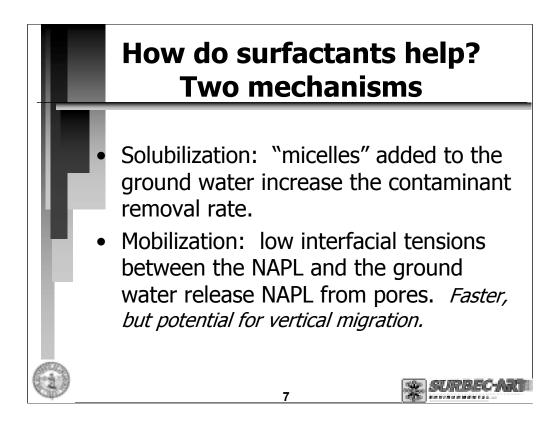
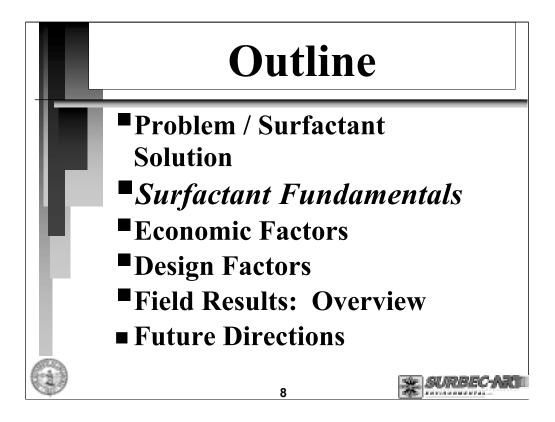
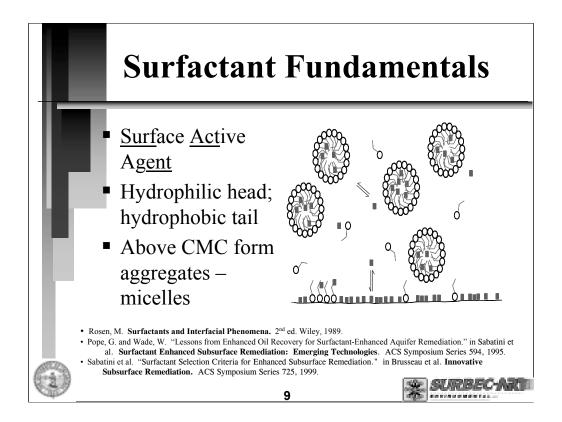


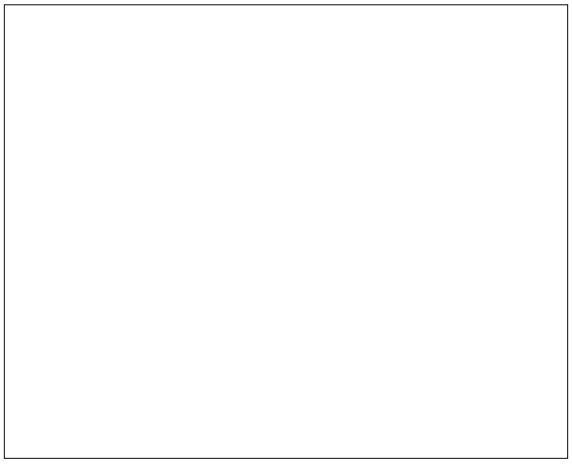
The basic problem in removing nonaqueous phase liquids (NAPLs) from an aquifer is the trapping of the NAPL in the pores of the aquifer matrix by interfacial tension forces. The hydrodynamic forces produced by pumping water through the contaminated zone are too small to cause drops of the NAPL to move from the injection wells toward the recovery wells. So, the level of contaminated liquid is slowly reduced by dissolving it into the ground water as it passes by the droplets. This is a slow, inefficient, and expense process which has been suspended in many places because of depletion of the ground water itself.

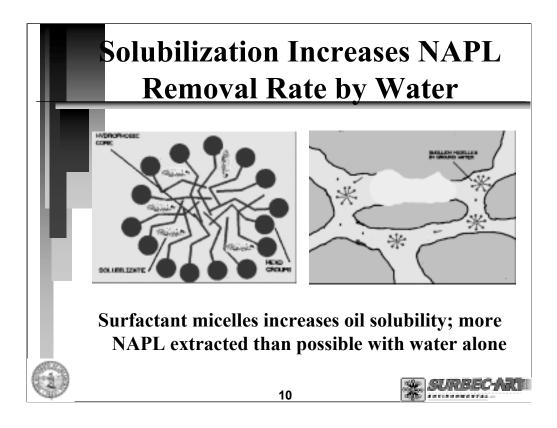


The two types of remediation mechanisms possible with surfactants are called solubilization and mobilization. The former enhances the dissolution of the contaminant, the latter un-traps it.

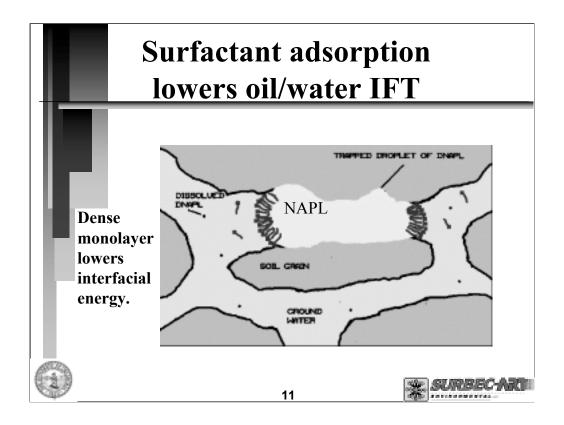




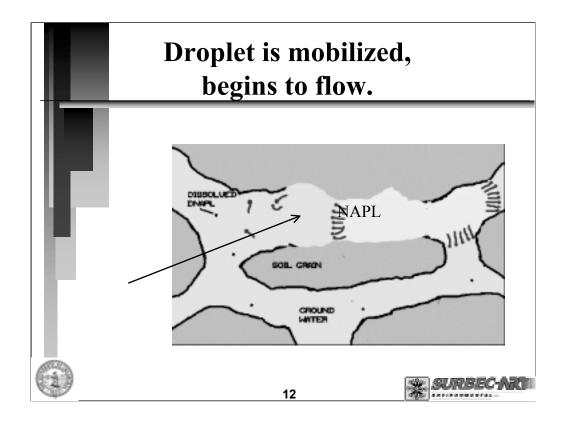




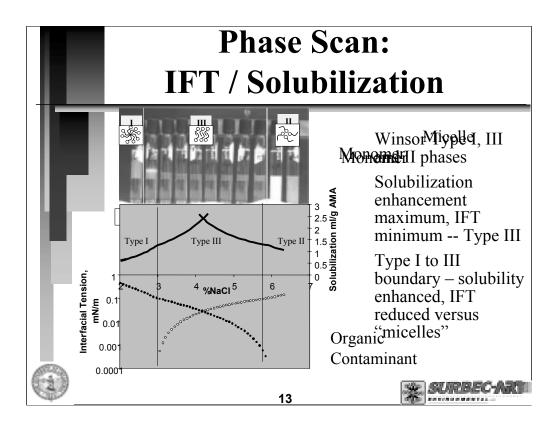
In solubilization micelles of the surfactant increase the concentration of the contaminant in the ground water, speeding the rate at which the contaminant is removed from the subsurface. The increase can be by over an order of magnitude.



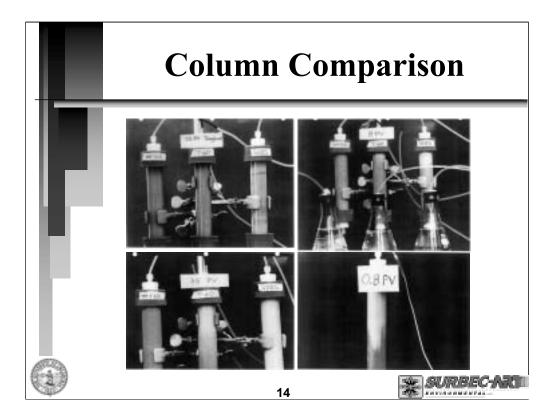
In the mobilization mechanism, the surfactant must adsorb at the interface between the NAPL and the ground water, resulting in the lowering of the interfacial tension between the phases.

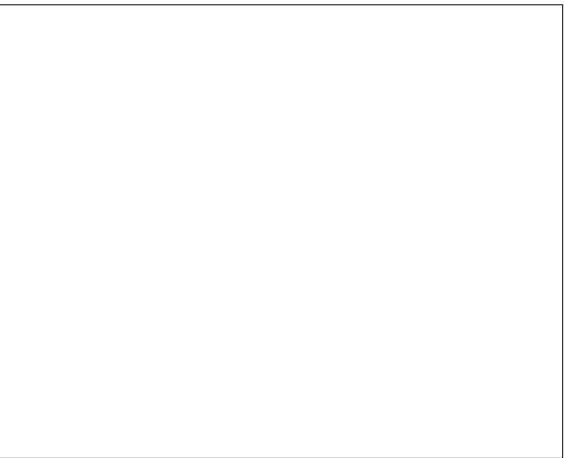


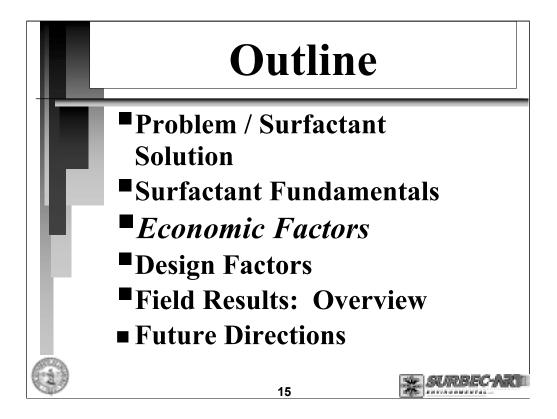
As the interfacial tension becomes ultra low, as is seen in the formation of middle phase microemulsions, the drop becomes mobile. This is the same phenomenon that was proposed for enhanced oil recovery in the late 70s.

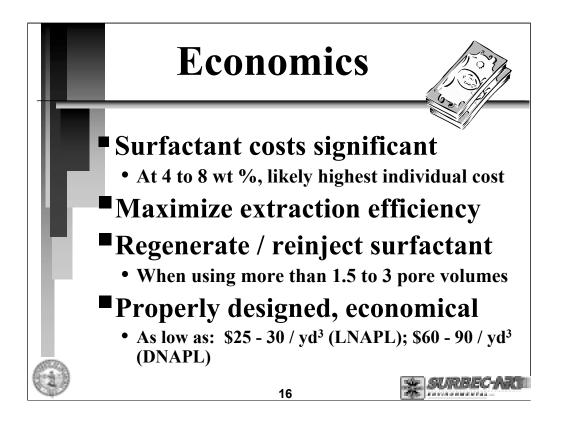


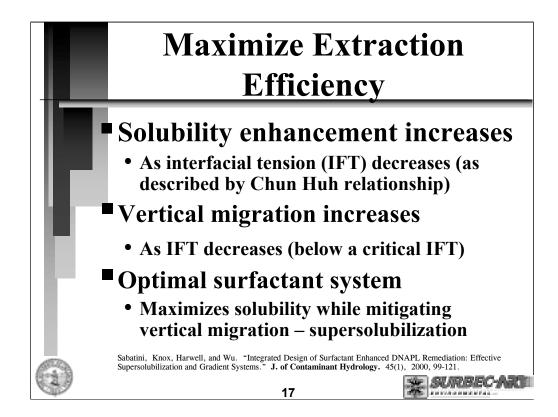


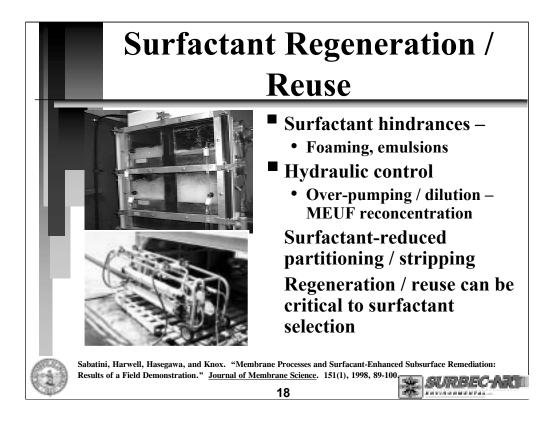


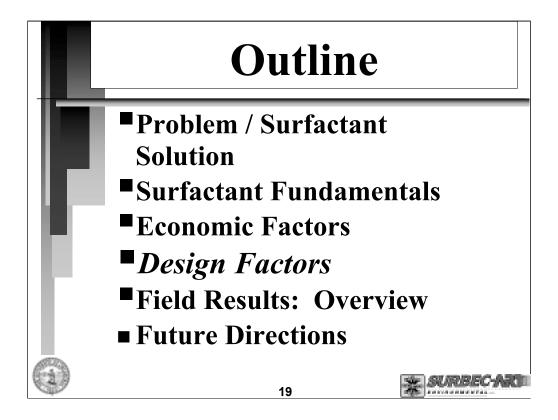


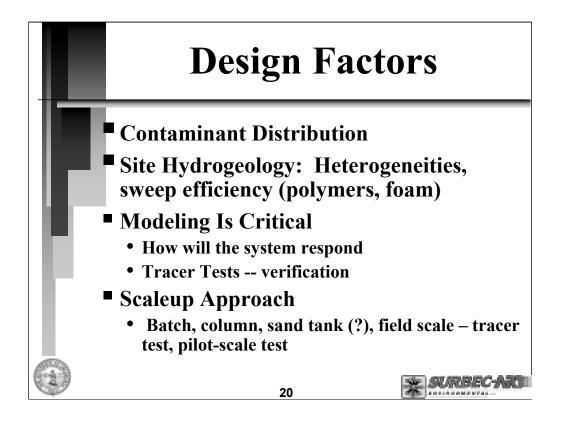


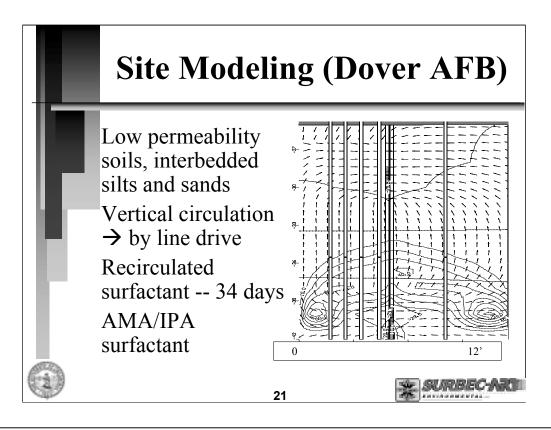




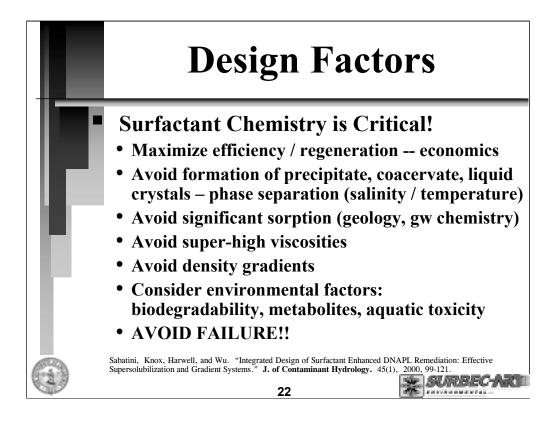


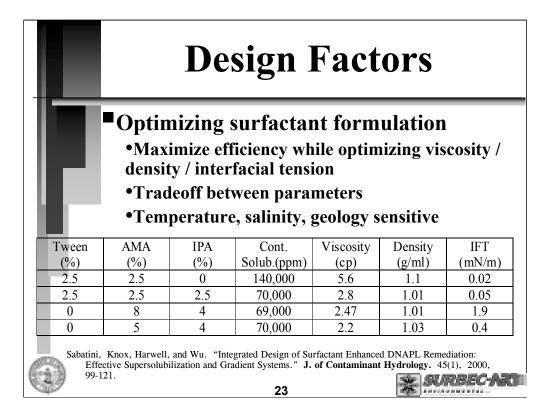


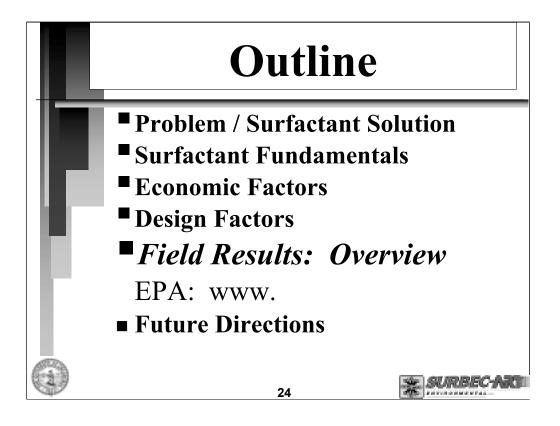


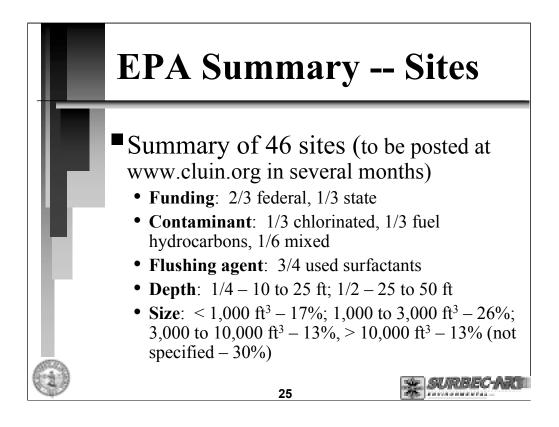




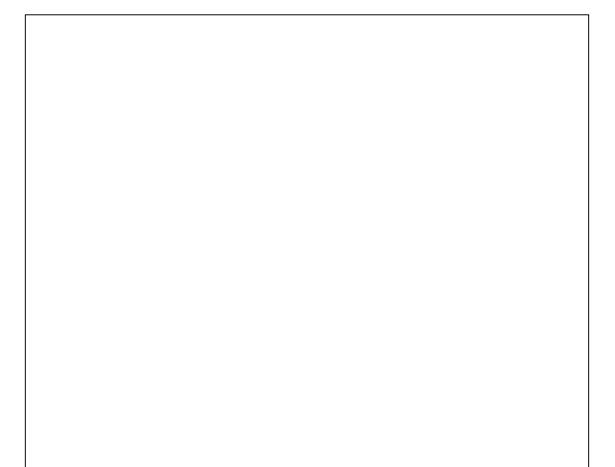


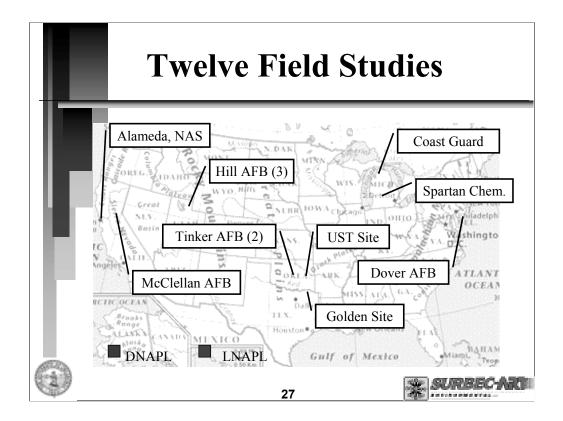


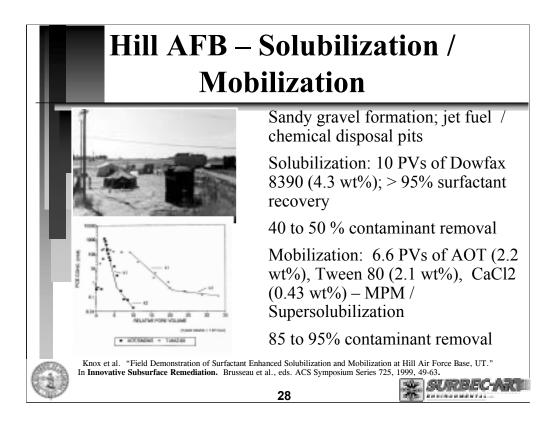


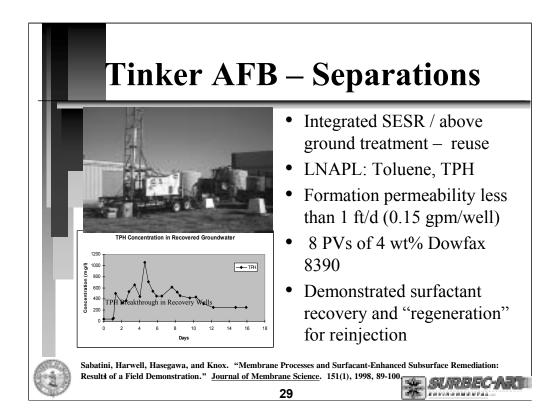


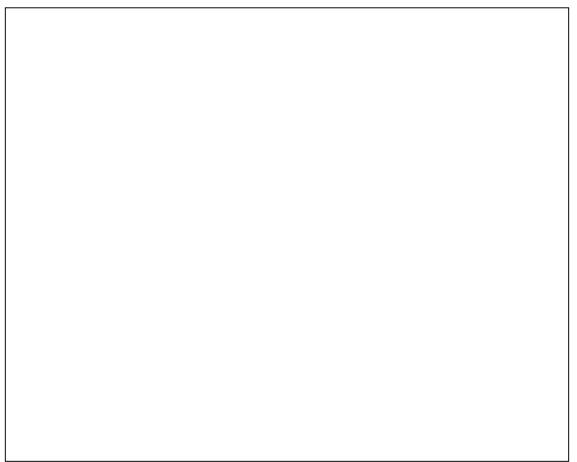
	SEAR Field Demonstrations					
Loc	ation (year)	NAPL Composition	Swept Pore Volume (m ³)	Reduction in NAPL Mass (%)	NAPLSaturation (%) After Surfactant	
	den, Ontario PV 2% surfactant (1991)	PCE	9.1	77	0.2	
	ssomption, Quebec PV surfactant (1994)	Multicomponent DNAPL	6.1	86	0.45	
	AFB OU1 PV 3% surfactant (1996)	Multicomponent LNAPL	4.5	86	0.8	
	AFB OU2 PV 8% surfactant (1996)	Multicomponent DNAPL, 70% TCE	57	99	0.03	
	AFB OU 2 surfactant + foam (1997)	Multicomponent DNAPL, 70% TCE	31	90	0.03	
	np Lejeune V 4% surfactant (1999)	PCE DNAPL	18	72	0.5	
	meda Point V 7% surfactant (1999)	DNAPL, TCA, TCE	32	98	0.03	
	rl Harbor PV 8% surfactant (1999)	Nav al Special Fuel Oil, 1000 cp	7.5	86	0.35	
	AFB OU2 PV 4% surfactant (2000)	Multicomponent DNAPL	188	94	0.07	
	E					











Tinker A	AFB U	nit Di	mensions
	Unit	Dimension	Media
	Air Stripper - Packed Tower	0.66 ft ID 8.0 ft tall	1 in Polyethylene Flexirings
H.	Air Stripper - Hollow Fiber	0.33 ft ID 2.5 ft tall	Celgar X 30; 0.24 mm ID, 30 nm pores fibers
	Ultrafilter	2.0 ft long 0.5 ft ID	10,000 MWCO
	30		

