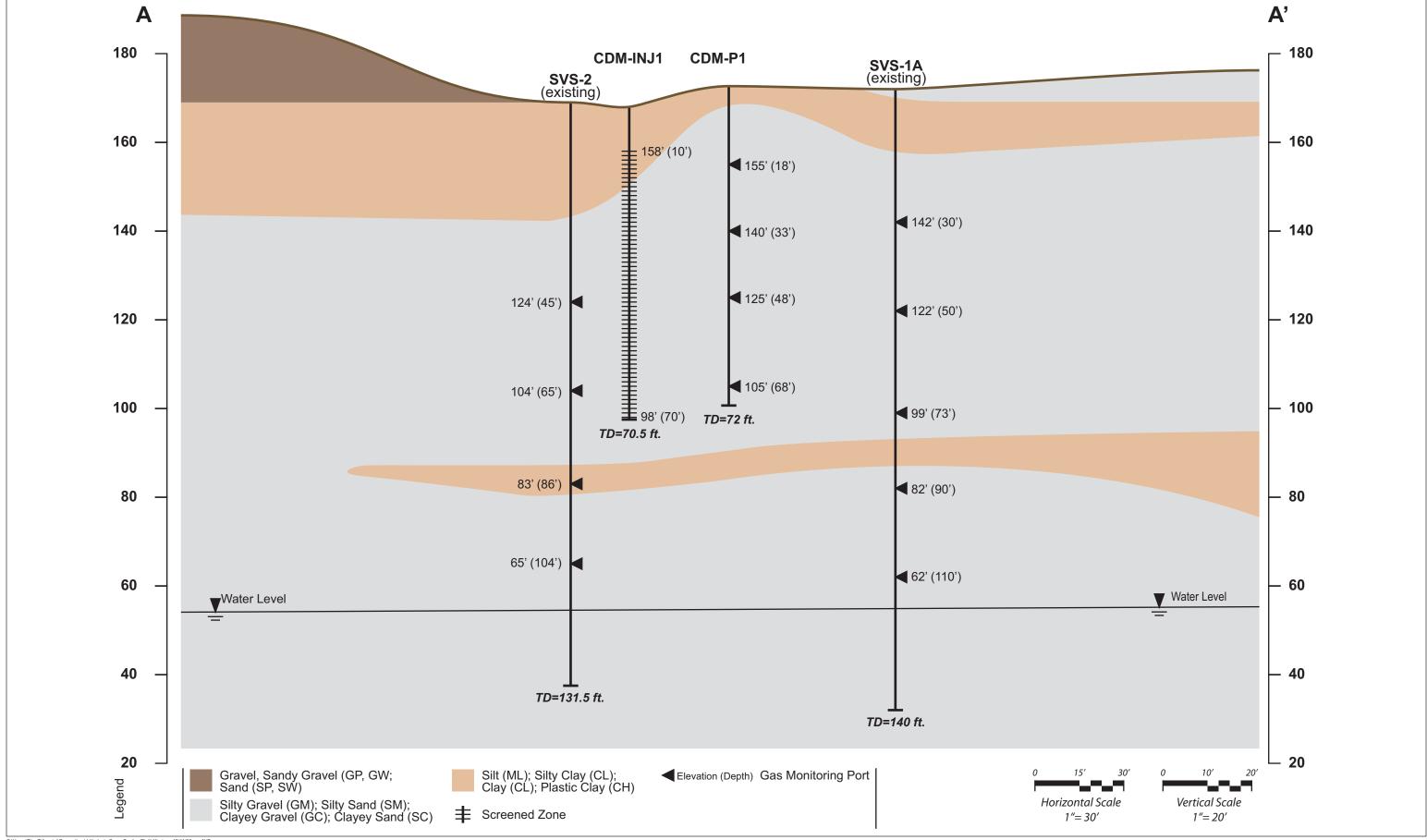


Figure 2-5 CDM-P1 Grain Size Distribution





C:\Users\TitusT\Aerojet\Generalized Lithologic Cross Section(FigX-X).ai 10/11/06 A

Source: Remedial Investigation Report for the Vador Zone at the Propellant Burn Area, Inactive Rancho Cordova Test Site HSI GEOTRANS, Inc., May 2000

### 2.6 Analytical Chemistry

The results for soil samples that were collected are presented in **Table 2-2**. Data for perchlorate, nitrate/nitrite, and moisture are graphically presented in **Figures 2-7** and **2-8**.

For soil from boring CDM-INJ1, the data indicate that nitrate/nitrite concentrations were less than 5 mg-N/kg and perchlorate ranged from 3.7 to 59 mg/kg based on field screening analyses. Field screening results generally correlated to laboratory confirmatory analyses. Perchlorate was present in greater concentrations at shallower depths and was associated with the finer grained soils based on comparison to **Figure 2-4**. Greater concentrations of perchlorate were also associated with greater moisture contents. The maximum moisture content in soil from CDM-INJ1 was 34 percent and the minimum moisture content was 6.5 percent.

For soil from boring CDM-P1, nitrate/nitrite concentrations were similar but perchlorate was nondetectable at shallow depths and ranged from 0.45 to 9.8 mg/kg at greater depths. Field screening results for perchlorate correlated generally well with laboratory results except at concentrations near the limit of detection for the ion-selective probe (about 0.2 mg/kg). Moisture ranged from 6.9 to 18 percent. For soil from both borings, soil moisture ranged from 6.9 to 16 percent in the more permeable soils (i.e., not silt or clay).

Total organic carbon (TOC) was generally nondetectable or near the limit of detection (0.2 to 0.3 mg/kg) and pH ranged from 6.9 to 8.1.

**Table 2-2 Soil Analytical Chemistry Results** 

					CDM A	nalysis		Laucks Analysis							
Well	Date	Depth (bgs)	Sample Type	Perchlorate (mg/kg)	Moisture	USCS	Moisture Non-Clay Silt	Perchlorate (mg/kg)	Difference (%)	Moisture	Difference (%)	pН	Nitrate & Nitrite as Nitrogen (mg/kg)	TOC	Total Solids (%)
CDM-P1	7/27/2006	5	sample	0.15	18.1	ML		(mg/kg)					(IIIg/Kg)		
CDM-P1	7/27/2006	5	duplicate	0.13		ML									
CDM-P1	7/27/2006	10	sample	0.12	7.5	GM	7.5								
CDM-P1	7/27/2006	15	sample	0.17	8.4	GM	8.4	< 0.011	991.0	10.1	-16.0	8.1	3.2	< .21	89.9
CDM-P1	7/27/2006	15	duplicate		8.3	GM							<i>3.2</i> 		
CDM-P1	7/27/2006	20	sample	0.079	9.4	GM	9.4								
CDM-P1	7/27/2006	25	sample	0.45	9.0	GC	9.0	1.3	-65.0	12.6	-29.0	7.7	4	< .23	87.4
CDM-P1	7/27/2006	30	sample	0.45	7.5	GC	7.5						· 		
CDM-P1	7/27/2006	35	sample	0.69	6.9	GC/SP	6.9	5	-86.0	6.9	0.0	7.8	1.8	<.21	93.1
CDM-P1	7/27/2006	40	sample	3.6	13.9	GC	13.9								
CDM-P1	7/27/2006	45	sample	7.3	9.5	GC/SM	9.5	8.5	-14.0	10.8	-12.0	7.5	2.2	0.24	89.2
CDM-P1	7/27/2006	50	sample	9.0	11.8	SM	11.8								
CDM-P1	7/27/2006	55	sample	6.2	12.0	SM	12.0								
CDM-P1	7/27/2006	55	duplicate		10.7	SM									
CDM-P1	7/27/2006	60	sample	5.0	7.1	SM	7.1								
CDM-P1	7/27/2006	65	sample	3.2	15.9	SC/SM	15.9								
CDM-P1	7/27/2006	65	duplicate	3.1		SC/SM									
CDM-P1	7/27/2006	70	sample	9.8	13.3	SM	13.3	12	-18.0	16.7	-20.0	7.4	1.3	<.22	83.3
CDM-INJ1	7/31/2006	5	sample	59	25.7	ML									
CDM-INJ1	7/31/2006	10	sample	49	32.9	ML/CL									
CDM-INJ1	7/31/2006	15	sample	30	18.5	ML		41	-27.0	19.9	-7.0	7	5.2	0.34	80.1
CDM-INJ1	7/31/2006	20	sample	58	34.3	CL/GC		73	-21.0	34.6	-1.0	6.9	10	<.3	65.4
CDM-INJ1	7/31/2006	25	sample	18	13.2	GC/SM	13.2								
CDM-INJ1	7/31/2006	30	sample	10	10.2	SM	10.2								
CDM-INJ1	7/31/2006	35	sample	5.6	11.2	SM	11.2	17	-67.0	13.7	-18.0	7.6	2.3	<.23	86.3
CDM-INJ1	7/31/2006	40	sample	6.7	11.9	SM	11.9								
CDM-INJ1	7/31/2006	45	sample	4.9	7.9	SM	7.9								
CDM-INJ1	7/31/2006	45	duplicate	4.2		SM									
CDM-INJ1	7/31/2006	50	sample	5.6	8.8	SM	8.8	7.7	-27.0	13.2	-33.0	7.8	2.2	<.22	86.8
CDM-INJ1	7/31/2006	55	sample	4.6	7.6	SM	7.6								
CDM-INJ1	7/31/2006	60	sample	4.1	7.4	SM	7.4								
CDM-INJ1	7/31/2006	65	sample	3.7	6.5	SM	6.5								
CDM-INJ1	7/31/2006	70	sample	4.1	6.5	SM	6.5	5.7	-28.0	7.8	-17.0	7.7	1.6	<.21	92.2
CDM-INJ1	7/31/2006	70	duplicate		7.5	SM				8	-0.1	7.7			0.9

#### Notes:

bgs = below ground surface

mg/kg = milligrams per kilogram

<20 = Not detected at indicated detection limit TOC = Total organic

-- = Not analyzed

ML = silt

GM = silty

GL = clayey

SP = poorly graded sand

SL = clayey sand

SM = silty sand

CL = clay

Figure 2-7 CDM-INJ1 Contaminant and Moisture Distribution

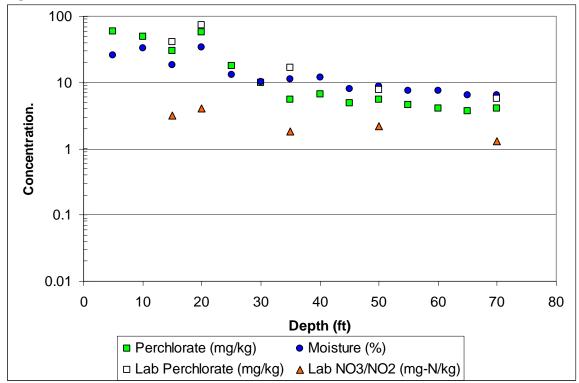
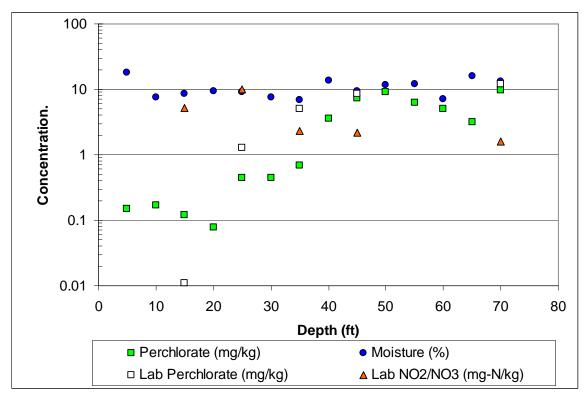


Figure 2-8 CDM-P1 Contaminant and Moisture Distribution



### 3.0 Microcosm Tests

#### 3.1 Abstract

Sacrificial batch microcosm tests were used to rapidly assess the ability of gaseous electron donors and various moisture contents to achieve optimal perchlorate remediation in vadose zone soil taken from the Aerojet Propellant Burn Area site in California. The electron donor candidates tested were hydrogen, 1-hexene, ethyl acetate, and liquefied petroleum gas (LPG) also known as propane. Each electron donor was tested at two different concentrations under two different soil moisture contents that were representative of minimum and maximum site moisture contents at the site. No perchlorate reduction occurred in low moisture (7%) bottles after an incubation time of 125-187 days, and all bottles except ethyl acetate achieved complete or partial perchlorate reduction in high moisture (16%) bottles. Results from these microcosm tests indicate that hydrogen is the most promising of the tested electron donors for the treatment of perchlorate in vadose zone soil, achieving complete perchlorate degradation within 35-42 days, with a perchlorate reduction rate of 0.1327-0.1894 d<sup>-1</sup>. LPG promoted complete perchlorate reduction at the high LPG dose and 1-hexene promoted partial perchlorate reduction at both doses; however, when compared to hydrogen, these donors had more significant lag periods of 21 - 49 days and lower perchlorate reduction rates of 0.0083-0.0326 d<sup>-1</sup> and 0.0079-0.0161 d<sup>-1</sup>, respectively.

### 3.2 Materials and Methods

### 3.2.1 Soil Characterization

The soil used in this test was collected using sonic drilling methods from the site and shipped to The Pennsylvania State University in six 5-gallon buckets in August 4, 2006. The day after arrival, the soil was processed as follows. After removing large stones by hand and passing the soil through a ½ inch sieve, all of the soil was well mixed together in a large container and then transferred to four buckets, sealed, and stored at room temperature. The following day, duplicate grab samples were taken from each bucket and tested for perchlorate, nitrate, pH, and soil moisture. The resulting standard deviation of perchlorate concentration was approximately 41% of the average concentration, so the soil was remixed and redistributed to four buckets again and retested for perchlorate, nitrate, pH, and soil moisture, as well as for total nitrogen and total carbon. The remaining soil was stored at room temperature in the sealed buckets for 10 days until the experiments were performed.

### 3.2.2 Experimental Design and Setup

The microcosm tests were performed in a standard statistical factorial design (**Table 3-1**). Soil moisture content, electron donor type, and electron donor concentration were the variables evaluated in the test. According to the lowest and highest moisture level naturally present at the field site, the moisture contents tested were 7 and 16%. The electron donors tested were hydrogen, ethyl acetate, 1-hexene, and commercial liquid petroleum gas (LPG), the main component of which is propane. These electron donors were selected because of their high vapor pressures and high Henry's constants (**Table 3-2**), making them well-suited to transport in the vadose zone. Low and high electron donor concentrations were designed to be three and ten

times the quantity required to stoichiometrically reduce all of the oxygen, nitrate, and perchlorate present in the soil. The concentrations listed in Table 3-1 reflect these stoichiometric calculations based on the actual nitrate and perchlorate concentrations, and conservatively assume that the entire headspace is air. A negative control containing no electron donor and a positive control containing ethanol, which was previously shown by CDM to give positive perchlorate degradation results, were also tested.

For each test condition shown in **Table 3-1**, nine replicate bottles were established to enable periodic sacrificial analysis of the soil, and half of the active tests (tests 1, 2, 6, 7, 11, 12, 13, and 16) were randomly selected to be run in duplicate. To setup the 234 microcosms, soil from the field site was transferred in 10-gram (g) aliquots to 150-mL glass serum bottles. After the bottles were sealed with thick butyl rubber stoppers and aluminum crimp tops, the gas in the bottles was purged with 10-psi ultra-high purity nitrogen gas for at least 15 minutes to remove oxygen and maintain anoxic conditions. Ten percent (10%) of the bottles were randomly chosen for headspace oxygen analysis. Greater than 1% oxygen was detected in one of the bottles in the Test 5 set, so all nine bottles in Test 5 were re-purged with nitrogen, retested for oxygen, and passed. After degassing all of the bottles, one of the candidate electron donors and de-ionized water were injected into the bottles to achieve the desired test conditions. During the injection, liquid electron donors (ethyl acetate and 1-hexene) were dropped onto the wall of the bottles and allowed to completely vaporize into the gaseous phase rather than injecting the electron donor liquid directly onto the soil. Prior to injecting the gaseous electron donors (hydrogen and LPG), an equivalent volume of nitrogen gas was withdrawn from the bottles to avoid increasing pressure. Carbon dioxide at 748 and 2508 mg/kg was added as a carbon source to microcosms containing hydrogen. The amount of carbon dioxide needed in the hydrogen microcosms was conservatively assumed to be half of the electron donor concentration (in mol/L), in order to ensure that lack of carbon would not be a limiting factor for bioremediation. See Appendix A-3 for additional details about the microcosm setup.

The total setup time for all 234 bottles was 48 days (extended due to an instrumentation problem) during which time the bottles were stored at room temperature on the open bench. After adding the electron donor and shaking to facilitate homogeneous headspace-soil contact, the first bottle of each test condition was sacrificed immediately as the time zero measurement. The remaining bottles were incubated in the dark at room temperature for a total of two to three months and were shaken about 3 times per week to help gaseous electron donor distribution and increase headspace-soil contact.

**Table 3-1 Matrix of Experimental Conditions Tested in the Microcosm Experiments** 

Test Number	Electron Donor	Electron donor concentration (mg/kg soil)	Soil moisture
1	H <sub>2</sub> (+CO <sub>2</sub> )	34 (+374)	7%
2	Ethyl acetate	150	7%
3	1-Hexene	80	7%
4	LPG	75	7%
5	$H_2$ (+ $CO_2$ )	114 (+1254)	7%
6	Ethyl acetate	501	7%
7	1-Hexene	165	7%
8	LPG	250	7%
9	$H_2$ (+ $CO_2$ )	34 (+374)	16%
10	Ethyl acetate	150	16%
11	1-Hexene	80	16%
12	LPG	75	16%
13	$H_2$ (+ $CO_2$ )	114 (+1254)	16%
14	Ethyl acetate	501	16%
15	1-Hexene	165	16%
16	LPG	250	16%
17	Negative Control	0	16%
18	Positive Control	436 (Ethanol)	16%

**Table 3-2 Properties of Tested Electron Donors in Microcosm Tests** 

Electron donor Candidates	Molecular formula	Formula weight (g/mol)	H (atm-m <sup>3</sup> /mol)	P <sub>sat</sub> (mm Hg)
Hydrogen	$H_2$	2	1.28E+00	760
Ethyl Acetate	CH <sub>3</sub> CH <sub>2</sub> COOCH <sub>3</sub>	88.11	1.34E-04	60
1-Hexene	CH <sub>3</sub> (CH <sub>2</sub> ) <sub>3</sub> CHCH <sub>2</sub>	84.16	4.17E-01	100
LPG (Liquefied Petroleum Gas, 90% propane)	CH <sub>3</sub> CH <sub>2</sub> CH <sub>3</sub>	44.1	6.00E-01	5700
Ethanol	C <sub>2</sub> H <sub>5</sub> OH	46.07	5.00E-06	40

During the incubation, one of the replicates of each test condition was analyzed every one to four weeks, the frequency depending on the observed rate of perchlorate degradation. During the analysis process, the headspace electron donor concentration,  $O_2$ , and  $CO_2$  were tested first, and then the bottles were sacrificed (i.e., opened) to test the soil for perchlorate, nitrate, nitrite,

chlorate, chlorite, and chloride concentration, moisture content, and pH. Between every two sampling points, the concentration of electron donor in the headspace was tested weekly.

### 3.2.3 Chemical Analyses

An Agilent model 6890N gas chromatograph (GC) equipped with a DB-624 column and a flame ionization detector (FID) was used to test the electron donors (ethyl acetate, 1-hexene, propane, and ethanol). Headspace samples (1000  $\mu$ L) were transferred from the microcosm bottles in a gas-tight locking syringe to the injector which was held at a temperature of 150°C. Helium was used as the carrier gas at a flow rate of 0.2 mL/min. The oven temperature was held at 45°C for 4 minutes, and then ramped to 60°C at a rate of 10°C /min, ramped to 100°C at a rate of 20°C /min and then held at 100°C for 1 minute, giving a total run time of 8.5 minutes. The detector was held at 240°C where hydrogen, air, and nitrogen (as make up gas) supplied the flame at flow rates of 32, 400, and 30.7 mL/min, respectively.

Hydrogen and oxygen concentrations were quantified using a SRI 8610 B gas chromatograph (GC) equipped with a thermal conductivity detector (TCD) and a Molesieve 5A molecular sieve column (Alltech). Argon was used as the carrier gas at a pressure of 20 psi and the oven was held isothermally at 73°C. Carbon dioxide concentration in headspace of samples was measured using a SRI GC (Model 310) equipped with a TCD and a Porapak Q column. Helium was used as the carrier gas at a pressure of 20 psi and the oven was held isothermally at 83°C.

Perchlorate, chlorate, chloride, nitrate, and nitrite were extracted from 5-g soil by vortexing for 1 minute in a 50-mL centrifuge vial containing 20-mL deionized water. A preliminary experiment conducted in triplicate demonstrated that 106.58±6.1% of perchlorate was recovered from the soil after only 0.5 minutes of vortexing. After vortexing, the extracts were centrifuged at 5000 rpm for 15 minutes and the supernatant filtered through a 0.2-um-pore-diameter filter to remove soil particles. The anion concentrations were measured using a DX-500 ion chromatograph (Dionex), equipped with an AS-11 column, and an ED40 Electrochemical Detector. A sodium hydroxide solution eluent with a flow rate of 1 mL/min was used to separate the species over a 30 minute run time. The eluent was composed of 98.7% DI water and 1.3% 200 mM sodium hydroxide at the beginning of each run and held for 10 minutes, then ramped to 96.4% DI water and 3.6% 200 mM sodium hydroxide and held until the time was 17.4 min, ramped to 65.5% DI water and 34.5% 200 mM sodium hydroxide and held from 18.8 min to 23 min, then ramped back to 98.7% DI water and 1.3% 200 mM sodium hydroxide and held until the run ended. The detection limit of nitrate was determined according to the procedure in USEPA Definition and Method for MDL (USEPA, 1986) and was found to be 150 ppm.

Soil moisture content was determined gravimetrically according to D 2216-98 Standard Test Method for Laboratory Determination of Water (Moisture) Content of Soil and Rock by Mass (ASTM, 1999), and the pH of the extracts after centrifuging was measured with a Fisher Accumet AB 15 pH meter equipped with an Orion Thermo Electron combination pH electrode. Total carbon and total nitrogen were determined using a Combustion-Fisons NA 1500 Elemental Analyzer by the Agricultural Analytical Services Laboratory at The Pennsylvania State University.

### 3.3 Microcosm Test Results

Before the microcosms were initiated, the homogenized soil from the Aerojet site was chemically characterized. The results of the soil characterization are provided in the column marked "original" in Table 3-3. The percentage of total nitrogen of the soil sample was  $0.016\% \pm 0.006\%$  and total carbon was  $0.037\% \pm 0.021\%$  (triplicate averages).

During the microcosm tests, the soil moisture content remained relatively constant in both the low and high soil moisture sets. The soil pH remained near 7. No intermediate perchlorate reduction products (chlorate and chlorite) were detected during the treatment. The nitrate concentration was reduced below the detection limit (150 ppb) at the time zero sampling point in all microcosms at both moisture levels. Nitrite (NO<sub>2</sub>), the intermediate product of nitrate reduction, was also below detection (**Appendix A-3**). This high rate of denitrification indicates that anoxic conditions were achieved in the microcosms and that electron donor was available throughout the soil. The average final conditions of all the analytes in the soil after 125-187 days of treatment with the different electron donors under high soil moisture content are summarized in **Table 3-3**. Complete data sets and profiles for each test condition are provided in **Appendix A-3**.

Table 3-3 Original and Final Conditions of the Aerojet Site Soil after 125-187 Days of Treatment Using Different Electron Donors at 16% Soil Moisture. (Table Shows Duplicate Averages Except where Noted.)

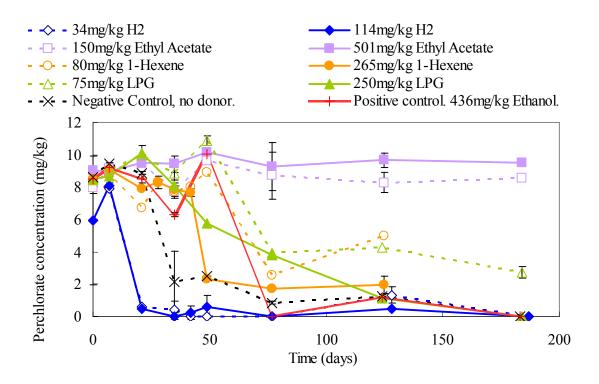
		Original	Ethyl Acetate		1-hexene		LPG		Hydrogen	
	mg/kg	-	150	501	80	265	75	250	34	114
Soil moisture	%	8±0.6*	15	15.4	14.72	15.6	12.9	13.85	15.21	15.31
Soil pH	-	6.85±0.3*	6.82	6.58	6.97	6.97	7.84	7.56	7.15	6.38
perchlorate	mg/kg	8.2±1.3*	8.53	9.52	5	1.96	2.71	ND	ND	ND
chloride	mg/kg	-	2.93	3.36	6.21	4.26	6.85	6.03	7.27	8.12
nitrate	mg/kg	2.1±0.3*	ND	ND	ND	ND	ND	ND	ND	ND
electron										
donor	mg/kg	-	ND	ND	68.07	121	142.5	491.35	56.98	83.33

<sup>\* =</sup> average of soil from 4 buckets after the second time of mixing with two duplicate measurements each. ND = non-detect

Perchlorate reduction was not observed in any of the 7% soil moisture sets (**Appendix A-3**), regardless of which electron donor was present. Under high soil moisture (16%), the bioremediation of perchlorate was supported by all the electron donors tested except ethyl acetate (**Figure 3-1**). Complete perchlorate removal was achieved in 35 and 42 days with hydrogen at high and low concentration, respectively. After 184 days of incubation, perchlorate concentration was reduced to less than detectable concentrations in high LPG concentration bottles, but had a residual of 2.71 ppm in low LPG concentration bottles. The concentration of perchlorate was reduced to 1.96 ppm and 5 ppm in high and low 1-hexene concentration bottles, respectively. The 1-hexene bottles were only incubated for 125 days in total due to the higher

frequency of sacrificing at the beginning of the test. Complete perchlorate reduction occurred within 77 days in the positive control and 183 days in the negative control, both of which were only run at 16% soil moisture. The interesting implications of perchlorate reduction in the absence of an external electron donor are explored further in the Discussion section that follows.

Figure 3-1 Perchlorate Degradation in Microcosm Tests with Different Electron Donors at 16% Soil Moisture.



Although the rates of perchlorate degradation are difficult to accurately quantify in this experiment due to the observed shouldering (lag) effect and relatively low sampling frequency, it does appear that perchlorate reduction followed a first order decay (**Figure 3-2**). First order perchlorate reduction has been observed by others (Logan et al., 2001), so this result is not unexpected. Average first order rate constants for perchlorate reduction were estimated for each electron donor based on the slopes of the curves of each profile past the shoulder in **Figure 3-2** (i.e., the slopes of negative ln([ClO<sub>4</sub>-]/[ClO<sub>4</sub>-]<sub>0</sub>) vs. time), with the exception of hydrogen and the positive control, which were determined based on the initial straight portion of the curve past the shoulder. Maximum rates of perchlorate degradation were also estimated for each electron donor by choosing the maximum slopes in **Figure 3-2**. The resulting estimated first-order rates of perchlorate degradation, k<sub>ClO4-(average)</sub> and k<sub>ClO4-(maximum)</sub>, for each electron donor are provided in **Table 3-4**. The highest rates of perchlorate reduction, k<sub>ClO4-(maximum)</sub>, were found for ethanol and hydrogen (high concentration), followed by hydrogen (low concentration); 1-hexene (high

concentration), negative control, LPG (high concentration), 1-hexene (low concentration), LPG (low concentration), and finally ethyl acetate.

Figure 3-2 Relative Change in Perchlorate Concentration Over Time Used to Estimate First Order Rate Constants.

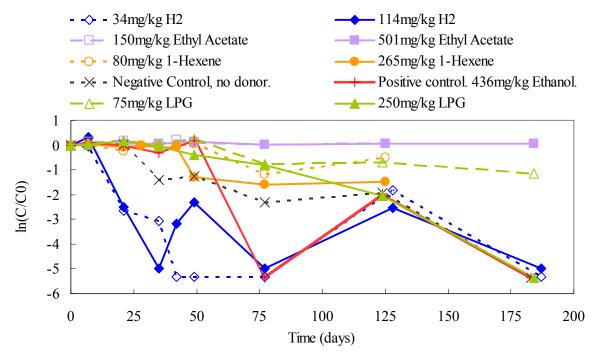


Table 3-4 First Order Perchlorate Degradation Rate Constants, Lag Periods, and Final Perchlorate Concentrations for the Electron Donors Tested in the Microcosm Tests at 16% Soil Moisture.

		k <sub>ClO4</sub> . (average) <sup>#</sup> (day <sup>-1</sup> )	k <sub>ClO4</sub> . (maximum)* (day <sup>-1</sup> )	Lag period (days)	C <sub>CIO4</sub> final (mg/kg)
$\mathbf{H}_2$	Low	0.13	0.19	7	$0.04^{*}$
	High	0.19	0.20	7	$0.04^{*}$
LPG	Low	0.0083	0.037	49	2.71
	High	0.033	0.055	21	$0.04^{*}$
1-hexene	Low	0.0079	0.045	28	2.54
	High	0.016	0.17	28	1.96
Ethyl acetate	Low	0	0	>125	8.53
	High	0	0	>184	9.52
Negative Control		0.0027	0.10	21	2.12
<b>Positive Control</b>		0.20	0.20	49	0.04*

<sup>#</sup> Rates were estimated based on the slopes of the whole curves past lag periods except for  $H_2$  and Positive control. The rates of  $H_2$  were determined from the data of 7-42 days for low concentration and 7-35 days for high concentration. The rate for the positive control was determined by the data of 49-77 days.

The calculation was based on the data from:

H<sub>2</sub> (low): 7-21 days; H<sub>2</sub> (high): 7-21 days; LPG (low): 49-77 days; LPG (high): 124-184 days; 1-hexene (low): 49-77 days; 1-hexene (high): 42-49 days; Negative control: 21-35 days; Positive Control: 49-77 days.

### 3.4 Discussion

From the results of the microcosm test, it is obvious that high soil moisture is critical to perchlorate bioremediation. Another study which tested the GEDIT technology also concluded that soil moisture is the key factor (Evans and Trute, 2006). A similar conclusion was obtained in a pilot study of *in situ* perchlorate bioremediation at The Longhorn Army Ammunition Plant (LAAP) (Nzengung et al., 2003), which found that the best treatment results were achieved in the wettest (saturated) soils. For GEDIT, however, it may be impractical to increase in situ soil moisture. In this microcosm test, 7% was too low to support perchlorate bioremediation and 16% was successful at reducing perchlorate in most bottles, but 16% may not be the minimum required moisture. The purpose of this study was to determine the potential for perchlorate biodegradation at the observed limits of ambient soil moisture. This study clearly demonstrated

<sup>\*</sup> The maximum perchlorate reduction rate observed for each donor during incubation.

<sup>\*</sup> Perchlorate was non-detectable. The number 0.04 is ten times the method detection limit.

that perchlorate biodegradation may be limited in soil containing 7% moisture. In the field demonstration, it will be important to assess further the relationship between soil moisture content and perchlorate reduction and also to determine the optimum moisture for both perchlorate bioremediation and electron donor transport.

Of the electron donors tested, hydrogen appears to be the most promising for several reasons. The high Henry's constant of hydrogen gives it excellent mobility in the gaseous phase (**Table 3-2**), and its small molecular size enables it to easily diffuse into zones of low permeability. In addition, the simple hydrogen molecule is readily utilized by microorganisms. Hydrogen has been widely used as an electron donor for isolating perchlorate-reducing bacteria and has also been used in the treatment of (per)chlorate contaminated water (Miller & Logan, 2000; Nerenberg et al., 2002; Kroon & van Ginkel, 2004).

In this experiment there was a 7 day lag period in both high and low hydrogen bottles before perchlorate degradation began. This lag period is similar to the 14 day lag period observed in another study of perchlorate bioremediation in vadose zone soil with hydrogen as the electron donor (Nozawa-Inoue et al., 2005). Shorter lag periods for perchlorate degradation with hydrogen/carbon dioxide than other electron donors may also imply that there are more autotrophic than heterotrophic perchlorate-reducing microbial populations in the soil. The observed perchlorate reduction rate  $k_{CIO4}^{-}$  was almost the same in the low and high hydrogen concentration bottles. There is not sufficient data, however, to imply a relationship between hydrogen concentration and perchlorate reduction rate due to lack of sampling points between day 7 and day 21. To examine how higher hydrogen concentrations affect perchlorate reduction rate, a higher sacrificing frequency between 7 and 21 days of incubation is needed. Assuming a first order reaction (Logan et al., 2001), the maximum observed perchlorate reduction rate,  $k_{CIO4}^{-}$  (maximum), obtained from this research is on the same order of magnitude as those obtained by others with slurry sediments/soils (**Table 3-5**). This indicates that saturated soil conditions are not necessary to produce high perchlorate reduction rates.

Table 3-5 First Order Perchlorate Reduction Rates Observed in the Literature and Their Experimental Conditions.

	<b>Electron Donor</b>			
Soil	(mg/kg)	Soil moisture	Rate $k_{ClO4}$ (d <sup>-1</sup> )	Source
HW84 Sidestream	TVS (115.9)	Slurry	0.37±0.07	
HW84 Mainstream	TVS (84.5)	Slurry	0.14±0.02	
Longhorn	TVS (43.3)	Slurry	0.16±0.08	Tan, 2003
HW317	TVS (160.5)	Slurry	1.42±0.67	
HW317/MN	TVS (70.6)	Slurry	0.11±0.03	
	H <sub>2</sub> (34 -114)	16%	0.19-0.20	
	LPG (75 – 250)	16%	0.037-0.056	
Aerojet	1-hexene (80-165)	16%	0.045-0.17	This research
	None (H <sub>2</sub> ?)	16%	0.10	
	Ethanol	16%	0.20	

TVS = Total volatile solids in the sediments/soils (a rough approximation of the amount of organic matter content in the sediments. Tested with the standard method (APHA et al., 1998)).

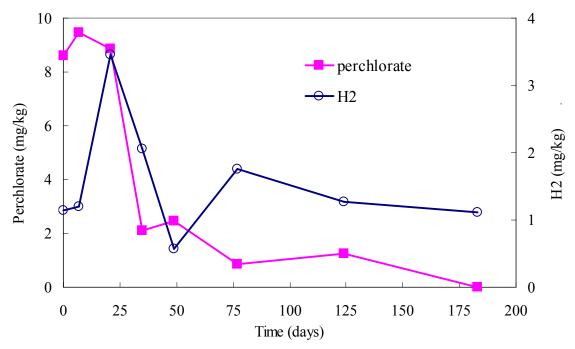
The overall observed favorability of electron donors in this experiment, taking into account both the rates and extent of perchlorate reduction, was ethanol >  $H_2$  > LPG > 1-hexene > ethyl acetate. The reason why ethyl acetate failed to serve as electron donor for perchlorate remediation in this microcosm test is not clear. Ethyl acetate was tested in another study of GEDIT (Evans and Trute, 2006), in which approximately 10% perchlorate removal was observed in the middle and end of a column containing 10% soil moisture while no perchlorate reduction occurred at the first 1/3 of column after 34 days of incubation. Ethanol was also tested in that research and showed promising perchlorate reduction but poor transport in column tests. Propane has been tested to a limited extent; however, it was shown to support perchlorate reduction only in one case. (Envirogen, 2002; Hoponick, 2006). To the best of our knowledge this is the first research reporting the use 1-hexene as an electron donor for perchlorate bioremediation.

Nitrate was not detected after the t = 0 sampling point, and nitrite was below detection throughout the experiment. The ability of gaseous electron donors to support denitrification has significant implications for the potential remediation of this common subsurface contaminant. The National Water Quality Assessment (NAWQA), a program of the US Geological Survey, has documented that nitrate is the pollutant that most frequently exceeds its standard limits (Squillace et al., 2002). According to the EPA, more than 59 millions pounds of nitrite/nitrate were released to water, and more than 53 millions of pounds to land, between 1991 and 1993. High nitrate levels are usually found in shallow aquifers underneath agricultural areas with well drained soils and permeable vadose zones (Spalding and Exner, 1993; Squillace et al., 2002). This research indicates that GEDIT could be used to treat nitrate in these high-risk, permeable vadose zones, thereby reducing potential nitrate contamination of groundwater supplies.

The intermediate products of perchlorate reduction (chlorate and chlorite) were not detected during these microcosm tests, similar to the results of other research which documented that perchlorate reduction to chlorate is the rate limiting step. Chlorate accumulation has been reported, however, in both mixed and pure cultures of hydrogen-oxidizing, perchlorate-reducing bacteria (Nerenberg et al., 2002, Nerenberg et al., 2006).

Complete perchlorate reduction occurred in the negative control which contained no external electron donor, and the degradation rate was higher than that observed for 1-hexene (low concentration), LPG, and ethyl acetate. Although there was sufficient carbon in the soil (total C = 0.037% = 308 umol in 10 g soil) to theoretically account for this perchlorate degradation (10 mg/kg = 1 umol in 10 g soil) if it was bioavailable, all treatments would have had similar benefit. The only other explanation for why the negative control exhibited such a high rate of perchlorate reduction is that another electron donor was generated and subsequently utilized in the negative control bottles. During the experimental setup, the bottles were filled with soil, purged with nitrogen, and allowed to sit on the open lab bench for at least one day. Immediately after flushing with nitrogen, no hydrogen was detected in the headspace, but after sitting in the light of the laboratory, a small amount of hydrogen was detected in all of the bottles, before any electron donor was injected. This hydrogen peak remained in all of the bottles throughout the entire incubation, except for the negative control. In the negative control bottles, the change of perchlorate concentration and hydrogen concentration seems related (Figure 3-3). During the first 14 days, hydrogen was accumulating during the lag period prior to perchlorate biodegradation. Then, perchlorate and hydrogen concentration dropped simultaneously. The measured hydrogen concentration change (1.4 mg/kg) from day 14 to day 49 is approximately twice the stoichiometric electron donor requirement for perchlorate reduction (with a 6.4 ppm perchlorate concentration change). The  $k_{ClO4}$  in the negative control, however, was only 1/5 of that for the low concentration hydrogen bottles (**Table 3-4**). There was also a longer lag period. This may indicate the perchlorate degradation in the negative control was limited by the concentration of hydrogen.

Figure 3-3 Perchlorate and hydrogen concentration changes over time in negative control microcosms containing no external electron donor at 16% soil moisture.



To prove that the hydrogen detected in non-hydrogen-injected bottles was produced biologically, a small experiment was performed. For this experiment, microcosm bottles were set up in duplicate in the same way as described in the Materials and Methods section with a nitrogen gas  $(N_2)$  headspace and Aerojet soil at 16% moisture. The following four conditions were tested: 1) Empty Controls containing only  $N_2$ ; 2) Autoclaved Controls containing autoclaved soil; 3) Active-Light containing soil incubated in the light on the bench; and 4) Active-Dark containing soil incubated in dark (**Table 3-6**). All bottles were incubated on the bench for one day except the Active-Dark which were incubated in a dark drawer. No hydrogen accumulation was detected in either the empty or autoclaved controls (kept on the open bench), which eliminated the possibility that the hydrogen was introduced with the nitrogen gas or was the result of an abiotic reaction in the soil. For the Active ones, the two bottles left in the light on the open lab bench (as what happened in the microcosm test) generated hydrogen which was detected the next day, whereas the two bottles incubated in the dark immediately after setup showed no hydrogen production (**Table 3-6**.)

Table 3-6 Setup and Results of the 1-day Hydrogen Production Test with the Aerojet Soil at 16% Soil Moisture.

	Soil	Purged w/ N <sub>2</sub>	Autoclaved	Incubate	Initial H <sub>2</sub> (uM)	Final H <sub>2</sub> (uM)	Hydrogen Produced
Empty Control	No	Yes	No	Light	0	0	No
Autoclaved Control	Yes	Yes	Yes	Light	0	0	No
Active-Light	Yes	Yes	No	Light	0	3.06±0.34	Yes
Active-Dark	Yes	Yes	No	Dark	0	0	No

Based on the results of this experiment, it seems that hydrogen producing microorganisms are present in the Aerojet site soil and that they are photoautotrophic. These ubiquitous, sporeforming organisms (Cheong and Hansen, 2006) were likely washed down into the subsurface soil in spore-form during rainfall events and after the soil moisture was adjusted, anoxic conditions achieved, and light applied in the laboratory, they germinated because the conditions in microcosm bottles were favorable. H<sub>2</sub>-photoproducing microorganisms, such as purple bacteria (BioCycle, 2004), can convert organic residuals in the soil to hydrogen and carbon dioxide in the presence of light as shown in the equation below (this equation is written for the simplest carbon source, carbon monoxide, but it can similarly be balanced for other organic compounds):

$$CO + H_2O + light \rightarrow H_2 + CO_2$$

Even though hydrogen production should be companied by carbon dioxide production as shown in the equation above, no carbon dioxide was detected in the negative control bottles. It is possible that the concentration of carbon dioxide was too low to be detected by the GC, and it is also possible that part of the carbon dioxide produced was used as a carbon source for perchlorate biodegradation, or remained dissolved as bicarbonate. In those bottles with external electron donors of ethyl acetate, 1-hexene (low concentration), and LPG, even though small amount of hydrogen was also detected, the perchlorate degradation rate was lower than that in the negative control. This may indicate that these chemicals are toxic to hydrogenogens and/or perchlorate reducing microorganisms and inhibited their activity, but no evidence has been found in the literature to support this conjecture. To better explain the results, a study of the microbial community in the Aerojet soil using molecular microbial ecology techniques, and a study of the possible toxicity of the tested electron donors to these bacteria, may be needed. However, since photoautotrophic hydrogenogens require light to produce hydrogen, it is unlikely that they would provide any benefit to the *in situ* remediation being proposed, regardless of which external electron donor is applied.

#### 4.0 Column Test Results

#### 4.1 Abstract

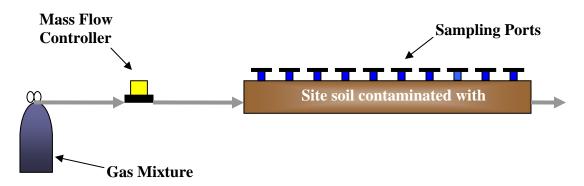
A series of column studies were conducted to quantify the transport rate of the best performing electron donor from the microcosm study through vadose zone soil from the site containing 10% soil moisture. After quantifying the transport rate, the columns were incubated for one to two months to evaluate the resulting extent of perchlorate degradation. In the first column study, 20% hydrogen (H<sub>2</sub>) (balance nitrogen, N<sub>2</sub>) was tested as the sole electron donor, without any added carbon source. Hydrogen breakthrough times were 3.4 and 5.6 hours. Complete nitrate reduction was achieved in both columns but no perchlorate degradation was detected in column #1 after 4 weeks of incubation or in column #2 after 10 weeks of incubation. To eliminate the possibility of carbon limited perchlorate reduction and to leverage the positive microcosm results with propane, a mixture of 2% propane, 10% CO<sub>2</sub>, 20% H<sub>2</sub>, and 68% N<sub>2</sub> was tested in the second column study. The breakthrough times of hydrogen were 7.2 hours and 8.0 hours. Complete nitrate reduction was achieved in both columns #3 and 4 but no perchlorate degradation was detected in column #3 after 4 weeks of incubation or in column #4 after 8 weeks of incubation. A small batch test conducted after the column experiment indicated that that storage of the soil prior to conducting the column study and low soil moisture content both resulted in the lack of perchlorate degradation.

#### 4.2 Materials and Methods

#### 4.2.1 Experimental Design and Setup

The column studies were conducted in columns made of clear polyvinylchloride (PVC) pipes measuring 2 inches in diameter and 5 feet in length. The ends were capped with 2-inch-diameter PVC caps and stainless steel Swagelok fittings. Sampling ports consisting of drilled holes plugged with thick butyl rubber stoppers were placed every 2 inches along the length of the columns (29 in total) to enable the discrete measurement of gaseous electron donor transport (**Figure 4-1**).

Figure 4-1 Schematic and Photograph of the GEDIT Column System in the Laboratory.





Prior to packing the columns, the soil moisture was adjusted to 10% by adding distilled water and mixing well. An attempt was made to run the columns at the average soil moisture of the microcosm tests (12%), but at this level the monitoring of electron donor concentrations along the column length was impeded due to the high-moisture soil clogging the gas-tight syringe needle as soon as it was inserted into the column. Therefore, 10% soil moisture content was chosen as a compromise that enabled easier monitoring of soil gas in the columns. The columns were packed by adding 1-2" lifts of soil and tapping the sides of the column between lifts to promote even soil distribution. Each column was packed with a total of 4.94 kg soil to achieve a soil density of 1.6 g/ml. After packing, the column caps and the stoppers placed in the sampling ports were sealed with Epoxy glue. Duplicate columns were made for each test. Prior to injecting the electron donor, the tubing connections and column sampling ports were leak-tested while the column was being purged with nitrogen gas at a flow rate of 4.9 ml/min.

#### 4.2.1.1 Hydrogen Column Setup

Two duplicate columns (Column #1 and #2) were set up on January 21 and 22, 2007, to test hydrogen as the sole external electron donor. Before introducing hydrogen to each column, the columns were purged with nitrogen gas at a flow rate of 4.9 ml/min (0.01 cm/s average linear velocity) for approximately 10 hours (2.4 pore volumes) until less than 1% oxygen was detectable in the column effluent to ensure anoxic conditions. A gas mixture consisting of 20% hydrogen and 80% nitrogen was then purged through the columns at a flow rate of 4.9 ml/min via mass flow rate controllers (AALBORG, Model# GFC17). The effluents of the columns were tested for hydrogen concentration every half hour to capture breakthrough curves. After hydrogen was observed to travel from the beginning to the end of the columns and reached the same hydrogen concentration throughout, the gas injection was stopped and the column ends capped. Headspace samples were taken with a 250-uL gas-tight locking syringe (Hamilton) from seven ports spaced evenly along the column length to construct a hydrogen profile. The columns were then incubated in dark at room temperature for 4-10 weeks. During incubation, headspace samples were taken along the column length to check hydrogen and oxygen concentration every 1-2 weeks. Columns were repurged with the 20% hydrogen / 80% nitrogen gas mixture every 2-3 weeks when >1% oxygen concentration was detected in the column, or when the hydrogen concentration was observed to significantly decrease.

After 4 weeks of incubation, Column #1 was sacrificed and the soil samples behind every other sampling port analyzed for perchlorate, chlorate, chlorite, chloride, nitrate, nitrite, pH and soil moisture. The other duplicate column (Column #2) was sacrificed after 10 weeks of incubation and the soil similarly analyzed.

#### 4.2.1.2 Four-Gas Mixture Column Setup

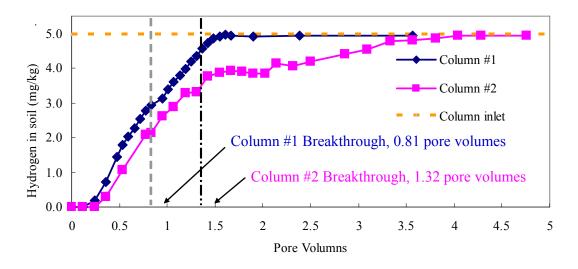
Another column study was similarly performed in which 10% carbon dioxide (CO<sub>2</sub>) was added as a carbon source, 20% hydrogen and 2% propane (the main component of LPG) were added as electron donors, and the balance was nitrogen. The resulting four-gas-mixture, consisting of 2% propane, 10% carbon dioxide, 20% hydrogen, and 68% nitrogen was added into columns #3 and #4 on March 28 and 30, 2007. Columns #3 and #4 were monitored, sacrificed, and analyzed as described above after 4 and 8 weeks of incubation, respectively.

#### 4.3 Results

#### 4.3.1 Hydrogen Column

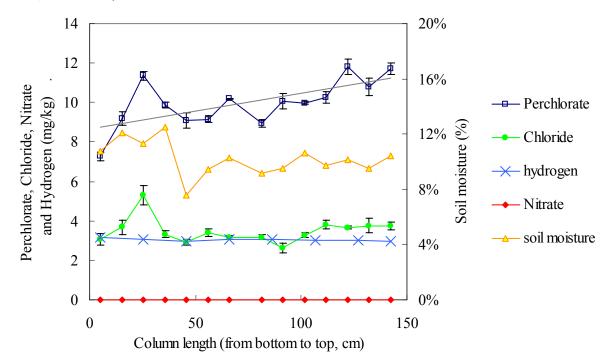
In Column #1, hydrogen breakthrough time was calculated as 3.4 hours (0.81 pore volumes) (Shackelford, 1994), while it took approximately 5.58 hours (1.32 pore volumes) for hydrogen to breakthrough in Column #2 (**Figure 4-2**, see **Appendix A-4** for breakthrough time calculations). After 21 days of incubation, the hydrogen concentration in both Columns #1 and #2 were found to have decreased to 1% of the incubated concentration, and oxygen was detected in Column #2. A leak at the column outlet cap was detected in Column #2 and repaired. Both columns were repurged with 20% hydrogen / 80% nitrogen gas mixture and then incubated. Before sacrificing, Column #2 was re-purged for two more times at 42-days and 63-days of incubation to replenish the hydrogen concentration (no oxygen was detected in column #2 during this period).

Figure 4-2 Hydrogen Breakthrough Curves for Column #1 and #2 with 10% Soil Moisture.



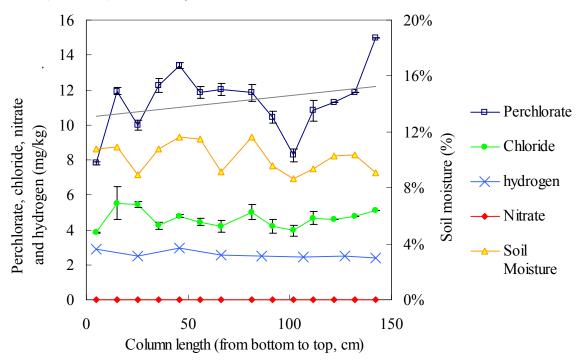
After 4 weeks of incubation, no appreciable perchlorate degradation was detected in Column #1 (**Figure 4-3**), and no chlorate or chlorite were observed. The concentration of hydrogen was decreased from the initial conditions, but approximately uniform with length at 3 mg/kg, indicating that no hydrogen "floating" occurred. Soil moisture was retained its original value at approximately 10% along the column length, and pH was approximately 6.5. No nitrate (NO<sub>3</sub>) or nitrite was detected in any of the soil samples from Column #1, compared to the original background concentration in the soil of 2.1±0.3 ppm NO<sub>3</sub>.

Figure 4-3 Perchlorate, Chloride, Hydrogen, Nitrate, and Soil Moisture Along Column Length in Column #1 after 4 Weeks of Incubation. Intermediate degradation products (chlorate, chlorite, and nitrite) were not detected.



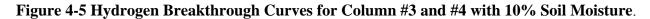
After another 6 weeks, Column #2 was sacrificed after being purged two more times with the  $20\% H_2 / 80\% N_2$  gas mix, but still no perchlorate reduction or perchlorate intermediates were observed (**Figure 4-4**). Along column length, hydrogen concentrations were fairly uniform, at 2.5 mg/kg. Soil moisture was approximately 10% along the column length and pH was approximately 6.6. Nitrate and nitrite were not detected in any soil samples from Column #2.

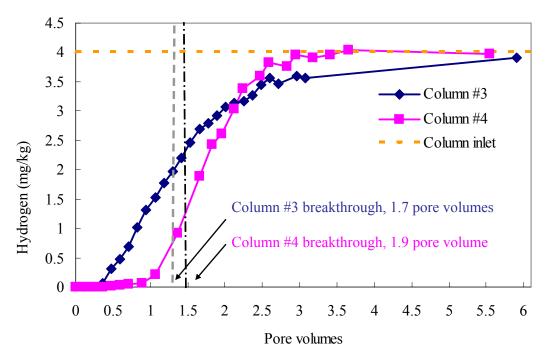
Figure 4-4 Perchlorate, Chloride, Hydrogen, Nitrate, and Soil Moisture Along Column Length in Column #2 after 10 Weeks of Incubation. Intermediate Degradation Products (Chlorate, Chlorite, and Nitrite) Were Not Detected.



#### 4.3.2 Four-Gas-Mixture Column

The hydrogen breakthrough occurred at almost the same time (7.2 hours (1.7 pore volumes) and 8.04 hours (1.9 pore volumes)) in columns #3 and #4, respectively, even though there was a longer lag period in column #4 (**Figure 4-5**).





The component gas concentrations were also monitored along the column length. Immediately after the columns were capped, the percentage of propane, carbon dioxide and hydrogen in the column was approximately the same as designed: 2% propane, 10% carbon dioxide, and 20% hydrogen (**Figure 4-6** and **Figure 4-7**).

Figure 4-6 LPG,  $H_2$ , and  $CO_2$  Profiles Along the Length of Column #3 at the Start of Incubation.

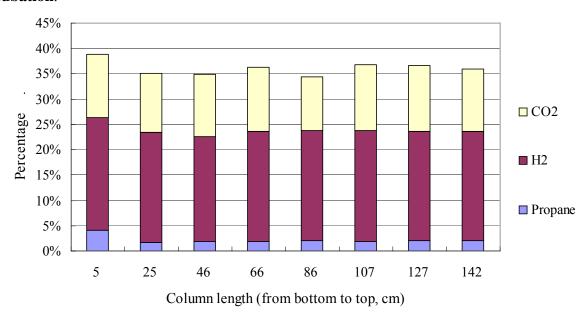
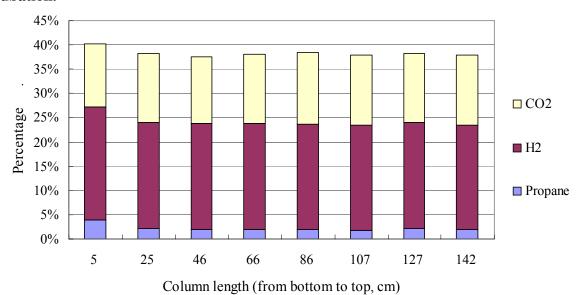
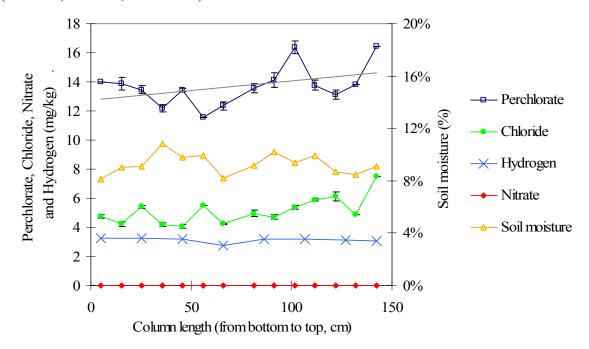


Figure 4-7 LPG,  $H_2$ , and  $CO_2$  Profile Along the Length of Column #4 at the Start of Incubation.



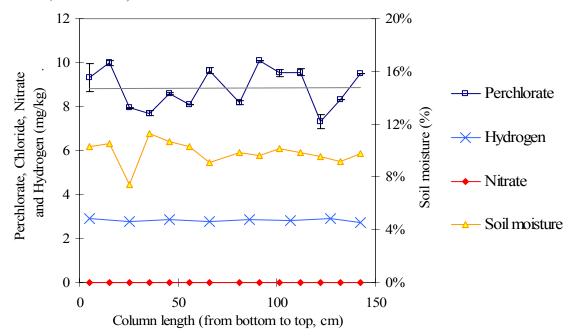
Column #3 was purged with the 4 gas mixture (2% propane / 10% CO<sub>2</sub> / 20% H<sub>2</sub> / 68% N<sub>2</sub>) once at 23 days of incubation to replenish diminishing hydrogen levels. After 4 weeks of incubation, no appreciable perchlorate degradation was detected in Column #3 (**Figure 4-8**), and no chlorate or chlorite were observed. The concentration of hydrogen was decreased from the initial conditions, but approximately uniform with length at 3.1 mg/kg. Soil moisture was maintained near its original value at an average 9.3% along the column length, and pH was approximately 7.0. No nitrate (NO<sub>3</sub>) or nitrite was detected in any of the soil samples from Column #3.

Figure 4-8 Perchlorate, Chloride, Hydrogen, Nitrate, and Soil Moisture along Column Length in Column #3 after 4 Weeks of Incubation. Intermediate Degradation Products (Chlorate, Chlorite, and Nitrite) Were Not Detected.



Column #4 was purged twice with the four gas mixture (2% propane / 10% CO<sub>2</sub> / 20% H<sub>2</sub> / 68% N<sub>2</sub>) at 22 and 47 days of incubation, but no perchlorate reduction or perchlorate intermediates were observed after 8 weeks of incubation (**Figure 4-9**). Along column length, hydrogen concentrations were fairly uniform, at an average of 2.8 mg/kg. Soil moisture was an average of 9.8% along the column length and the pH was approximately 7.6. Nitrate and nitrite were not detected in any soil samples from Column #4. To check for the possibility of biofouling, a traceable manometer pressure vacuum gauge (Fisher Scientific) was used to monitor the pressure change across the length of Column #4. A change of only 0.008 psi was observed from the top to the bottom of the column, indicating that biofouling was likely not occurring in this column.

Figure 4-9 Perchlorate, Hydrogen, Nitrate, and Soil Moisture along the Column Length in Column #4 after 8 Weeks of Incubation. Intermediate Degradation Products (Chlorate, Chlorite, and Nitrite) Were Not Detected.



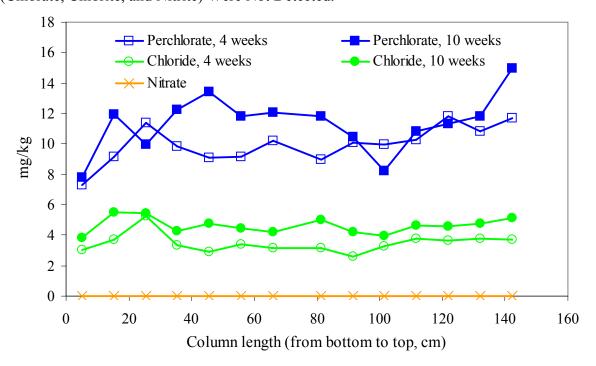
#### 4.4 Discussion

Even though the columns were packed in the same way and had the same density as the site soil, the H<sub>2</sub> breakthrough curves were variable between columns. This variability may have been caused by different soil particle sizes and relative locations in each column causing preferential pathways and therefore different retention times. Longer sitting (i.e., settling) time may have changed the micro-distribution of soil in the columns as well. Columns that were packed and then immediately purged (Columns #2 and #4), seemed to have longer retention times than those that were allowed to settle before being purged (Columns #1 and #3). Compared with the theoretical breakthrough time calculated as 4.23 hours (Appendix A-4), all columns took a longer time to breakthrough except Column #1. This may be because Column #1 was the "oldest" column had been packed the earliest and purged with gas several times before conducting the column test. Column #2 was later found to have a leak, so this could be the reason for delayed breakthrough in this column. The columns with the 4-gas-mixture propane/CO<sub>2</sub>/H<sub>2</sub>/N<sub>2</sub> (columns #3 and #4) had significantly longer H<sub>2</sub> breakthrough times than the columns containing the 2-gas-mixture,  $H_2/N_2$ . It seems that the components of the gas mixture altered transport through the column. Propane is a significantly larger molecule than hydrogen with a greater affinity for soil sorption, so it is possible that hydrogen molecules became entrapped in soil micropores that were blocked by propane molecules at the pore throats. The phenomenon of size exclusion and pore blockage has been documented in the literature for other

compounds (Poulsen et al., 2006; Kwon and Pignatello, 2005), however, we were unable to find documentation of this occurrence for propane and hydrogen.

Complete denitrification was achieved in all columns, but no perchlorate reduction was observed. Even though many researchers have reported preferential nitrate reduction prior to the onset of perchlorate degradation (Nozawa-Inoue et al., 2005), there was no change in perchlorate concentration between columns #1 and #2 even after incubating for more than 10 weeks (Figure **4-10**). There are several reasons which may be responsible for the lack of perchlorate degradation in the columns including oxygen infiltration, low soil moisture, lack of carbon source, insufficient electron donor, and/or extended soil storage time. The column was made with clear PVC, which is a slightly oxygen permeable material (Doyon et al., 2006). Therefore, it is possible that the electron donor concentration was decreasing because it was being consumed by oxygen infiltrating into the column, and perchlorate degradation was inhibited by the presence of oxygen. Lack of moisture may have also impeded perchlorate reduction in the columns. Microcosm test results showed that 7% moisture content is too low to support perchlorate biodegradation. Ten percent in this column test is higher than 7%, but it is not clear that if it is high enough to support perchlorate reduction. In future tests, a method for sampling the soil gas in the columns even in the presence of high soil moisture should be developed. Lack of available carbon could also have impeded perchlorate degradation in Column tests #1 and #2 since no carbon dioxide was injected with the hydrogen gas. The natural organic carbon in the soil (0.037% = 150 mmol total carbon) was theoretically enough to support complete degradation of perchlorate in the columns (10 mg/kg perchlorate = 0.5 mmol perchlorate requiring 1.0 mmol carbon if H<sub>2</sub> is the electron donor source, based on stoichiometry); however, at least 0.7% of the natural carbon in the soil must be bioavailable and present as organic carbon for this to occur. The amount of electron donor that could be added to the column at a given time was less than that used for the microcosm studies (i.e., mg electron donor per kilogram soil). While additional electron donor was added to the columns as it was consumed or otherwise lost, the total concentration of electron donor added to soil in the column studies was less than that in the microcosm studies. This may have also affected the results. Another reason for lack of perchlorate reduction could be the extended storage time of the soil before the column experiments were performed. The soil was collected in August 2006, and was sitting in the lab for over 5 months before the column study was initiated, which may have compromised the bacterial community and may have resulted in the lack of perchlorate reduction observed.

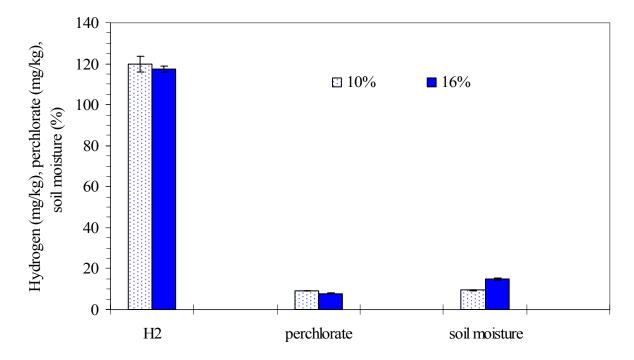
Figure 4-10 Perchlorate, Chlorate, and Nitrate Concentrations in Hydrogen Columns with 10% Soil Moisture after 4 and 10 Weeks of Incubation. Intermediate Degradation Products (Chlorate, Chlorite, and Nitrite) Were Not Detected.



To quickly test if extended storage time and/or soil moisture was responsible for the lack of perchlorate degradation in the column experiments, a small batch test was performed in duplicate with the stored soil at two soil moisture contents: 10% and 16%. Similar to the setup of the microcosm experiments described in the treatability study report, soil from the field site was transferred in 10-gram (g) aliquots to four 150-mL glass serum bottles. After degassing the bottles, 0.44 mL or 1.19 mL de-ionized water was injected into the bottles to achieve 10 or 16% soil moisture, respectively. After withdrawing an equivalent amount of headspace, 13570 µL pure hydrogen gas was injected into each bottle to achieve the same hydrogen concentration as the "high concentration" Microcosm tests. Carbon dioxide was not added to the microcosms to better mimic conditions of columns #1 and #2. The bottles were incubated in the dark at room temperature for a total of 3 weeks. No significant perchlorate reduction was observed in bottles with 10% soil moisture after 21 days of incubation; however, in bottles with 16% soil moisture, partial perchlorate reduction (1.32  $\pm$  0.09 mg/kg or 14.6% perchlorate reduced) was observed during this same time period (Figure 4-11). These results indicate that the perchlorate reducing bacteria were still active in the stored soil, and that the higher moisture content promoted perchlorate reduction. A significantly higher rate of perchlorate reduction was observed in the original Microcosms with hydrogen and carbon dioxide at 16% soil moisture, in which 94% of the soil perchlorate was reduced in 21 days (see Section 3.0). This small batch test, therefore, does not rule out the possibility that extended storage and/or lack of carbon source negatively

affected perchlorate reduction in the column experiments. It does demonstrate, however, that soil moisture contents greater than 10% are needed to promote significant perchlorate reduction in this aged soil. Had the column experiments been performed with 16% soil moisture, it is reasonable to assume that perchlorate reduction would have been observed.

Figure 4-11 Hydrogen, Perchlorate, and Soil Moisture Concentrations in Hydrogen Microcosms with 10% or 16% Soil Moisture after 21 Days of Incubation. Intermediate Degradation Products (Chlorate, Chlorite, and Nitrite) Were Not Detected.



#### **5.0** Air Injection Test

#### 5.1 Introduction and Method

An air injection test was conducted at the IRCTS-PBA site using the newly installed injection well (CDM-INJ1) and piezometer (CDM-P1) in combination with the two existing wells at the site (SVS1A and SVS2). The objectives of the air injection test were to:

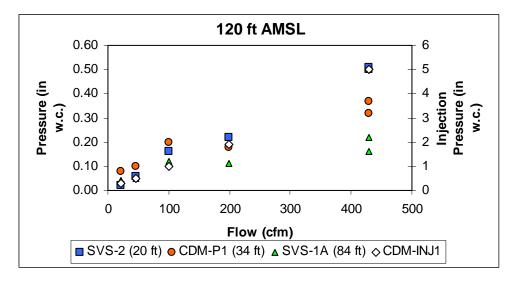
- Estimate the corresponding backpressures for various gas flow rates; and
- Estimate the pneumatic zone of influence of gas injection;

An air compressor was used to inject air into injection well CDM-INJ1 at different flow rates. Pressures were measured at the injection well head and at the different monitoring points in CDM-P1, SVS-1A, and SVS-2. The flow rates were tested in a series of steps from lowest to highest. Wellhead pressure was recorded using a pressure gauge. Actual flow rates to the injection well were controlled/measured using an air velocity meter, pressure regulator, and globe valve. Pressures were allowed to stabilize prior to increasing flow to the next level.

#### 5.2 Results

**Figure 5-1** shows the effect of air injection flow rate on pressures at the injection well (CDM-INJ1) and the piezometers at an approximate elevation of 120 feet above mean sea level (ft amsl) which corresponded to about 50 ft bgs (see **Figure 2-6**). The data show minimal pressure at the injection well (5 inches water column or less) and a positive effective of air injection on the piezometers located up to 84 feet from the injection well.

Figure 5-1 Effect of Air Injection Flow on Pressure at 120 ft amsl.



**Figure 5-2** shows the relationship between pressure measured at each piezometer and distance for various flow rates. Log-linear relationships between these parameters were observed at the greater flow rates (r<sup>2</sup> greater than 0.96) in accordance with the one-dimensional, steady-state

equation for compressible, radial flow modified for gas injection (U. S. Army Corps of Engineers, 1999; U. S. Army Corps of Engineers, 2002):

$$P_2 - P_1 = \frac{Q_v \mu}{4\pi b k_a} \ln \left(\frac{r_1}{r_2}\right),$$

where P is the absolute pressure,  $Q_v$  is the flow rate,  $\mu$  is the viscosity, b is the well screen length,  $k_a$  is the permeability, and r is the distance (radius) from the injection well. The subscripts 1 and 2 refer to individual monitoring points located different distances away from the injection well. The average permeability (k) based on these data was calculated to be 5.6E-4  $\pm$  0.9E-4 cm<sup>2</sup> permeability at 120 ft amsl. This permeability is high and typically associated with unconsolidated gravels. Because of this high permeability, the radius of pneumatic influence at the maximum flow rate of 420 cfm was determined to be at least 84 ft. Pneumatic effects were observed at a distance of 34 ft at the lowest flow rate tested – 21 cfm.

Pneumatic effects were observed at elevations down to about 120 ft amsl or about 50 ft bgs. Based on this result, the remaining injection wells and piezometers will be installed only to a depth of 50 ft bgs rather than 70 ft bgs.

Figure 5-2 Relationship between Distance from Injection Well CDM-INJ1 and Piezometer Pressure at 120 ft amsl.

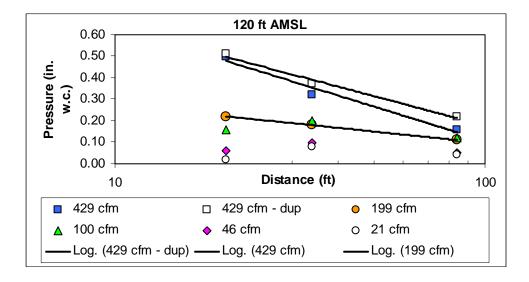


Figure 5-3 Effect of Air Flow on Pressure at Piezometer SVS-2.

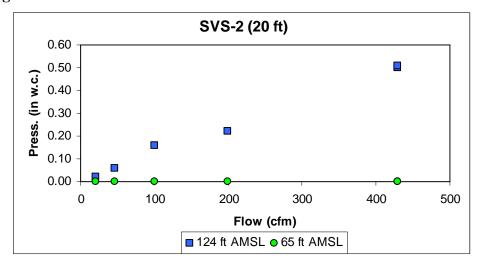


Figure 5-4 Effect of Air Flow on Pressure at Piezometer CDM-P1.

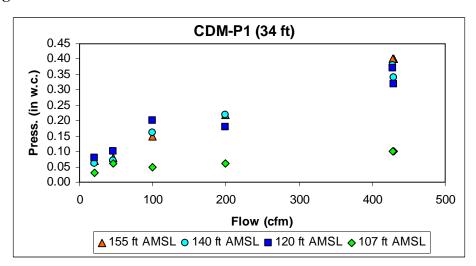
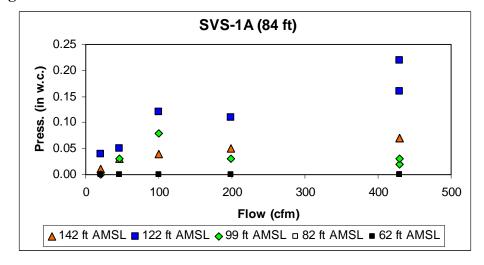


Figure 5-5 Effect of Air Flow on Pressure at Piezometer SVS-1A.



#### **6.0 Overall Data Assessment**

This section presents a deviations from the work plan (CDM, 2006) and evaluations of data quality and the data quality objectives.

#### 6.1 Deviations from the Work Plan

The following deviations from the work plan were made:

- Piezometer was constructed using 3/8-inch tubing with porous steel vapor probes rather than continuous multi-chamber tubing (CMT) as a cost-savings measure.
- The air injection test was conducted with a maximum flow of 429 cfm rather than 1,000 cfm because of equipment availability.
- Transport rates of ethyl acetate and hexene were not determined because these were not the best two electron donors. Rather, the transport rates of hydrogen and LPG were determined.
- The effective concentration of electron donor delivered to soil in the column studies was less than that used in the microcosm studies because of an observed lack of donor consumption.

#### 6.2 Evaluation of Data Quality and Data Quality Objectives

The intended use of the data is determination of the design requirements for the technology demonstration and not regulatory compliance. The quality of the data with respect to precision, accuracy, representativeness, completeness, comparability, and sensitivity were suitable for their intended use

The following decision rules and responses were established in the work plan:

- Decision Rule 1: Use the relationship between perchlorate concentrations and soil lithology to focus the GEDIT design in the Phase II Technology Demonstration Plan.
  - Perchlorate was observed in both fine-grained and coarse-grained soils. The soil
    moisture was generally greater in the fine-grained materials. Therefore, the
    technology demonstration will address both fine-grained and coarse-grained soils.
- Decision Rule 2: Use the pneumatic zone of influence data to design the injection well and piezometer spacing in the Phase II Technology Demonstration Plan.
  - The pneumatic zone of influence data were used to design injection wells with a 20-foot spacing and with piezometers spaced in from 5 to 25 feet away from the injection wells.
- Decision Rule 3: Use the flow-backpressure data in combination with the pneumatic zone of influence data to specify the gas injection equipment for the Phase II Demonstration.

- o Minimal backpressure was observed during injection therefore minimal gas injection pressure is required. Pneumatic influences were observed at flow rates as low as 21 cfm (i.e., the lowest flow rate tested). Therefore, the gas injection equipment will be capable of operating at flow rates of 10 to 30 cfm per well.
- Decision Rule 4: Select the best electron donors based on extent and rate of perchlorate biodegradation in site soil for further evaluation in the treatability study. Also use the microcosm data to select the rate of electron donor injection for the column test to ensure that stoichiometric requirements for biological reduction are satisfied.
  - Hydrogen and LPG were observed to be the best electron donors with respect to
    effectiveness. Two column studies were conducted One contained hydrogen and
    the other contained hydrogen and LPG as electron donors. The effective
    concentration of electron donor that was delivered to soil in the column was less
    than in the microcosm studies because of an observed lack of donor consumption.
- Decision Rule 5: Select the two best electron donors for column biodegradation tests based on the results of Decision Rule 4 and the electron donor transport rates estimated using the columns.
  - o Hydrogen and LPG were selected as the electron donors for further use.
- Select one or both of the electron donors identified in decision rule 5 to be used in the
  Phase II demonstration. The selected electron donors should have demonstrated ability to
  promote perchlorate biodegradation in the microcosm and column systems. Also
  consider potential for regulatory acceptance, engineering considerations, and cost when
  deciding which electron donors to use in Phase II.
  - O Both hydrogen and LPG were observed to be the best electron donors with respect to effectiveness, handling, and cost. A mixture of these electron donors was therefore selected for the Phase II technology demonstration. Perchlorate destruction was only observed microcosm tests, but this may have due to age of the soil used for the column tests or other factors that are not representative of field conditions.

#### 7.0 Conclusions

The following conclusions are based on the results of this treatability test:

- Soil borings completed at the site indicate that sufficient perchlorate (i.e., greater than 1 mg/kg) is present in soil for the purposes of this demonstration. Soil moisture ranges from 7 to 16% in non-clayey/silty soil where gas transport is expected to be most effective. Nitrate is present at detectable but relatively low concentrations. Soil is generally comprised of sands and gravels with some clay and silt at shallow and deeper zones.
- The microcosm study demonstrated that hydrogen/carbon dioxide and propane (LPG) were capable of promoting nitrate and perchlorate biodegradation. Biodegradation was observed at 16% moisture but not at 6% moisture. These data indicate that, as expected, moisture will be an important parameter affecting the rate and extent of perchlorate biodegradation. Hexene was partially capable of promoting perchlorate biodegradation and ethyl acetate was not capable of promoting perchlorate biodegradation. Based on these results, a mixture of hydrogen, carbon dioxide, and LPG is recommended for the field demonstration.
- The column studies demonstrated that, as expected, hydrogen and LPG were effectively transported through soil. Over time, no evidence of hydrogen "floating" was observed. Perchlorate biodegradation was not observed. However, supplemental microcosm studies indicated that either the soil moisture was too low or the soil used for the column tests was too old to support biodegradation.
- The air injection test demonstrated a high permeability that was consistent with the soil lithology. The pneumatic radius of influence was at least 30 feet and possibly as great at 80 feet. Relatively low flow rates were capable of promoting pneumatic influences at reasonable distances away from the injection well.

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## Appendix A-1 Well Report

CALL FOR INSPECTIONS EH (916) <del>875-8422</del> HAZMAT(916) <del>875-8464-</del> \$75-8524

# WELL APPLICATION AND PERMIT FORM

ENVIRONMENTAL MANAGEMENT DEPARTMENT 8475 JACKSON ROAD, SUITE 230/240 SACRAMENTO, CA 95826-3904

Inspecting Division: ENVIRONMENTAL HEALTH SITE ADDRESS: LNACTIVE PRAICHOR COCPOUN TEST SITE City: CANCING COCPOUN ZIP: DST42  Nearest Major Cross Street: WHITE TOUR CAPED Property Owner Only Contractor: HITE TOUR CAPED Property Owner Only Contractor WHITE PROPERTY CAPED Property Owner Only Contractor WHITE PROPERTY CAPED Property Contractor WHITE PROPERTY CAPED Property Contractor Address: Page 14 Tour Contractor Address: Page 15 Tour Caped Property Contractor Address: Page 15 Tour Caped Property Contractor WHITE Property Co	FOR OFFICE USE ONLY  DISAPPROVED APPROVED  APPROVED WITH CONDITIONS (See attachment)  By:  Date:  Total Fee:  Grout Inspection By:  Actual Well Depth:  Actual Grout Depth:  Well Destruction Inspection By:  Date:  Well Destruction Inspection By:  Comments:
SITE ADDRESS: INACTIVE PANIAND COLORDA TEST SITE  CITY FANIAND COLORDA TEST SITE  CITY FANIAND COLORDA TEST SITE  CITY FANIAND COLORDA TEST SITE  Parcel Number: 1712-0730-0000  Property Owner: AREADER TO ADDRESS: CASH TO ADDRESS TO	11505 Dovelas Road
WORK TO BE PERFORMED: (License Required)   Construct Well (C-57)	SITE ADDRESS: INACTIVE PANCIAC LORDWA TEST SITE City: RANCHO CORPOUR Zip: 95742  Nearest Major Cross Street:: WHITE IZOUK ROKP Parcel Number: 072 - 0370 - 070 -0000  Property Owner: APROJET GENERAL CORPOTATION Phone Number: 416 - 355 - 516 1  Well Contractor: WDC License Number: 283326 OK Type: C-57  Contractor Address: 70 BOX 141 / 9580 CONTY RD 938 Expiration Date: 6-30 - 48)
Install New Pump (C-57)   Destroy Well (C-57)   Inactivation Permit, (Owner Only)	
Stream, Ditch, Drainage Canal:   Sec FT   100 Year Flood Plain:   7   MILE	Install New Pump (C-57) Destroy Well (C-57) Inactivation Permit, (Owner Only)
Domestic/Private	DISTANCE TO NEAREST: Leach Field: > 500 FT Leach Pit: > 500 FT Septic Tank: > 500 FT Sewer Line: > 500 FT
Domestic/Private	Stream, Ditch, Drainage Canal: > > 100 Year Flood Plain: > 1 MILE
Public Water System	INTENDED USE: DRILLING METHOD: CONSTRUCTION SPECIFICATIONS:
Irrigation	Domestic/Private Auger BOREHOLE: Diameter: 10-14 Depth: 70 FT Gravel Pack: Yes X No
Cathodic Protection	Public Water System Cable Tool CASING: Diameter: 6-17 Depth: 70 FT
Monitoring   Material:   Monitoring   Moni	Irrigation Driven If Steel, Gauge: Or Thickness:
Extraction/Recovery   Scitic   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Diameter: 10 w   Depth: 8 FC   Sealing Material: Bed 42-1E   GROUT: Be	Cathodic Protection Rotary If Plastic, Type: Sch 40 PVC (MUST MEET ASTM F-480)
Heat Exchanger  TRANSITION SEAL: Material: Denter License Number:  PUMP INSTALLATION/REPAIR:  Contractor:  Horse Power: License Type: Expiration Date: 7/7/26  WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:  I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature: Property Owner   Well Contractor   Well Contracto	
PUMP INSTALLATION/REPAIR: Contractor: License Type: Expiration Date: 7/7/15  WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:  I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature: Property Owner Well Contractor	Extraction/Recovery GROUT: Diameter: 10 to Depth: 8 FT Sealing Material: Paratite (2000)
PUMP INSTALLATION/REPAIR: Contractor: License Number: Type of Pump: Horse Power: License Type: Expiration Date: 7/7/06  WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:  I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature: Property Owner Well Contractor	
Type of Pump: Horse Power: License Type: Expiration Date: 77766  WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:  I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature: Well Contractor Well Contractor	The Other (state) Comments: VAPUSE ZOIJE INJECTION WELL FOR INSTITUTE BECKEMEDIATED PILOT TEST
WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water: I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature: Well Contractor Well Contractor	
I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature:  Property Owner  Well Contractor	Type of Pump: Horse Power: License Type: Expiration Date: 7/7/06
grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.  Signature:  Property Owner  Well Contractor	WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:
4041	grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.
	40AV
Company: Phone: 116 - 567 - 1900 Field Phone # if Available: 916 - 108 - 3 149	
Mailing Address: LIYS UNTRUMY DAKS STE 240 City, State, Zip: SACRUM WITD A 95833	

CALL FOR INSPECTIONS 875-8422 WELL APPLICATION AND PERMIT FORM EH (916) 875-8422 HAZMAT (916) 875-8464

ENVIRONMENTAL MANAGEMENT DEPARTMENT 8475 JACKSON ROAD, SUITE 230/240 SACRAMENTO, CA 95826-3904

FOR OFFICE USE ONLY
□ DISAPPROVED Date Received: 1776 Permit Number: 258
By: Date: Date Issued: SR Number: SR Number: Receipt Number: SR Number:
Grout Inspection By: Date:/
Actual Well Depth: Actual Grout Depth: Final Inspection By: Date:
Depth to first Water: Well Destruction Inspection By: Date:
Comments:
1505 Pordas Road
1703 Volgas par
Inspecting Division: ENVIRONMENTAL HEALTH HAZARDOUS MATERIALS
SITE ADDRESS: WALTIVE PAPELLED COMPANY TEST SITE CITY: PANCHO COLDUN ZIP: 95742
Nearest Major Cross Street:: WHITE PULK PURA PARCE Number: 072-0370-0000
Property Owner: AEMOSET GENERAL CONTOCATION Phone Number: 916 - 355 - 5161
Well Contractor: WUL License Number: (283326) EK Type: L-57
Contractor Address: P.O. Box 141 9580 Curstry PD 13 B Expiration Date: 6-30-09
City: 2 Amora Zip: 95098 Phone: 800 - 8.13 - 30-73 Well/Boring Identification Number: DM-PI
WORK TO BE PERFORMED: (License Required)
X Construct Well (C-57) Repair/Modify Well or Pump (C-57, C-61, Class A) Test Hole Soil Boring With Destruction (C-57)
Install New Pump (C-57)  Destroy Well (C-57)  Inactivation Permit, (Owner Only)
Comments:
DISTANCE TO NEAREST: Leach Field: ) 500 FT Leach Pit: ) 500 FT Sewer Line: > 500 FT
Stream, Ditch, Drainage Canal: 7 560 F7 100 Year Flood Plain: 7 1 Mice
INTENDED USE: DRILLING METHOD: CONSTRUCTION SPECIFICATIONS:
Domestic/Private Auger BOREHOLE: Diameter: Depth: 70 FT Gravel Pack: Yes & No
Public Water System Cable Tool CASING: Diameter: 1.5 - 1.4 Depth: 70 FT
Irrigation Driven If Steel, Gauge: Or Thickness:
Cathodic Protection Rotary If Plastic, Type: LINT MOUTI - POIT (MUST MEET ASTM F-480)
( LISTLON)
Court Company
Extraction/Recovery GROUT: Diameter: W 12 Depth: N 20 FT Sealing Material: Beatto, atte 61037
Heat Exchanger TRANSITION SEAL: Material: Benziste CHIPS Interval: A 20 25 FT
Other (state) Comments: PIEZOMETER
PUMP INSTALLATION/REPAIR: Contractor: License Number:
Type of Pump: Horse Power: License Type: Expiration Date:
WELL/TEST HOLE/ SOIL BORING DESTRUCTION: Diameter: Total depth: Depth to Water:
I will comply with all Codes, Rules and Regulations of the State and County pertaining to or regulating well construction/destruction, call for a grout/destruction inspection at least 24 hours prior to placement of sealing material, notify the Department within 5 days of the completion of my work so a final inspection can be made, and obtain final approval before placing the well in service.
Signature: Property Owner Well Contractor
Print Name: Tom Tito's Agent for Property Owner* Agent for Well Contractor*
Company: CDM Phone: 116 - 567 - 4900 Field Phone # if Available: 516 - 798 - 3749
Mailing Address: 2295 GARENAY DAKS STE 240 City, State, Zip: SALEAMONTO LA 95833

## Appendix A-2 Boring Logs

#### 18581 Teller Avenue, Suite 200 Irvine, CA 92612 (949) 752-5452 BORING/WELL CONSTRUCTION LOG (949) 752-1307 (FAX) PROJECT NUMBER 4000-46738 BORING/WELL NUMBER CDM-INJ1 PROJECT NAME Aerojet DATE DRILLED 07/31/06 CASING TYPE/DIAMETER Sch 40 PVC/6-inch LOCATION Rancho Cordova, CA SCREEN TYPE/SLOT 6-inch Sch 40 PVC/20 Slot **DRILLING METHOD** Sonic SAMPLING METHOD Continuous Core **GRAVEL PACK TYPE** No. 3 Monterey Beach Sand GROUND SURFACE ELEVATION (FT MSL) NA GROUT TYPE/QUANTITY Bentonite Grout STATIC WATER LEVEL (FT BELOW TOC) NA TOP OF CASING ELEVATION (FT MSL) NA LOGGED BY T.Titus GROUND WATER ELEVATION (FT MSL) REMARKS RECOVERY (inches) BLOW COUNTS GRAPHIC LOG CONTACT DEPTH PID (ppm) EXTENT U.S.C.S. DEPTH (ft. bgs) SAMPLE LITHOLOGIC DESCRIPTION WELL DIAGRAM SILT: brown (10YR 4/3); 100% silt, firm, low plasticity; dry, Cement Grout (0-6 ft bgs) Casing (0-10 ft bgs) ML 0.0 Bentonite (6-8 ft bgs) 10.0 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, 0.0 high plasticity; moist, no odor. CL 13.0 SILT: brown (10YR 4/3); 100% silt, firm, low plasticity; moist, no odor. Screen (10-70 0.0 ML ft bgs) 18.0 CLAY: dark yellowish brown (10YR 3/4); 100% clay, soft, CL high plasticity; moist, no odor. 20.0 -Sand (8-70.5 ft CLAYEY GRAVEL: brown (7.5YR 4/3); 60% gravel, well 0.0 bgs) graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; 30% clay, soft, medium plasticity; 10% cobbles, maximum diameter of 5 inches, subrounded to rounded; moist, no odor. 25.0 SILTY SAND WITH GRAVEL: brown (7.5YR 4/3); 40% 0.0 sand, well graded, fine to coarse grained, angular to rounded; 30% silt, very soft, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; trace cobbles, maximum diameter of 6 inches, rounded; moist, no odor.

Cobbles from 35 to 38 feet below ground surface.

NEWGINT AEROJET 042806.GPJ NEWGINT.GDT 8/3/06

0.0



NEWGINT AEROJET\_042806.GPJ NEWGINT.GDT 8/3/06

18581 Teller Avenue, Suite 200 Irvine, CA 92612 (949) 752-5452 (949) 752-1307 (FAX)

### **BORING/WELL CONSTRUCTION LOG**

 PROJECT NUMBER
 4000-46738
 BORING/WELL NUMBER
 CDM-INJ1

 PROJECT NAME
 Aerojet
 DATE DRILLED
 07/31/06

PROJECT NAME	Aeroje	et		<b>DATE DRILLED</b> 07/31/06		
				Continued from Previous Page		
PID (ppm) BLOW COUNTS	RECOVERY (inches) SAMPLE ID. EXTENT DEPTH (ft. bgs)		U.S.C.S. GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT	WELL DIAGRAM
0.0		   - 45- 		SILTY SAND WITH GRAVEL: brown (7.5YR 4/2); 60% sand, well graded, fine to coarse grained, angular to subrounded; 20% silt, soft, non-plastic; 20% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to rounded; trace cobbles, maximum diameter of 5 inches, rounded; moist, no odor.		Screen (10-70 ft bgs)
0.0		-50-	SM			Sand (8-70.5 f bgs)
0.0		-55-	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	OU TV CAND WITH ODAYEL have (7 EVD 4/0), ccc/		
0.0		   - 65 - 	9 9 9	SILTY SAND WITH GRAVEL: brown (7.5YR 4/2); 60% sand, well graded, fine to coarse grained, angular to subrounded; 20% silt, soft, non-plastic; 20% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to angular; moist, no odor.		
0.0		-70-		Total depth of borehole was 70.5 feet below ground surface.	70.5	
		75 -				
		85 -				

#### 18581 Teller Avenue, Suite 200 Irvine, CA 92612 (949) 752-5452 BORING/WELL CONSTRUCTION LOG (949) 752-1307 (FAX) PROJECT NUMBER 4000-46738 BORING/WELL NUMBER CDM-P1 PROJECT NAME Aerojet DATE DRILLED 07/27/06 Rancho Cordova, CA CASING TYPE/DIAMETER Poly Tubing/0.25-inch ID LOCATION **DRILLING METHOD** Sonic SCREEN TYPE/SLOT 0.25-inch Stainless Steel Vapor Probe SAMPLING METHOD Continuous Core **GRAVEL PACK TYPE** No. 3 Monterey Beach Sand GROUND SURFACE ELEVATION (FT MSL) NA GROUT TYPE/QUANTITY Bentonite Grout STATIC WATER LEVEL (FT BELOW TOC) NA TOP OF CASING ELEVATION (FT MSL) NA GROUND WATER ELEVATION (FT MSL) LOGGED BY T.Titus REMARKS RECOVERY (inches) BLOW COUNTS GRAPHIC LOG CONTACT DEPTH PID (ppm) EXTENT U.S.C.S. DEPTH (ft. bgs) SAMPLE LITHOLOGIC DESCRIPTION WELL DIAGRAM SILT: yellowish brown (10YR 5/4); 100% silt, soft, non-plastic; dry; no odor. ML 0.0 6.0 (0-16 ft bgs) GRAVELLY SILT: yellowish brown (10YR 5/4); 60% silt, soft, non-plastic; 40% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subround to rounded; dry, no odor. GM Poly Tubing 0.0 (0-18, 0-33,ft bgs) 13.0 GRAVELLY SILT WITH SAND: brown (7.5YR 4/3); 50% silt, soft, non-plastic; 35% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches,

Cement Grout 0-48, and 0-68 0.0 subangular to rounded; 15% sand, poorly graded, medium to coarse grained, subrounded; moist, no odor. Bentonite (16-17 ft bgs) Sand (17-19.5 ft bgs) Vapor Probe (18-18.5 ft bgs) 0.0 23.0 CLAYEY GRAVEL WITH SAND: dark yellowish brown (10YR 4/4); 45% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to 0.0 rounded; 35% clay, soft, low plasticity; 20% sand, poorly -Bentonite graded, coarse grained, subrounded to rounded; moist, no (19.5-32 ft bgs) NEWGINT AEROJET 042806.GPJ NEWGINT.GDT 8/3/06 GC 0.0 Sand (32-34.5 ft bgs) Vapor Probe 34.0 (33-33.5 ft bgs) SAND: pale brown (10YR 6/3); 100% sand, poorly graded, 35.0 fine grained; dry, no odor.
CLAYEY GRAVEL WITH SAND: dark yellowish brown 0.0 (10YR 4/4); 45% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, subangular to Bentonite (34.5-47 ft bgs) rounded; 35% clay, soft, low plasticity; 20% sand, poorly graded, coarse grained, subrounded to rounded; moist, no Continued Next Page PAGE 1 OF 2



18581 Teller Avenue, Suite 200 Irvine, CA 92612 (949) 752-5452 (949) 752-1307 (FAX)

### **BORING/WELL CONSTRUCTION LOG**

PROJECT NUMBER4000-46738BORING/WELL NUMBERCDM-P1PROJECT NAMEAerojetDATE DRILLED07/27/06

								Continued from Previous Page		
PID (ppm)	BLOW	RECOVERY (inches)	SAMPLE ID.	EXTENT	DEPTH (ft. bgs)	U.S.C.S.	GRAPHIC LOG	LITHOLOGIC DESCRIPTION	CONTACT DEPTH	WELL DIAGRAM
0.0					   45-	GC		SILTY SAND: dark yellowish brown (10YR 4/4); 70%	45.0	<ul><li>Poly Tubing (0-18, 0-33, 0-48, and 0-6 ft bgs)</li></ul>
0.0					   50-	SM		sand, poorly graded, fine to medium, subrounded to subangular; 30% silt, firm, non-plastic; moist, no odor.	F2.0	Sand (47-49) ft bgs)  Vapor Probe (48-48.5 ft bg
0.0					  55- 	SM		SILTY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse grained, subangular to subrounded; 30% silt, firm, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; moist, no odor.	52.0	
0.0					 60  			CLAYEY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse	62.0	■ Bentonite (49.6-67 ft b
0.0					 65  	SC	0	grained, subangular to subrounded; 30% clay, firm, low plasticity; 30% gravel, well graded, fine and coarse grained, maximum diameter of 3 inches, angular to rounded; moist, no odor.  SILTY SAND WITH GRAVEL: dark yellowish brown (10YR 4/4); 40% sand, well graded, fine to coarse grained, subangular to subrounded; 30% silt, firm, non-plastic; 30% gravel, well graded, fine and coarse grained, maximum	65.0	Sand (67-69 bgs) Vapor Probe (68-68.5 ft b
0.0					70  		9	diameter of 3 inches, angular to rounded; moist, no odor.  Total depth of borehole was 72 feet below ground surface.	72.0	<ul> <li>■ Bentonite</li> <li>(69-72 ft bgs</li> </ul>
					75 - - - -					
					80 -					
					85 -					

### Appendix A-3 Microcosm Test Data

## **A.1 Microcosm Setup Details**

		Design			soil			moistu	ire		Elect	ron Donor	
Test #	Electron Donor	Electron donor conc. (mg/kg)	Soil moisture	mass per bottle (g)	No. of bottles	Total mass soil per batch (g)	Final (%)	Initial (%)	Water Added per batch (mL)	Name	Final Conc (mg/kg)	Pure e.d. injected into each bottle (µL)	CO2 injected into each bottle (uL)
1*	H2	34	7%	10	18	180	7%	7.0%	0.00	H2	34	4046.8	2023.4
2*	Ethyl acetate	150	7%	10	18	180	7%	7.0%	0.00	Ethyl acetate	150	1.7	
3	1-Hexene	80	7%	10	9	90	7%	7.0%	0.00	1-Hexene	80	1.2	
4	LPG	75	7%	10	9	90	7%	7.0%	0.00	LPG	75	408.9	
5	H2	114	7%	10	9	90	7%	7.0%	0.00	H2	114	13568.7	6784.3
6*	Ethyl acetate	501	7%	10	18	180	7%	7.0%	0.00	Ethyl acetate	501	5.6	
7*	1-Hexene	265	7%	10	18	180	7%	7.0%	0.00	1-Hexene	265	3.9	
8	LPG	250	7%	10	9	90	7%	7.0%	0.00	LPG	250	1363.0	
9	H2	34	16%	10	9	90	16%	7.0%	9.64	H2	34	4046.8	2023.4
10	Ethyl acetate	150	16%	10	9	90	16%	7.0%	9.64	Ethyl acetate	150	1.7	
11*	1-Hexene	80	16%	10	18	180	16%	7.0%	19.29	LPG	80	1.2	
12*	LPG	75	16%	10	18	180	16%	7.0%	19.29	Propane	75	408.9	
13*	H2	114	16%	10	18	180	16%	7.0%	19.29	H2	114	13568.7	6784.3
14	Ethyl acetate	501	16%	10	9	90	16%	7.0%	9.64	Ethyl acetate	501	5.6	
15	1-Hexene	265	16%	10	9	90	16%	7.0%	9.64	1-Hexene	265	3.9	
16*	LPG	250	16%	10	18	180	16%	7.0%	19.29	LPG	250	1363.0	
17	Negative control	0	16%	10	9	90	16%	7.0%	9.64	None	0	0.0	
18	Positive control	436	16%	10	9	90	16%	7.0%	9.64	Ethanol	436	5.5	

<sup>\* =</sup> Tests that were randomly chosen to be run in duplicate.



### **A.2 Microcosm Tests Data**

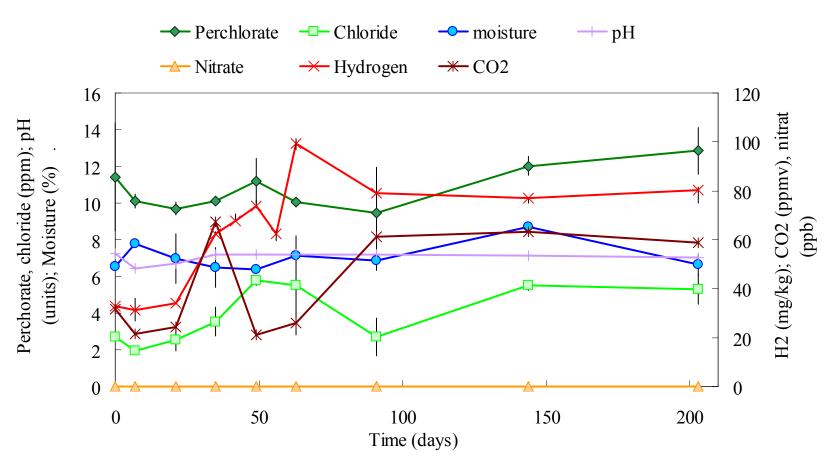
A.2.1 Test 1: 7% moisture, 34 mg/kg H<sub>2</sub>

								Time (	days)					
		0	7	14	21	28	35	42	49	56	63	91	144	203
Perchlorate	average (ppm)	11.42	10.1	-	9.7	-	10.1	-	11.21	-	10.05	9.46	12.021	12.84
Teremorate	std. dev.	2.94	0.39	-	0.35	-	0.13	-	1.22	-	0.1	2.5	0.5215	1.265
Chloride	average (ppm)	2.7	1.92	-	2.54	-	3.54	-	5.81	-	5.49	2.7	5.53	5.29
Cilioride	std. dev.	0.08	0.03	-	0.58	-	0.76	-	0.27	-	2.7	1.04	0.28	0.8
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	-	J	J	J	0
Millate	std. dev.	-	-	-	-	-	-	-	-	-	-	-	-	0
Hydrogen	average (mg/kg)	32.91	31.28	-	33.86	-	62.63	67.7	73.6	62.44	99.28	78.931	76.9	80.106
Trydrogen	std. dev.	0.31	4.62	-	0.16	-	0.67	2.75	2.5	1.18	2.04	4.93	0	1.48
$CO_2$	average (ppmv)	31.49	21.638	-	24.315	-	67.3	-	20.92	-	25.85	61.29	63.26	58.62
CO2	std. dev.	0	0	-	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	6.56	7.79	-	6.98	-	6.49	-	6.39	-	7.12	6.87	8.71	6.64
moisture	std. dev.	0.15	0.119	-	1.37	-	1.1	-	0.25	-	0.31	0.56	0	0.57
nН	average	7.24	6.45	-	6.69	-	7.2	-	7.19	-	7.2	7.19	7.14	7.02
рН	std. dev.	0.05	0.05	-	0.01	1	0.08		0.04	-	0.15	0.08	0	0.08

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method).



Test1: 7% moisture, 34mg/kg H2



### A.2.2 Test 2: 7% moisture, 150 mg/kg ethyl acetate

					Time	(days)									
		0	7	14	21	28	35	42	49	56	63	70	91	143	202
Perchlorate	average (ppm)	11.06	11.14	-	10.68	-	10.72	-	10.29	-	10.45	-	10	12.404	11.68
Teremorate	std. dev.	0.26	1.05	-	0.14	-	0.55	-	1.94	-	0.19	-	1.68	0.2755	1.14
Chloride	average (ppm)	1.75	2.33	-	2.83	-	1.62	-	5.06	-	2.79	-	3.18	4.99	5.8
Cilioride	std. dev.	1.17	0.86	-	0.17	-	0.29	-	0.61	-	0.14	-	0.81	0.77	0.32
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	-	J	-	J	J	0
Millate	std. dev.	-	-	-	-	-	-	-	-	-	-	-	-	-	0
Ethyl Acetate	average (mg/kg)	53.35	28.35	-	8.31	0.11	4.43	0.02	10.22	0	0	1.36	0	0	0
Acetate	std. dev.	2.14	5.34	-	6.9	0.14	5.84	0	14.45	0	0	0.09	0	0	0
CO <sub>2</sub>	average (ppmv)	0	0	-	0	-	0	-	0	-	0	-	0	0	0
	std. dev.	0	0	-	0	-	0	-	0	-	0	-	0	0	0
moisture	average (%)	6.55	7.3	-	6.81	-	6.41	-	7.86	6.13	6.83	-	6.49	7.7	7.37
moistare	std. dev.	0.54	1.06	-	0.32	-	0.88	-	0.92	0.08	0.37	-	0.5	0.24	0.3
рН	average	6.71	6.63	-	6.79	-	6.64	-	6.7	-	6.38	-	7.17	7.02	6.81
pm	std. dev.	0.01	0.08	-	0.11		0.16	-	0.04	-	0.03		0.06	0.13	0.04

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method).



→ Perchlorate --- Chloride -- moisture <del>----</del>рН → Nitrate → Ethyl Acetate <del>-</del>★ CO2 Ethyl Acetate (mg/kg); CO2 (ppmv), nitrate (ppb)

Test 2: 7% moisture, 150mg/kg Ethyl Acetate

Time (days)



0 \*

Perchorate, chloride (ppm); pH

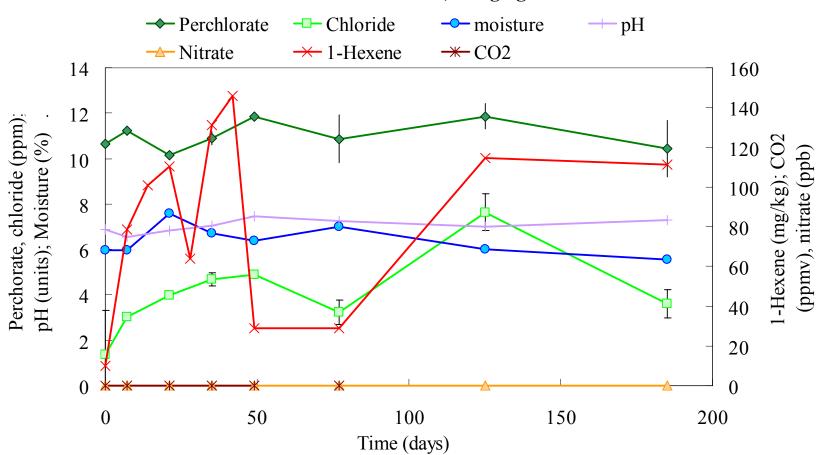
(units); Moisture (%)

## A.2.3 Test 3: 7% Moisture, 80 mg/kg 1-hexene

					Time	(days)						
		0	7	14	21	28	35	42	49	77	125	185
Perchlorate	average (ppm)	10.64	11.21	-	10.16	-	10.9	-	11.86	10.86	11.86	10.44
1 Cicinorate	std. dev.	0.01	0.01	-	0.14	-	0.29	-	0	1.05	0.55	1.25
Chloride	average (ppm)	1.37	3.02	-	3.99	-	4.67	-	4.87	3.22	7.64	3.59
Cilioride	std. dev.	1.93	0.02	-	0.07	-	0.29	-	0	0.54	0.8	0.62
Nitrate	average (ppm)	J	J	-	J	-	J	-	J	J	J	0
Nittate	std. dev.	0	-	-	-	-	-	-	-	-	-	0
1-Hexene	average (mg/kg)	9.96	78.432	100.738	110.49	63.67	131.351	145.61	29.04	29.03	114.541	111.087
CO <sub>2</sub>	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	5.95	5.96	-	7.56	-	6.72	-	6.39	6.99	6.01	5.55
pН	average	6.89	6.54	-	6.84	-	7.04	-	7.44	7.25	6.98	7.29

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)





Test 3: 7% moisture, 80mg/kg 1-Hexene



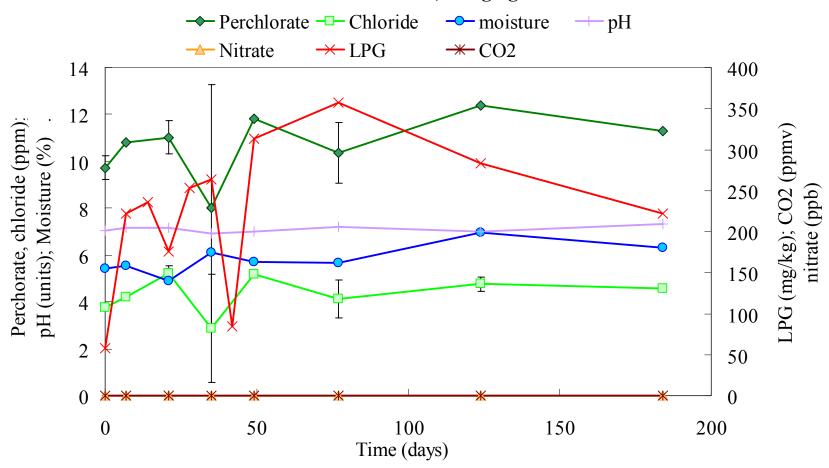
# A.2.4 Test 4: 7% Moisture, 75 mg/kg LPG

						Time	(days)					
		0	7	14	21	28	35	42	49	77	124	184
Perchlorate	average (ppm)	9.73	10.81	-	11.01	-	8.03	-	11.81	10.36	12.4	11.29
1 Cicinorate	std. dev.	0.52	0.01	-	0.71	-	5.23	-	0	1.3	0.03	0
Chloride	average (ppm)	3.78	4.22	-	5.23	-	2.88	-	5.18	4.13	4.76	4.58
Cilioride	std. dev.	0.04	0.02	-	0.32	-	2.3	-	0	0.81	0.29	0
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
TVILLACE	std. dev.	-	-	-	-	-	-	-	-	-	-	0
LPG	average (mg/kg)	58.152	221.69	235.62	176.01	253.02	263.4	84.653	312.976	356.734	283.645	221.692
$CO_2$	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	5.41	5.56	-	4.88	-	6.1	-	5.72	5.67	6.94	6.32
pН	average	7.03	7.17	-	7.18	-	6.91	-	6.99	7.2	7.01	7.32

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 4: 7% moisture, 75mg/kg LPG





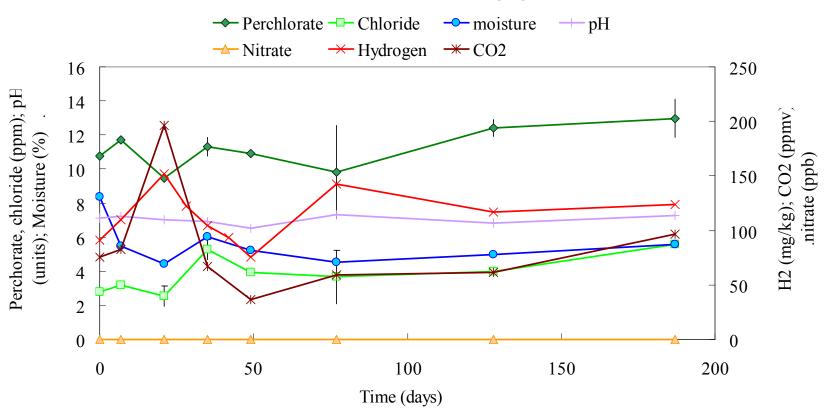
# A.2.5 Test 5: 7% Moisture, 114 mg/kg $H_{\rm 2}$

					Tir	ne (days)						
		0	7	14	21	28	35	42	49	77	128	187
Perchlorate	average (ppm)	10.76	11.7	-	9.48	-	11.3	-	10.91	9.82	12.4176	12.98
1 eremorate	std. dev.	0.04	0.04	-	0.1	-	0.54	-	0.03	2.75	0.5	1.13
Chloride	average (ppm)	2.79	3.17	-	2.53	-	5.28	-	3.93	3.68	4	5.56
Cilioride	std. dev.	0.05	0.03	-	0.6	-	0.58	-	0.09	1.57	0.16	0.1
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
Millate	std. dev.	1	-	-	-	-	-	-	-	-	-	-
Hydrogen	average (mg/kg)	91.43	109.8	_	152	122.56	104.38	93.36	75.198	142.173	116.498	123.574
$CO_2$	average (ppmv)	75.79	82.6	-	196.24	-	66.83	-	36.73	59.31	61.33	96.8
moisture	average (%)	8.39	5.49	-	4.45	-	6.05	-	5.25	4.54	5	5.57
рН	average	7.11	7.23	-	7.05	-	6.92	-	6.54	7.31	6.85	7.3

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 5: 7% moisture, 114mg/kg H2





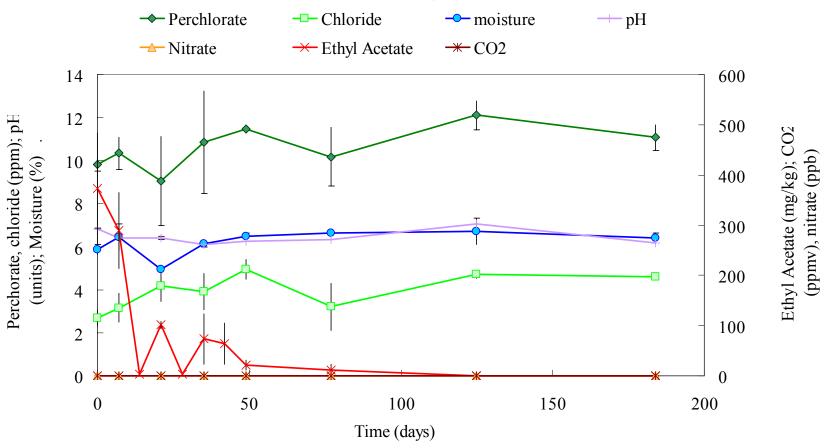
# A.2.6 Test 6: 7% Moisture, 501 mg/kg ethyl acetate

					Time (da	ys)						
		0	7	14	21	28	35	42	49	77	125	184
Perchlorate	average (ppm)	9.8	10.35	-	9.04	-	10.87	-	11.48	10.18	12.11	11.1
1 Cicinorate	std. dev.	0.28	0.75	-	2.07	-	2.38	-	0.02	1.35	0.68	0.58
Chloride	average (ppm)	2.68	3.16	-	4.18	-	3.92	-	4.95	3.21	4.7	4.62
Cilioride	std. dev.	0.37	0.66	-	0.72	-	0.85	-	0.47	1.1	0.19	0.12
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J J		J
Nittate	std. dev.	-	-	-	-	-	-	-	-	-	-	0
Ethyl	average											
Acetate	(mg/kg)	373.7	289.14	3.83	101.12	2.48	73.22	63.87	21.3	11.7	0	0
Acctate	std. dev.	110.1	75.95	0.26	7.65	1.29	50.65	40.6	9.34	11.9	0	0
	average											
$CO_2$	(ppmv)	0	0	-	0	-	0	-	0	0	0	0
	std. dev.	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	5.86	6.45	-	4.96	-	6.13	-	6.48	6.65	6.71	6.39
moisture	std. dev.	0.23	0.61	-	0.06	-	0.08	-	0.17	0.04	0.62	0.24
рН	average	6.84	6.39	-	6.4	-	6.08	-	6.24	6.32	7.07	6.18
1	std. dev.	0.01	0.06	-	0.07	-	0.1	-	0.014	0.05	0.06	0.23

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 6: 7% moisture, 501mg/kg Ethyl Acetate





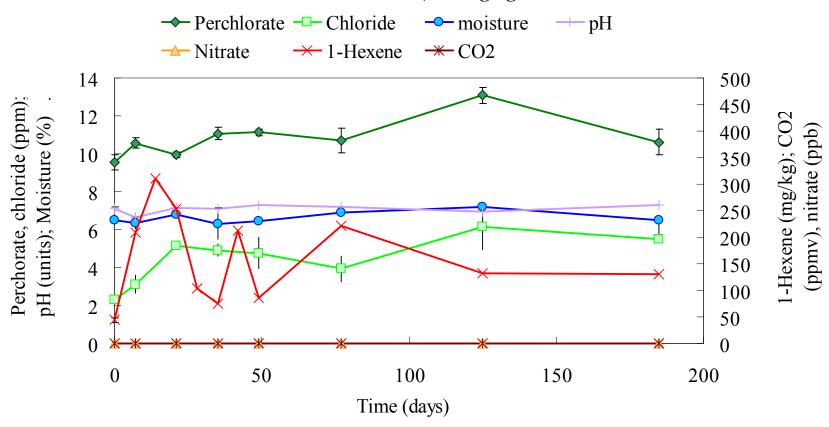
# A.2.7 Test 7: 7% Moisture, 265 mg/kg 1-hexene

					Time (da	ays)						
		0	7	14	21	28	35	42	49	77	125	185
Perchlorate	average (ppm)	9.55	10.57	-	9.96	-	11.07	-	11.14	10.68	13.09	10.62
Teremorate	std. dev.	0.39	0.28	-	0.15	-	0.34	-	0.17	0.65	0.42	0.68
Chloride	average (ppm)	2.28	3.12	-	5.16	-	4.92	-	4.76	3.93	6.17	5.52
Cilioride	std. dev.	0.07	0.49	-	0.045	-	0.31	-	0.82	0.68	1.2	0.67
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
TVILLACC	std. dev.	-	-	-	-	-	-	-	-	-	-	0
1-Hexene	average (mg/kg)	43.8	209.426	311.334	253.403	102.724	74.896	213.139	85.59	221.272	131.273	129.52
	std. dev.	4.5	-	-	-			-	-	-	-	-
$CO_2$	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
	std. dev.	0	0	=	0	-	0	-	0	0	0	0
moisture	average (%)	6.51	6.37	-	6.81	-	6.31	-	6.47	6.9	7.21	6.52
moisture	std. dev.	0.21	0.32	-	0.17	-	0.8	-	0.1	0.73	0.02	0.44
pН	average	7.08	6.65	-	7.15	-	7.125	-	7.325	7.185	6.965	7.31
pII	std. dev.	0.13	0	-	0.01	-	0.035	-	0.06	0.02	0.01	0.01

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 7: 7% moisture, 265mg/kg 1-Hexene



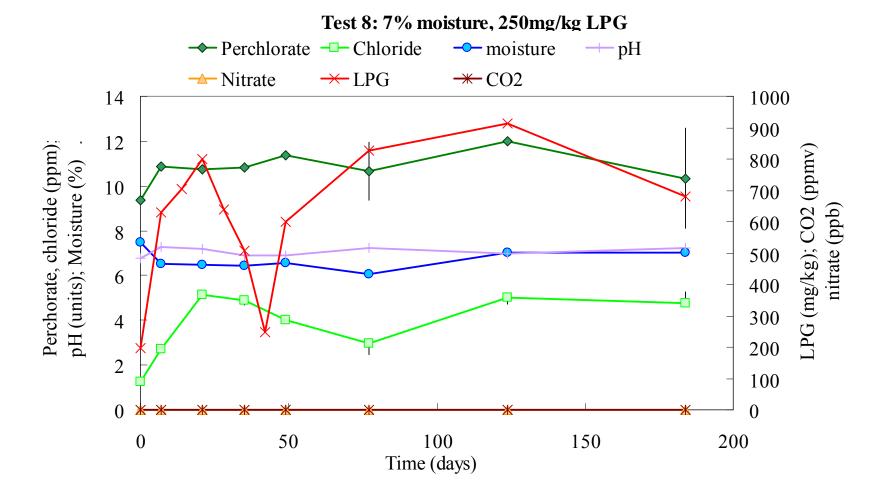


#### A.2.8 Test 8: 7% Moisture, 250 mg/kg LPG

						Ti	me (days	)				
		0	7	14	21	28	35	42	49	77	124	184
Perchlorate	average (ppm)	9.38	10.85	-	10.73	-	10.83	-	11.38	10.66	11.98	10.34
1 eremorate	std. dev.	0.17	0.11	-	0.19	-	0.22	-	0	1.28	0.04	2.25
Chloride	average (ppm)	1.27	2.71	-	5.16	-	4.89	-	4.03	2.98	5.03	4.76
Cilioride	std. dev.	0.02	0.06	-	0.05	-	0.2	-	0	0.5	0.32	1.26
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
Nitrate	std. dev.	-	-	-	-	-	-	-	-	-	-	0
LPG	average (mg/kg)	198.05	628.76	705.87	798.79	638.8	506.9	248.261	600.656	826.349	914.157	680.5
$CO_2$	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	7.48	6.51	-	6.46	-	6.44	-	6.56	6.05	7.03	7.01
pН	average	6.77	7.27	-	7.18	-	6.89	-	6.91	7.22	6.98	7.25

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)







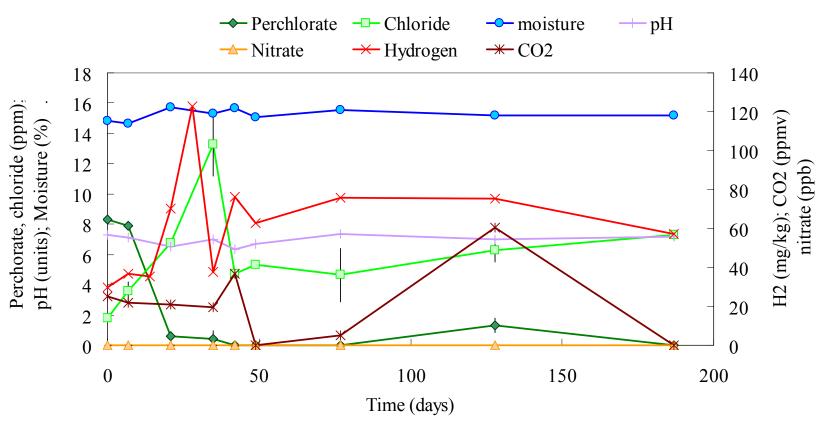
# A.2.9 Test 9: 16% Moisture, 34 mg/kg $H_{\rm 2}$

					Ti	me (days)						
		0	7	14	21	28	35	42	49	77	128	187
Perchlorate	average (ppm)	8.34	7.91	-	0.58	-	0.39	0	0	0	1.33	0
Teremorate	std. dev.	0.04	0.05	-	0.02	-	0.54	0	0	0	0.49	0
Chloride	average (ppm)	1.8	3.57	-	6.77	-	13.26	4.75	5.35	4.65	6.3	7.27
Cilioride	std. dev.	0.08	0.61	-	0.1	-	2.07	0.26	0.2	1.77	0.8	0.31
Nitrate	average (ppb)	J	J	-	J	-	J	J	J	J	J	0
Millate	std. dev.	-	-	-	-	-	-	-	-	-	-	0
Hydrogen	average (mg/kg)	29.67	36.88	35.35	70.1	122.56	37.795	76.115	62.626	75.689	75.463	56.981
CO <sub>2</sub>	average (ppmv)	25.14	22.03	-	20.92	-	19.61	36.75	0	5.22	60.5	0
moisture	average (%)	14.84	14.66	-	15.71	-	15.32	15.65	15.06	15.56	15.17	15.21
pН	average	7.28	7.14	=	6.5	-	7.01	6.32	6.71	7.36	7.01	7.15

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 9: 16% moisture, 34mg/kg H2



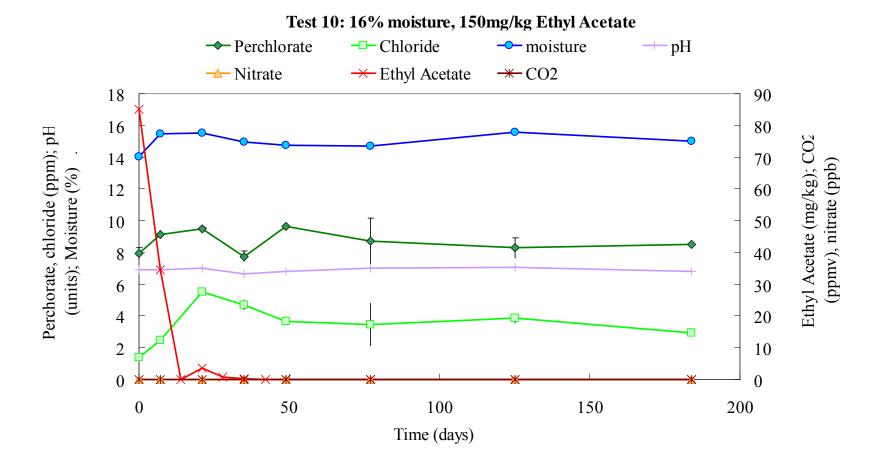


## A.2.10 Test 10: 16% Moisture, 150 mg/kg ethyl acetate

						Ti	me (days)								
			0		7	14	21	28	35	42	49	77		125	184
Perchlorate	average (ppm)		7.96		9.12	-	9.47	-	7.75	-	9.64	8.71		8.28	8.53
1 ercinorate	std. dev.		0.36		0.002	-	0.1	-	0.34	-	0	1.44		0.63	0
Chloride	average (ppm)		1.41		2.46	-	5.53	-	4.67	-	3.64	3.46		3.85	2.93
Cilioride	std. dev.		0.08		0.01	-	0.04	-	0.31	-	0	1.33		0.27	0
Nitrate	average (ppb)	J		J		-	J	-	J	-	J	J	J		0
TVILLACE	std. dev.	-		-		-	-	-	-	-	-	-	-		0
Ethyl	average		0.5		245	0.07	2 (72	0.72	0.1.42	0	0	0		0	0
Acetate	(mg/kg)		85		34.5	0.07	3.672	0.73	0.142	0	0	0		0	0
$CO_2$	average (ppmv)		0		0	-	0	-	0	-	0	0		0	0
moisture	average (%)		14.05		15.46	-	15.54	-	14.94	-	14.76	14.7	•	15.59	15
pН	average		6.9		6.9	=	7	-	6.64	-	6.81	6.99		7.05	6.82

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)





CDM

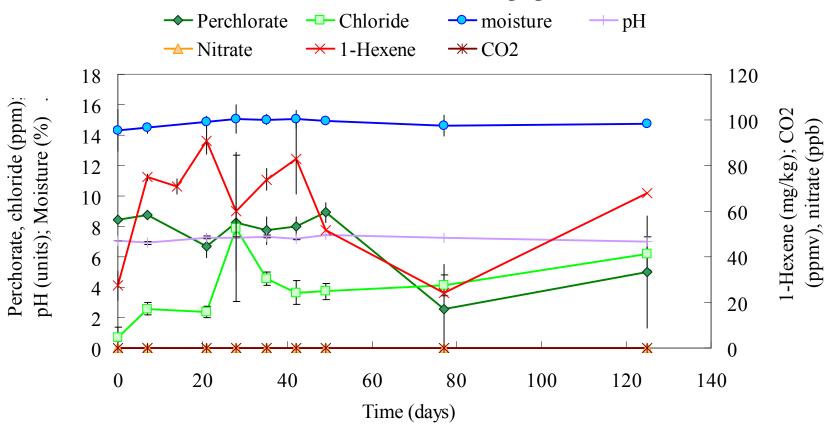
A.2.11 Test 11: 16% Moisture, 80 mg/kg 1-hexene

					Tim	e (days)					
		0	7	14	21	28	35	42	49	77	125
Perchlorate	average (ppm)	8.44	8.76	-	6.7	8.23	7.72	8.02	8.91	2.54	5
reiciiorate	std. dev.	0.28	0.23	-	0.79	0.77	0.9	0.62	0.65	2.94	3.68
Chloride	average (ppm)	0.66	2.59	-	2.38	7.87	4.55	3.65	3.74	4.14	6.21
Cilioride	std. dev.	0.74	0.43	-	0.38	4.83	0.42	0.78	0.53	0.68	1.11
Nitrate	average (ppb)	J	J	-	J	J	J	J	J	J	J
Millate	std. dev.	-	-	-	-	-	-	-	-	-	-
1-Hexene	average (mg/kg)	27.4	74.89	70.99	90.9	59.96	73.87	83.11	51.536	24.262	68.065
	std. dev.	6.42	1.36	3.3	5.89	25.8	4.88	15.61	28.79	6.2	8
$CO_2$	average (ppmv)	0	0	-	0	0	0	0	0	0	0
	std. dev.	0	0	-	0	0	0	0	0	0	0
moisture	average (%)	14.32	14.48	-	14.9	15.05	15.02	15.05	14.96	14.65	14.72
moisture	std. dev.	1.38	0.34	-	0.38	0.95	0.36	0.6	0.3	0.69	0.18
рН	average	7.08	6.91	-	7.26	7.28	7.34	7.16	7.415	7.27	6.97
pm	std. dev.	0.01	0.08	-	0.09	0.04	0.11	0.04	0.12	0.04	0

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 11: 16% moisture, 80mg/kg 1-Hexene



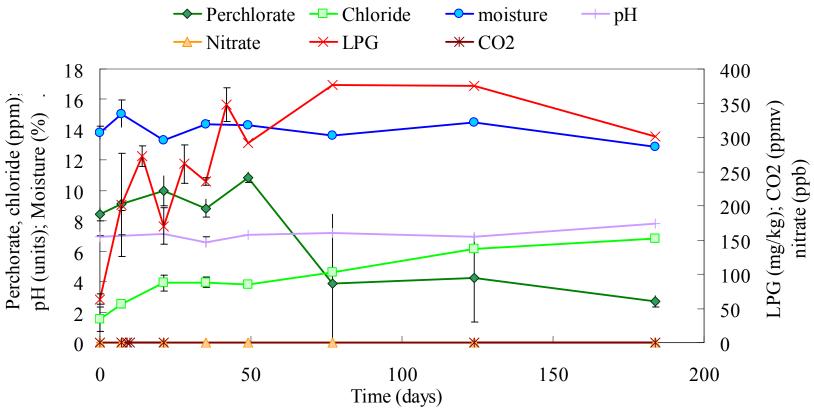
## **A.2.12 Test 12: 16% Moisture, 75 mg/kg LPG**

					Time (da	ays)						
		0	7	14	21	28	35	42	49	77	124	184
Perchlorate	average (ppm)	8.45	9.1	-	10	-	8.84	-	10.87	3.9	4.25	2.71
reicinorate	std. dev.	0.42	0.4	-	0.99	-	0.57	-	0.32	4.53	2.92	0.35
Chloride	average (ppm)	1.56	2.52	-	3.94	-	3.97	-	3.81	4.64	6.14	6.85
Cilioride	std. dev.	0.79	0.25	-	0.52	-	0.34	-	0.13	1.28	1.18	1.69
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	J
Milate	std. dev.	-	-	-	-	-	-	-	-	-	-	-
LPG	average (mg/kg)	63.53	201.05	272.06	170.12	261.36	235.2	347.99	292.187	377.18	374.665	301.312
	std. dev.	7.26	75.67	14.98	26.66	27.9	5.53	24.7	5.2	34.92	5.97	0
CO <sub>2</sub>	average (ppmv)	0	0	-	0	-		-	0	0	0	0
	std. dev.	0	0	-	0	-	1105	-	0	0	0	0
moisture	average (%)	13.83	15.07	-	13.31	-	14.36	-	14.28	13.62	14.46	12.87
	std. dev.	0.44	0.92	-	0.15	-	0.24	-	1.89	0.81	1.2	0
рН	average	6.96	7	-	7.13	-	6.62	-	7.11	7.2	6.96	7.84
PII	std. dev.	0.07	0.06	-	0.03	-	0.33		0.11	0.02	0	0

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)









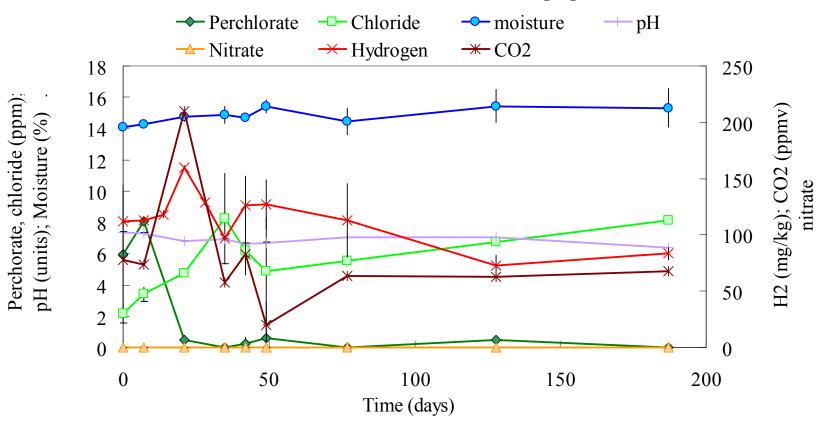
## A.2.13 Test 13: 16% Moisture, 114 mg/kg $H_2$

					Time (c	lays)						
		0	7	14	21	28	35	42	49	77	128	187
Perchlorate	average (ppm)	5.93	8.05	-	0.49	-	0	0.25	0.59	0	0.466	0
Tercinorate	std. dev.	3.99	0.23	-	0.05	-	0	0.43	0.69	0	0.024	0
Chloride	average (ppm)	2.16	3.42	-	4.76	-	8.26	6.22	4.87	5.52	6.73	8.12
Cilionae	std. dev.	0.61	0.45	-	0.12	-	2.88	0.36	3.44	1.65	0.59	1.96
Nitrate	average (ppb)	J	J	-	J	-	J	J	J	J	J	J
Nitrate	std. dev.	-	-	-	-	-	-	-	-	-	-	-
Hydrogen	average (mg/kg)	111.77	112.7	118.12	159.82	128.91	97.22	126.455	126.96	112.945	72.85	83.326
	std. dev.	32.6	1.6	3.07	1.14	2.37	1.7	26.02	21.87	32.67	9.02	5.153
$CO_2$	average (ppmv)	77.67	73.88	-	210.15	-	57.35	82.48	19.98	63.52	62.38	68.14
	std. dev.	2.27	0.61	-	0.78	-	2.36	18.45	20.38	67.18	3.01	0.43
moisture	average (%)	14.11	14.28	-	14.76	-	14.86	14.71	15.42	14.45	15.42	15.31
moisture	std. dev.	0.02	0.13	-	0.3	-	0.55	0.02	0.44	0.86	1.06	1.23
рН	average	7.33	7.31	-	6.79	-	6.95	6.6	6.68	7.04	7.045	6.38
p11	std. dev.	0.07	0.05		0.04	-	0.04	0.08	0.06	0.56	0.08	0.1

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



**Test 13: 16% moisture, 114mg/kg H2** 



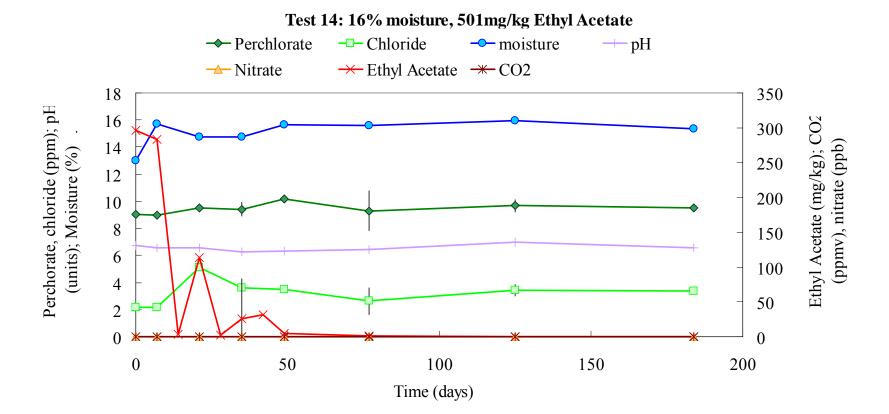


#### A.2.14 Test 14: 16% Moisture, 501 mg/kg ethyl acetate

						Time (	days)					
		0	7	14	21	28	35	42	49	77	125	184
Perchlorate	average (ppm)	9.04	8.97	-	9.52	-	9.42	-	10.15	9.29	9.67	9.52
1 eremorate	std. dev.	0.16	0.04	-	0.13	-	0.51	-	0	1.49	0.44	0
Chloride	average (ppm)	2.14	2.16	-	5.11	-	3.59	-	3.48	2.62	3.42	3.36
Cilioride	std. dev.	0.09	0.05	-	0.19	-	0.18	-	0	0.98	0.42	0
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
TVILLACE	std. dev.		-	-	-	-	83	-	-	-	-	0
Ethyl Acetate	average (mg/kg)	296.38	282.763	3.75	113.974	1.92	25.84	31.99	4.913	1.015	0	0
CO <sub>2</sub>	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	12.99	15.74	-	14.75	-	14.74	-	15.64	15.59	15.97	15.4
рН	average	6.75	6.56	-	6.55	-	6.25	-	6.3	6.45	6.99	6.58

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)





CDM

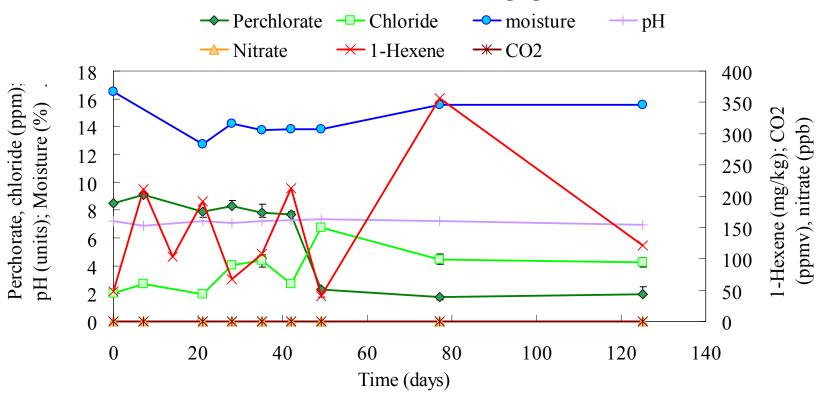
## A.2.15 Test 15: 16% Moisture, 265 mg/kg 1-hexene

			Time (days)										
		0	7	14	21	28	35	42	49	77	125		
Perchlorate	average (ppm)	8.51	9.11	-	7.91	8.3	7.85	7.67	2.32	1.75	1.96		
1 elcillorate	std. dev.	0.01	0.05	-	0.01	0.4	0.56	0.22	0	0.016	0.54		
Chloride	average (ppm)	2.05	2.68	-	1.97	4.05	4.36	2.69	6.75	4.48	4.26		
Cilioride	std. dev.	0.04	0.03	-	0.06	0.01	0.46	0.14	0	0.4	0.34		
Nitrate	average (ppb)	J	J	-	J	J	J	J	J	J	J		
Millate	std. dev.	ı	-	=	=	=	-	-	-	-	-		
1-Hexene	average (mg/kg)	48.215	211.11	103.13	191.27	67.84	108.556	212.885	40.65	356.845	120.96		
CO <sub>2</sub>	average (ppmv)	0	0	-	0	0	0	0	0	0	0		
moisture	average (%)	16.51	-	-	12.76	14.23	13.78	13.83	13.83	15.58	15.57		
pН	average	7.22	6.88	-	7.18	7.08	7.22	7.3	7.33	7.24	6.97		

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 15: 16% moisture, 265mg/kg 1-Hexene





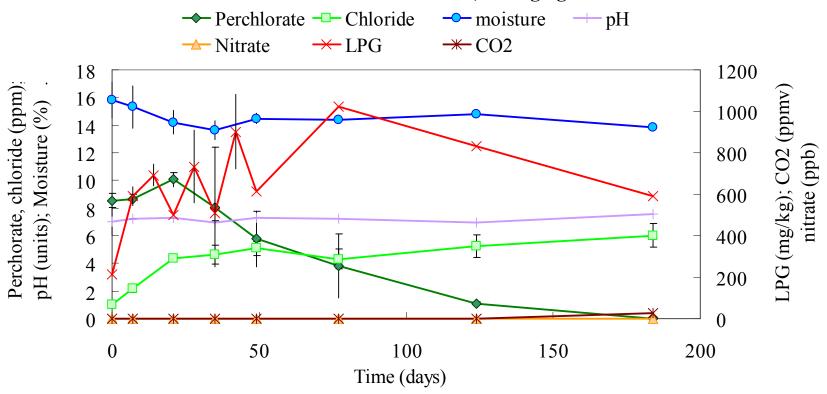
# A.2.16 Test 16: 16% moisture, 250 mg/kg LPG

		Time (days)										
		0	7	14	21	28	35	42	49	77	124	184
Perchlorate	average (ppm)	8.51	8.67	-	10.08	-	8.06	-	5.77	3.83	1.1	0
	std. dev.	0.57	0.31	-	0.52	-	4.32	-	2	2.33	0.13	0
Chloride	average (ppm)	1.04	2.19	-	4.36	-	4.66	-	5.09	4.3	5.26	6.03
Cinoriae	std. dev.	0.18	0.28	-	0.12	-	0.69	-	0.51	0.72	0.81	0.83
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
Nitrate	std. dev.	-	-	-	-	-	-	-	-	-	-	0
LPG	average (mg/kg)	214.2	590.55	693.16	498.5	733.52	509.3	901.34	615.87	1022.21	830.391	589.22
	std. dev.	0.25	46.56	52.29	0.07	176.48	69.4	180.8	21.3	82.93	158.8828	2.76
$CO_2$	average (ppmv)	0	0	-	0	-	0	-	0	0	0	27.5
	std. dev.	0	0	-	0	=	0	-	0	0	0	38.89
moisture	average (%)	15.84	15.31	-	14.2	-	13.64	-	14.47	14.38	14.78	13.85
moisture	std. dev.	1.29	1.54	-	0.85	-	0.68	=	0.37	0.07	0.15	0.05
рН	average	7.04	7.23	-	7.28	-	6.96	-	7.3	7.245	6.975	7.56
PII	std. dev.	0.99	0.02	-	0.04	-	0.1	-	0.13	0.007	0.01	0.08

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 16: 16% moisture, 250mg/kg LPG





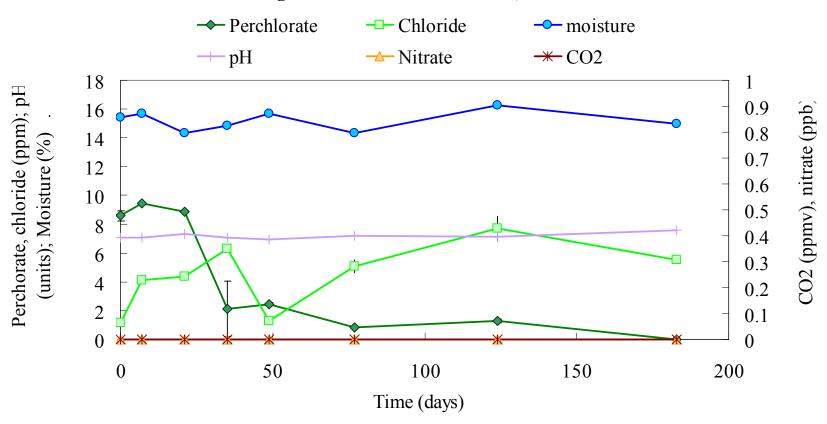
#### A.2.17 Test 17: Negative control. 16% Moisture, no external electron donor.

					Time	(days)						
		0	7	14	21	28	35	42	49	77	124	183
Perchlorate	average (ppm)	8.59	9.47	-	8.87	-	2.12	-	2.47	0.85	1.26	0
1 cremorate	std. dev.	0.35	0.03	-	0.08	-	1.91	-	0	0.086	0.13	0
Chloride	average (ppm)	1.16	4.12	-	4.34	-	6.28	-	1.3	5.09	7.7	5.5
Cinoriac	std. dev.	0.09	0.004	-	0.04	-	0.02	-	0	0.44	0.88	0.23
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
Nitrate	std. dev.	-	-	-	-	-	-	-	-	-	-	0
Electron Donor	average (mg/kg)	0	0	0	0	0	0	0	0	0	0	0
CO <sub>2</sub>	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	15.41	15.67	-	14.36	-	14.87	-	15.7	14.36	16.25	14.95
рН	average	7.07	7.09	-	7.3	-	7.05	-	6.97	7.23	7.13	7.58

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 17: Negative control. 16% moisture, no electron donor.





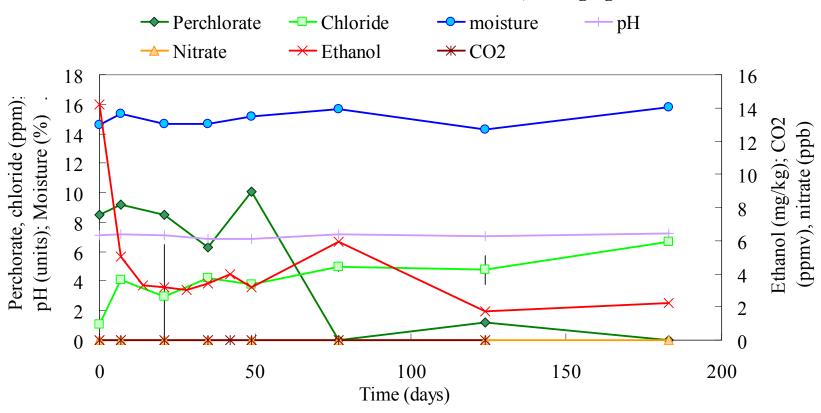
#### A.2.18 Positive control. 16% Moisture, 436 mg/kg ethanol.

		Time (days)										
		0	7	14	21	28	35	42	49	77	124	183
Perchlorate	average (ppm)	8.49	9.2	-	8.5	-	6.29	-	10.04	0	1.17	0
1 erciliorate	std. dev.	0.08	0.04	-	0.27	-	0.11	-	0	0	0.08	0
Chloride	average (ppm)	1.07	4.06	-	2.96	-	4.2	-	3.8	4.99	4.77	6.64
Cilioride	std. dev.	0.03	0.03	-	3.53	-	0	-	0	0.31	0.97	0.68
Nitrate	average (ppb)	J	J	-	J	-	J	-	J	J	J	0
Nitrate	std. dev.	-	-	-	-	-	-	-	-	-	0.08 4.77 0.97 J	0
Ethanol	average (mg/kg)	14.23	5.034	3.32	3.184	3.04	3.412	3.964	3.183	5.93	1.742	2.257
$CO_2$	average (ppmv)	0	0	-	0	-	0	-	0	0	0	0
moisture	average (%)	14.63	15.34	-	14.65	-	14.69	-	15.14	15.67	14.27	15.8
рН	average	7.11	7.15	-	7.14	-	6.86	-	6.89	7.15	7.05	7.22

J = below the detection limit (the substance in question was detected, but at levels below that which can be accurately characterized by the test method)



Test 18: Positive control. 16% moisture, 436mg/kg Ethanol.





# Appendix A-4

# **Column Test Data**

#### B.1 H<sub>2</sub> Column Study Theoretical Breakthrough Calculations

Electron Donor: Hydrogen

Soil moisture: 10%

Bulk gas velocity: 0.01 cm/s

- 1. Measure the moisture content of the stored soil in duplicate. Add DDI water if necessary to raise the soil moisture to 10%.
- 2. Weigh out the mass of soil to be packed into the two duplicate columns to make the soil density in each column similar to the site conditions (1.6 g/mL, GEDIT\_calc\_Nov2005 spreadsheet).

Column Dimensions:  $D = 2 \text{ in} = 2 \text{in} \times 2.54 \text{ cm/in} = 5.08 \text{ cm}$ 

 $H = 5 \text{ ft} = 5 \times 30.48 \text{ cm/ft} = 152.4 \text{ cm}$ 

Area =  $\pi D^2/4 = \pi (5.08 \text{ cm})^2/4 = 20.27 \text{ cm}^2$ 

 $V = Area \times H = 152.4 cm \times 20.27 cm^2 = 3089.15 cm^3 = 3089.15 mL$ 

So the mass of soil that needs to be packed into each column is:

Soil mass =  $3089.15 \text{ mL} \times 1.6 \text{ g/mL} = 4942.64 \text{ g} =$ **4.94 kg** 

- 3. Pack the soil into two columns made of clear polyvinylchloride (PVC) pipe. Pack the columns by adding 1-2" lifts of soil and tapping the side of the column between lifts to promote even soil distribution within the column.
- 4. Purge both of the columns with nitrogen gas until less than 1% oxygen is detectable in the column effluent.
- 5. Inject 20% hydrogen and 80% nitrogen mixed gas at a bulk gas average linear velocity,  $v_{ave} = 0.01$  cm/s, assuming a soil porosity, n = 40%.

Flow rate,  $Q = (v_{ave} \times n) \times A$ 

= 
$$(0.01 \text{ cm/s} \times 0.4) \times 20.27 \text{ cm}^2 = 0.081 \text{ cm}^3/\text{s} \times 60 \text{ s/min} = 4.86 \text{ cm}^3/\text{min} = 4.86$$

mL/min

The mass flow controllers will be set to **4.9 mL/min**.

6. The effluent of the column will be tested for H<sub>2</sub> concentration **every 30 minutes** for the first 2 hours, and then after an increase in H<sub>2</sub> has been observed, samples will be taken approximately every 10 minutes to capture a breakthrough curve that contains a minimum of five points for each column.

Time to breakthrough, t = H/v=  $(152.4cm)/(0.01 cm/s) \times (1 hour/3600 sec) = 4.23 hours$ 

7. After hydrogen has been observed to travel from the beginning to the end of the duplicate columns, gas injection will be stopped, and the column ends capped. Headspace samples for hydrogen will then be taken (at t=0) with a 250 uL gas-tight syringe from seven sampling ports spaced evenly along the column length (i.e., out of the 28 total ports on the column, every third port will be sampled). The columns will then be incubated at room temperature in the dark for 2-4 weeks.

- 8. After 2 4 weeks, 200 uL headspace samples will again be withdrawn from every third sampling port of both columns to measure hydrogen and oxygen concentrations and test for "hydrogen floating". If hydrogen levels have dropped below 2 mg/kg, the columns will be repurged with the 20% H<sub>2</sub> / 80% N<sub>2</sub> gas mixture as before, and then capped. The hydrogen concentrations along the length of the column will be remeasured prior to continued incubation.
- 9. After approximately 2 months of total incubation, the headspace will again be sampled for hydrogen and oxygen as before, and then one of the duplicate columns will be sacrificed and the soil behind **every other sampling port** (i.e., 14 out of the total 28 ports on the column) will be analyzed for perchlorate, chlorate, chlorite, chloride, nitrate, nitrite, pH, and soil moisture. If, at this time, perchlorate levels are below detection, then the second column will also be sacrificed and analyzed; if not, it will be allowed to incubate approximately one more month before being sacrificed and analyzed as described above.

#### **Appendix**

#### **Electron donor sufficiency calculation:**

Void fraction of soil = 40% (GEDIT\_Evans\_calc\_Nov2005 spreadsheet) Volume of H<sub>2</sub> in the column =  $40\% \times V_{column} \times 10\% = 40\% \times 3089.15 \text{ mL} \times 10\% = 123.57 \text{ mL}$ Mass of H<sub>2</sub> in the column =  $1.013 \times 10^5 \text{ Pa} \times 123.57 \text{mL} \times 1 \text{m}^3 / 1000 \text{mL} = 5.10 \text{ mol}$  $8.314472 \text{ [m}^3 \cdot \text{Pa} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}] \times 295 \text{ K}$ 

Perchlorate concentration in the soil is about 10ppm.

Perchlorate mass in the column =  $4.94 \text{ kg soil} \times 10 \text{ mg/kg} = 49.4 \text{ mg} / 99.45 \text{g/mol} = 0.5 \text{ mmol}$ 

Degrade 1mol perchlorate needs 4 mol hydrogen,

So  $H_2$  mass needed to degrade all of the perchlorate in column = 0.5 mmol  $\times$  4 = 2 mmol.

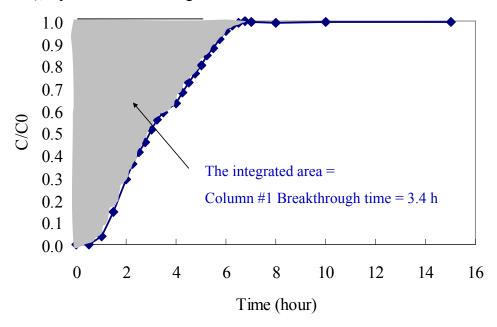
Safety factor =  $5.10 \times 10^3$  mmol / 2 mmol = 2550 The hydrogen is sufficient!

# **B.2** Experimental Breakthrough Time Calculation

Using column #1 as an example, the breakthrough time was calculated as below: Inlet hydrogen concentration  $C_0 = 4.96$  mg/kg.

		ion C <sub>0</sub> – 4.96 i						
Time	Peak	H <sub>2</sub> in Soil (C)	c/c0	Integration				
(hour)	Area	(mg/kg)	0	$(C_2/C_0-C_1/C_0)*t_2$				
0	0.000	0.000	0	0				
0.5	0	0.000	0	0				
1	18.088	0.186	0.037402	0.037402				
1.5	71.017	0.728	0.146847	0.164167				
2	141.871	1.455	0.293356	0.293019				
2.25	173.72	1.782	0.359212	0.148177				
2.5	199.008	2.041	0.411502	0.130724				
2.75	221.248	2.269	0.457489	0.126465				
3	248.329	2.547	0.513486	0.167992				
3.25	269.721	2.766	0.55772	0.143759				
3.5	285.291	2.926	0.589915	0.112683				
4	305.7185	3.135	0.632155	0.168957				
4.25	329.778	3.382	0.681904	0.211435				
4.5	350.768	3.598	0.725306	0.195311				
4.75	369.112	3.786	0.763238	0.180173				
5	388.053	3.980	0.802403	0.195828				
5.25	409.748	4.202	0.847263	0.235516				
5.5	425.169	4.361	0.87915	0.175379				
5.75	444.397	4.558	0.918909	0.228614				
6	461.248	4.731	0.953753	0.209064				
6.25	474.469	4.866	0.981091	0.170862				
6.5	480.1355	4.924	0.992808	0.076161				
6.75	483.188	4.956	0.99912	0.042605				
7	481.6182	4.940	0.995874	0				
8	479.245	4.915	0.990967	0				
10	480.799	4.931	0.99418	0				
15	481.866	4.942	0.996387	0				
				SUM= 3.414292 (Breakthrough time)				

Plot the breakthrough curve with time as the x-axis and  $C/C_0$  as the y-axis. The area surrounded by the breakthrough curve, the y-axis, and the  $C/C_0=1$  line (as illustrated by the darkened area in the plot below), equals the breakthrough time.



# Meter Calibration Log ESTCP Project ER-0511

Carbon Dioxide (%)			Oxygen - low (%)			Oxygen - high (%)			Propane - low* (% or %LEL)				Propane - high* (% or %LEL)				Hydrogen (%)						
Date	Standard	Reading	Deviation	Recalibrated Standard	Reading	Deviation	Recalibrated	Standard	Reading	Deviation	Recalibrated	Standard Rea	ading	Deviation	Recalibrated	Standard	Reading	Deviation	Recalibrated	Standard	Reading [	Deviation	Recalibrated
4/7/200	3 2.5	2.5	0.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
4/14/200	3 2.5	2.44	-2.4%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
4/29/200	3 2.5	2.38	-4.8%	N 0.0	0.0	#DIV/0!	N	12.00	12.10	0.8%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
5/13/200	3 2.5	2.58	3.2%	N 0.0	0.0	#DIV/0!	N	12.00	12.10	0.8%	N	49.00	50.00	2.0%	N		NA		NA	2.00	1.80	-10.0%	N
5/20/200	3 2.5	2.6	4.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.30	2.5%	N	49.00	50.00	2.0%	N		NA		NA	2.00	1.80	-10.0%	N
5/23/200	3 2.5	2.4	-4.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.20	1.7%	N	49.00	48.00	-2.0%	N		NA		NA	2.00	1.80	-10.0%	N
5/27/200	3 2.5	2.7	8.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.20	1.7%	N	49.00	51.00	4.1%	N		NA		NA	2.00	1.90	-5.0%	N
6/4/200	3 2.5	2.5	0.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.30	2.5%	N	49.00	48.00	-2.0%	N		NA		NA	2.00	1.80	-10.0%	N
6/12/200	3 2.5	2.28	-8.8%	Y 0.0	0.0	#DIV/0!	N	12.00	12.30	2.5%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
6/20/200	3 2.5	2.48	-0.8%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.70	-15.0%	N
6/25/200	3 2.5	2.42	-3.2%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
7/2/200	3 2.5	2.4	-4.0%	N 0.0	0.0	#DIV/0!	N	12.00	11.80	-1.7%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.70	-15.0%	N
7/7/200	3 2.5	2.18	-12.8%	N 0.0	0.0	#DIV/0!	N	12.00	11.80	-1.7%	N	0.90	0.84	-6.7%	N		NA		NA	2.00	1.60	-20.0%	N
7/11/200	3 2.5	2.46	-1.6%	N 0.0	0.0	#DIV/0!	N	12.00	11.90	-0.8%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.70	-15.0%	N
7/18/200	3 2.5	2.42	-3.2%	N 0.0	0.0	#DIV/0!	N	12.00	11.90	-0.8%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.70	-15.0%	N
7/24/200	3 2.5	2.4	-4.0%	N 0.0	0.0	#DIV/0!	N	12.00	11.90	-0.8%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
7/31/200	3 2.5	2.5	0.0%	N 0.0	0.0	#DIV/0!	N	12.00	11.90	-0.8%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
8/7/200	3 2.5	2.48	-0.8%	N 0.0	0.2	#DIV/0!	N	12.00	11.80	-1.7%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
8/12/200	3 2.5	2.48	-0.8%	N 0.0	0.0	#DIV/0!	N	12.00	11.80	-1.7%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.80	-10.0%	N
8/18/200	3 2.5	NA	#VALUE!	N 0.0	NA	#VALUE!	N	12.00	12.30	2.5%	N	0.90	0.82	-8.9%	N		NA		NA	2.00	1.80	-10.0%	N
9/8/200	3 2.5	NA	#VALUE!	N 0.0	NA	#VALUE!	N	12.00	12.00	0.0%	N	0.90	0.86	-4.4%	N		NA		NA	2.00	1.60	-20.0%	N
9/15/200	3 2.5	2.48	-0.8%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.94	4.4%	N	10.00	8.50	-15.0%	Υ	2.00	1.70	-15.0%	N
9/29/200	3 2.5	2.38	-4.8%	N 0.0	0.1	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.94	4.4%	N	10.00	9.50	-5.0%	N	2.00	1.70	-15.0%	N
10/13/200	3 2.5	2.36	-5.6%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.96	6.7%	N	10.00	10.00	0.0%	N	2.00	1.80	-10.0%	N
10/20/200	3 2.5	2.4	-4.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	49.00	52.00	6.1%	N	10.00	10.00	0.0%	N	2.00	1.70	-15.0%	N
11/5/200	3 2.5	2.48	-0.8%	N 0.0	0.1	#DIV/0!	Υ	12.00	11.90	-0.8%	N	0.90	0.96	6.7%	N	10.00	10.00	0.0%	N	2.00	1.80	-10.0%	N
11/17/200	3 2.5	2.36	-5.6%	N 0.0	0.0	#DIV/0!	N	12.00	11.80	-1.7%	N	0.90	0.94	4.4%	N	10.00	10.00	0.0%	N	2.00	1.70	-15.0%	N
12/1/200	3 2.5	2.4	-4.0%	N 0.0	0.0	#DIV/0!	N	12.00	12.00	0.0%	N	0.90	0.96	6.7%	N	10.00	9.50	-5.0%	N	2.00	1.80	-10.0%	N

<sup>\*</sup>iso-butane used as standard. Low level was reported either as percent (0.9%) or percent of LEL (49%)

LEL - Lower explosive limit

## Soil Precision Results

Sample	Perchlo	rate	Nitrate	Moisture		
•	μg/kg (dry)	RPD	mg-N/kg (dry)	RPD	%	RPD
Baseline						
P4-15-102907	25000	34%	6.4	11%	36	12%
P4-15-D	17647		5.7		32	
P4-40-102907	19403	4%	6.9	3%	33	28%
P4-40-D	18667		7.1		25	
CDM-INJ2-25-102607	5921	28%	5.0	24%	24	8%
CDM-INJ2-25-D	4459	2070		2470	26	0 /0
			3.9			
P2-05-102507	597222	25%	5.8	93%	28	10%
P2-05-D	463768		15.9		31	
P2-20-102507	242857	46%	15.7	6%	30	7%
P2-20-D	388889		16.7		28	
CDM-CB-1-041808-30	7018	96%	0.6	91%	31.6	70%
CDM-CB-1-041808-30D	2479		0.2		15.3	
CDM-CB-2-041808-30	2576	67%	0.2	24%	37.9	96%
CDM-CB-2-041808-30D	5196		0.1		13.4	
CDM-CB3-30-061008	3869	41%	0.1	146%	9.53	44%
CDM-CB3-30D-061008	5875		0.7		14.9	
CDM-CB4-30-061008	12135	16%	0.8	16%	9.35	11%
CDM-CB4-30D-061008	14192		1.0		8.4	
CDM-CB7-30-090208	8000	10%	0.9	6%	31.5	5%
CDM-CB7-30D-090208	8800		0.9		33	
CDM-CB8-30-090208	16000	51%	0.2	42%	4.4	43%
CDM-CB8-30D-090208	27000		0.2		6.8	
CDM-CB9-30-120208	150	7%	0.3	44%	11.3	18%
CDM-CB9-30D-120208	140		0.2		9.4	
CDM-CB10-30-120208	270	70%	0.2	40%	10.3	8%
CDM-CB10-30D-120208	130	0.40/	0.2	000/	9.5	400
CDM-CB11-30-120308	23000	24%	0.1	26%	16.9	13%
CDM-CB11-30D-120308	18000	57%	0.1	00/	14.9	5%
CDM-CB12-30-120308 CDM-CB12-30D-120308	1400 780	3/%	0.1	0%	9.3 9.8	5%
CDM-CB12-30D-120308	15000	0%	0.1	32%	11.4	6%
CDM-CB13-30D-120308	15000	0 70	0.1	JZ /0	10.7	07
CDM-CB14-30-120308	1400	70%	0.1	50%	6.8	149
CDM-CB14-30D-120308	2900	. 0 70	0.1	0070	7.8	,
CDM-CB15-30-120308	1200	91%	0.1	65%	9.1	6%
CDM-CB15-30D-120308	3200		0.1		9.7	
CDM-CB16-30-120308	13	0%	0.1	18%	25.6	9%
CDM-CB16-30D-120308	13		0.1		23.4	
CDM-CB17-30-120308	8800	26%	0.1	27%	11.60	20%
CDM-CB17-30D-120308	6800		0.1		9.50	
CDM-CB18-30-120308	7400	29%	0.1	21%	19.40	15%
CDM-CB18-30D-120308	9900		0.2		16.70	
CDM-CB19-30-120308	13000	43%	0.1	18%	7.50	3%
CDM-CB19-30D-120308	8400		0.1		7.70	

Notes

μg/kg - Micrograms per kilogram mg-N/kg - Milligrams nitrogen per kilogram RPD - Relative percent difference

# **Appendix E: Quality Assurance and Quality Control**

This appendix includes specific QAQC-related information as specified in ESTCP guidance for the Final Report.

## E.1 Calibration of Analytical Equipment

#### **E.1.1 Field Instrumentation**

Calibration checks of the H2scan and RKI field instruments were conducted in the field at the beginning of each day. Standards used for calibration included 0.0 percent oxygen, 12 percent oxygen, 2.5 percent carbon dioxide, 2.0 percent hydrogen, 0.9 percent iso-butane, and 10 percent iso-butane. iso-Butane was used as a standard for calibration of the propane sensor based on manufacturer recommendations and availability of the standard. The RKI instrument was very stable and generally did not require re-calibration. Readings were generally within five percent of the standard concentration. If these deviations were exceeded the instrument was recalibrated. Field instrument calibration procedures were performed in accordance with the manufacturer's recommendations. The H2scan instrument was also stable and readings were generally within 10 to 15 percent of the standard concentration. The H2scan was not capable of being field calibrated. A meter calibration log is included at the end of this Appendix

#### **E.1.2 Laboratory Equipment Calibration**

Pace Analytical Services Inc. 4 conducted laboratory analyses. Initial and continuing calibration procedures for laboratory instruments were conducted in accordance with the laboratory's QA manual.

#### **E.2 Quality Assurance Sampling and Analysis**

Field duplicates were collected by the sampling team for analysis by the off-site laboratories. Field duplicates were collected to provide site-specific, field-originated information regarding the homogeneity of the sample matrix and the consistency of the sampling effort and to provide an assessment of precision including sampling and handling error. Field duplicates were collected at a frequency of approximately 10 percent of the total field samples (i.e. 1 field duplicate for every 10 field samples) and were collected concurrently with the field samples so at to equally represent the medium at a given time and location. A precision goal of 35 percent was established for soil samples.

Twenty-two complete data pairs (i.e., duplicate samples) were evaluated for precision and data are included at the end of this Appendix. Ten perchlorate data pairs (45 percent) exceeded the 35 percent goal and the greatest relative percent deviation (RPD) was 96 percent. Eight nitrate data pairs (36 percent) exceeded the 35 percent goal and the greatest RPD was 146 percent. Four moisture data pairs (18 percent) exceeded the 35 percent goal and the greatest RPD was 96 percent. While a significant percentage of data exceeded the RPD goals, these data are representative of a highly heterogeneous site and highlight the challenges in demonstrating soil

<sup>&</sup>lt;sup>4</sup>Laboratory analyses were initially conducted by Laucks Testing Laboratories which was later acquired by Pace.

remediation technologies. These data are considered useable based on comparison of the observed RPD values to the performance goals of 90 percent contaminant removal. The worst case perchlorate of 96 percent RPD corresponded to concentrations of 7,018 and 2,479 µg/kg. If the greater value is assumed to be an "initial" concentration, a percent removal of 65 percent is calculated. This value is less than the 90 percent performance goal and thus observed removals of perchlorate were associated with actual degradation rather than heterogeneity. Similarly, the worst case perchlorate of 146 percent RPD corresponded to concentrations of 0.1 and 0.7 mg-N/kg. If the greater value is assumed to be an "initial" concentration, a percent removal of 86 percent is calculated. This value is less than the 90 percent performance goal and thus observed removals of nitrate were associated with actual degradation rather than heterogeneity.

#### **E.3 Decontamination Procedures**

Decontamination procedures used at the site were limited to drilling rig sampling equipment. The drilling rig and soil sampling components were decontaminated prior to arriving at the site. After each boring was completed, decontamination of all downhole drilling equipment and associated tools was performed. Equipment and tools were decontaminated by washing in a solution of Alconox or equivalent non-phosphate detergent, followed by a double rinsing with clean water. Excess soil on the drill rig and support vehicles was removed by steam cleaning, when appropriate. Pertinent field activities associated with drilling, well installation, and well development were documented in a field notebook in accordance with CDM Standard Operating Procedures described in the Quality Assurance Project Plan (Appendix C) of the Technology Demonstration Plan.

#### **E.4 Sample Documentation**

The sampling documentation program included field logbooks, data entry forms, photographs, chain-of-custody forms, and laboratory data. Field logbooks were used to document drilling events, site visits, material deliveries, and other pertinent project-related activities. Field logbooks and data entry forms included soil boring log forms, injection test monitoring forms, and instrument calibration forms. Laboratory data were received both electronically and in hard-copy formats. Data were transcribed to Excel spreadsheets for data analysis. Raw data are included in Appendix C. Digital photographs were taken periodically during the project to document site layout, equipment setup and configuration, and other technical aspects.

# **Appendix F: GEDIT General Engineering Guidance**

## 1.0 Introduction

This document provides general engineering guidance for implementation of gaseous electron donor injection technology (GEDIT). It is organized as follows:

- Section 1 is this Introduction.
- Section 2 provides a description of the technology and its intended applications.
- Section 3 provides engineering design guidance include pre-design data and testing requirements.
- Section 4 provides information on operations of the process.
- Section 5 describes monitoring, sampling, and analysis requirements.
- Section 6 describes health and safety considerations.

This guidance does not purport to address all engineering, health and safety, or regulatory requirements for implementation of GEDIT. Professional engineering judgment and standard of care is required prior to implementation of GEDIT at any site. GEDIT is covered by U.S. Patent Number 7,282,149 and a patent pending.

## 2.0 Technology Description

GEDIT involves injection of gaseous electron donors into the soil with the purpose of promoting anaerobic bioremediation of perchlorate to water and chloride ion. This technology can be viewed as bioventing in reverse as illustrated in Figure 1. Bioventing, a proven bioremediation technology, involves the injection of a gaseous electron acceptor (e.g., oxygen) into the vadose zone resulting in the biodegradation of an electron donor (e.g., hydrocarbons). In the present application, the electron acceptor and donor are reversed with the gaseous electron donor being injected in order to biodegrade the electron acceptor.

Bioventing is an effective technology because it relies on the excellent mass transfer characteristics of gases and their ability to distribute oxygen through the vadose zone. Similarly, the injection of gaseous electron donors for perchlorate biodegradation in vadose zone soil benefits from these same gas mass transfer and distribution characteristics. The superior mass transfer and distribution of gases as compared to liquids is the major advantage of this technology over current attempts to introduce liquids into the vadose zone. Diffusion of gases in the vadose zone improves the ability to deliver the electron donor throughout the soil volume and helps to overcome problems associated with liquid flow through preferential pathways. Additionally, gaseous electron donor technology does not require the capture and treatment of infiltrated liquids that could otherwise adversely impact groundwater.

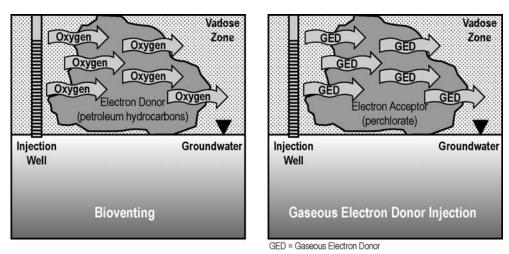


Figure 1 – Comparison of Bioventing and Gaseous Electron Donor Injection Technology

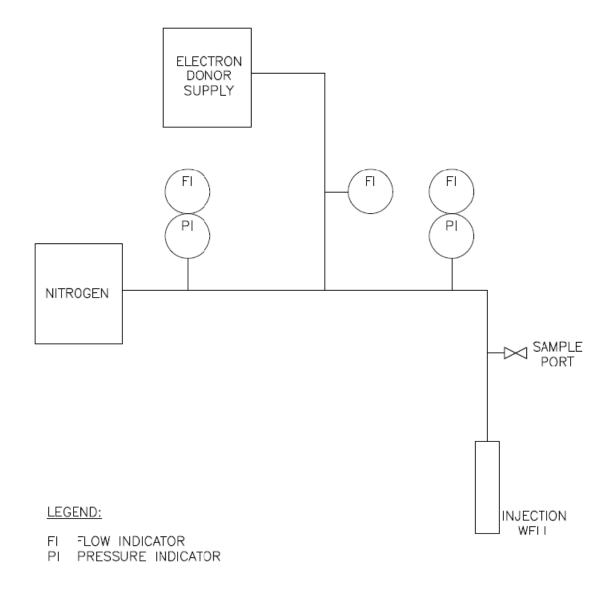
GEDIT involves injection of gaseous electron donors into the soil using injection wells in combination with optional soil vapor extraction wells. These gaseous electron donors can include hydrogen, propane, or volatile organic compounds such as methanol, ethanol, butanol, acetic acid, ethyl acetate, butyl acetate, hexene, etc. The injected concentration of the electron donor is less than its saturation vapor pressure so that the injected electron donor truly exists as a gas and not as a mist. As the gaseous electron donor material is injected into the vadose zone it partitions between soil moisture and the vadose zone pore space. After it has partitioned into the soil moisture, anaerobic, perchlorate-reducing bacteria can use the electron donor to reductively

degrade perchlorate. Any soil nitrate or oxygen that is present in the pore space will first be reduced using the injected gaseous electron donor. The remaining electron donor will be available for use by perchlorate-reducing bacteria. The rate at which the gaseous electron donor is transported through the vadose zone is primarily a function of soil moisture, electron donor Henry's constant, void volume, bulk soil density, bulk gas velocity, soil permeability, and biodegradation rate (Evans and Trute, 2006). GEDIT is similar to anaerobic bioventing (U.S. EPA, 2006b). Anaerobic bioventing has been described to involve injection of hydrogen and carbon dioxide into soil to promote anaerobic biodegradation of organic contaminants including chlorinated hydrocarbons and dichlorodiphenytrichloroethane (DDT). GEDIT can include use of hydrogen/carbon dioxide and can additionally use liquid electron donors that can be vaporized into a gaseous carrier stream. In addition, GEDIT was developed specifically for treatment of perchlorate.

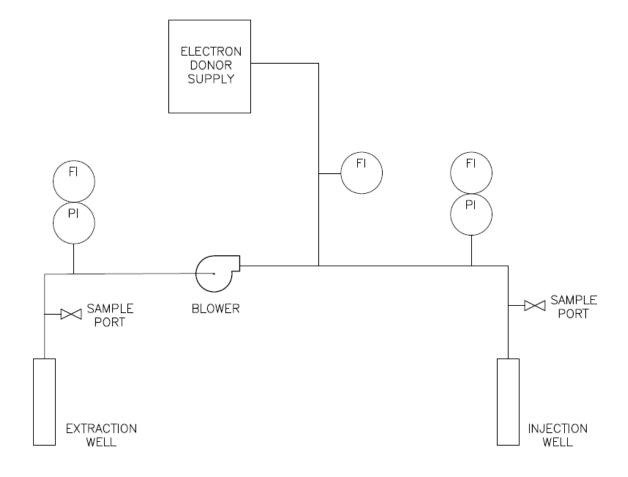
GEDIT can be implemented in various configurations two of which are illustrated in Figures 2 and 3. In the gas injection configuration, nitrogen from a generator or a liquid nitrogen supply is amended with gaseous electron donor and then injected into the perchlorate-impacted vadose zone. The presence of nitrogen serves to flush oxygen from the soil gas, enhancing conditions for the degradation of perchlorate. In the SVE configuration, soil vapor is extracted, amended with gaseous electron donor, and then injected back into the perchlorate-impacted vadose zone. As the reductive degradation of perchlorate progresses, the oxygen content of the extracted soil is reduced, thereby facilitating further perchlorate degradation. Well spacing for both of the configurations will depend on the pneumatic radius of influence and the specific gaseous electron donor selected for use.

Potential applications of GEDIT include treatment of a wide variety of oxidized contaminants in soil. A partial list of oxidized contaminants that are potentially treatable using GEDIT include:

- Perchlorate
- Chlorate
- Nitrate
- Nitrite
- Selenate
- Arsenate
- Chromate and dichromate (i.e., hexavalent chromium)
- Uranylate
- Pertechnetate
- N-Nitrosodimethylamine (NDMA)
- Trichloroethene (TCE)
- Trichloroethane (TCA)
- Highly energetic compounds including nitro-aromatics such as TNT, RDX, and HMX.



**Figure 2 – Example Gas Injection GEDIT Process and Instrumentation Diagram** 



## LEGEND:

FI FLOW INDICATOR

PI PRESSURE INDICATOR

Figure 3 – Example SVE GEDIT Process and Instrumentation Diagram

## 3.0 Engineering Design

This section includes engineering design considerations for injection wells, monitoring piezometers, process equipment, and instrumentation and controls. It also includes a description of pre-design data and testing requirements.

#### 3.1 General Design Considerations and Approach

The GEDIT process should be designed with the objective of minimizing oxygen concentrations and distributing sufficiently high concentrations of the gaseous electron donor(s) throughout the vadose zone. The absolute concentrations of oxygen and electron donors that are required are dependent on the particular contaminant of concern.

In general, contaminants that have a greater free energy for reduction (e.g., nitrate and chromate) will require lower oxygen concentrations than contaminants with a lower free energy for reduction (e.g., perchlorate, selenate, and uranylate). With respect to perchlorate, oxygen concentrations less than 1 percent appeared to be sufficient to promote biological reduction based on demonstration results. With respect to nitrate, greater concentrations – 10 percent or greater – were sufficiently low to support biological reduction.

The particular electron donor type and concentration are also dependent on the particular contaminant of concern. Hydrogen was determined to be required for perchlorate reduction whereas liquefied petroleum gas (LPG) was sufficient for nitrate reduction. The minimum concentration of hydrogen necessary to support perchlorate reduction was 0.5 percent. Carbon dioxide may also be required to support growth of autotrophic bacteria during contaminant degradation with the electron donor hydrogen. The requirement for carbon dioxide is site-specific and depends in part on the natural alkalinity (i.e., bicarbonate and carbonate) present in site soil. The minimum concentration of LPG necessary to support nitrate reduction was not determined but may be as low as 1 percent.

Achieving these concentrations of oxygen and electron donor(s) requires injection of the electron donor(s) and possibly other gases such as nitrogen and/or carbon dioxide. Reduction of oxygen concentrations in the vadose zone can occur via two processes: displacement and aerobic biodegradation. Displacement can be accomplished using any gas though certain gases are more effective than others. For example, because of varying densities, hydrogen floats, LPG sinks, and nitrogen does neither. Thus injection of nitrogen is effective at oxygen displacement horizontally from the point of injection, hydrogen is effective at oxygen displacement vertically upward from the point of injection, and LPG is effective at oxygen displacement vertically downward from the point of injection. Gaseous electron donors such as hydrogen and LPG can also remove oxygen when they are biodegraded by aerobic bacteria. These bacteria use hydrogen and LPG as electron donors and consume oxygen during the biodegradation process.

Other general considerations include soil lithology, permeability, and moisture content. The lithology and permeability will affect bulk transport of gas and diffusive transport of the electron donor. Permeability will also affect the rate of back diffusion or advection (e.g., barometric pumping) of oxygen into the treatment zone. Hydrogen is a small molecule with high diffusivity. Thus it has greater potential to diffuse into low permeability soils. Based on demonstration

results, GEDIT was determined to be effective in both low and high permeability soil types. Therefore, GEDIT is applicable to all soil lithologies; however, the design and operating conditions will likely vary and be site-specific. Moisture content often correlates with soil lithology. Moisture can affect permeability and also affects biological activity. Very low moisture contents can be inhibitory to biological activity. Based on demonstration results, acceptable perchlorate biodegradation was observed with soil moisture as low as 7 percent. This concentration may not be translatable to other sites and the minimum moisture content may be dependent on the soil lithology. Thus the minimum moisture content must be determined experimentally in a treatability test. This test will also serve to determine if other inhibitory compounds are present in the soil.

Recommended approaches to GEDIT design based on these general guidelines are described in the following sections.

## 3.2 Pre-Design Testing and Data Requirements

Laboratory treatability testing and field pilot testing are recommended as part of the GEDIT design process. Laboratory treatability testing is used to select electron donors, electron donor concentrations, and determine soil moisture limits. Field pilot testing is used to determine site permeability and gas flow rate requirements.

#### 3.2.1 Laboratory Testing

Soil microcosms are recommended to determine electron donor requirements and soil moisture limitations. In addition, microcosms can give an indication of the potential rate and extent of contaminant degradation. Detailed procedures for conducting the microcosms are included in the ESTCP Final Report. The general approach for conducting testing is presented here.

Prior to conducting the laboratory testing it is helpful to have an indication of the range of lithologies and moisture contents in vadose zone soil at the site and the range of contaminant concentrations. In addition, since contaminant concentration can be correlated with lithology and/or moisture content (e.g., perchlorate being associated with finer grained soil that also have higher moisture content), an understanding of such a correlation is helpful. The variation in soil lithology, moisture content, and contaminant concentration will determine the number of soil types and moisture contents that should be evaluated during the treatability test. Testing a minimum of two moisture contents is recommended. These ideally would be representative of low and high moisture contents in soil at the site where contaminant concentrations are well in excess of cleanup levels.

Soil for the microcosms is preferably collected by drilling or excavation immediately prior to setup of the treatability test. Soil is then homogenized and moisture content is adjusted if necessary. Increasing moisture is conducted by adding distilled water to the soil followed by homogenization. Soil drying in air can be conducted if the soil is too moist, however, collection of soil that is representative of low moisture content conditions is preferable. Following adjustment of moisture and homogenization the soil is placed in serum bottles (e.g., 50 grams in a 250-mL serum bottle) or other air-tight container with septa. Thick butyl rubber septa are inserted into the serum bottles and a gas manifold is used to replace the air in the serum bottle

headspace with the desired gas mixture. The number of gas mixtures to be tested will be dependent on contaminant of concern and the desired scale of the study. For perchlorate the minimum recommended gas compositions are 1) 100 percent nitrogen (control), 2) 1 percent hydrogen in nitrogen, 3) 1 percent hydrogen plus 1 percent carbon dioxide in nitrogen), 4) 10 percent hydrogen in nitrogen, and 5) 10 percent hydrogen plus 1 percent carbon dioxide in nitrogen). Multiple bottles are setup for each condition to allow sacrificial sampling and replication. At a minimum 10 bottles should be setup for each condition.

Sampling and analysis of the headspace is conducted for oxygen (i.e., to verify its absence) and electron donor(s). Sampling and analysis of soil contaminants requires sacrificial sampling of the microcosms and analysis using standard analytical methods such as distilled water extraction and ion chromatography for perchlorate.

Results are evaluated with respect to rate and extent of contaminant degradation relative to the control. If multiple experimental conductions are capable of promoting contaminant degradation, then economic and engineering analyses are recommended to identify which electron donor should be used in the field.

#### **3.2.2 Field Pilot Testing**

Field pilot testing is recommended to determine optimal operating conditions for gas injection and quantify radius of influence. In addition, pilot testing can be conducted to evaluate different injection well designs. The demonstration included a pilot test to evaluate soil pneumatic permeability and an optimization test to evaluate different well designs and injection configurations. Detailed procedures for conducting these tests are included in the ESTCP Final Report. The general approach for conducting testing is presented here and is based on lessons learned from the demonstration.

The optimized injection well design for the ESTCP demonstration is shown in Figure 4. This design is based on use of 6-inch porous vapor probes embedded in sand packs and located every 10 feet of boring depth. This design is recommended as a starting point but may not be optimal for all sites. The injection well design is also recommended for the soil gas monitoring piezometers. This approach allows use of piezometers as injection wells if desired. Injection wells and piezometers should be installed in different lithologic zones to allow assessment of soil types on gas injection. A minimum of one injection well and two piezometers is recommended for the pilot test. The depth and number of vapor probes will be dependent on site lithology and heterogeneity but a minimum of four probes per well/piezometer is recommended.

The recommended basic pilot test approach involves injection of nitrogen. Nitrogen can be supplied using a nitrogen generator, in liquefied form, or in multiple cylinders. Nitrogen is injected at one or more depths in the injection well at pre-determined flow rates and oxygen is monitored in the piezometers at all depths. A recommended starting flow rate is 50 ft<sup>3</sup>/min at each injection well depth. Oxygen is monitored in the piezometers to determine which operating conditions result in the maximal reduction of oxygen concentration. Analytical equipment for monitoring oxygen is discussed in Section 5.2. Various conditions are tested to identify the

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<sup>&</sup>lt;sup>5</sup> Note that for the ESTCP demonstration the injection well (i.e., P4) was called a piezometer.

optimal operating condition that maximizes the radius of influence for oxygen displacement and minimizes gas flow. Pressures are also measured at the injection well and at the piezometer.

The next recommended level of pilot testing involves use of selected gaseous electron donors in addition to nitrogen. This level of pilot testing can be important because of the tendency of certain electron donors to float (e.g., hydrogen) or sink (e.g., LPG). A manifold will be necessary to adjust flow rates of each gas and mix the gases prior to injection. Monitoring of individual gases at the piezometers may require additional analytical equipment. Analytical equipment for monitoring electron donors is discussed in Section 5.2.

Analysis of pilot test results will involve determination of the optimal operating conditions (e.g., flow rate, injection pressure, gas composition, injection depths, etc.) required to maximize the radius of influence and minimize gas flow rate. The radius of influence is the maximum distance from point of the injection where oxygen and electron donor concentrations are acceptable based on laboratory test results or other pertinent data.

#### 3.3 Wells and Piezometers

Design of gas injection wells and monitoring piezometers will be based on pilot test results, standard practices for well design, and applicable regulations. Figure 4 illustrates the injection well/piezometer design used for the ESTCP demonstration. This design is recommended as a starting point but site specific lithology and advances in understanding of gas injection for GEDIT will likely lead to modifications of this design.

The number and location of injection wells will be dependent on the area and depth requiring treatment, pilot test results, and economic evaluations. Pilot test results will establish the radius of influence for injection using a single well unless a multiple-well pilot test is conducted. A single well pilot test does not account for potential efficiencies of using multiple wells. Nevertheless, conservative well spacing based on the experimentally determined radius of influence is recommended. Potential for gas migration along subsurface utilities or into basements and buildings should also be considered when selecting injection well and piezometer placement.

The number and location of piezometers will be based on pilot test results, site heterogeneity, regulatory requirements, and cost. Piezometers in general should be located equidistant from injection wells. At a minimum, the number of piezometers should be selected to allow monitoring of site heterogeneity effects on gas transport.

The ESTCP demonstration design included 1/2-inch and 3/8-inch diameter (OD) poly tubing with 1/2-inch diameter by 6-inch long stainless steel vapor sampling probes. This design was used for gas injection and monitoring. The tubing diameter for injection wells may need to be increased if flows significantly greater than 50 scfh are used.

#### 3.4 Process Equipment

GEDIT process equipment includes the gas supply, the gas mixing manifold, and the gas distribution system. Each of these process equipment categories are discussed below. The

process and instrumentation diagram (P&ID) for the ESTCP demonstration is presented in Figure 5. This P&ID illustrates the three process equipment categories that are described in detail in the following sections.

#### 3.4.1 Gas Supply

Gas supply equipment will be dependent on the particular gas mixture composition and flow rate. Depending on the total flow rate required, some supply configurations will be more appropriate and cost-effective than others. For example, relatively low flow rates of gases will be better suited through use of gas cylinders or liquefied gases. Relatively greater flow rates will be better suited through the use of gas generators. The best gas supply configuration will be determined by conducting an engineering analysis of alternatives.

Nitrogen can be supplied as a compressed gas, a liquefied gas, or via various air separation systems. Compressed nitrogen is typically provided in cylinders that contain about 228 (K cylinder) or 304 (T cylinder) cubic feet of gas each. These cylinders can be manifolded together but in general will not be capable of supplying sufficient nitrogen for most GEDIT applications. Liquefied nitrogen was used during the ESTCP demonstration and was contained in a portable trailer with a capacity of 150,000 standard cubic feet. Larger liquefied nitrogen storage systems are available (e.g., 1.2 million standard cubic feet) but these are not portable. Nitrogen generators can be used to produce high purity nitrogen from air. Two primary types of generators are available: pressure swing adsorption (PSA) and membrane. PSA generators use two alternating trains of molecular sieves to separate nitrogen from oxygen. One train is separating the gases while the other is being regenerated. Membrane separators continuously generate nitrogen via diffusive separation in specialty membranes. Both of these nitrogen generators are capable of generating high flow rates of high purity nitrogen but require electricity to operate. They also require air compressors to operate. The nitrogen purity is also dependent on the design and operation of each system. Greater nitrogen purity will require more costly equipment and will increase operating costs.

Hydrogen can be supplied as a compressed gas, a liquefied gas, or via various generation systems. Compressed hydrogen is typically provided in cylinders that contain about 195 (K cylinder) or 261 (T cylinder) cubic feet of gas each. These cylinders can be manifolded together and 18-packs of K cylinders were used in the ESTCP demonstration. Larger volumes of hydrogen can be supplied using compressed hydrogen tube trailers or liquefied hydrogen tanks. Hydrogen can also be generated electrolytically or via reformation. Electrolytic hydrogen generators convert distilled water to hydrogen and oxygen using electricity. The hydrogen and oxygen are separated. Hydrogen reformers use a fuel such as methane or propane to produce hydrogen under high temperature and pressure. These systems require the fuel and electricity.

Liquefied petroleum gas (LPG) can be used as a gaseous electron donor and/or as a carrier gas. LPG is commonly available and typical odorized organosulfur compounds such as ethyl mercaptan. LPG cylinders are available in a variety of volumes.

Other electron donors are conceivable and may include organic compounds that are liquid at room temperature such as ethyl acetate or 1-hexene and can be supplied in drums. These liquids would be vaporized in a nitrogen carrier gas prior to injection. Carbon dioxide may be required

as a carbon source when using hydrogen as an electron donor. Carbon dioxide is available in cylinders and is liquid at room temperature when compressed. A K cylinder of carbon dioxide contains 560 standard cubic feet of gas.

A major consideration in evaluation of gas supply options is availability of utilities. Compressed and liquefied gases do not require electricity or water. This is an advantage for implementation at remote sites that do not have ready access to utilities. Electricity can be generated but may require significant fuel (e.g., diesel) storage. Distilled water can be generated from groundwater following pretreatment (e.g., ion exchange, reverse osmosis) but may necessitate brine disposal.

The gas supply configuration that was used for the ESTCP demonstration is shown in Figure 6. This configuration included liquefied nitrogen (150,000 standard cubic feet capacity), three 18-packs of hydrogen K cylinders, one 18-pack of carbon dioxide K cylinders, and a 120-gallon tank of LPG. This configuration was used to supply 100 standard cubic feet per minute of a gas mixture comprised of 89 percent nitrogen, 10 percent hydrogen, 10 percent LPG, and 1 percent carbon dioxide. A cylinder of helium is also shown in Figure 6 but this was used only for initial tracer tests and is not considered part of the standard gas supply configuration.

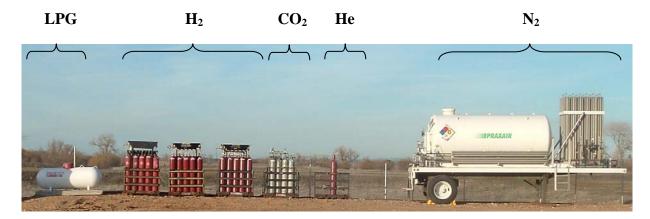


Figure 6 – Gas Supply for the Demonstration

## 3.4.2 Gas Mixing Manifold

A gas mixing manifold is required to allow control of individual gas flow rates and generate a gas mixture of the desired composition at the desired total flow rate. The manifold design will be dependent on the specific gas mixture and flow rates but will in most cases include the following elements:

- Connections from the gas supplies to the manifold
- On-off valves to control flow of the gas supplies
- Flow meters to monitor flow rate of individual gases and gas mixtures
- Pressure gauges to monitor pressures of individual gases and gas mixtures
- A static mixer or other device to ensure the gases are well mixed prior to distribution to the injection wells
- A sample valve to allow collection of samples for onsite or off-site gas analysis
- Connections from the manifold to the gas distribution system

Figure 7 includes photographs of the front and back of the manifold used for the ESTCP demonstration. This design is based on the P&ID presented in Figure 5. Alternative designs including use of non-metallic tubing suitable for compressed gases (i.e., not PVC) may be appropriate. The design of the ESTCP demonstration manifold piping was based on the Compressed Gas Association (CGA) Standard for Hydrogen Piping Systems at Consumer Locations (G-5.4-2005) which states that 300 series stainless or carbon steel shall be used for piping. A professional engineer should be consulted with regard to





Figure 7 – Gas Supply Control Panel

local code requirements and whether this particular standard applies to a specific application and in particular to gas mixtures containing low percentages of hydrogen.

Other considerations for gas mixing manifold design include:

- Installation location Locate the manifold outside rather than inside a building or container so potential gas leaks have a greater potential for dispersion.
- Automation Consider whether manual or automatic monitoring and control is desired.
   One factor that will affect the need for automation is whether the gaseous electron donor will be injected continuously or pulsed. Automatic monitoring and control of flow will increase capital costs but has the potential to reduce operating costs. Also, use of electronic sensors and controls while using a potentially flammable electron donor gas mixture will need to comply with electrical classification requirements under the National Electrical Code.
- Rotameter correction Ensure that readings from variable area flow meters also known as rotameters are appropriately compensated for pressure and gas composition. Most rotameters are calibrated for air at ambient pressure.
- System pressure Calculate the saturation pressure for gas mixtures containing condensable gases (e.g., LPG) and ensure that the operating manifold system pressure is less than the saturation pressure to prevent condensation.
- Multiple gas mixtures Determine during pilot testing whether different gas
  compositions will be injected at different depths. For example, it may be desirable to
  inject hydrogen at deeper locations and LPG at shallower locations. With this approach
  hydrogen can float up through the zone of influence and LPG can sink. Multiple gas
  mixtures will require multiple gas mixing manifolds.

## 3.4.3 Gas Distribution System

The gas distribution system is used to transfer the gas mixture from the gas mixing manifold to the injection well(s) in a GEDIT design based on gas injection only. A GEDIT design that is based on soil vapor extraction, electron donor amendment, and re-injection will have additional requirements. The ESTCP demonstration was based on the gas injection approach and this section addresses this approach. The design of this system will depend on gas flow rates, the distance from the gas mixing manifold to the injection wells, and site-specific constraints such as vehicle traffic and security.

The ESTCP demonstration used 3/8-inch diameter tubing for the distribution system with pneumatic quick-connect fittings for connection to wellhead tubing. The tubing was laid on the ground which may not be applicable for all sites. Alternatively, tubing can be run through metallic or plastic pipe or conduit for greater security. If necessary the tubing can be buried. Regardless, pressure drop is a primary consideration and must be calculated to determine the appropriate tubing size. The pressure drop must be sufficiently low to prevent too high a gas pressure at the gas distribution system (see Section 3.4.2) and sufficiently high to ensure delivery to each well point (see Section 3.2.2). Gas distribution tubing or piping materials must be suitable for use with compressed gases. For example, PVC pipe should never be used with compressed gas systems.

## 4.0 Operations

Operational requirements of the GEDIT system will be specific to the particular design. However, several operational considerations can be generalized for most systems and are described below. These considerations are focused on optimization of operating conditions to minimize gas use and ensure that subsurface conditions are suitable.

Operating variables for a GEDIT system associated with process optimization include the following:

- Injection wells where gas is injected
- Depths in each well where gas is injected
- Gas flow rate for each injection location
- Gas composition for each injection location
- Gas injection strategy continuous or pulsed
- Total time that gas is injected at each point

Other operating considerations include the following:

- Ensuring that gas supplies are sufficient and refilled or maintained accordingly
- Maintaining the system to ensure that leaks are identified and repaired
- Adjusting flow rates and gas compositions as necessary to ensure that the actual values are in line with the target values

Process optimization will necessitate monitoring of operating conditions and sampling and analysis of soil vapor and soil (see Section 5.0 for details on monitoring, sampling, and analysis). The objective of process optimization is to minimize gas use while ensuring that the soil vapor composition meets pre-determined specifications. The gas composition specifications will be determined during bench-scale and field-scale testing (see Section 3.2). In general, operating conditions will be adjusted to ensure that, at each monitoring location, oxygen concentrations will be less than a specified maximum value and electron donor concentration(s) will be greater than a specified minimum value. Additionally, operating conditions will be optimized to minimize gas use while meeting these specified gas concentrations at all piezometer locations. Analytical data from individual piezometer gas samples will be used to identify specific injection wells and depths where gas flow rates and/or compositions should be adjusted to meet gas composition specifications. The number and locations of installed piezometers will directly affect the extent to which process optimization can be accomplished.

Sampling and analysis of soil gas is conducted to determine whether the soil gas composition is supportive of contaminant biodegradation. It is not a direct measurement of contaminant biodegradation. For nonvolatile contaminants (e.g., perchlorate) collection of soil samples is the only means to assess contaminant biodegradation. Sampling of soil requires drilling and must be conducted judiciously. Heterogeneity can also complicate data analysis. Nevertheless, analysis of

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<sup>&</sup>lt;sup>6</sup> In situ microcosms can be considered but representativeness of the results would need to be established.

soil samples and comparison to cleanup goals will ultimately determine whether GEDIT operation is complete or continued gas injection is necessary.

# 5.0 Monitoring, Sampling, and Analysis

#### **5.1 Process Monitoring**

Process monitoring variables will include at a minimum flow rates, pressures, and gas composition being delivered to the injection wells. Additional process monitoring variables, depending on the GEDIT design, will include gas supply pressures or tank levels, fuel levels in the case of on-site power generation, and likely other parameters.

Monitoring of flow rates will depend on the actual flow meter being used. In the case of rotameters, corrections for gas composition and pressure may be necessary. Rotameters are typically calibrated for air at atmospheric pressure. Rotameter readings are affected by gas pressure and density. The rotameter readings must be corrected when measuring the flow rate of gases other than air and at pressures other than atmospheric. The following equation<sup>7</sup> can be used to make these corrections:

$$Q_i = CF_i \widehat{Q}_i \sqrt{\frac{P_i}{P}},$$

where,

 $Q_i$  is the actual flow rate of gas i (i.e.,  $H_2$ ,  $N_2$ ,  $CO_2$ , or LPG) in units of scfm or scfh;

 $CF_i$  is the correction factor for gas i and is based on the relative densities of gas I and the rotameter calibration gas (i.e., air). The values of  $CF_i$  are specific to the gas composition and the rotameter and are presented in Table 1;

 $\widehat{Q}_{i}$  is the rotameter reading for gas i in units of scfm or scfh;

 $P_i$  is the absolute pressure of gas i at the rotameter; and

**P** is the atmospheric pressure (1 atmosphere or 14.696 psia).

**Table 1 – Correction Factors for Key Instruments Rotameters** 

<u>i</u>	$CF_i$
$N_2$	$1.0\overline{2}$
Propane (LPG)	0.80
$H_2$	3.81
$CO_2$	0.81

Monitoring of pressure can be conducted using standard pressure gauges. Monitoring of gas composition in the gas mixing manifold is described in Section 5.2.

<sup>&</sup>lt;sup>7</sup>Provided by Key Instruments.

Process monitoring can be conducted manually as described above or automatically using flow and pressure transmitters. These will increase capital costs but have the potential to decrease lifecycle costs through more cost-effective monitoring and control. These transmitters may need to be intrinsically safe or enclosed in explosion proof housings depending on the electrical classification of the area.

## 5.2 Gas Sampling and Analysis

Gas samples from the gas mixing manifold and the piezometer can be manually collected and analyzed using field instruments. Alternatively, samples can be submitted to a laboratory for analysis. Specialized instruments can also be used to continuously monitor gas composition.

The ESTCP demonstration involved manual sampling and use of field instruments. Figure 8 is a photograph of the field sampling and analysis equipment used for the demonstration. This equipment was suitable for sample collection and analysis of oxygen, propane, hydrogen, temperature, and relative humidity. Oxygen, propane, and carbon dioxide were monitored using an RKI Eagle gas monitor. This instrument included a gas sampling pump that drew soil gas from the piezometers and had the following sensors:

- Oxygen was measured using an electrochemical cell.
- Propane was quantified using an infrared sensor which allowed specific quantification without interference from hydrogen.
- Carbon dioxide was measured using an infrared sensor.

Hydrogen was monitored using a H2SCAN HY-ALERTA 500. This instrument is specific for hydrogen. Relative humidity and temperature were monitored using Vaisala HMT360 meter.

The RKI Eagle was determined to be a robust and cost-effective field instrument capable of measuring multiple gasses during GEDIT operation. Alternative portable instruments are also available. When selecting an instrument for use it is important to determine the effect of varying oxygen concentrations on the quantification of electron donor concentrations. For example, use of a flammability sensor that measures percentage of the lower explosion limit (LEL) might be considered for use. However, most of these sensors employ catalytic bead technology which requires the presence of oxygen to function. Since depletion of oxygen is necessary for GEDIT, this type of an instrument in not suitable for electron donor analysis. Use of an infrared sensor for measurement of hydrocarbons is suitable and is unaffected by oxygen. Use of a hydrogen-specific sensor such as the H2SCAN HY-ALERTA 500 is suitable for hydrogen measurement and was determined to be minimally affected by oxygen.



Figure 8 – Gas Sampling and Analysis Train

# 5.3 Soil Sampling and Analysis

Soil sampling and analysis is required for overall determination of GEDIT effectiveness unless the contaminant of concern is volatile. Methods for conducting soil sampling and analysis are well established and are not discussed further. On the other hand, soil heterogeneity is an important consideration when selecting soil sampling locations. If calculation of percent contaminant removal is of interest then it is important to collect before and after samples as close to each other as possible. The reason for this approach is to minimize effects of heterogeneity on data interpretation. If determination of whether soil concentrations are below a cleanup level then grid sampling or other standard sampling techniques are appropriate.

When collecting samples for analysis, discrete samples are recommended. Analysis of these samples for the contaminant(s) of concern and moisture is recommended to allow determination of the effects of moisture on contaminant removal. In addition, the soil type should be characterized using the Unified Soil Classification System (USCS) or a grain size analysis should be conducted.

## **6.0 Health and Safety**

Health and safety considerations must be addressed during design, construction, and operation phases. Issues that must be considered include but are not limited to:

- Flammability hazards including requirements for electrical classification
- Energy hazards including pressure
- Cold exposure hazards when handling liquefied gases
- Vapor intrusion issues when injecting gases into the subsurface
- Oxygen deficient atmosphere hazards
- Drilling hazards
- Construction hazards
- Secondary containment requirements
- Contaminant exposure hazards

These and other issues as appropriate must be addressed early on during the design process. Design of the process by a licensed professional engineer is required. Depending on local regulatory requirements, a hazardous materials plan may be required. During operation, regular monitoring of the working environment for oxygen and LEL will be necessary and should be specified in the site health and safety plan. Regular checking of the GEDIT process equipment and piping for leaks using suitable instruments is also necessary.

Factors that affect this optimization will include:

- Number of injection wells The optimal number of injection wells will be a balance of well installation costs and gas consumption. More wells spaced closely together will allow use of lower gas flow rates. While this plan specifies the number and placement of wells based on pneumatic air injection tests, the data obtained during this demonstration will be used to develop optimization strategies for well placement in future applications of the technology.
- Gas flow rate Increasing gas flow rates will maximize radius of influence but will result in greater costs because of greater gas consumption rates.
- Oxygen infiltration rate The rate of oxygen infiltration will be influenced by variations in barometric pressure, soil permeability, and diffusion.
- Electron donor consumption rate The rate of electron donor consumption will be influenced by the rate of oxygen infiltration, soil moisture, and biological activity.
- Gas injection pulsing duration and frequency Gas injection pulsing will minimize costs by allowing use of greater gas flow rates while minimizing gas consumption. However, the rate of electron donor consumption and the rate of oxygen infiltration will limit the duration between pulses.
- Soil drying Prolonged gas injection may result in soil drying which may inhibit microbial activity.
- Injection gas composition Greater concentrations of electron donor in nitrogen will promote increased perchlorate biodegradation but will result in greater costs. The composition used in this demonstration is based on the treatability studies.

•	Electron donor injection volume – The injected electron donor volume must be sufficient to result in perchlorate biodegradation but should not be in great excess to minimize costs.						